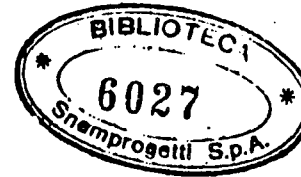


6 DEC 1976



## PART I

# THE 'PIPING GUIDE'

## A COMPACT REFERENCE FOR THE DESIGN AND DRAFTING OF INDUSTRIAL PIPING SYSTEMS

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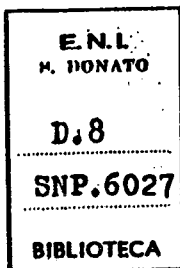
The text refers to standards and codes, using designations such as ANSI B31.1, ASTM A-53, ISA S5.1—1968, etc. Full titles of these standards and codes will be found in tables 7.3 thru 7.15.

References: Numbers in straight brackets (thus: [12]) refer to sources of published information listed under 'References', at the end of the index.

Sections, figures, charts and tables in Part I are referred to numerically, and are located by the margin index. Charts and tables in Part II are identified by letter.

**FOR TERMS NOT EXPLAINED IN THE TEXT,  
REFER TO THE INDEX.  
ABBREVIATIONS ARE GIVEN IN CHAPTER 8.**

The authors are grateful to the companies, designers, and engineers who assisted in the development of the Piping Guide. Apart from source material, individual acknowledgements are not made because neither these contributors nor the authors assume liability or responsibility for designs using information presented herein. The user is responsible for complying with the various codes and standards, Federal, State, and Municipal regulations, and other legal obligations which may pertain to the construction of plants, industrial installations, etc. Discussion or mention of products does not necessarily imply endorsement.



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The 'PIPING GUIDE'.....■ Brings together information of especial value to designers, draftsmen, and systems engineers concerned with piping technology

- Discusses in detail the design and drafting of piping systems
- Describes pipe, piping components most commonly used, valves, and equipment
- Presents charts, tables, and examples for daily reference
- Lists piping terms and abbreviations concerned with piping technology
- Provides a design reference for companies and consultants
- Supplements existing company standards, information, and methods
- Serves as an instructional aid

D.8.SNP.6027

'PART I' explains.....■ Current techniques of piping design

- Piping terms, assembling of piping from components, and methods for connecting to equipment
- Office organization, and methods to translate concepts into finished designs from which plants are built

'PART II' provides.....■ Frequently-needed design data and information, arranged for quick reference

- Principal dimensions and weights for pipe, fittings, flanges, valves, structural steel, etc.
- Direct-reading metric conversion tables for dimensions

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# PIPING:

## USES, EXPENDITURES, & PLANT CONSTRUCTION

### USES OF PIPING

1.1

Piping is used for industrial (process), marine, transportation, civil engineering, and for 'commercial' (plumbing) purposes.

This book is primarily concerned with industrial piping for processing and service systems. *Process piping* is used to transport fluids between storage tanks and processing units. *Service piping* is used to convey steam, air, water, etc., for processing. Piping here defined as 'service' piping is sometimes referred to as 'utility' piping, but, in the Guide, the term 'utility piping' is reserved for major lines supplying water, fuel gases, and fuel oil (that is, for commodities usually purchased from utilities companies and bulk suppliers).

*Marine piping* for ships is often extensive. Much of it is fabricated from welded and screwed carbon-steel piping, using pipe and fittings described in this book.

*Transportation piping* is normally large-diameter piping used to convey liquids, slurries and gases, sometimes over hundreds of miles. Crude oils, petroleum products, water, and solid materials such as coal (carried by water) are transported thru pipelines. Different liquids can be transported consecutively in the same pipeline, and branching arrangements are used to divert flows to different destinations.

*Civil piping* is used to distribute public utilities (water, fuel gases), and to collect rainwater, sewage, and industrial waste waters. Most piping of this type is placed underground.

*Plumbing (commercial piping)* is piping installed in commercial buildings, schools, hospitals, residences, etc., for distributing water and fuel gases, for collecting waste water, and for other purposes.

### COMMISSIONING, DESIGNING, & BUILDING A PLANT

1.2

When a manufacturer decides to build a new plant or to expand an existing one, he will either employ an engineering company to undertake design and construction, or, if his engineering department is large enough, he will do the design work, manage the project, and employ one or more contractors to do the construction work.

In either procedure, the manufacturer supplies information concerning the purposes of buildings, production rates, processes, design criteria to meet his practices, details of existing plant, and site surveys, if any.

Chart 1.1 shows the principals involved, and the flow of information and materiel.

SCHEMATIC FOR PLANT CONSTRUCTION

CHART 1.1

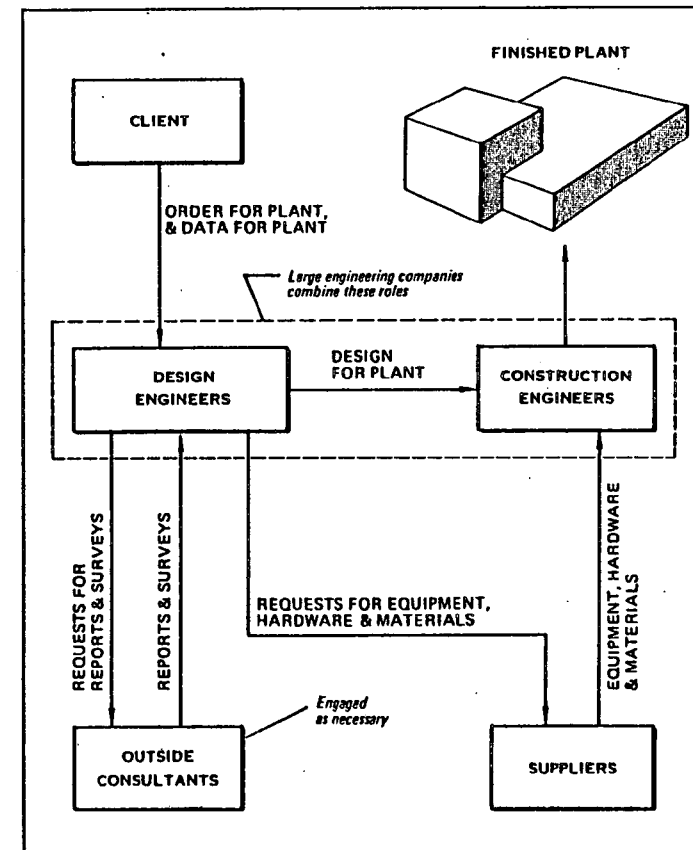


CHART  
1.1

The designing and building of an industrial plant is a complex undertaking. Except for the larger industrial concerns, who may maintain their own design staffs, the design and construction of plants and related facilities is usually undertaken by specialist companies.

The Guide describes in 4.1 the organization and responsibilities of design engineering, with special reference to the duties of individuals engaged in the development of piping designs for plants.

US expenditures over the years 1967 thru 1971 averaged 14.1 billion dollars per year for new plants and equipment in the petroleum, chemical, food and beverage, paper, rubber, and textile industries, according to the 'Survey of current business' compiled by the US Department of Commerce.

For these quoted industries, the average cost of piping is about one fifth of the cost of the finished plant and equipment: large variations from this ratio are possible, however.

# PIPE, FITTINGS, FLANGES, & LINE EQUIPMENT

2 | .1  
| .1.3

## PROCESS PIPE

2.1

### PIPE & TUBE

2.1.1

Tubular products are termed 'tube' or 'pipe'. Tube is customarily specified by its outside diameter and wall thickness, expressed either in BWG (Birmingham wire gage) or in thousandths of an inch. Pipe is customarily identified by 'nominal pipe size', with wall thickness defined by 'schedule number', 'API designation', or 'weight', as explained in 2.1.3. Non-standard pipe is specified by nominal size with wall thickness stated.

The principal uses for tube are in heat exchangers, instrument lines, and small interconnections on equipment such as compressors, boilers, and refrigerators.

### SIZES & LENGTHS COMMONLY USED FOR STEEL PIPE

2.1.2

Manufacturers offer pipe in established sizes (see 2.1.3) ranging from 1/8 thru 44 inch nominal diameter ('nominal pipe size'). Pipe sizes normally stocked include: 1/2, 3/4, 1, 1 1/4, 1 1/2, 2, 2 1/2, 3, 3 1/2, 4, 5, 6, 8, 10, 12, 14, 16, 18, 20 and 24. Sizes 1 1/4, 2 1/2, 3 1/2, and 5 inch are seldom used (unusual sizes are sometimes required for connecting to equipment, but piping is normally run in the next larger stock size after connection has been made). 1/8, 1/4, 3/8 and 1/2-inch pipe is usually restricted to instrument lines or to service and other lines which have to mate with equipment. 1/2-inch pipe is extensively used for steam tracing and for auxiliary piping at pumps, etc.

Straight pipe is supplied in 'random' lengths (17 to 25 ft), and sometimes 'double random' lengths (38 to 48 ft), if preferred. The ends of these lengths are normally either plain (PE), beveled for welding (BE), or threaded and supplied with one coupling per length ('threaded and coupled', or 'T&C'). If pipe is ordered 'T&C', the rating of the coupling is specified—see chart 2.3. Other types of ends, such as grooved for special couplings, can be obtained to order.

### DIAMETERS & WALL THICKNESSES OF PIPE

2.1.3

The size of all pipe is identified by the nominal pipe size, abbreviated 'NPS', which is seldom equal to the true bore (internal diameter) of the pipe—the difference in some instances is large. 14-inch NPS and larger pipe has outside diameter equal to the nominal pipe size.

Pipe in the various sizes is made in several wall thicknesses for each size, which have been established by three different sources:—

- (1) The American National Standards Institute, thru 'schedule numbers'
- (2) The American Society of Mechanical Engineers and the American Society for Testing and Materials, thru the designations 'STD' (standard), 'XS' (extra-strong), and 'XXS' (double-extra-strong), drawn from dimensions established by manufacturers. *In the Guide, these designations are termed 'manufacturers' weights'*
- (3) The American Petroleum Institute, thru its standards 5L and 5LX. These dimensions have no references for individual sizes and wall thicknesses

'Manufacturers' weights' (second source) were intended, as long ago as 1939, to be superseded by schedule numbers. However, demand for these wall thicknesses has caused their manufacture to continue. Certain fittings are available only in manufacturers' weights.

Pipe dimensions from the second and third sources are incorporated in American National Standard B36.10-1970. Table P-1 lists dimensions for welded and seamless steel pipe in this standard, and gives derived data.

**IRON PIPE SIZES** were initially established for wrought-iron pipe, with wall thicknesses designated by the terms 'standard', 'extra-strong', and 'double-extra-strong'. ANSI B36.10-1970 lists these wrought-iron pipe dimensions (in table 3). Wrought-iron pipe has been almost completely supplanted by steel pipe. Before the schedule number scheme for steel pipe was first published by the American Standards Association in 1935, the iron pipe sizes were modified for steel pipe by slightly decreasing the wall thicknesses (leaving the outside diameters constant) so that the weights per foot (lb/ft) equalled the iron pipe weights. Table P-1, which is reproduced by permission of the Crane Company (Midwest Fitting Division), lists steel pipe data under the heading 'iron pipe sizes'. As ANSI B36.10-1970 states that "the size of all pipe is identified by nominal pipe size", the Guide uses the term 'manufacturers' weights' to denote the STD, XS, and XXS designations applied by manufacturers to steel pipe and fittings.

**LIGHT-WALL** (also termed 'light-gage') is a commercially-accepted designation corresponding to SCH 10S (ANSI B36.19) and SCH 10 (ANSI B36.10) in certain sizes. Table P-1 lists these sizes under 'L'.

**STAINLESS-STEEL SIZES** American National Standard B36.19-1965 (revised 1971) establishes a range of thin-walled sizes for stainless-steel pipe, identified by schedules 5S and 10S. These sizes are included in table P-1.

## MATERIALS FOR PIPE

2.1.4

### REFERENCES

- 'Metallic piping'. Masek J.A. 1968. Chemical Engineering, Jun 17. 215-29  
'Materials of construction: 19th Biennial CE Report'. Aldrich C.K. 1960. Chemical Engineering, Nov 14  
'Lined pipe systems'. Ward J.R. 1968. Chemical Engineering, Jun 17. 238-42  
'Non-metallic pipe: promise and problems'. Wright C.E. 1968. Chemical Engineering, Jun 17. 230-7

Engineering companies have materials engineers to determine materials to be used in piping systems. Most pipe is of carbon steel and (depending on service) is manufactured to ASTM A-53.

**STEEL PIPE** Straight-seam-welded and spiral-welded pipe is made from plate, and seamless pipe is made by piercing solid billets.

Carbon-steel pipe is strong, ductile, weldable, machineable, reasonably durable and is nearly always cheaper than pipe made from other materials. If carbon-steel pipe can meet the requirements of pressure, temperature, corrosion resistance and hygiene, it is the natural choice.

The most readily-available carbon-steel pipe is made to ASTM A-53 in schedules 40, 80, STD, and XS sizes, in electric-resistance-welded (Grade A and Grade B—the latter grade has the higher tensile strength) and in seamless (Grades A and B) constructions. Common finishes are 'black' ('plain' or 'mill' finish) and galvanized.

Most sizes and weights are also available in seamless carbon steel to ASTM A-106, which is a comparable specification to A-53, but prescribing more stringent testing. Three grades of A-106 are available—Grades A, B, and C, in order of increasing tensile strength. Charts 2.1, 2.2 and 2.3 indicate pipe specifications most used industrially.

Steel specifications in other countries may correspond with USA specifications. Some corresponding European standards for carbon steels and stainless steels are listed in table 2.1.

**IRON** pipe is made from cast-iron and ductile-iron. The principal uses are for water, gas, and sewage lines. Wrought-iron pipe is seldom employed.

**OTHER METALS & ALLOYS** Pipe or tube made from copper, lead, nickel, brass, aluminum and various stainless steels can be readily obtained. These materials are relatively expensive and are selected usually either because of their particular corrosion resistance to the process chemical, their good heat transfer, or for their tensile strength at high temperatures. Copper and copper alloys are traditional for instrument lines, food processing, and heat transfer equipment, but stainless steels are increasingly being used for these purposes.

**PLASTICS** Pipe made from plastics may be used to convey actively corrosive fluids, and is especially useful for handling corrosive or hazardous gases and dilute mineral acids. Plastics are employed in three ways: as all-plastic pipe, as 'filled' plastic materials (glass-fiber-reinforced, carbon-filled, etc.) and as lining or coating materials. Plastic pipe is made from polypropylene, polyethylene (PE), polybutylene (PB), polyvinyl chloride (PVC), acrylonitrile-butadiene-styrene (ABS), cellulose acetate-butyrate (CAB), polyolefins, and polyesters. Pipe made from polyester and epoxy resins is frequently glass-fiber-reinforced ('FRP') and commercial products of this type have good resistance to wear and chemical attack.

COMPARABLE USA & EUROPEAN SPECIFICATIONS FOR STEEL PIPE				TABLE 2.1
	USA	UK	W. GERMANY	SWEDEN
CARBON-STEEL PIPE	ASTM A53 Grade A SMLS Grade B SMLS	BS 3601 HFS 27 & CDS 22 HFS 27 & CDS 27	DIN 1629 St 36 St 45	SIS 1233-06 SIS 1434-06
	ASTM A53 Grade A ERW Grade B ERW	BS 3601 ERW 22 ERW 27	DIN 1629 Blatt 3 St 34-2 ERW Blatt 3 St 37-2 ERW	
	ASTM A53 FW	BS 3601 BW 22	DIN 1629 Blatt 3 St 34-2 ERW	
	ASTM A106 Grade A Grade B Grade C	BS 3602 HFS 23 HFS 27 HFS 35	DIN 17175* St 35-8 St 45-8	SIS 1234-06 SIS 1435-06
	ASTM A134	BS 3601 EFW	DIN 1629 Blatt 2 EFW	
	ASTM A135 Grade A Grade B	BS 3601 ERW 22 ERW 27	DIN 1629 Blatt 3 St 34-2 ERW Blatt 3 St 37-2 ERW	SIS 1234-06 SIS 1434-06
	ASTM A139 Grade A Grade B	BS 3601 EFW 22 EFW 27	DIN 1629 Blatt 2 St 37 Blatt 2 St 42	
	ASTM A155 Class 2 C 45 C 50 C 55 KC 55 KC 60 KC 65 KC 70	BS 3602  EFW 28 EFW 28S	DIN 1629, Blatt 3, with certification C St 34-2 St 37-2 St 42-2 St 42-2* St 52-3 St 52-3	
	API 5L Grade A SMLS Grade B SMLS	BS 3601 HFS 27 & CDS 22 HFS 27 & CDS 27	DIN 1629 St 36 St 45	SIS 1233-05 SIS 1434-05
	API 5L Grade A ERW Grade B ERW	BS 3601 ERW 22 ERW 27	DIN 1629 Blatt 3 St 34-2 ERW Blatt 4 St 37-2 ERW	SIS 1233-06 SIS 1434-06
	API 5L Grade A EFW Grade B EFW	BS 3601 Double-welded EFW 22 EFW 27	DIN 1629 Blatt 3 St 34-2 FW Blatt 4 St 37-2 FW	
	API 5L FW	BS 3601 BW 22	DIN 1629 Blatt 3 St 34-2 FW	
*Specify "S-killed" †Specify API 5L Grade B testing procedures for these steels				
STAINLESS-STEEL PIPE	ASTM A312 TP 304 TP 304H TP 304L TP 316 TP 316H TP 316L TP 317 TP 321 TP 321H TP 347 TP 347H	BS 3605 Grade 801 Grade 811 Grade 801L Grade 805 Grade 845  Grade 855 Grade 845L Grade 846 Grade 822 Ti Grade 832 Ti Grade 822 Nb Grade 832 Nb	WSN Designation: 4301 X 6 CrNi 18 9 4306 X 2 CrNi 18 9 4841 X 15 CrNiSi 25 20 4401/ X 5 CrNiMo 18 10 4436  4404 X 2 CrNiMo 18 10 4541 X 10 CrNiTi 18 9 4550 X 10 CrNiNb 18 9	SIS 2333-02 SIS 2352-02 SIS 2361-02 SIS 2343-02  SIS 2353-02 SIS 2337-02 SIS 2338-02
ADDRESSES				
American National Standards Institute, 1430 Broadway, New York, NY 10018, USA British Standards Institution, Sales Branch, 101 Pentonville Road, London N1, England Deutscher Normenausschuss, 1 Berlin 15, Unter den Eichen 175, West Germany Sveriges Standardiseringsnämnd, Box 3295, 10366, Stockholm J, Sweden				
*Piping Guide, PO Box 277, Colton, CA 95926, USA				

The American National Standards Institute has introduced several schedules for pipe made from various plastics. These ANSI standards and others for plastic pipe are listed in table 7.4.

**GLASS** All-glass piping is used for its chemical resistance, cleanliness and transparency. Glass pipe is not subject to 'crazing' often found in glass-lined pipe and vessels subject to repeated thermal stresses. Pipe, fittings, and hardware are available both for process piping and for drainage. Corning Glass Works offers a Pyrex 'Conical' system for process lines in 1, 1½, 2, 3, 4 and 6-inch sizes (ID) with 450 F as the maximum operating temperature, and pressure ranges 0–65 PSIA (1 in. thru 3 in.), 0–50 PSIA (4 in.) and 0–35 PSIA (6 in.). Glass cocks, strainers and thermowells are available. Pipe fittings and equipment are joined by flange assemblies which bear on the thickened conical ends of pipe lengths and fittings. Corning also offers a Pyrex Acid-Waste Drainline system in 1½, 2, 3, 4 and 6-inch sizes (ID) with beaded ends joined by Teflon-gasketed nylon compression couplings. Both Corning systems are made from the same borosilicate glass.

**LININGS & COATINGS** Lining or coating carbon-steel pipe with a material able to withstand chemical attack permits its use to carry corrosive fluids. Lengths of lined pipe and fittings are joined by flanges, and elbows, tees, etc., are available already flanged. Linings (rubber, for example) can be applied after fabricating the piping, but pipe is often pre-lined, and manufacturers give instructions for making joints. Linings of various rubbers, plastics, metals and vitreous (glassy) materials are available. Polyvinyl chloride, polypropylene and copolymers are the most common coating materials. Carbon-steel pipe zinc-coated by immersion into molten zinc (hot-dip galvanized) is used for conveying drinking water, instrument air and various other fluids. Rubber lining is often used to handle abrasive fluids.

**TEMPERATURE & PRESSURE LIMITS** 2.1.5

Carbon steels lose strength at high temperatures. Electric-resistance-welded pipe is not considered satisfactory for service above 750 F, and furnace-butt-welded pipe above about 650 F. For higher temperatures, pipe made from stainless steels or other alloys should be considered.

The Midwest catalog 61 [54], the Taylor Forge catalog 571 and the Ladish catalog 55 [33] give pressure limits for carbon-steel pipe at various temperatures. These tables are derived from the ANSI B31 Code for Pressure Piping (detailed in table 7.2).

**METHODS FOR JOINING PIPE** 2.2

The joints used for most carbon-steel and stainless-steel pipe are:

- BUTT-WELDED . . . . . SEE 2.3
- SOCKET-WELDED . . . . . SEE 2.4
- SCREWED . . . . . SEE 2.5
- BOLTED FLANGE . . . . . SEE 2.3.1, 2.4.1 & 2.5.1
- BOLTED QUICK COUPLINGS . . . . . SEE 2.8.2

**WELDED & SCREWED JOINTS** 2.2.1

Lines 2-inch and larger are usually butt-welded, this being the most economic leakproof way of joining larger-diameter piping. Usually such lines are subcontracted to a piping fabricator for prefabrication in sections termed 'spools', then transported to the site. Lines 1½-inch and smaller are usually either screwed or socket-welded, and are normally field-run by the piping contractor from drawings. Field-run and shop-fabricated piping are discussed in 5.2.9.

**SOCKET-WELDED JOINTS** 2.2.2

Like screwed piping, socket welding is used for lines of smaller sizes, but has the advantage that absence of leaking is assured: this is a valuable factor when flammable, toxic, or radioactive fluids are being conveyed—the use of socket-welded joints is not restricted to such fluids, however.

**BOLTED-FLANGE JOINTS** 2.2.3

Flanges are expensive and for the most part are used to mate with flanged vessels, equipment, valves, and for process lines which may require periodic cleaning.

Flanged joints are made by bolting together two flanges with a gasket between them to provide a seal. Refer to 2.6 for standard forged-steel flanges and gaskets.

**FITTINGS** 2.2.4

Fittings permit a change in direction of piping, a change in diameter of pipe, or a branch to be made from the main run of pipe. They are formed from plate or pipe, machined from forged blanks, cast, or molded from plastics.

Chart 2.1 shows the ratings of butt-welding fittings used with pipe of various schedule numbers and manufacturers' weights. For dimensions of butt-welding fittings and flanges, see tables D-1 thru D-7, and tables F-1 thru F-9. Drafting symbols are given in charts 5.3 thru 5.5.

Screwed or socket-welding forged-steel fittings are rated to the nominal cold non-shock working pressure in pounds per square inch (PSI) of the fitting. Fittings rated at 2000, 3000, and 6000 PSI are available and are used with pipe as shown in table 2.2:

**SCREWED & SOCKET-WELDING FORGED-STEEL FITTINGS TO BE USED WITH CARBON-STEEL PIPE OF VARIOUS WEIGHTS** TABLE 2.2

FORGED-STEEL FITTING (ANSI B18.11)		SCREWED			SOCKET-WELDING	
PRESSURE RATING OF FITTING (PSI)		2000	3000	6000	3000	6000
PIPE 'WEIGHT' USUALLY USED WITH FITTING (ANSI B36.10)	SCHEDULE NUMBER	40	80		80	160
	MANUFACTURERS' WEIGHT	STD	XS	XXS	XS	

Sections 2.1.3 thru 2.2.4 have shown that there is a wide variety of differently-rated pipe, fittings and materials from which to make a choice. Charts 2.1 thru 2.3 show how various weights of pipe, fittings and valves can be combined in a piping system.

## COMPONENTS FOR BUTT-WELDED PIPING SYSTEMS

2.3

**WHERE USED:** For most process, utility and service piping

**ADVANTAGE OF JOINT:** Most practicable way of joining larger pipes and fittings which offers reliable, leakproof joints

**DISADVANTAGE OF JOINT:** Intruding weld metal may affect flow

**HOW JOINT IS MADE:** The end of the pipe is beveled as shown in chart 2.1. Fittings are similarly beveled by the manufacturer. The two parts are aligned, properly gapped, tack welded, and then a continuous weld is made to complete the joint

Chart 2.1 shows the ratings of pipe, fittings and valves that are commonly combined or may be used together. It is a guide only, and not a substitute for a project specification.

## FITTINGS, BENDS, MITERS & FLANGES FOR BUTT-WELDED SYSTEMS

2.3.1

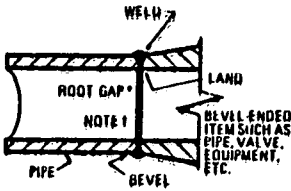
Refer to tables D, F and W-1 for dimensions and weights of fittings and flanges.

**ELBOWS** or 'ELLS' make 90- or 45-degree changes in direction of the run of pipe. The elbows normally used are 'long radius' (LR) with centerline radius of curvature equal to 1½ times the nominal pipe size for 3/4-inch and larger sizes. 'Short radius' (SR) elbows with centerline radius of curvature equal to the nominal pipe size are also available. 90-degree LR elbows with a straight extension at one end ('long tangent') are still available in STD weight, if required.

**REDUCING ELBOW** makes a 90-degree change in direction with change in line size. Reducing elbows have centerline radius of curvature 1½ times the nominal size of the pipe to be attached to the larger end.

**RETURN** changes direction of flow thru 180 degrees, and is used to construct heating coils, vents on tanks, etc.

**BENDS** are made from straight pipe. Common bending radii are 3 and 5 times the pipe size (3R and 5R bends, where R = nominal pipe size—nominal diameter, *not* radius). 3R bends are available from stock. Larger radius bends can be custom made, preferably by hot bending. Only seamless or electric-resistance-welded pipe is suitable for bending.

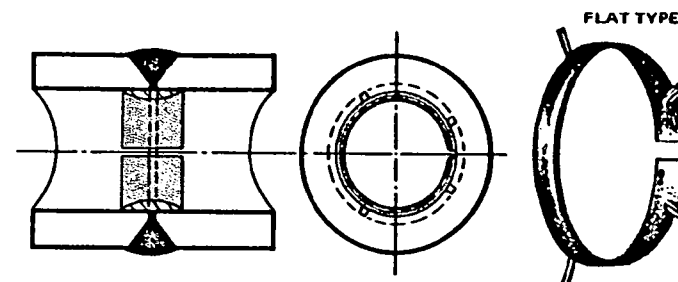
BUTT-WELDED PIPING		CHART 2.1		
CARBON-STEEL PIPE & FORGED-STEEL FITTINGS				
END PREPARATION OF PIPE, & METHOD OF JOINING TO BEVEL-ENDED PIPE, FITTING, FLANGE, VALVE, OR EQUIPMENT				
MINIMUM LINE SIZE NORMALLY BUTT-WELDED		2-INCH		
WEIGHT OF PIPE & FITTINGS NORMALLY USED. CHOICE OF OTHER MATERIALS OR HEAVIER-WEIGHT PIPE & FITTINGS WILL DEPEND ON PRESSURE, TEMPERATURE &/OR THE CORROSION ALLOWANCE REQUIRED. 2-INCH AND LARGER PIPE IS USUALLY ORDERED TO ASTM A-53, Grade B. SEE 2.1.4		FOR NOMINAL PIPE SIZE:	2 to 8 INCH	8 INCH and larger CALCULATE WALL THICKNESS FROM CODE
		SCHEDULE NUMBER	SCH 40	SCH 20 or SCH 30
		MFRS' WEIGHT	STD	—
VALVES				
PRESSURE RATING IN PSI	FOR 2-INCH AND LARGER VALVES	150, 300, 600, 900 AND HIGHER ACCORDING TO SYSTEM PRESSURE		
	FOR 1½-INCH AND SMALLER VALVES	SEE CHARTS 2.2 AND 2.3		
	FOR CONTROL VALVES	USUALLY 300 MINIMUM (SEE 1.1.10)		
"Piping Guide", P.O. Box 277, Corvallis, OR 97331, U.S.A.				

\*See 5.3.5 under 'Dimensioning spools'

1A 'backing ring'—sometimes termed a 'chill ring'—may be inserted between any butt welding joint prior to welding. Preventing weld spatter and spikes ('icicles') of weld metal from forming inside the pipe during welding, the ring also serves as an alignment aid. Normally used for severe service, but should be considered for process fluids such as fibrous suspensions, where weld icicles could result in material collecting at joints and choking lines. See 2.11

BACKING RING

FIGURE 2.1



(COURTESY TUBE TURNS DIV. OF CHEMETRON INC)

# **ELBOWS & RETURNS** (COURTESY TAYLOR FORGE & PIPE WORKS)

FIGURE 2.2

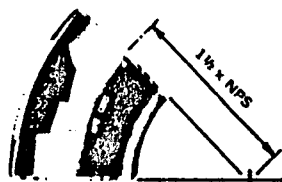
90° LONG-RADIUS  
ELBOW



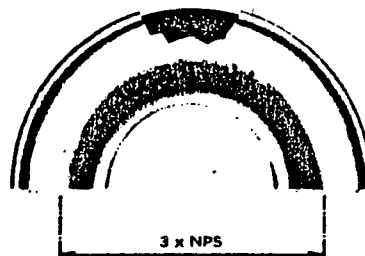
90° SHORT-RADIUS  
ELBOW



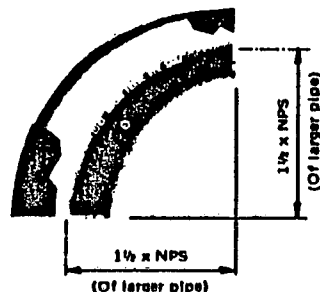
45° ELBOW  
(LR)



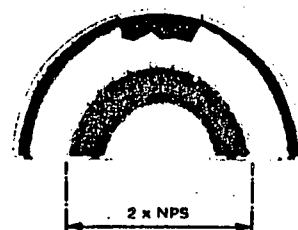
LONG-RADIUS  
RETURN



REDUCING  
ELBOW



SHORT-RADIUS  
RETURN



**REDUCER (or INCREASER)** joins a larger pipe to a smaller one. The two available types, concentric and eccentric, are shown. The eccentric reducer is used when it is necessary to keep either the top or the bottom of the line level--offset equals  $\frac{1}{2} \times$  (larger ID minus smaller ID).

## **REDUCERS**

(COURTESY TUBE TURNS DIV. OF CHEMETRON INC.)

FIGURE 2.3

CONCENTRIC



ECCENTRIC



**SWAGE** is employed to connect butt-welded piping to smaller screwed or socket-welded piping. In butt-welded lines, used as an alternative to the reducer when greater reductions in line size are required. Regular swages in concentric or eccentric form give abrupt change of line size, as do reducers. The 'venturi' swage allows smoother flow. Refer to table 2.3 for specifying swages for joining to socket-welding items, and to table 2.4 for specifying swages for joining to screwed piping. For offset, see 'Reducer'.

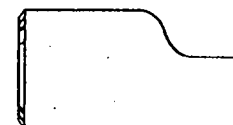
## **SWAGES, or SWAGED NIPPLES**

FIGURE 2.4

CONCENTRIC



ECCENTRIC



VENTURI TYPE

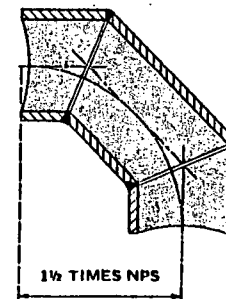


**MITERED ELBOWS** are fabricated as required from pipe—they are not fittings. The use of miters to make changes in direction is practically restricted to low-pressure lines 10-inch and larger if the pressure drop is unimportant; for these uses regular elbows would be costlier. A 2-piece, 90-degree miter has four to six times the hydraulic resistance of the corresponding regular long-radius elbow, and should be used with caution. A 3-piece 90-degree miter has about double the resistance to flow of the regular long-radius elbow—refer to table F-10. Constructions for 3-, 4-, and 5-piece miters are shown in tables M-2.

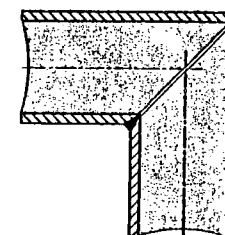
## **3-PIECE & 2-PIECE MITERS**

FIGURE 2.5

3-PIECE MITER



2-PIECE MITER



THE 2-PIECE MITER HAS HIGH FLOW RESISTANCE (See TABLE F-10)

CHART  
2.1

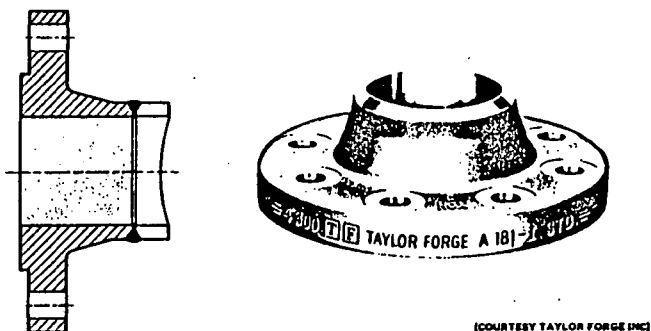
FIGURES  
2.1–2.5

The following five flange types are used for butt-welded lines. The different flange facings available are discussed in 2.6.

**WELDING-NECK FLANGE, REGULAR & LONG** *Regular welding-neck flanges are used with butt-welding fittings.* Long welding-neck flanges are primarily used for vessel and equipment nozzles, rarely for pipe. Suitable where extreme temperature, shear, impact and vibratory stresses apply. Regularity of the bore is maintained. Refer to tables F for bore diameters of these flanges.

WELDING-NECK FLANGE

FIGURE 2.6

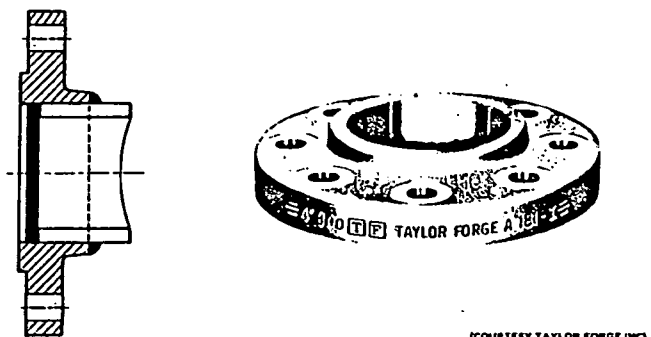


[COURTESY TAYLOR FORGE INC]

**SLIP-ON FLANGE** is properly used to flange pipe. Slip-on flanges can be used with long-tangent elbows, reducers, and swages (not usual practice). The internal weld is slightly more subject to corrosion than the butt weld. The flange has poor resistance to shock and vibration. It introduces irregularity in the bore. It is cheaper to buy than the welding-neck flange, but is costlier to assemble. It is easier to align than the welding-neck flange. Calculated strengths under internal pressure are about one third that of the corresponding welding-neck flanges. The pipe or fitting is set back from the face of the flange a distance equal to the wall thickness  $-0'' + 1/16''$ .

SLIP-ON FLANGE

FIGURE 2.7



[COURTESY TAYLOR FORGE INC]

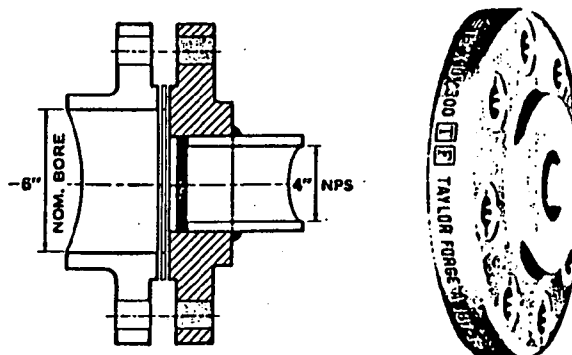
**REDUCING FLANGE** Suitable for changing line size, but should not be used if abrupt transition would create undesirable turbulence, as at pump connections. Available to order in welding-neck and eccentric types, and from stock in slip-on types. Specify by line size of the smaller pipe and the OD of the flange to be mated. Example: a slip-on reducing flange to connect 4-inch pipe to a 6-inch line-size flange for 150 PSI service is ordered:

RED FLG 4"x11"OD 150 # SO

For a welding-neck reducing flange, correct bore is obtained by giving the pipe schedule number or manufacturers' weight of the pipe to be welded on.

REDUCING SLIP-ON FLANGE

FIGURE 2.8

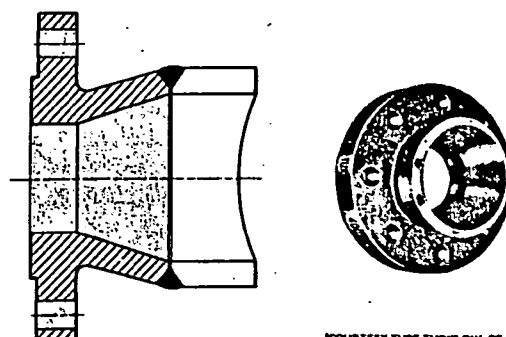


[COURTESY TAYLOR FORGE INC]

**EXPANDER FLANGE** Application as for welding-neck flange see above. Increases pipe size to first or second larger size. Alternative to using reducer and welding-neck flange. Useful for connecting to valves, compressors and pumps. Pressure ratings and dimensions are in accord with ANSI B16.5. Available from the Tube Turns Division of the Chemetron Corporation, and from the Tube-Line Manufacturing Company.

EXPANDER (or INCREASER) FLANGE

FIGURE 2.9



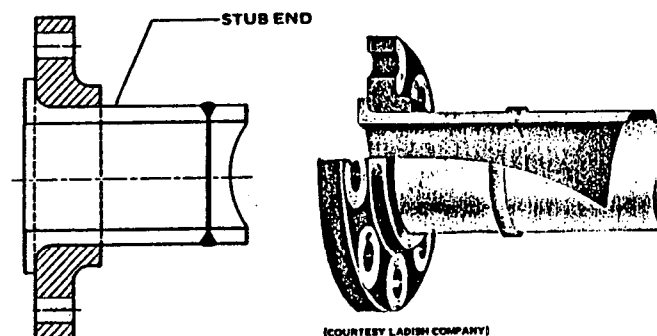
[COURTESY TUBE TURNS DIV. OF CHEMETRON INC]



**LAP-JOINT, or 'VAN STONE', FLANGE** Economical if costly pipe such as stainless steel is used, as the flange can be of carbon steel and only the lap-joint stub end need be of the line material. A stub end must be used in a lap joint, and the cost of the two items must be considered. If both stub and flange are of the same material they will be more expensive than a welding-neck flange. Useful where alignment of bolt holes is difficult, as with spools to be attached to flanged nozzles of vessels.

LAP-JOINT FLANGE (with Stub-end)

FIGURE 2.10



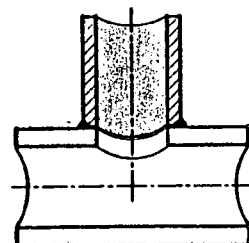
### BUTT-WELDING FITTINGS FOR BRANCHING FROM BUTT-WELDED SYSTEMS

2.3.2

**STUB-IN** Term for a branch pipe welded directly into the side of the main pipe run—it is not a fitting. This is the commonest and least expensive method of welding a full-size or reducing branch for pipe 2-inch and larger. A stub-in can be reinforced by means set out in 2.11.

STUB-IN

FIGURE 2.11



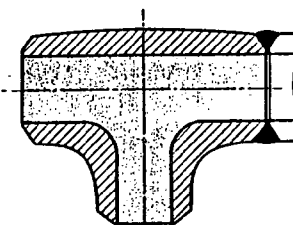
**BUTT-WELDING TEES, STRAIGHT or REDUCING**, are employed to make 90-degree branches from the main run of pipe. Straight tees, with branch the same size as the run, are readily available. Reducing tees have branch smaller than the run. Bullhead tees have branch larger than the run, and are very seldom used but can be made to special order. None of these tees requires reinforcement. Reducing tees are ordered as follows:—

### SPECIFYING SIZE OF BUTT-WELDING REDUCING TEES

HOW TO SPECIFY TEES:	RUN INLET	RUN OUTLET	BRANCH	EXAMPLE
REDUCING ON BRANCH	6"	6"	4"	RED TEE 6" x 6" x 4"

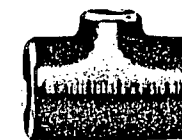
BUTT-WELDING TEES

FIGURE 2.12



STRAIGHT BUTT-WELDING TEE

REDUCING BUTT-WELDING TEE



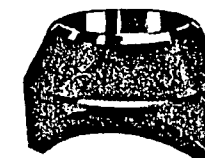
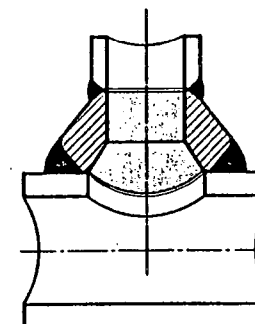
(COURTESY TUBE TURNS DIV. OF CHEMETRON INC)

The next four branching fittings are made by Bonney Forge and Foundry Inc. These fittings offer an alternate means of connecting into the main run, and do not require reinforcement. They are preshaped to the curvature of the run pipe.

**WELDOLET** makes a 90-degree branch, full-size or reducing, on straight pipe. Closer manifolding is possible than with tees. Flat-based weldolets are available for connecting to pipe caps and vessel heads.

WELDOLET

FIGURE 2.13

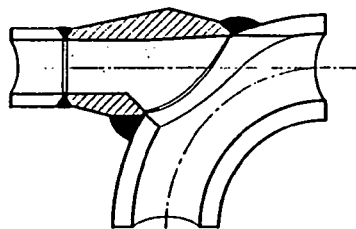


(COURTESY BONNEY FORGE & FOUNDRY INC)

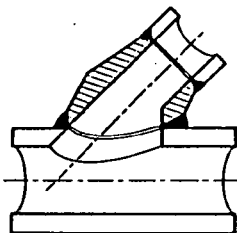
FIGURES  
2.6–2.13

**BUTT-WELDING ELBOLET** makes a reducing tangent branch on long-radius and short-radius elbows.

**ELBOLET**  
**FIGURE 2.14**



**BUTT-WELDING LATROLET**  
**FIGURE 2.15**

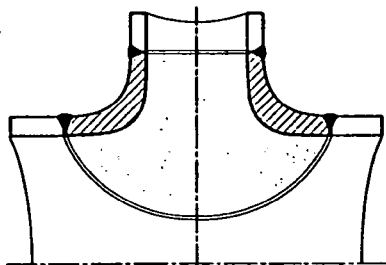


**BUTT-WELDING LATROLET** makes a 45-degree reducing branch on straight pipe.

**SWEEPOLET** makes a 90-degree reducing branch from the main run of pipe. Primarily developed for high-yield pipe used in oil and gas transmission lines. Provides good flow pattern, and optimum stress distribution.

**SWEEPOLET**

**FIGURE 2.16**



(COURTESY BONNEY FORGE & FOUNDRY INC)

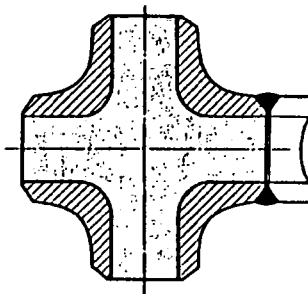


The next three fittings are usually used for special designs:

**CROSS, STRAIGHT or REDUCING** Straight crosses are usually stock items. Reducing crosses may not be readily available. For economy, availability and to minimize the number of items in inventory, it is preferred to use tees, etc., and not crosses, except where space is restricted, as in marine piping or 're-vamp' work. Reinforcement is not needed.

**BUTT-WELDING CROSS**

**FIGURE 2.17**

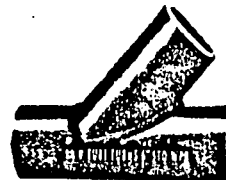
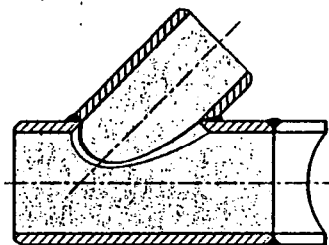


(COURTESY TUBE TURNS DIV. OF CHEMETRON INC)

**LATERAL, STRAIGHT or REDUCING**, permits odd-angled entry into the pipe run where low resistance to flow is important. Straight laterals with branch bore equal to run bore are available in STD and XS weights. Reducing laterals and laterals at angles other than 45 degrees are usually available only to special order. Reinforcement is required where it is necessary to restore the strength of the joint to the full strength of the pipe. Reducing laterals are ordered similarly to butt-welding tees, except that the angle between branch and run is also stated.

**LATERAL**

**FIGURE 2.18**

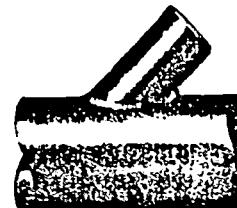
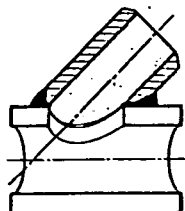


(COURTESY TUBE TURNS DIV. OF CHEMETRON INC)

**SHAPED NIPPLE** Now rarely used, but can be obtained from stock in 90- and 45-degree angles, and in any size and angle, including offset, to special order. The run is field-cut, using the nipple as template. Needs reinforcement if it is necessary to bring the strength of the joint up to the full strength of the pipe.

**SHAPED NIPPLE**

**FIGURE 2.19**



**CAP** is used to seal the end of pipe. (See figure 2.20(a).)

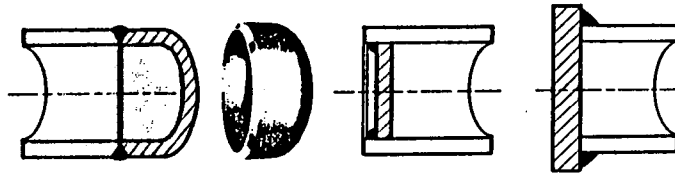
**FLAT CLOSURES** Flat plates are normally cut especially from plate stock by the fabricator or erector. (See figure 2.20 (b) and (c).)

## THREE WELDED CLOSURES

FIGURE 2.20

(a) BUTT-WELDING CAP

(b) FLAT CLOSURE (c) FLAT CLOSURE



(COURTESY MIDWEST FITTING DIVISION, CRANE CO.)

**ELLIPSOIDAL, or DISHED, HEADS** are used to close pipes of large diameter, and are similar to those used for constructing vessels.

## COMPONENTS FOR SOCKET-WELDED PIPING SYSTEMS

2.4

## WHERE USED:

For lines conveying flammable, toxic, or expensive material, where no leakage can be permitted. For steam: 300 to 600 PSI, and sometimes 150 PSI steam. For corrosive conditions, see Index under 'Corrosion'

## ADVANTAGES OF JOINT:

- (1) Easier alignment on small lines than butt welding. Tack welding is unnecessary
- (2) No weld metal can enter bore
- (3) Joint will not leak, when properly made

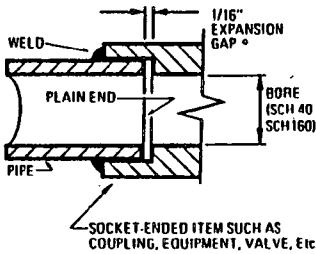
## DISADVANTAGES OF JOINT:

- (1) The 1/16-inch recess in joint (see chart 2.2) pockets liquid
- (2) Use not permitted by ANSI B31.1.0-1967 if severe erosion or crevice corrosion is anticipated

## HOW JOINT IS MADE:

The end of the pipe is finished flat, as shown in chart 2.2. It is located in the fitting, valve, flange, etc., and a continuous fillet weld is made around the circumference

Chart 2.2 shows the ratings of pipe, fittings and valves that are commonly combined, or may be used together. The chart is a guide only, and not a substitute for a project specification.

SOCKET-WELDED PIPING				CHART 2.2	
CARBON-STEEL PIPE & FORGED-STEEL FITTINGS					
END PREPARATION OF PIPE, AND METHOD OF JOINING TO FITTING, FLANGE, VALVE, OR EQUIPMENT					
MAXIMUM LINE SIZE NORMALLY SOCKET WELDED			1½-INCH (2½-INCH IN MARINE PIPING)		
AVAILABILITY OF FORGED-STEEL SOCKET-WELDING FITTINGS			1/8- TO 4-INCH		
WEIGHTS OF PIPE AND PRESSURE RATINGS OF FITTINGS WHICH ARE COMPATIBLE*	PIPE	SCHEDULE NUMBER	SCH 40	SCH 80	SCH 160
		MFRS' WEIGHT	STD	XS	—
	FITTINGS	FITTING RATING	3000 PSI	3000 PSI	6000 PSI
		FITTING BORED TO:	SCH 40	SCH 40	SCH 160
<div>↑</div> <div>MOST COMMON COMBINATION: CHOICE OF MATERIAL OR HEAVIER-WEIGHT PIPE AND FITTING WILL DEPEND ON PRESSURE, TEMPERATURE AND/OR CORROSION ALLOWANCE REQUIRED. PIPE 1½-INCH AND SMALLER IS USUALLY ORDERED TO ASTM SPECIFICATION A-106 Grade B. REFER TO 2.1.4</div>					
VALVES					
MINIMUM PRESSURE RATING IN PSI	CONTROL VALVES (USUALLY FLANGED)		USUALLY 300 (SEE 3.1.10)		
	VALVES OTHER THAN CONTROL VALVES		600 (ANSI) 800 (API)		

\* ANSI B16.11-1968 recommends a 1/16th-inch gap to prevent weld from cracking under thermal stress  
 †Socket-ended fittings are now only made in 3000 and 6000 PSI ratings (ANSI B16.11-1968)

## FITTINGS & FLANGES FOR SOCKET-WELDED SYSTEMS

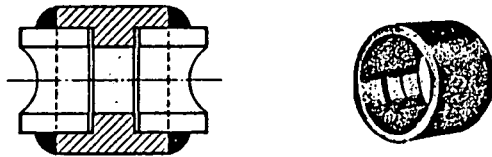
2.4.1

Dimensions of fittings and flanges are given in tables D-8 and F-8.

**FULL-COUPLING** (termed 'COUPLING') joins pipe to pipe, or to a nipple, swage, etc.

FULL-COUPLING

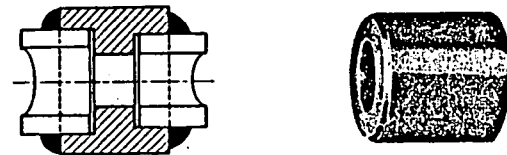
FIGURE 2.21



**REDUCER** joins two different diameters of pipe.

REDUCER

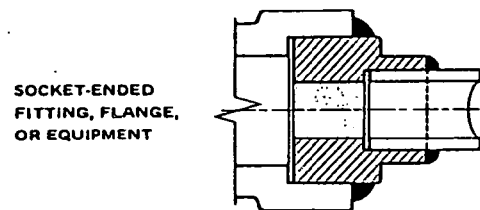
FIGURE 2.22



**REDUCER INSERT** A reducing fitting used for connecting a small pipe to a larger fitting. Socket-ended reducer inserts can be made in any reduction by boring standard forged blanks.

SOCKET-WELDING REDUCING INSERTS

FIGURE 2.23



THREE FORMS  
OF REDUCER  
INSERT:

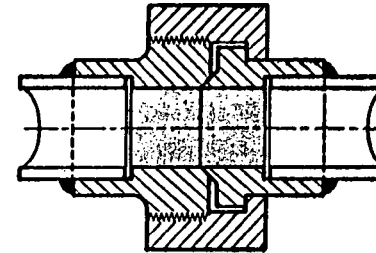


(COURTESY LADISH COMPANY)

**UNION** is used primarily for maintenance and installation purposes. This is a screwed joint designed for use with socket-welded piping systems. See explanation in 2.5.1 of uses given under 'screwed union'. Union should be screwed tight before the ends are welded, to minimize warping of the seat.

SOCKET-WELDING UNION

FIGURE 2.24



**SWAGED NIPPLES** According to type, these allow joining: (1) Socket-ended items of different sizes—this type of swaged nipple has both ends plain (PBE) for insertion into socket ends. (2) A socket-ended item to a larger butt-welding pipe or fitting—this type of swaged nipple has the larger end beveled (BLE) and the smaller end plain (PSE) for insertion into a socket-ended item. A swaged nipple is also referred to as a 'swage' (pronounced 'swedge') abbreviated on drawings as 'SWG' or 'SWG NIPP'. When ordering a swage, state the weight designations of the pipes to be joined: for example, 2"(SCH 40) x 1"(SCH 80). Examples of the different end terminations that may be specified are as follows:—

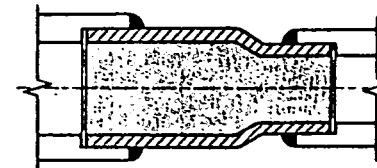
SPECIFYING SIZE & END FINISH  
OF SOCKET-WELDING SWAGES

TABLE 2.3

SWAGE FOR JOINING— LARGER to SMALLER		EXAMPLE NOTE ON DRAWING
SW ITEM BW FITTING or PIPE	SW ITEM SW ITEM	SWG 1½" x 1" PBE SWG 2" x 1" BLE -PSE
ABBREVIATIONS:		SW = Socket welding BW = Butt welding PBE = Plain both ends PLE = Plain large end PSE = Plain small end BLE = Bevel large end

SWAGE (PBE)

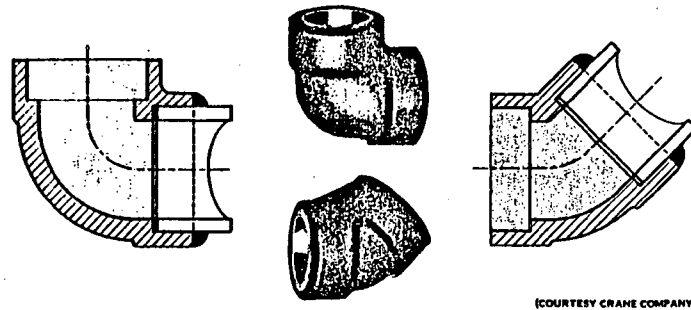
FIGURE 2.25



ELBOWS make 90- or 45-degree changes of direction in the run of pipe.

#### SOCKET-WELDING ELBOWS

FIGURE 2.26

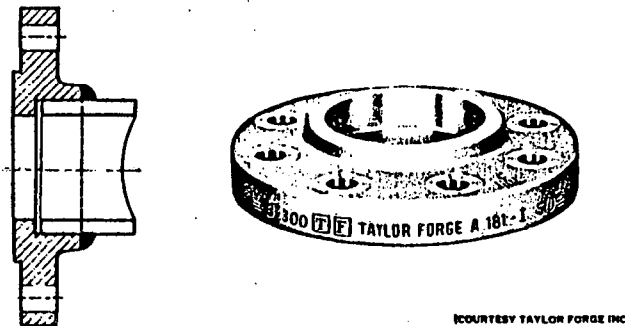


**SOCKET-WELDING FLANGE** Regular type is available from stock. Reducing type is available to order. For example, a reducing flange to connect a 1-inch pipe to a 1½-inch line-size flange for 150 PSI service is specified:

RED FLG 1" x 5" OD 150# SW

#### SOCKET-WELDING FLANGE

FIGURE 2.27



#### FITTINGS FOR BRANCHING FROM SOCKET-WELDED SYSTEMS

2.4.2

#### BRANCH FROM SOCKET-WELDED RUN

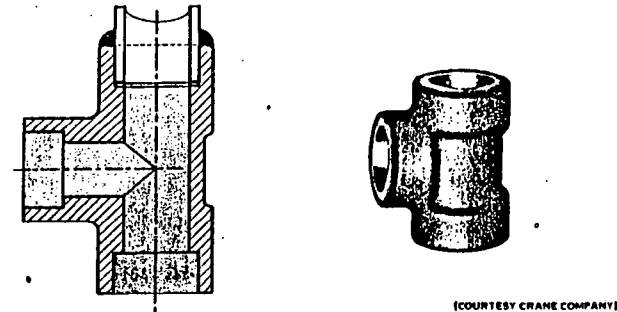
**TEE, STRAIGHT or REDUCING**, makes 90-degree branch from the main run of pipe. Reducing tees are custom-fabricated by boring standard forged blanks.

#### SPECIFYING SIZE OF SOCKET-WELDING TEES

HOW TO SPECIFY TEES:	RUN INLET	RUN OUTLET	BRANCH	EXAMPLE
REDUCING ON BRANCH	1½"	1½"	1"	RED TEE 1½" x 1½" x 1"
REDUCING ON RUN (SPECIAL APPLICATIONS ONLY)	1½"	1"	1½"	RED TEE 1½" x 1" x 1½"

#### SOCKET-WELDING TEE

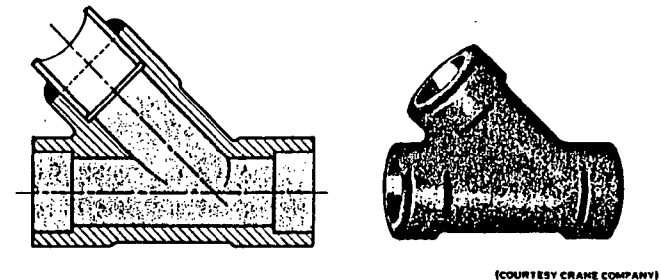
FIGURE 2.28



**LATERAL** makes full-size 45-degree branch from the main run of pipe.

#### SOCKET-WELDING LATERAL

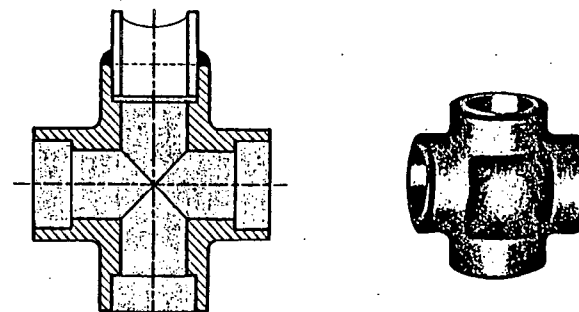
FIGURE 2.29



**CROSS** Remarks for butt-welding cross apply—see 2.3.2. Reducing crosses are custom-fabricated by boring standard forged blanks.

#### SOCKET-WELDING CROSS

FIGURE 2.30



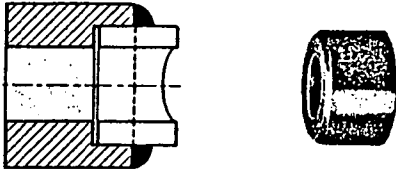
FIGURES  
2.21–2.30

TABLE  
2.3

**HALF-COUPLING** The full-coupling is not used for branching or for vessel connections, as the half-coupling is the same length and is stronger. The half-coupling permits 90-degree entry into a larger pipe or vessel wall. The socketlet is more practicable as shaping is necessary with the coupling.

SOCKET-WELDING HALF-COUPLING

FIGURE 2.31

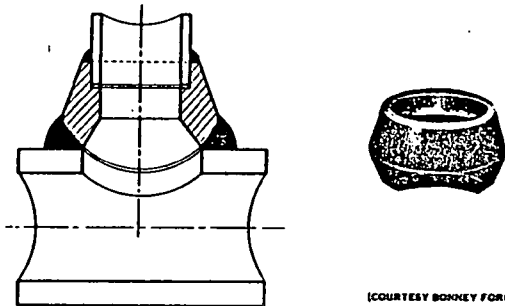


The next four fittings are made by Bonney Forge and Foundry Inc, and offer an alternate method of entering the main pipe run. They have the advantage that the beveled welding ends are shaped to the curvature of the run pipe. Reinforcement for the butt-welded piping or vessel is not required.

**SOCKOLET** makes a 90-degree branch, full-size or reducing, on straight pipe. Flat-based socketlets are available for branch connections on pipe caps and and vessel heads.

SOCKOLET

FIGURE 2.32

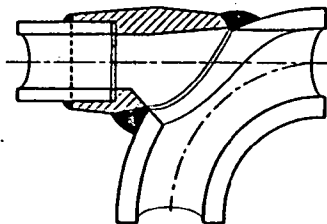


(COURTESY BONNEY FORGE & FOUNDRY INC)

**SOCKET-WELDING ELBOLET** makes a reducing tangent branch on long-radius and short-radius elbows.

SOCKET-WELDING ELBOLET

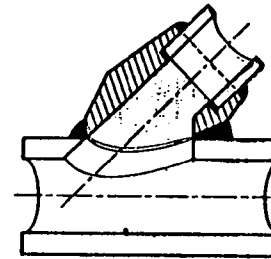
FIGURE 2.33



**SOCKET-WELDING LATROLET** makes a 45-degree reducing branch on straight pipe.

SOCKET-WELDING LATROLET

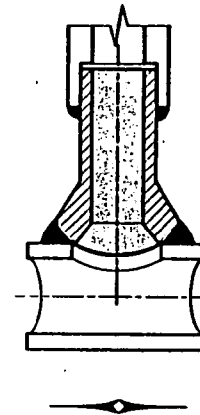
FIGURE 2.34



**NIPOLET** A variant of the socketlet, having integral plain nipple. Primarily developed for small valved connections—see figure 6.47.

NIPOLET

FIGURE 2.35



**STUB-IN** See comments in 2.3.2. Not preferred for lines under 2-inch due to risk of weld metal entering line and restricting flow.

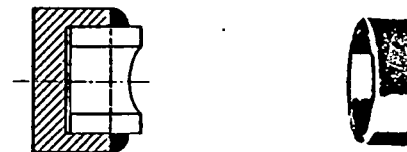
CLOSURE

2.4.4

**SOCKET-WELDING CAP** seals plain-ended pipe.

SOCKET-WELDING CAP

FIGURE 2.36



(COURTESY KERRY VOST MACHINE CO.)

## COMPONENTS FOR SCREWED PIPING SYSTEMS

2.5

- WHERE USED:** For lines conveying services, and for smaller process piping
- ADVANTAGES:**
- (1) Easily made from pipe and fittings on site
  - (2) Minimizes fire hazard when installing piping in areas where flammable gases or liquids are present
- DISADVANTAGES:**
- (1)\* Use not permitted by ANSI B31.1.0-1967, if severe erosion, crevice corrosion, shock, or vibration is anticipated, nor at temperatures over 925 F. For corrosive conditions, see Index under 'Corrosion'
  - (2) Possible leakage of joint
  - (3)\* Seal welding may be required—see footnote to chart 2.3
  - (4) Strength of the pipe is reduced, as forming the screwthread reduces the wall thickness

\*These remarks apply to systems using forged-steel fittings.

### FITTINGS & FLANGES FOR SCREWED SYSTEMS

2.5.1

A wide range of screwed fittings has been developed by many manufacturers for special purposes, and for plumbing in buildings. Most of these fittings are not utilized in process piping, although their pressure and temperature ratings may be suitable.

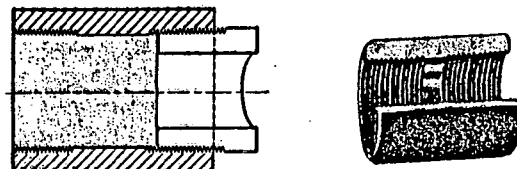
Galvanized 150 and 300 PSI malleable-iron fittings and similarly-rated valves are used with SCH 40 pipe for drinking water and air lines. The overall economics are in favor of utilizing as few different types of screwed fittings as possible. Material specifications, drafting, checking, purchasing and warehousing are simplified. Dimensions of malleable-iron fittings are given in table D-9.

Screwed forged-steel fittings are used more extensively than cast-iron and malleable-iron fittings because of their greater mechanical strength. Dimensions of forged-steel screwed fittings are given in table D-10.

**FULL-COUPLING** (termed 'COUPLING') joins pipe or items with threaded ends.

**FULL-COUPLING**

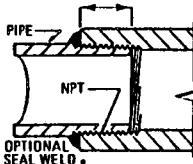
FIGURE 2.37



## SCREWED PIPING

CHART 2.3

Chart 2.3 shows the ratings of pipe, fittings and valves that are commonly combined, or may be used together. The chart is a guide only, and not a substitute for a project specification.

SCREWED PIPING			CHART 2.3		
CARBON-STEEL PIPE & FORGED-STEEL FITTINGS					
END PREPARATION OF PIPE, AND METHOD OF JOINING TO FITTING, FLANGE, VALVE OR EQUIPMENT			<div>THREAD ENGAGEMENT</div>  <div>SCREWED ITEM SUCH AS VALVE, COUPLING, EQUIPMENT, ETC.</div>		
MAXIMUM LINE SIZE NORMALLY SCREWED			1½-INCH		
AVAILABILITY OF FORGED-STEEL SCREWED FITTINGS			1/8- TO 4-INCH		
WEIGHTS OF PIPE AND PRESSURE RATINGS OF FITTINGS WHICH ARE COMPATIBLE	PIPE	SCHEDULE NUMBER	SCH 40	SCH 80	—
		MFERS' WEIGHT	STD	XS	XXS
		FITTING RATING	2000 PSI	3000 PSI	6000 PSI
<div>↑</div> <div>MOST COMMON COMBINATION: THE MINIMUM RATING FOR FITTINGS PREFERRED IN MOST INSTANCES FOR MECHANICAL STRENGTH IS 3000 P S I. CHOICE OF MATERIAL OR HEAVIER-WEIGHT PIPE &amp; FITTING WILL DEPEND ON PRESSURE, TEMPERATURE AND/OR CORROSION ALLOWANCE REQUIRED. PIPE 1½-INCH &amp; SMALLER IS USUALLY ORDERED TO ASTM SPECIFICATION A-106 Grade B. REFER TO 2.1.4</div>					
VALVES					
MINIMUM PRESSURE RATING IN PSI	CONTROL VALVES (USUALLY FLANGED)		USUALLY 300 (SEE 3.1.10)		
	VALVES OTHER THAN CONTROL VALVES		600 (ANSI) 800 (API)		
"Piping Outlet", PO Box 277, Colton, CA 95728, USA					

\* ANSI B31.1.0-1967 states that seal welding shall not be considered to contribute to the strength of the joint

### SEAL WELDING APPLICATIONS

On-plot: On all screwed connections within battery limits, with the exception of piping carrying air or other inert gas, and water  
Off-plot: On screwed lines for hydrocarbon service and for lines conveying dangerous, toxic, corrosive or valuable fluids

2 .4.3  
.5.1

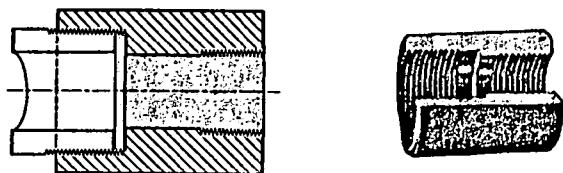
CHART  
2.3

FIGURES  
2.31-2.37

**REDUCING COUPLING, or REDUCER,** joins threaded pipes of different sizes. Can be made in any reduction by boring and tapping standard forged blanks.

#### REDUCING COUPLING

FIGURE 2.38

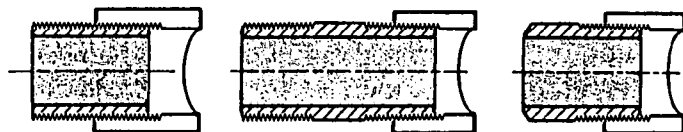


**NIPPLES** join unions, valves, strainers, fittings, etc. Basically a short length of pipe either fully threaded (close nipple) or threaded both ends (TBE), or plain one end and threaded one end (POE-TOE). Available in various lengths—see tables D-9 and D-10. Nipples can be obtained with a Victaulic groove at one end.

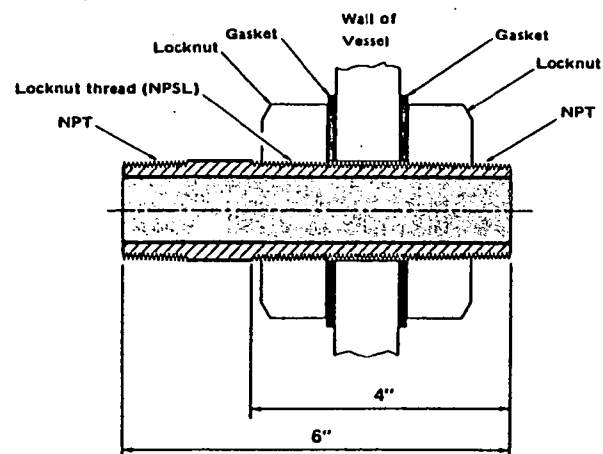
#### NIPPLES FOR SCREWED ITEMS

FIGURE 2.39

- (a) CLOSE NIPPLE      (b) LONG (or SHORT) NIPPLE (TBE)      (c) NIPPLE (POE-TOE)



#### (d) TANK NIPPLE

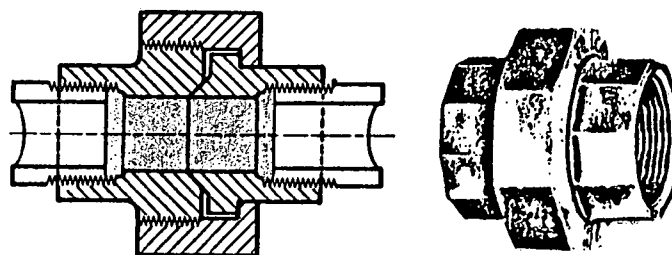


**TANK NIPPLE** is used for making a screwed connection to a non-pressure vessel or tank in low-pressure service. Overall length is usually 6 inches with a standard taper pipe thread at each end. On one end only, the taper pipe thread runs into a ANSI lock-nut thread.

**UNION** makes a joint which permits easy installation, removal or replacement of lengths of pipe, valves or vessels in screwed piping systems. Examples: to remove a valve it must have at least one adjacent union, and to remove piping from a vessel with screwed connections, each outlet from the vessel should have one union between valve and vessel. Ground-faced joints are preferred, although other facings are available.

#### SCREWED UNION

FIGURE 2.40

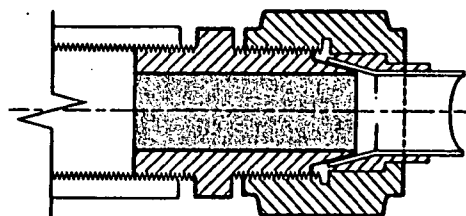


(COURTESY STANLEY Q. FLAGG & CO. INC.)

**PIPE-TO-TUBE CONNECTOR** For joining threaded pipe to tube. Figure 2.41 shows a connector fitted to specially-flared tube. Other types are available.

#### PIPE-TO-TUBE CONNECTOR

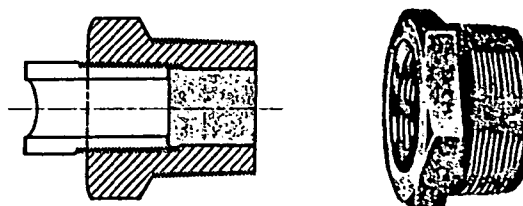
FIGURE 2.41



**HEXAGON BUSHING** A reducing fitting used for connecting a smaller pipe into a larger screwed fitting or nozzle. Has many applications to instrument connections. Reducing fittings can be made in any reduction by boring and tapping standard forged blanks. Normally not used for high-pressure service.

#### HEXAGON BUSHING

FIGURE 2.42



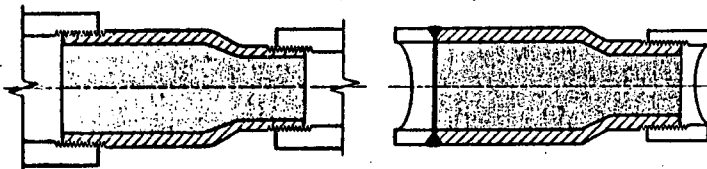


**SWAGED NIPPLE** This is a reducing fitting, used for joining larger diameter to smaller diameter pipe. Also referred to as a 'swage (pronounced 'swedge') and abbreviated as 'SWG' or 'SWG NIPP' on drawings. When ordering a swage, state the weight designations of the pipes to be joined: for example, 2"(SCH 40) x 1"(SCH 80). A swage may be used for joining: (1) Screwed piping to screwed piping. (2) Screwed piping to butt-welded piping. (3) Butt-welded piping to a screwed vessel nozzle. It is necessary to specify on the piping drawing the terminations required.

SPECIFYING SIZE & END FINISH OF SCREWED SWAGES TABLE 2.4

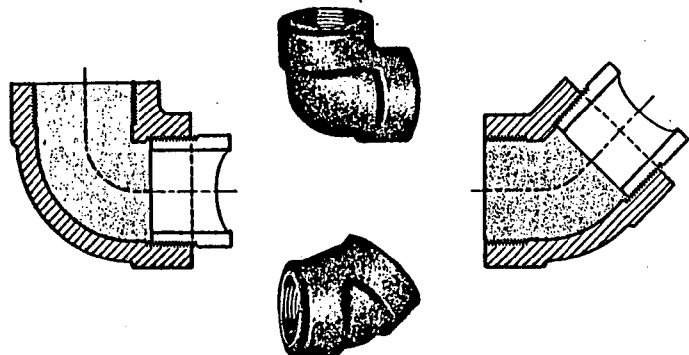
SWAGE FOR JOINING — LARGER to SMALLER		EXAMPLE NOTE ON DRAWING
SCRD ITEM BW ITEM or PIPE SCRD ITEM*	SCRD ITEM SCRD ITEM BW ITEM*	SWG 1½" x 1" TBE SWG 2" x 1" BLE-TSE SWG 3" x 2" TLE-BSE
* This example is not too common, but may occur when a butt-welded line is to be joined to a screwed nozzle (coupling) on a vessel		
ABBREVIATIONS:		BW = Butt welding      SCRD = Screwed TBE = Threaded both ends    TLE = Threaded large end TSE = Threaded small end BLE = Beveled large end    BSE = Beveled small end

SWAGED NIPPLES, TBE and BLE-TSE FIGURE 2.43



**ELBOWS** make 90- or 45-degree changes in direction of the run of pipe. Street elbows having an integral nipple at one end (see table D-9) are available.

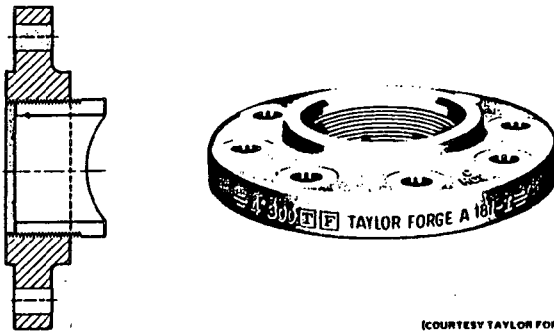
SCREWED ELBOWS, 45 and 90 DEGREE FIGURE 2.44



**SCREWED FLANGES** are used to connect screwed pipe to flanged items. Regular and reducing types are available from stock. For example, a reducing flange to connect 1-inch pipe to a 1½-inch line-size flange for 150 PSI service is specified:

RED FLG 1" x 5" OD 150# SCRD

SCREWED FLANGE FIGURE 2.45



(COURTESY TAYLOR FORGE INC)

FITTINGS FOR BRANCHING FROM SCREWED SYSTEMS 2.5.2

BRANCH FROM SCREWED MAIN RUN

**TEE, STRAIGHT or REDUCING**, makes a 90-degree branch from the run of pipe. Reducing tees are made by boring and tapping standard forged blanks.

SPECIFYING SIZE OF SCREWED REDUCING TEES

HOW TO SPECIFY TEES:	RUN INLET	RUN OUTLET	BRANCH	EXAMPLE
REDUCING ON BRANCH	1½"	1½"	1"	RED TEE 1½" x 1½" x 1"
REDUCING ON RUN (SPECIAL APPLICATIONS ONLY)	1½"	1"	1½"	RED TEE 1½" x 1" x 1½"

FIGURES  
2.38-2.46

SCREWED TEES, STRAIGHT and REDUCING FIGURE 2.46

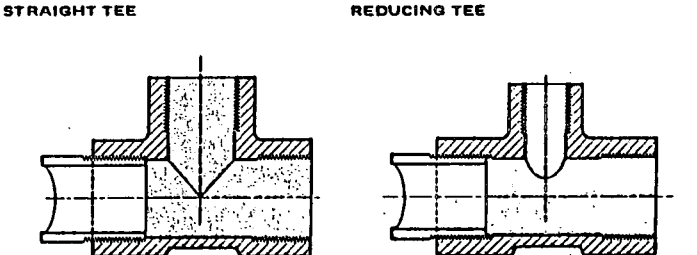
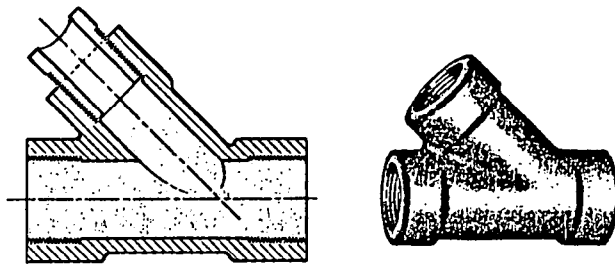


TABLE  
2.4

**LATERAL** makes full-size 45-degree branch from the main run of pipe.

**SCREWED LATERAL**

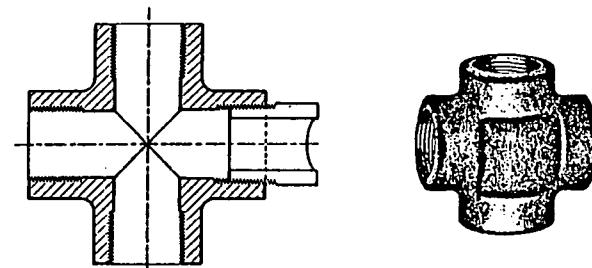
**FIGURE 2.47**



**CROSS** Remarks for butt-welding cross apply — see 2.3.2. Reducing crosses are made by boring and tapping standard forged blanks.

**SCREWED CROSS**

**FIGURE 2.48**



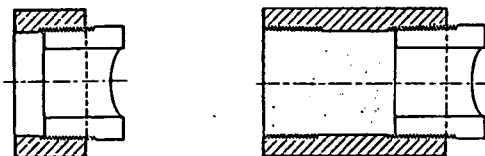
**FITTINGS FOR SCREWED BRANCH FROM VESSEL OR BUTT-WELDED MAIN RUN**

2.5.3

**HALF-COUPLING** can be used to make 90-degree screwed connections to pipes for instruments, or for vessel nozzles. Welding heat may cause embrittlement of the threads of this short fitting. Requires shaping.

**SCREWED HALF-COUPLING & FULL-COUPLING**

**FIGURE 2.49**



**FULL-COUPLING** Superior to half-coupling. Also requires shaping for connecting to pipe.

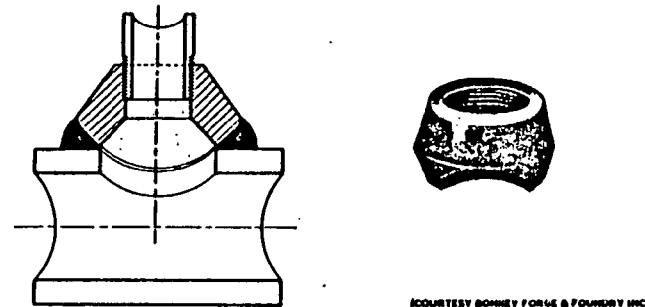
**TANK NIPPLE** See 2.5.1, figure 2.39(d).

The next four fittings for branching are made by Bonney Forge and Foundry Inc. These fittings offer a means of joining screwed piping to a welded run, and for making instrument connections. The advantages are that the welding end does not require reinforcement and that the ends are shaped to the curvature of the run pipe.

**THREDOLET** makes a 90-degree branch, full or reducing, on straight pipe. Flat-based thredolets are available for branch connections on pipe caps and vessel heads.

**THREDOLET**

**FIGURE 2.50**

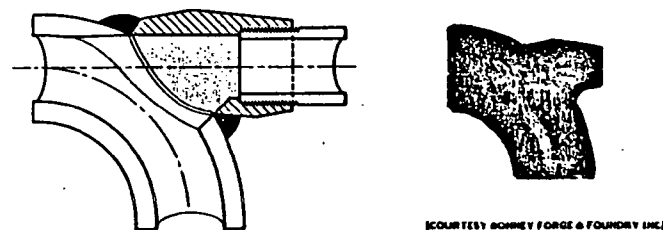


(COURTESY BONNEY FORGE & FOUNDRY INC.)

**SCREWED ELBOLET** makes reducing tangent branch on long-radius and short-radius elbows.

**SCREWED ELBOLET**

**FIGURE 2.51**

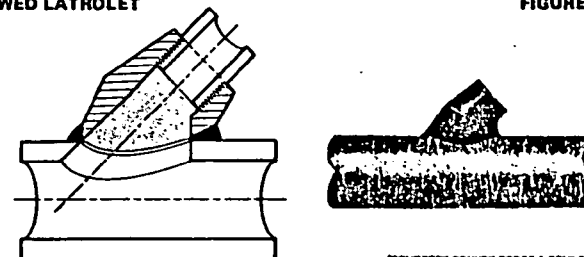


(COURTESY BONNEY FORGE & FOUNDRY INC.)

**SCREWED LATROLET** makes a 45-degree reducing branch on straight pipe.

**SCREWED LATROLET**

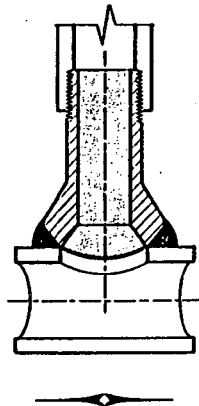
**FIGURE 2.52**



(COURTESY BONNEY FORGE & FOUNDRY INC.)

**SCREWED NIPOLET** A variant of the throolet with integral threaded nipple. Primarily developed for small valved connections—see figure 6.47.

**SCREWED NIPOLET**



**FIGURE 2.53**

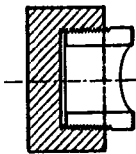
**STUB-IN** See comments in 2.3.2. Not preferred for branching from pipe smaller than 2-inch as weld metal may restrict flow.

**CLOSURES**

2.5.4

**CAP** seals the threaded end of pipe.

**SCREWED CAP**

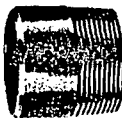
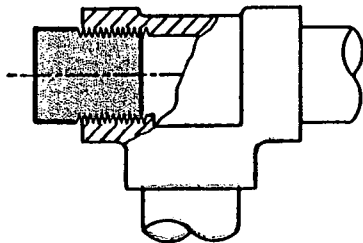


(COURTESY HENRY VOGT MACHINE CO.)

**FIGURE 2.54**

**BARSTOCK PLUG** seals the screwed end of a fitting. Also termed 'round-head plug'.

**BARSTOCK PLUG (IN TEE)**



(COURTESY LADISH COMPANY)

**FIGURE 2.55**

**PIPE THREADS**

2.5.5

It is sometimes necessary to determine the overall length of a run to be made from screwed fittings and pipe. Tables D-9 and D-10 give dimensions of screwed fittings. In calculating run lengths from these tables, allowance should be made for thread engagement (given in the tables).

The standard ANSI B2.1–1968 defines tapered and straight threads for pipe (and fittings, etc.). The ANSI tapered thread is normally used for screwed piping. The tapered threads change diameter at 1/16 inch per inch (of run).

The number of threads per inch is the same for ANSI B2.1–1968 straight or tapered threads for the same nominal pipe size. Tapered and straight threads will mate. Taper/taper and taper/straight (both types) joints are self-sealing with the use of pipe dope, plastic tape, etc. A straight/straight screwed joint requires a gasket and locknut(s) to ensure sealing.

The standard ANSI B2.2–1968 defines 'dryseal' pipe threads which do not require pipe dope or tape for sealing. ANSI B2.4–1966 defines hose coupling screw threads.

**ANSI B2.1–1968 : PIPE THREADS (EXCEPT DRYSEAL)**

Taper pipe thread . . . . .	NPT
Straight pipe thread in pipe couplings . . . . .	NPSC
Straight pipe threads for mechanical joints . . . . .	NPSM
Straight pipe thread for locknuts and locknut pipe thread . . . . .	NPSL
Straight pipe thread for hose couplings and nipples . . . . .	NPSH

**ANSI B2.2–1968 : DRYSEAL PIPE THREADS**

Dryseal taper pipe thread (lubricant optional) . . . . .	NPTF
Dryseal straight pipe thread (lubricant optional) . . . . .	NPSF
Dryseal internal straight pipe thread . . . . .	NPSI

## FLANGE FACINGS &amp; FINISHES

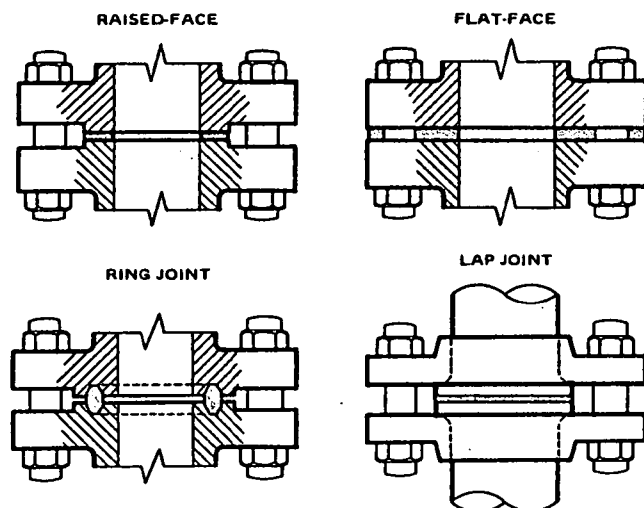
## 2.6.1

Many facings for flanges are offered by flange manufacturers, including various 'tongue and groove' types which must be used in pairs. However, only four types of facing are widely used, and these are shown in figure 2.56.

The raised face is used for about 80% of all flanges. The ring-joint facing, employed with either an oval-section or octagon-section gasket, is used mainly in the petrochemical industry.

THE MOST-USED FLANGE FACINGS

FIGURE 2.56



The **RAISED FACE** is 1/16-inch high for 150 and 300 PSI flanges, and 1/4-inch high for all other pressure classes. 250 PSI cast-iron flanges and flanged fittings also have the 1/16-inch raised face.

*Manufacturers' catalogs give a 'length thru hub' dimension which includes the 1/16th-inch raised face for 150 and 300 PSI ratings, but which excludes the 1/4-inch raised face for flanges rated 400 PSI and higher.*

**FLAT FACE** Most common uses are for mating with non-steel flanges on bodies of pumps, etc. and for mating with 125 PSI cast-iron valves and fittings. Flat-faced flanges are used with a gasket whose outer diameter equals that of the flange—this reduces the danger of cracking a cast-iron, bronze or plastic flange when the assembly is tightened.

**RING-JOINT FACING** is a more expensive facing, and considered the most efficient for high-temperature and high-pressure service. Both flanges of a pair are alike. The ring-joint facing is not prone to damage in handling as the surfaces in contact with the gasket are recessed. Use of facings of this type may increase as hollow metal O-rings gain acceptance for process chemical seals.

**LAP-JOINT FLANGE** is shaped to accommodate the stub end. The combination of flange and stub end presents similar geometry to the raised-face flange and can be used where severe bending stresses will not occur. Advantages of this flange are stated in 2.3.1.



The term 'finish' refers to the type of surface texture produced by machining the flange face which contacts the gasket. Two principal types of finish are now used, which may be referred to as 'serrated' and 'smooth'.

Flange faces are usually finished by machining to produce a spiral round-bottomed groove (which is more common and may be termed 'stock finish') or a vee-shaped spiral or concentric groove, termed 'serrated finish'. The pitch of the groove is 1/32 inch for steel flanges for lines 12-inch NPS and smaller.

'Smooth' finish is usually specially-ordered, and is available in two qualities. The smoother surface is termed 'cold-water finish'. The regular smooth finish (disused term: 'smooth plane') shows no tool marks to the naked eye.

Serrated finish is used with asbestos and other gaskets. The regular smooth finish is used with gaskets made from hard materials and with spiral-wound gaskets. Cold-water finish is normally used without gaskets.

## BOLT HOLES IN FLANGES

## 2.6.2

Bolt holes in flanges are equally spaced. Specifying the number of holes, diameter of the bolt circle and hole size sets the bolting configuration. Number of bolt holes per flange is given in tables F.

Flanges are positioned so that bolts straddle vertical and horizontal centerlines. This is the normal position of bolt holes on all flanged items.

## BOLTS FOR FLANGES

## 2.6.3

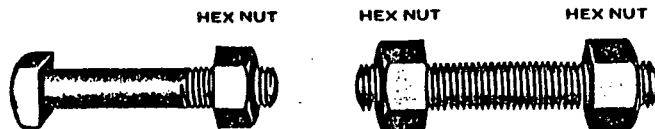
Two types of bolting are available: the studbolt using two nuts, and the machine bolt using one nut. Both boltings are illustrated in figure 2.57. Studbolt thread lengths and diameters are given in tables F.

Studbolts have largely displaced regular bolts for bolting flanged piping joints. Three advantages of using studbolts are:

- (1) The studbolt is more easily removed if corroded
- (2) Confusion with other bolts at the site is avoided
- (3) Studbolts in the less frequently used sizes and materials can be readily made from round stock

SQUARE-HEAD  
MACHINE BOLT

STUDBOLT



**UNIFIED SCREW THREADS** The Unified Standard for bolts and nuts is used in the USA, Canada and the UK. The standard is ANSI B1.1, and a metric translation is available—ANSI B1.1a. There are three Unified Screw Threads:

Unified Coarse (UNC), Unified Fine (UNF), and Unified Selected (UNS).

Only UNC (class 2, medium-fit bolt and nut) is used for bolts and studbolts in piping. The thread is specified as follows:—

OUTSIDE DIAMETER . . . . . INCHES  
THREAD . . . . . UNC  
THREAD DENSITY . . . . . THREADS PER INCH  
CLASS OF FIT . . . . . 2  
BOLT . . . . . A  
NUT . . . . . B

EXAMPLES: Bolt: ½ UNC 13–2A  
Mating Nut: ½ UNC 13–2B

**GASKETS**

2.6.4

Gaskets are used to make a fluid-resistant seal between two surfaces. The common gasket patterns for pipe flanges are the full-face and ring types, for use with flat-faced and raised-face flanges respectively. Refer to figure 2.56. Widely-used materials for gaskets are compressed asbestos (1/16-inch thick) and asbestos-filled metal ('spiral-wound', 0.175-inch thick). The filled-metal gasket is especially useful if maintenance requires repeated uncoupling of flanges, as the gasket separates cleanly and is often reusable.

Choice of gasket is decided by:

- (1) Temperature, pressure and corrosive nature of the conveyed fluid
- (2) Whether maintenance or operation requires repeated uncoupling
- (3) Code requirements that may apply
- (4) Cost

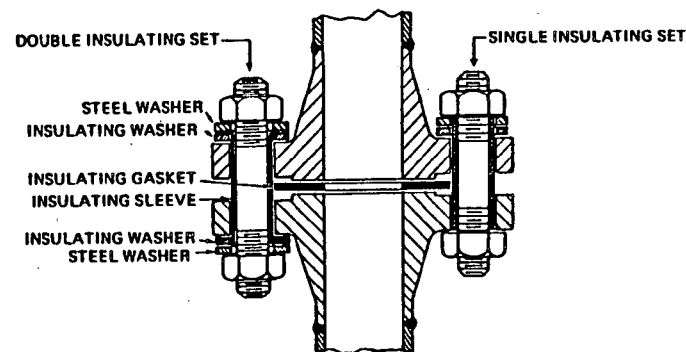
Garlock Incorporated's 'Industrial products catalog' includes tables giving the expected resistance of gasket materials to many process fluids and conditions. Table 2.5 gives some characteristics of gaskets, to aid selection.

It may be required that adjacent parts of a line are electrically insulated from one another, and this may be effected by inserting a flanged joint fitted with an insulating gasket set between the parts. A gasket electrically insulates the flange faces, and sleeves and washers insulate the bolts from one or both flanges, as illustrated in figure 2.58.

GASKET MATERIAL	EXAMPLE USE	MAXIMUM TEMPERATURE (Deg F)	MAXIMUM TP FACTOR Temperature x Pressure (Deg F x PSI)	AVAILABLE THICKNESS (INCHES)
Synthetic rubbers	Water, Air	250	15,000	1/32, 1/16, 3/32, 1/8, 1/4
Vegetable fiber	Oil	250	40,000	1/64, 1/32, 1/16, 3/32, 1/8
Synthetic rubbers with cloth insert ('CI')	Water, Air	250	125,000	1/32, 1/16, 3/32, 1/8, 1/4
Solid Teflon	Chemicals	500	150,000	1/32, 1/16, 3/32, 1/8
Compressed asbestos	Most	750	250,000	1/64, 1/32, 1/16, 1/8
Carbon steel	High-pressure fluids	750	1,600,000	For ring-joint gaskets, refer to table R-1, part II
Stainless steel	High-pressure &/or corrosive fluids	1200	3,000,000	
Spiral-wound: SS/Teflon CS/Asbestos SS/Asbestos SS/Ceramic	Chemicals Most Corrosive Hot gases	500 750 1200 1900	250,000+	Most-used thickness for spiral wound gaskets is 0.175. Alternative gasket thickness: 0.125.

INSULATING GASKET SET

FIGURE 2.58



TEMPORARY CLOSURES FOR LINES

2.7

IN-LINE CLOSURES

2.7.1

A completely leak-proof means of stopping flow in lines is necessary in piping systems when: (1) A change in process material to flow in the line is to be made and cross-contamination is to be avoided. (2) Periodic maintenance is to be carried out, and a hazard would be presented by flammable and/or toxic material passing a valve.

The valves described in 3.1 may not offer complete security against leakage, and one of the following methods of temporary closure can be used: Line-blind valve, line blind (including special types for use with ring-joint flanges), spectacle plate (so-called from its shape), 'double block and bleed', and blind flanges replacing a removable spool. The last three closures are illustrated in figures 2.59 thru 2.61.

SPECTACLE PLATE &amp; LINE BLIND

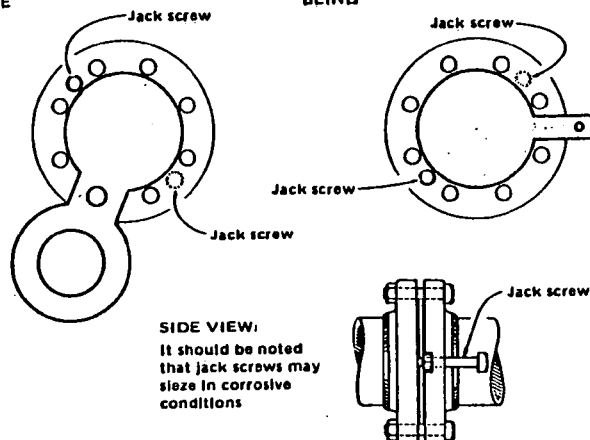
SPECTACLE  
PLATELINE  
BLIND

FIGURE 2.59

DOUBLE-BLOCK-AND-BLEED

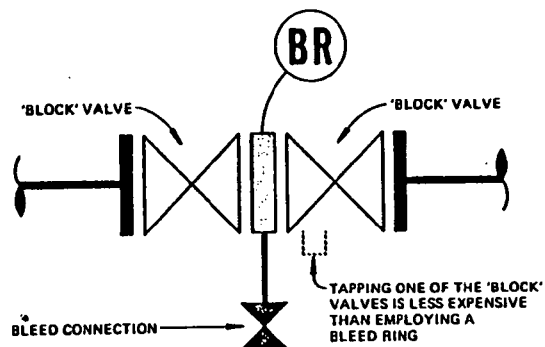


FIGURE 2.60

REMOVABLE SPOOL

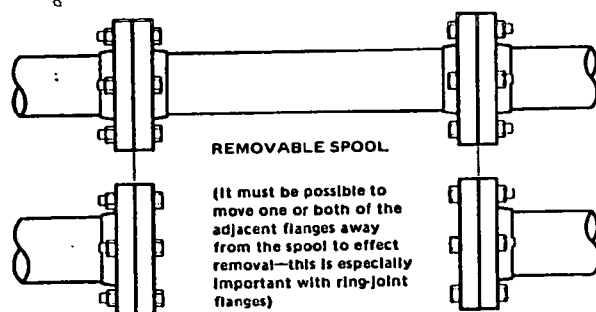


FIGURE 2.61

If a line is to be temporarily closed down with double-block-and-bleed, both valves are closed, and the fluid between drawn off with the bleed valve. The bleed valve is then left open to show whether the other valves are tightly shut.

Figure 2.60 shows the bleed ring connected to a bleed valve—see 3.1.11. The use of a tapped valve rather than a bleed ring should be considered, as it is a more economic arrangement, and usually can be specified merely by adding a suffix to the valve ordering number.

A line-blind valve is not illustrated as construction varies. This type of valve incorporates a spectacle plate sandwiched between two flanges which may be expanded or tightened (by some easy means), allowing the spectacle plate to be reversed. Constant-length line-blind valves are also available, made to ANSI dimensions for run length.

Table 2.6 compares the advantages of the four in-line temporary closures:

IN-LINE CLOSURES

TABLE 2.6

CLOSURE CRITERION	LINE BLIND VALVE	SPECTACLE PLATE, or LINE BLIND	DOUBLE BLOCK, & BLEED	REMOVABLE SPOOL
RELATIVE OVERALL COST	LEAST EXPENSIVE	MEDIUM EXPENSE, DEPENDING ON FREQUENCY OF CHANGEOVER		MOST EXPENSIVE
MANHOURS FOR DOUBLE CHANGEOVER	NEGLECTIBLE	1 to 3	NEGLECTIBLE	7 to 8
INITIAL COST	FAIRLY HIGH	LOW	VERY HIGH	HIGH
CERTAINTY OF SHUT-OFF	COMPLETE	COMPLETE	DOUBTFUL	COMPLETE
VISUAL INDICATION?	YES	YES	YES, BUT SUSPECT	YES
WHO OPERATES?	PLANT OPERATOR	PIPEFITTER	PLANT OPERATOR	PIPEFITTER

## CLOSURES FOR PIPE ENDS &amp; VESSEL OPENINGS

2.7.2

Temporary bolted closures include blind flanges using flat gaskets or ring joints, T-bolt closures, welded-on closures with hinged doors—including the boltless manhole cover (Robert Jenkins, England) and closures primarily intended for vessels, such as the Lanapa range (Bonney Forge) which may also be used with pipe of large diameter. The blind flange is mostly used with a view to future expansion of the piping system, or for cleaning, inspection, etc. Hinged closures are often installed on vessels; infrequently on pipe.

## QUICK CONNECTORS &amp; COUPLINGS

2.8

## QUICK CONNECTORS

2.8.1

Two forms of connector specifically designed for temporary use are:

(1) Lever type with double lever clamping, such as Evertite 'Standard' and Victaulic 'Snap Joint'. (2) Screw type with captive nut—'hose connector'.

Typical use is for connecting temporarily to tank cars, trucks or process vessels. Inter-trades agreements permit plant operators to attach and uncouple these boltless connectors. Certain temporary connectors have built-in valves. Evertite manufactures a double shut-off connector for liquids, and Schrader a valved connector for air lines.

## BOLTED QUICK-COUPPLINGS

2.8.2

Connections of this type may be suitable for either permanent or temporary use, depending on the joint and gasket, and service conditions. Piping can be built rapidly with them, and they are especially useful for making repairs to lines, for constructing short-run process installations such as pilot plants, and for process modification.

## COUPLINGS FOR GROOVED COMPONENTS & PIPE

Couplings of this type are manufactured by the Victaulic Company of America for use with steel, cast-iron, FRP or plastic pipe, either having grooved ends, or with Victaulic collars welded or cemented to the pipe ends.

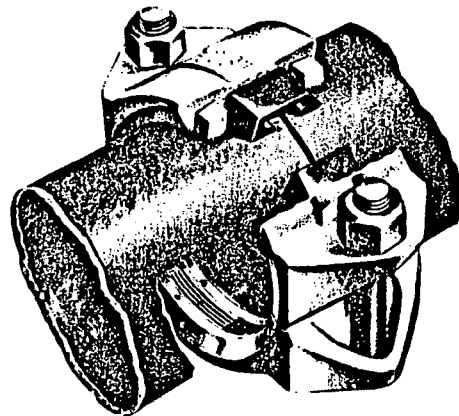
The following special fittings with grooved ends are available: elbow, tee (all types), lateral, cross, reducer, nipple, and cap. Groove-ended valves and valve adaptors are also available. Advantages: (1) Quick fitting and removal. (2) Joint can take up some deflection and expansion. (3) Suitable for many uses, with correct gaskets.

The manufacturer states that the biggest uses are for permanent plant air, water (drinking, service, process, waste) and lubricant lines.

**COMPRESSION SLEEVE COUPLINGS** are extensively used for air, water, oil and gas. Well-known manufacturers include Victaulic, Dresser and Smith-Blair. Advantages: (1) Quick fitting and removal. (2) Joint may take up some deflection and expansion. (3) End preparation of pipe is not needed.

## VICTAULIC COMPRESSION SLEEVE COUPLING

FIGURE 2.62



## EXPANSION JOINTS & FLEXIBLE PIPING

2.9

### EXPANSION JOINTS

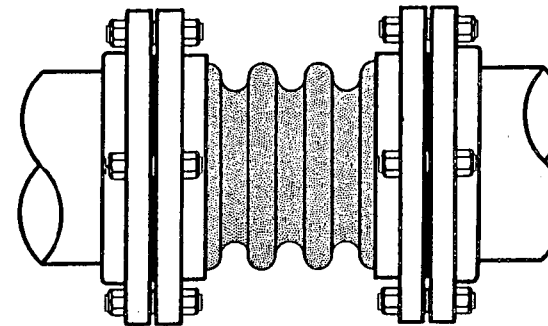
2.9.1

Figures 2.63 thru 2.66 show methods of accommodating movement in piping due to temperature changes, if such movement cannot be taken up by:

- (1) Re-routing or re-spacing the line.
  - (2) Expansion loops—see figure 6.1.
  - (3) Calculated placement of anchors.
  - (4) Cold springing—see 6.1.
- Bellows-type expansion joints of the type shown in figure 2.63 are also used to absorb vibration.

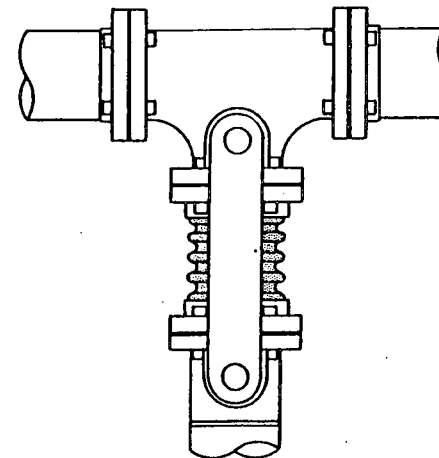
## SIMPLE BELLOWS

FIGURE 2.63



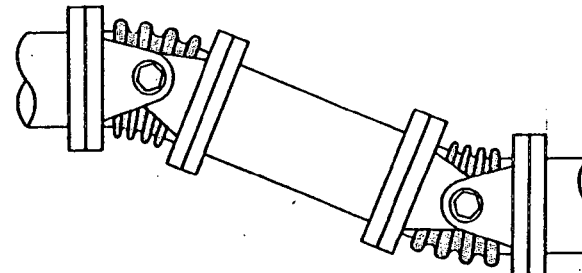
## ARTICULATED BELLOWS

FIGURE 2.64



## ARTICULATED TWIN-BELLOWS ASSEMBLY

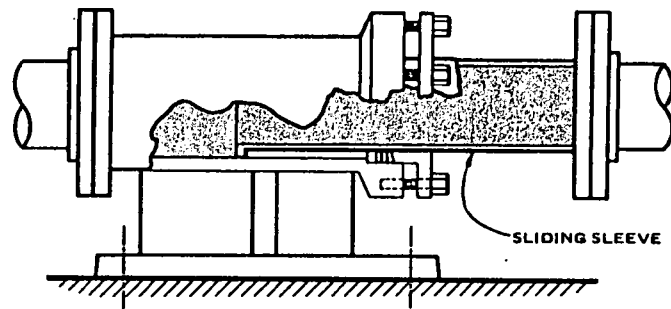
FIGURE 2.65



2 || .7.1  
|| .9.1

FIGURES  
2.59-2.65

TABLE  
2.6



## FLEXIBLE PIPING

2.9.2

For filling and emptying railcars, tankers, etc., thru rigid pipe, it is necessary to design articulated piping, using 'swiveling' joints, or 'ball' joints (the latter is a 'universal' joint). Flexible hose has many uses especially where there is a need for temporary connections, or where vibration or movement occurs. Chemical-resistant and/or armored hoses are available in regular or jacketed forms (see figure 6.39).

## SEPARATORS, STRAINERS, SCREENS &amp; DRIPLEGS 2.10

## COLLECTING UNWANTED MATERIAL FROM THE FLOW 2.10.1

Devices are included in process and service lines to separate and collect undesirable solid or liquid material. Pipe scale, loose weld metal, unreacted or decomposed process material, precipitates, lubricants, oils, or water may harm either equipment or the process.

Common forms of line-installed separator are illustrated in figures 2.67 and 2.68. Other more elaborate separators mentioned in 3.3.3 are available, but these fall more into the category of process equipment, normally selected by the process engineer.

Air and some other gases in liquid-bearing lines are normally self-collecting at piping high points and at the remote ends of headers, and are vented by discharge valves — see 3.1.9.

## SEPARATORS 2.10.2

These permanent devices are used to collect droplets from a gaseous stream, for example, to collect oil droplets from compressed air, or condensate droplets from wet steam. Figure 2.67 shows a separator in which droplets in the stream collect in chevroned grooves in the barrier and drain to the small well. Collected liquid is discharged via a trap—see 3.1.9 and 6.10.7.

## STRAINERS

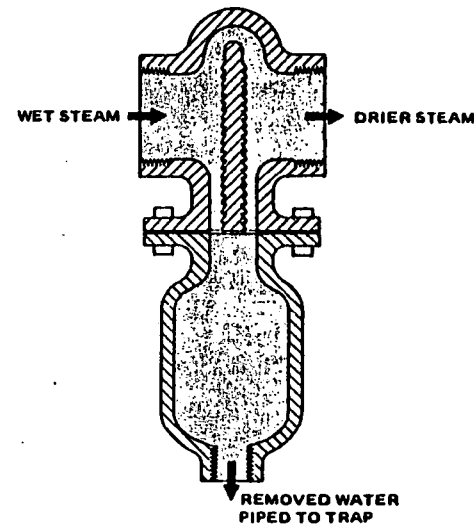
2.10.3

Inserted in lines immediately upstream of sensitive equipment, strainers collect solid particles in the approximate size range 0.02–0.5 inch, which can be separated by passing the fluid bearing them thru the strainer's screen. Typical locations for strainers are before a control valve, pump, turbine, or traps on steam systems. 20-mesh strainers are used for steam, water, and heavy or medium oils. 40-mesh is suitable for steam, air, other gases, and light oils.

The commonest strainer is the illustrated wye type where the screen is cylindric and retains the particles within. This type of strainer is easily dismantled. Some strainers can be fitted with a valve to facilitate blowing out collected material without shutting the line down—see figure 6.9, for example. Jacketed strainers are available.

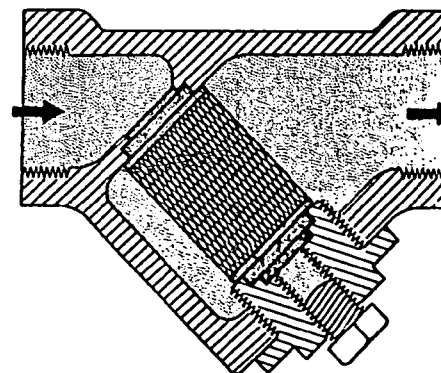
## SEPARATOR

FIGURE 2.67



## STRAINER

FIGURE 2.68



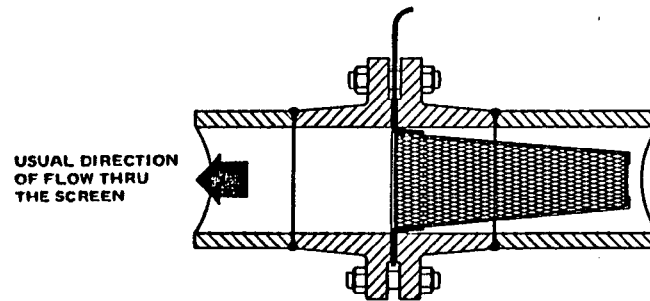


Simple temporary strainers made from perforated sheet metal and/or wire mesh are used for startup operations on the suction side of pumps and compressors, especially where there is a long run of piping before the unit that may contain weld spatter or material inadvertently left in the pipe. After startup, the screen usually is removed.

It may be necessary to arrange for a small removable spool to accommodate the screen. It is important that the flow in suction lines should not be restricted. Cone-shaped screens are therefor preferred, with cylindric types as second choice. Flat screens are better reserved for low-suction heads.

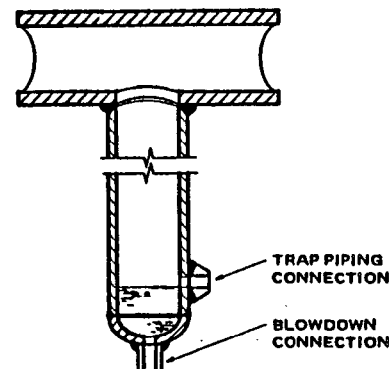
SCREEN BETWEEN FLANGES

FIGURE 2.69



DRIPLEG CONSTRUCTION

FIGURE 2.70



DRIPLEGS

2.10.5

Often made from pipe and fittings, the dripleg is an inexpensive means of collecting condensate. Figure 2.70 shows a dripleg fitted to a horizontal pipe. Removal of condensate from steam lines is discussed in 6.10. Recommended sizes for driplegs are given in table 6.10.

## BRANCH CONNECTIONS

'Reinforcement' is the addition of extra metal at a branch connection made from a pipe or vessel wall. The added metal compensates for the structural weakening due to the hole.

Stub-ins may be reinforced with regular or wraparound saddles, as shown in figure 2.71. Rings made from platestock are used to reinforce branches made with welded laterals and butt-welded connections to vessels. Small welded connections may be reinforced by adding extra weld metal to the joint.

Reinforcing pieces are usually provided with a small hole to vent gases produced by welding; these gases would otherwise be trapped. A vent hole also serves to indicate any leakage from the joint.

## STRAIGHT PIPE

If a butt weld joining two sections of straight pipe is subject to unusual external stress, it may be reinforced by the addition of a 'sleeve' (formed from two units, each resembling the lower member in figure 2.71 (b)).

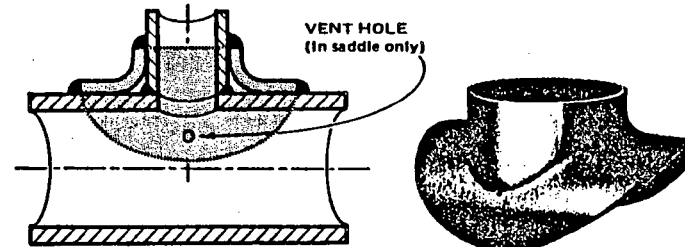
The code applicable to the piping should be consulted for reinforcement requirements. Backing rings are not considered to be reinforcements—see the footnote to chart 2.1.

## REINFORCING SADDLES

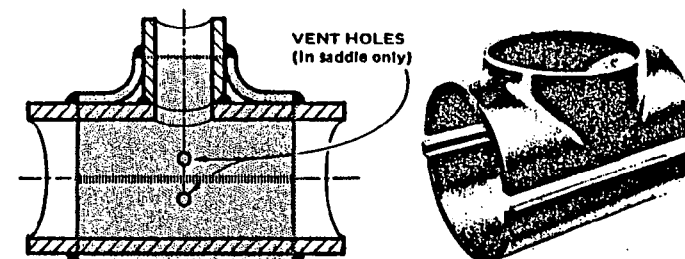
FIGURE 2.71

## (a) REGULAR SADDLE

(COURTESY MIDWEST FITTING DIVISION, CRANE CO.)

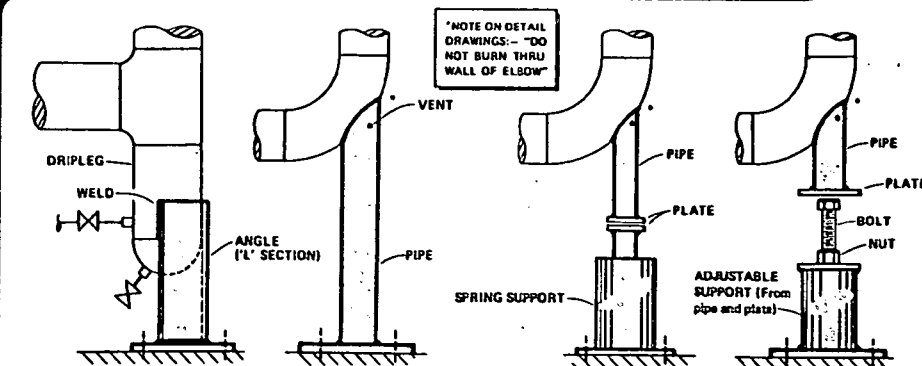
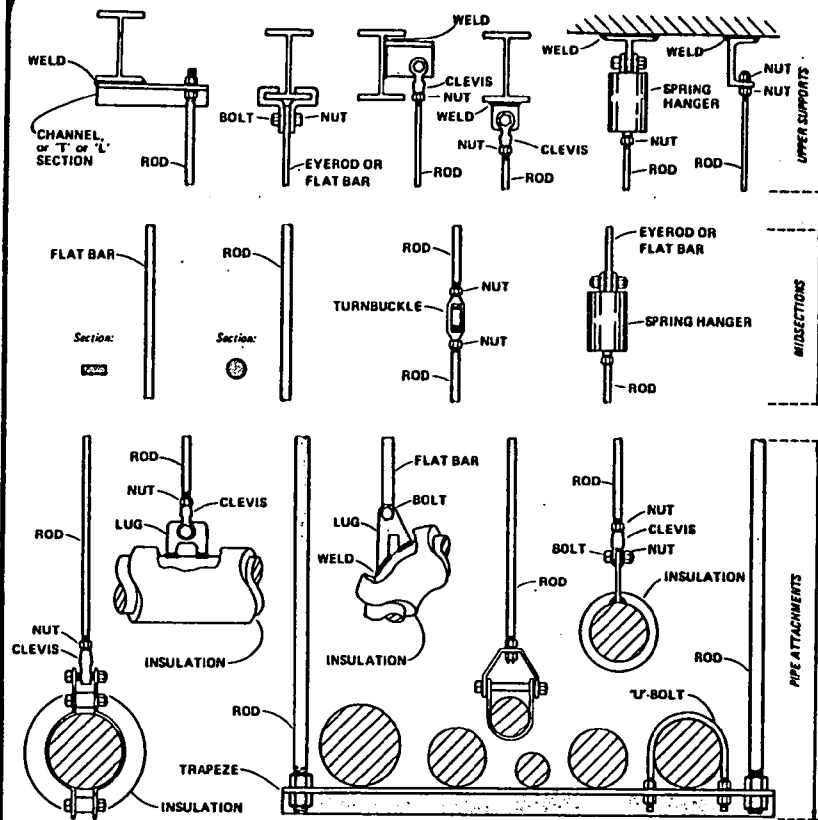


## (b) WRAPAROUND SADDLE

FIGURES  
2.66-2.71

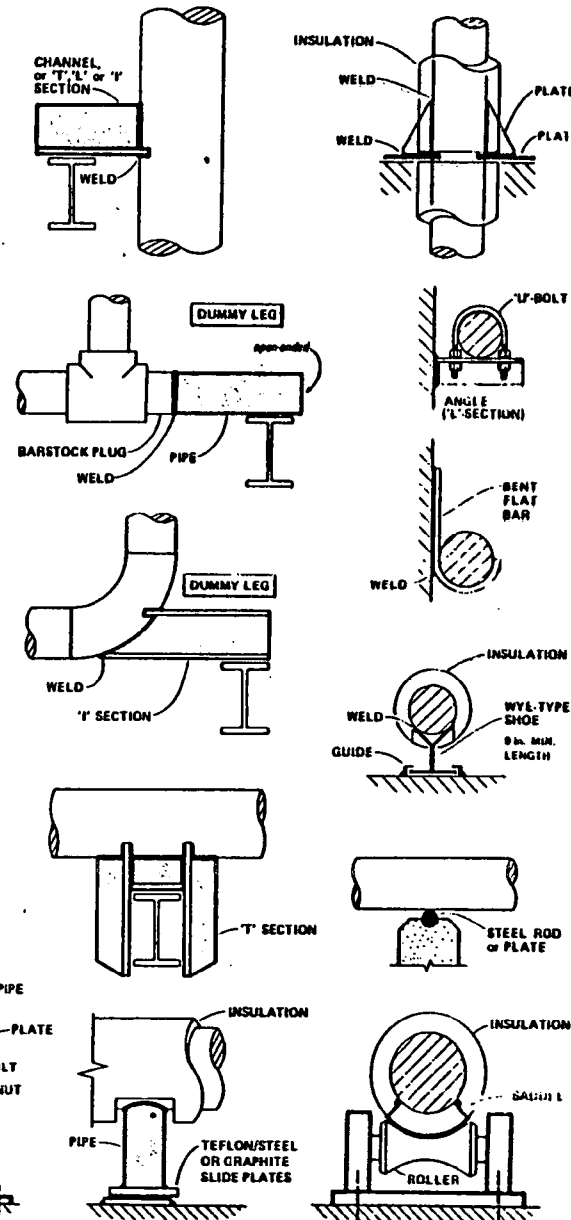
# PIPE SUPPORTS

## HANGERS



# FIGURE 2.72A

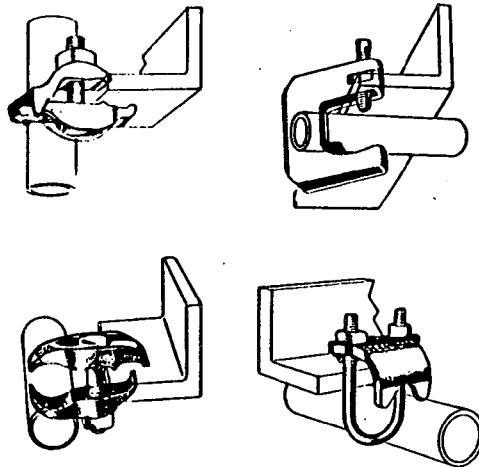
## SUPPORTS



# PIPE SUPPORTS

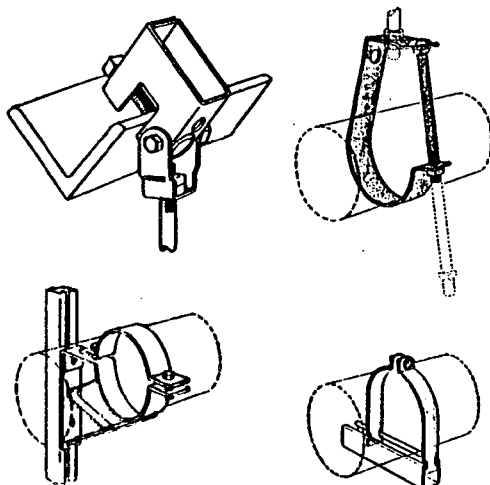
## SUPPORTING PIPE CLOSE TO STRUCTURAL STEEL

(COURTESY STEEL CITY DIVISION, MIDLAND-ROSS CORP)



"KINDORF SYSTEM"

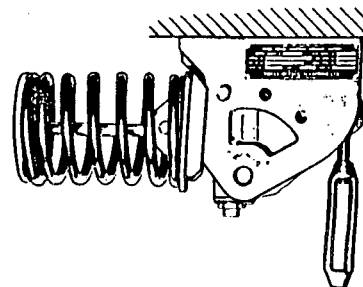
(COURTESY UNISTRUT CORPORATION)



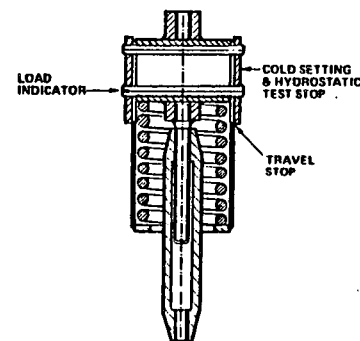
## SPRING HANGERS

(COURTESY VOKES-BERGEN-GENSPRING LTD)

### 1. CONSTANT LOAD TYPE

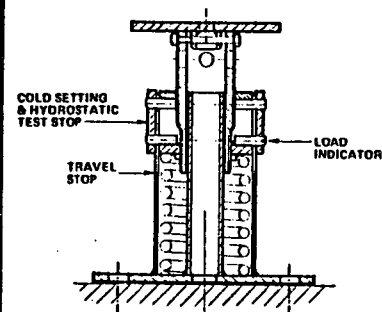


### 2. VARIABLE LOAD TYPE



## SPRING SUPPORT

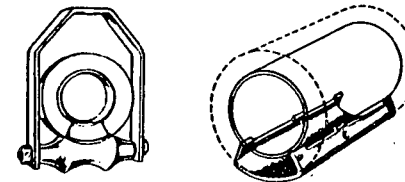
(COURTESY VOKES-BERGEN-GENSPRING LTD)



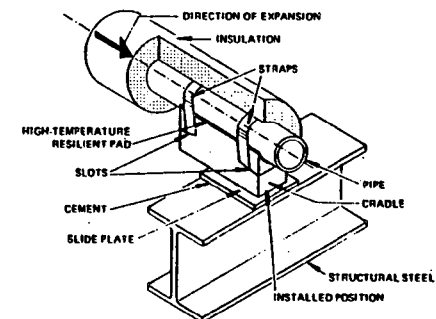
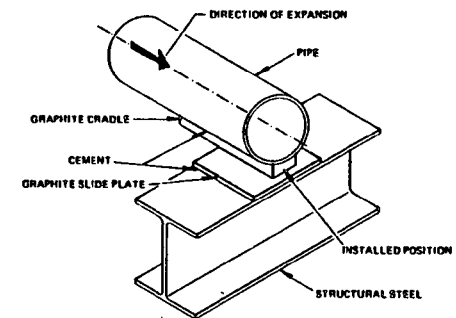
# FIGURE 2.72B

## SUPPORTS ALLOWING FREE MOVEMENT OF PIPE

(COURTESY STEEL CITY DIVISION, MIDLAND-ROSS CORP)



(COURTESY UNION CARRIDE)



FIGURES  
2.72A&B

## HARDWARE FOR SUPPORTING PIPING

2.12

Symbols for drafting various types of support are shown in chart 5.7. For designing support systems, see 6.2.

### PIPE SUPPORTS

2.12.1

Pipe supports should be as simple as conditions allow. Stock items are used where practicable, especially for piping held from above. To support piping from below, supports are usually made to suit from platestock, pipe, and pieces of structural steel.

A selection of available hardware for supporting is illustrated in figures 2.72A and B.

### TERMS FOR SUPPORTS

2.12.2

**SUPPORT** The weight of piping is usually carried on supports made from structural steel, or steel and concrete. (The term 'support' is also used in reference to hangers.)

**HANGER** Device which suspends piping (usually a single line) from structural steel, concrete or wood. Hangers are usually adjustable for height.

**ANCHOR** A rigid support which prevents transmission of movement (thermal, vibratory, etc.) along piping. Construction may be from steel plate, brackets, flanges, rods, etc. Attachment of an anchor to pipe should preferably encircle the pipe and be welded all around as this gives a better distribution of stress in the pipe wall.

**TIE** An arrangement of one or more rods, bars, etc., to restrain movement of piping.

**DUMMY LEG** An extension piece (of pipe or rolled steel section) welded to an elbow in order to support the line—see figure 2.72A and table 6.3.

The following hardware is used where mechanical and/or thermal movement is a problem:

**GUIDE** A means of allowing a pipe to move along its length, but not sideways.

**SHOE** A metal piece attached to the underside of a pipe which rests on supporting steel. Primarily used to reduce wear from sliding for lines subject to movement. Permits insulation to be applied to pipe.

**SADDLE** A welded attachment for pipe requiring insulation, and subject to longitudinal or rolling movement (resulting from temperature changes other than climatic). Saddles may be used with guides as shown in 6.2.8.

**SLIDE PLATE** A slide plate support is illustrated in figure 2.72A. Figure 2.72B shows applications of 'Ucar' graphite slide plates which are offered by Union Carbide Inc. The two plates used in a support are made from or faced with a material of low friction able to withstand mechanical stress and temperature changes. Plates are often made from graphite blocks. Steel plates with a teflon facing are available and may be welded to steel.

Spring hangers or supports allow variations in the length of pipe due to changes in temperature, and are often used for vertical lines. Refer to 6.2.5 figure 6.16. There are two types of spring hanger or support:

**'CONSTANT LOAD' HANGER** This device consists of a coil spring and lever mechanism in a housing. Movement of the piping, within limits, will not change the spring force holding up the piping; thus, no additional forces will be introduced to the piping system.

**'VARIABLE SPRING' HANGER, and SUPPORT** These devices consist of a coil spring in a housing. The weight of the piping rests on the spring in compression. The spring permits a limited amount of thermal movement. A variable spring hanger holding up a vertical line will reduce its lifting force as the line expands toward it. A variable spring support would increase its lifting force as the line expands toward it. Both place a load on the piping system. Where this is undesirable, a constant-load hanger can be used instead.



### HYDRAULIC DAMPENER, SHOCK, SNUBBER, or SWAY SUPPRESSOR

One end of the unit is attached to piping and the other to structural steel or concrete. The unit expands or contracts to absorb slow movement of piping, but is rigid to rapid movement.

**SWAY BRACE, or SWAY ARRESTOR**, is essentially a helical spring in a housing which is fitted between piping and a rigid structure. Its function is to buffer vibration and sway.

### WELDING TO PIPE

2.12.3

If the applicable code permits, lugs may be welded to pipe. Figure 2.72A illustrates some common arrangements using welded lugs, rolled steel sections and pipe, for:—

- (1) Fixing hangers to structural steel, etc.
- (2) Attaching to pipe
- (3) Supporting pipe

Welding supports to prelined pipe will usually spoil the lining, and therefore lugs, etc., must be welded to pipe and fittings before the lining is applied. Welding of supports and lugs to pipes and vessels to be stress-relieved should be done before heat treatment.

# VALVES,

## PUMPS, COMPRESSORS,

## & PROCESS EQUIPMENT

### VALVES 3.1

#### FUNCTIONS OF VALVES 3.1.1

Table 3.1 gives a basis for classifying valves according to function:

USES OF VALVES TABLE 3.1

VALVE ACTION	EXPLANATION	SEE SECTION:
ON/OFF	STOPPING OR STARTING FLOW	3.1.4 and 3.1.6
REGULATING	VARYING THE RATE OF FLOW	3.1.5, 3.1.6 and 3.1.10
CHECKING	PERMITTING FLOW IN ONE DIRECTION ONLY	3.1.7
SWITCHING	SWITCHING FLOW ALONG DIFFERENT ROUTES	3.1.8
DISCHARGING	DISCHARGING FLUID FROM A SYSTEM	3.1.9

Types of valve suitable for on/off and regulating functions are listed in chart 3.2. The suitability of a valve for a required purpose depends on its construction, discussed in 3.1.3.

#### PARTS OF VALVES 3.1.2

Valve manufacturers' catalogs offer a seemingly endless variety of constructions. Classification is possible, however, by considering the basic parts that make up a valve:

- (1) The 'disc' and 'seat' that directly affect the flow
- (2) The 'stem' that moves the disc — in some valves, fluid under pressure does the work of a stem
- (3) The 'body' and 'bonnet' that house the stem
- (4) The 'operator' that moves the stem (or pressurizes fluid for squeeze valves, etc.)

Figures 3.1 thru 3.3 show three common types of valve with their parts labeled.

#### DISC, SEAT, & PORT

Chart 3.1 illustrates various types of disc and port arrangements, and mechanisms used for stopping or regulating flow. The moving part directly affecting the flow is termed the 'disc' regardless of its shape, and the non-moving part it bears on is termed the 'seat'. The 'port' is the maximum internal opening for flow (that is, when the valve is fully open). Discs may be actuated by the conveyed fluid or be moved by a stem having a linear, rotary or helical movement. The stem can be moved manually or be driven hydraulically, pneumatically or electrically, under remote or automatic control, or mechanically by weighted lever, spring, etc.

The size of a valve is determined by the size of its ends which connect to the pipe, etc. The port size may be smaller.

#### STEM

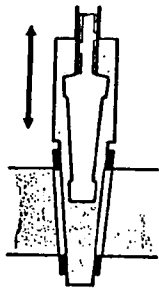
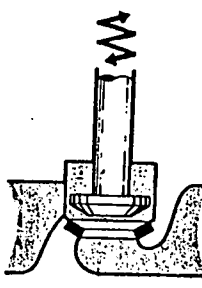
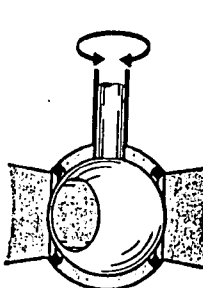
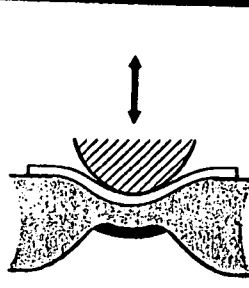
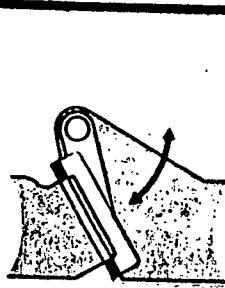
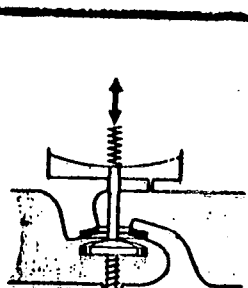
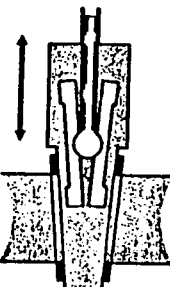
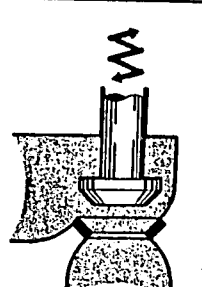
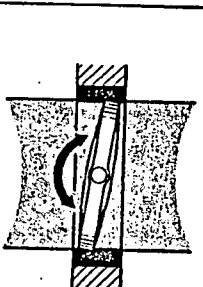
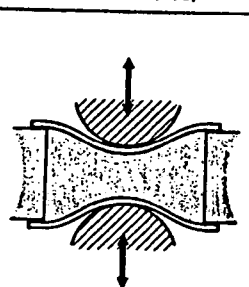
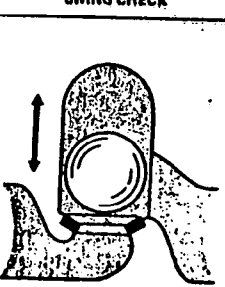
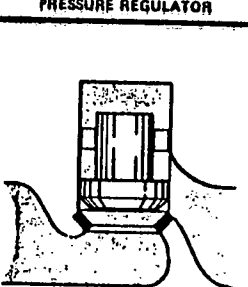
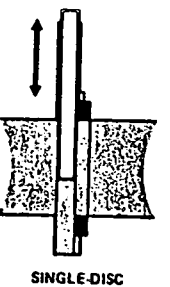
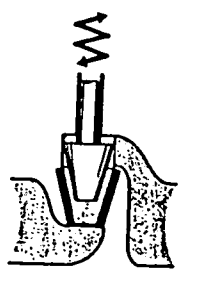
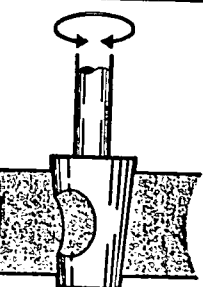
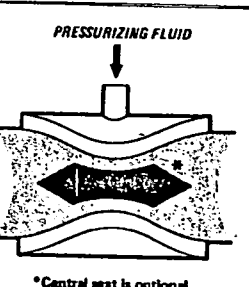
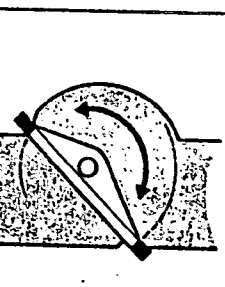
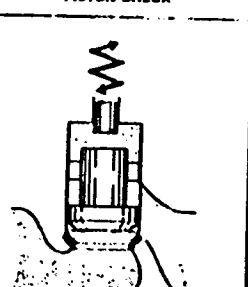
There are two categories of screwed stem: The rising stem shown in figures 3.1 and 3.2, and the non-rising stem shown in figure 3.3.

Rising stem (gate and globe) valves are made either with 'inside screw' (IS) or 'outside screw' (OS). The OS type has a yoke on the bonnet and the assembly is referred to as 'outside screw and yoke', abbreviated to 'OS&Y'. The handwheel can either rise with the stem, or the stem can rise thru the handwheel.

# BASIC VALVE MECHANISMS FLUID CONTROL ELEMENTS (DISCS)

CHART 3.1

IN THESE SCHEMATIC DIAGRAMS, THE DISC IS SHOWN WHITE, THE SEAT IN SOLID COLOR, & THE CONVEYED FLUID SHADED.

OPERATED VALVES				SELF-OPERATED VALVES	
GATE	GLOBE	ROTARY	DIAPHRAGM	CHECK	REGULATING
 <p>SOLID-WEDGE GATE</p>	 <p>GLOBE</p>	 <p>ROTARY-BALL</p>	 <p>DIAPHRAGM (SAUNDERS TYPE)</p>	 <p>SWING CHECK</p>	 <p>PRESSURE REGULATOR</p>
 <p>SPLIT-WEDGE GATE</p>	 <p>ANGLE GLOBE</p>	 <p>BUTTERFLY</p>	 <p>PINCH</p>	 <p>BALL CHECK</p>	 <p>PISTON CHECK</p>
 <p>SINGLE-DISC SINGLE-SEAT GATE</p>	 <p>NEEDLE</p>	 <p>PLUG or COCK</p>	 <p>PRESSURIZING FLUID</p> <p>*Central seat is optional</p> <p>SQUEEZE</p>	 <p>TILTING DISC CHECK</p>	 <p>STOP CHECK</p>

"Piping Guide", PO Box 277, Cotati, CA 94928, USA

Non-rising stem valves are of the gate type. The handwheel and stem are in the same position whether the valve is open or closed. The screw is inside the bonnet and in contact with the conveyed fluid.

A 'floor stand' is a stem extension for use with both types of stem, where it is necessary to operate a valve thru a floor or platform. Alternately, rods fitted with universal joints may be used to bring a valve handwheel within an operator's reach.

Depending on the size of the required valve and availabilities, selection of stem type can be based on:

- (1) Whether it is undesirable for the conveyed fluid to be in contact with the threaded bearing surfaces
- (2) Whether an exposed screw is liable to be damaged by abrasive atmospheric dust
- (3) Whether it is necessary to see if the valve is open or closed

In addition to the preceding types of stem used with gate and globe valves, most other valves have a simple rotary stem. Rotary-ball, plug and butterfly valves have a rotary stem which is moved by a permanent lever, or tool applied to a square boss at the end of the stem.

## BONNET

There are three basic types of attachment for valve bonnets: screwed (including union), bolted, and breechlock.

A screwed bonnet may occasionally stick and turn when a valve is opened. Although sticking is less of a problem with the union type bonnet, valves with screwed bonnets are best reserved for services presenting no hazard to personnel. Union bonnets are more suitable for small valves requiring frequent dismantling than the simple screwed type.

The bolted bonnet has largely displaced screwed and union bonnet valves in hydrocarbon applications. A U-bolt or clamp-type bonnet is offered on some small gate valves for moderate pressures, to facilitate frequent cleaning and inspection.

The 'pressure seal' is a variation of the bolted bonnet used for high-pressure valves, usually combined with OS&Y construction. It makes use of line pressure to tighten and seal an internal metal ring or gasket against the body.

The breechlock is a heavier infrequently-used and more expensive construction, also for high-pressure use, and involves seal-welding of the bonnet with the body.

FIGURE 3.1

(COURTESY JENKINS BROS.—VALVE MANUFACTURERS)

GATE VALVE (OS&Y, bolted bonnet, rising stem)

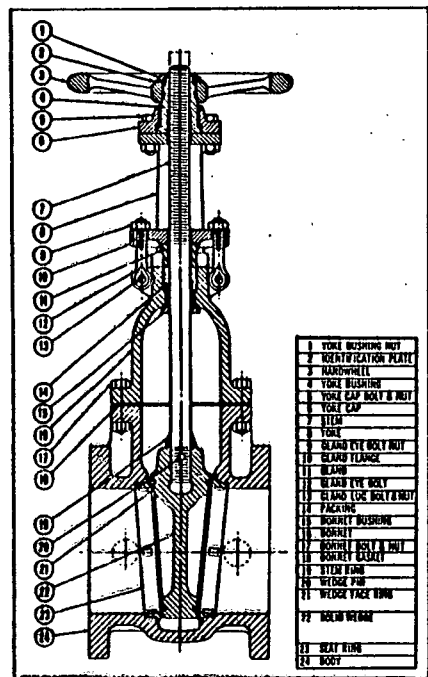


FIGURE 3.2

GLOBE VALVE (OS&Y, bolted bonnet, rising stem)

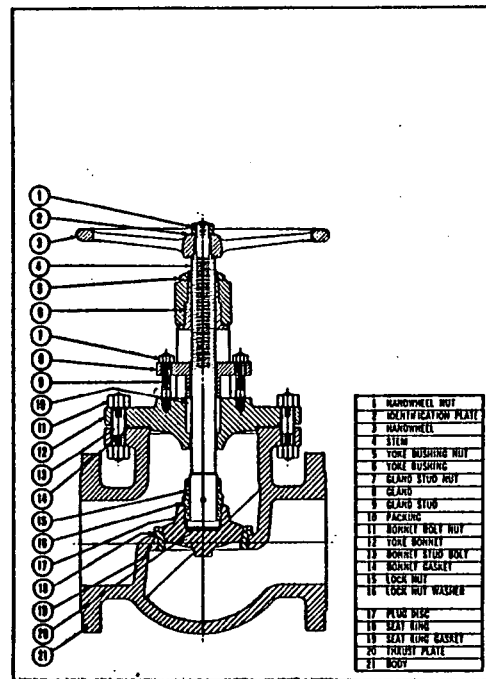


FIGURE 3.3

GATE VALVE (IS, bolted bonnet, non-rising stem)

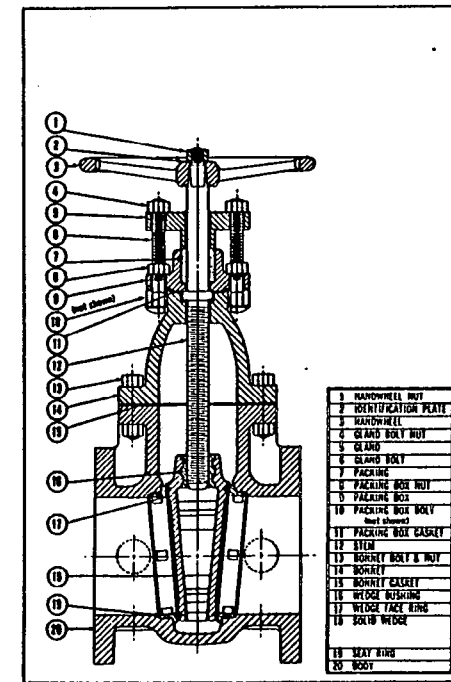


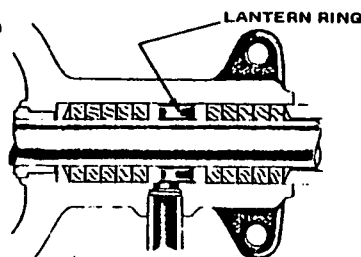
CHART  
3.1

FIGURES  
3.1-3.3

A critical factor for valves used for process chemicals is the lubrication of the stem. Care has to be taken in the selection of packing, gland design, and choice and application of lubricant. As an option the bonnet may include a 'lantern ring' which serves two purposes — either to act as a collection point to drain off any hazardous seepages, or as a point where lubricant can be injected.

#### LANTERN RING

(COURTESY WM. POWELL CO.)



#### BODY

Selection of material to fabricate the interior of the valve body is important with a valve used for process chemicals. There is often a choice with regard to the body and trim, and some valves may be obtained with the entire interior of the body lined with corrosion-resistant material.

Valves are connected to pipe, fittings or vessels by their body ends, which may be flanged, screwed, butt- or socket-welding, or finished for hose, Victaulic coupling, etc. Jacketed valves are also available—see 6.8.2.

#### SEAL

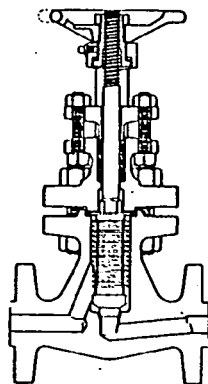
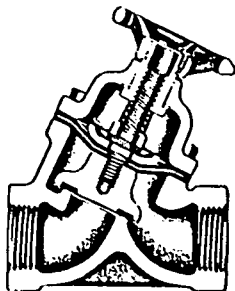
In most stem-operated valves, whether the stem has rotary or lineal movement, packing or seals are used between stem and bonnet (or body). If high vacuum or corrosive, flammable or toxic fluid is to be handled, the disc or stem may be sealed by a metal bellows, or by a flexible diaphragm (the latter is termed 'packless' construction). A gasket is used as a seal between a bolted bonnet and valve body.

#### BELLOWS-SEAL VALVE

(COURTESY HENRY VOGT MACHINE CO.)

#### 'PACKLESS' VALVE

(COURTESY CRANE COMPANY)



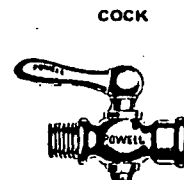
Flanged valves use gaskets to seal against the line flanges. Butterfly valves may extend the resilient seat to also serve as line gaskets. The pressure-seal joint utilizes the pressure of the conveyed fluids to tighten the seal — see 'Pressure seal' under 'Bonnet', this section.

#### MANUAL OPERATORS

**HANDLEVER** is used to actuate the stems of small butterfly and rotary-ball valves, and small cocks. Wrench operation is used for cocks and small plug valves.

#### HANDLEVERS ON SMALL VALVES

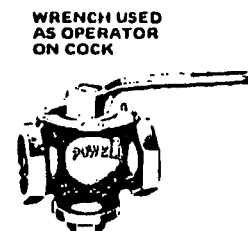
(COURTESY WM. POWELL CO.)



COCK



WRENCH

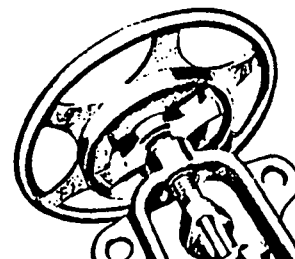


WRENCH USED AS OPERATOR ON COCK

**HANDWHEEL** is the most common means for rotating the stem on the majority of popular smaller valves such as the gate, globe and diaphragm types. Additional operating torque for gate and globe valves is offered by 'hammerblow' or 'impact' handwheels which may be substituted for normal handwheels if easier operation is needed but where gearing is unnecessary.

#### HAMMER-BLOW HANDWHEEL

(COURTESY WM. POWELL CO.)



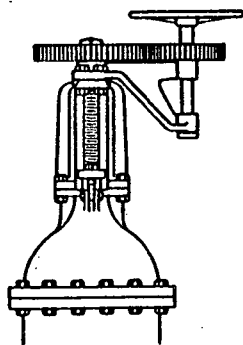
HAMMER ACTION IS PROVIDED BY TWO LUGS CAST ON UNDER-SIDE OF HANDWHEEL, WHICH HIT ANVIL PROJECTING BETWEEN

**CHAIN** operator is used where a handwheel would be out of reach. The stem is fitted with a chainwheel or wrench (for lever-operated valves) and the loop of the chain is brought within 3 ft of working floor level. Universal-type chainwheels which attach to the regular handwheel have been blamed for accidents: in corrosive atmospheres where an infrequently-operated valve has stuck, the attaching bolts have been known to fail. This problem does not arise with the chainwheel that replaces the regular valve handwheel.

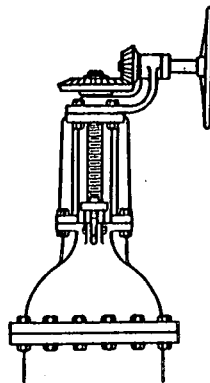
**GEAR** operator is used to reduce the operating torque. For manual operation, consists of a handwheel-operated gear train actuating the valve stem. As a guide, gear operators should be considered for valves of the following sizes and ratings: 125, 150, and 300 PSI, 14-inch and larger; 400 and 600 PSI, 8-inch and larger; 900 and 1500 PSI, 6-inch and larger; 2500 PSI, 4-inch and larger.



#### SPUR-GEAR OPERATOR



#### BEVEL-GEAR OPERATOR



#### POWERED OPERATORS

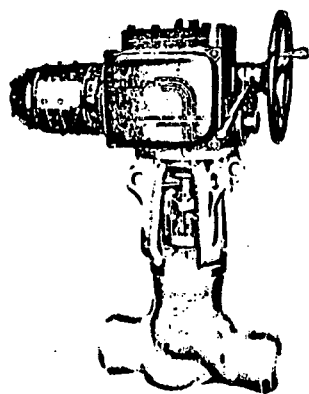
Electric, pneumatic or hydraulic operation is used: (1) Where a valve is remote from the main working area. (2) If the required frequency of operation would need unreasonable human effort. (3) If rapid opening and/or closing of a valve is required.

**ELECTRIC MOTOR** The valve stem is moved by the electric motor, thru reducing gears.

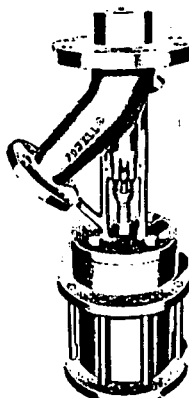
**SOLENOID** may be used with fast-acting check valves, and with on/off valves in light-duty instrumentation applications.

#### ELECTRIC MOTOR OPERATOR

(COURTESY POWELL VALVE COMPANY)



#### PNEUMATIC OPERATOR



**PNEUMATIC & HYDRAULIC OPERATORS** may be used where flammable vapor is likely to be present. They take the following forms: (1) Cylinder with double-acting piston driven by air, water, oil, or other liquid which usually actuates the stem directly. (2) Air motor which actuates the stem thru

gearing—these motors are commonly piston-and-cylinder radial types. (3) A double-acting vane with limited rotary movement in a sector casing, actuating the stem directly. (4) Squeeze type (refer to 'Squeeze valve').

#### QUICK-ACTING OPERATORS FOR NON-ROTARY VALVES (Manually-operated valves)

Quick-acting operators are used with gate and globe valves. Two stem movements are employed:—

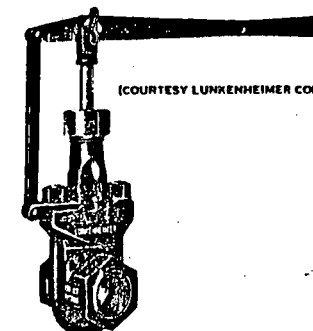
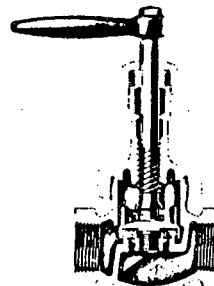
- (1) Rotating stem, rotated by a lever
- (2) Sliding stem, in which the stem is raised and lowered by lever

#### QUICK-ACTING LEVERS ON VALVES

- (1) Rotating stem on globe valve

- (2) Sliding stem on gate valve

(COURTESY JENKINS BROS. VALVE MANUFACTURERS)



(COURTESY LUNKENHEIMER COMPANY)

Steam and air whistles are examples of the use of sliding-stem quick-acting operators with globe valves.

#### SELECTING ON/OFF & REGULATING VALVES

3.1.3

The suitability of a valve for a particular service is decided by its materials of construction in relation to the conveyed fluid as well as its mechanical design. Referring to the descriptions in 3.1.2, the steps in selection are to choose: (1) Material(s) of construction. (2) The disc type. (3) Stem type. (4) Means of operating the stem — the 'operator'. (5) Bonnet type. (6) Body ends — welding, flanged, etc. (7) Delivery time. (8) Price. (9) Warranty of performance for severe conditions.

Chart 3.2 is a guide to valve selection, and indicates valves which may be chosen for a given service. The chart should be read from left to right. First, ascertain whether a liquid, gas or powder is to be handled by the valve. Next, consider the nature of the fluid—whether it is foodstuffs or drugs to be handled hygienically, chemicals that are corrosive, or whether the fluid is substantially neutral or non-corrosive.

Next consider the function of the valve — simple open-or-closed operation ('on/off'), or regulating for control or for dosing. These factors decided, the chart will then indicate types of valves which should perform satisfactorily in the required service.

If the publication is available, reference should also be made to the Crane Company's 1966 printing of 'Choosing the right valve'.

# VALVE SELECTION GUIDE

## CHART 3.2

CONVEYED FLUID	NATURE OF FLUID See Note (2) in Key	VALVE FUNCTION	TYPE OF DISC	SPECIAL FEATURES (—) denotes Limitation, (—) denotes Option
LIQUID	NEUTRAL (WATER, OIL, Etc.)	ON/OFF	GATE ROTARY BALL PLUG DIAPHRAGM BUTTERFLY PLUG GATE	NONE NONE NONE [For oil: No natural rubber] NONE NONE
		REGULATING	GLOBE BUTTERFLY PLUG GATE DIAPHRAGM NEEDLE	NONE NONE NONE [For oil: No natural rubber] NONE, (Small flows only)
	CORROSIVE (ALKALINE, ACID, Etc.)	ON/OFF	GATE GLOBE ROTARY BALL PLUG DIAPHRAGM BUTTERFLY	ANTI-CORROSIVE*, (OS&Y), (Bellows seal) ANTI-CORROSIVE*, (OS&Y) ANTI-CORROSIVE*, (Lined) ANTI-CORROSIVE*, (Lined) ANTI-CORROSIVE*, (Lined) ANTI-CORROSIVE*, (Lined)
		REGULATING	GLOBE DIAPHRAGM BUTTERFLY PLUG GATE	ANTI-CORR*, (OS&Y), (Diaphragm or Bellows Seal) ANTI-CORROSIVE*, (Lined) ANTI-CORROSIVE*, (Lined) ANTI-CORROSIVE*, (OS&Y)
	HYGIENIC (BEVERAGES, FOOD and DRUGS)	ON/OFF	BUTTERFLY DIAPHRAGM	SPECIAL DISC, WHITE SEAT † SANITARY LINING, WHITE DIAPHRAGM †
		REGULATING	BUTTERFLY DIAPHRAGM SQUEEZE PINCH	SPECIAL DISC, WHITE SEAT † SANITARY LINING, WHITE DIAPHRAGM † WHITE FLEXIBLE TUBE † WHITE FLEXIBLE TUBE †
	SLURRY	ON/OFF	ROTARY BALL BUTTERFLY DIAPHRAGM PLUG PINCH SQUEEZE	ABRASION-RESISTANT LINING ABRASION-RESIST. DISC, RESILIENT SEAT ABRASION-RESISTANT LINING LUBRICATED, (Lined) NONE CENTRAL SEAT
		REGULATING	BUTTERFLY DIAPHRAGM SQUEEZE PINCH GATE	ABRASION-RESIST. DISC, RESILIENT SEAT LINED* NONE NONE SINGLE SEAT, NOTCHED DISC
	FIBROUS SUSPENSIONS	ON/OFF & REGULATING	GATE DIAPHRAGM SQUEEZE PINCH	SINGLE SEAT, KNIFE-EDGED DISC, NOTCHED DISC NONE NONE NONE
GAS	NEUTRAL (AIR, STEAM, Etc.)	ON/OFF	GATE GLOBE ROTARY BALL PLUG DIAPHRAGM	NONE (Composition Disc), (Plug-Type Disc) NONE NONE, (Unsuitable for steam service) NONE, (Unsuitable for steam service)
		REGULATING	GLOBE NEEDLE BUTTERFLY DIAPHRAGM GATE	NONE NONE, (Small flows only) NONE NONE, (Unsuitable for steam service) SINGLE SEAT
	CORROSIVE (ACID VAPORS, CHLORINE, Etc.)	ON/OFF	BUTTERFLY ROTARY BALL DIAPHRAGM PLUG	ANTI-CORROSIVE* ANTI-CORROSIVE* ANTI-CORROSIVE* ANTI-CORROSIVE*
		REGULATING	BUTTERFLY GLOBE NEEDLE DIAPHRAGM	ANTI-CORROSIVE* ANTI-CORROSIVE*, (OS&Y) ANTI-CORROSIVE*, (Small flows only) ANTI-CORROSIVE*
	VACUUM	ON/OFF	GATE GLOBE ROTARY BALL BUTTERFLY	BELLOWS SEAL DIAPHRAGM or BELLOWS SEAL NONE RESILIENT SEAT
SOLID	ABRASIVE POWDER (SILICA, Etc.)	ON/OFF & REGULATING	PINCH SQUEEZE SPIRAL SOCK	NONE (CENTRAL SEAT) NONE
	LUBRICATING POWDER (GRAPHITE, TALC, Etc.)	ON/OFF & REGULATING	PINCH GATE SQUEEZE SPIRAL SOCK	NONE SINGLE SEAT (CENTRAL SEAT) NONE

\* Suitability of materials of construction with respect to the great variety of fluids encountered is a complex topic. A good general reference is the current edition of the Chemical Engineer's Handbook (8).

† The disc should be smooth, without bolts and recesses, in a sanitary material such as stainless steel, or fully coated with "white" plastic or rubber material. "White" means that the material does not contain a filler which is toxic or can discolor the product.

# KEY TO VALVE SELECTION GUIDE

## CHART 3.2

- Determine type of conveyed fluid—liquid, gas, slurry, or powder
- Determine nature of fluid:
  - Substantially neutral—not noticeably acid or alkaline, such as various oils, drinking water, nitrogen, gas, air, etc.
  - Corrosive—markedly acid, alkaline, or otherwise chemically reactive
  - 'Hygienic'—materials for the food, drug, cosmetic or other industries
  - Slurry—suspension of solid particles in a liquid can have an abrasive effect on valves, etc. Non-abrasive slurries such as wood-pulp slurries can choke valve mechanisms
- Determine operation:
  - 'On/off'—fully open or fully closed
  - Regulating—including close regulation (throttling)
- Look into other factors affecting choice:
  - Pressure and temperature of conveyed fluid
  - Method of operating stem—consider closing time
  - Cost
  - Availability
  - Special installation problems—such as welding valves into lines. Welding heat will sometimes distort the body and affect the sealing of small valves.\*

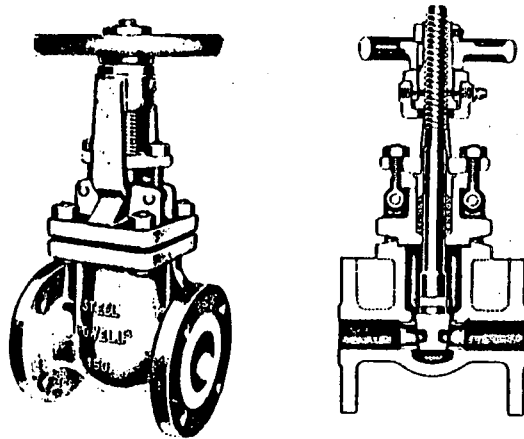
\* This problem is discussed in the William Powell Company's valve catalog, number 69, section 20, pages ED83 and ED84.

In industrial piping, on/off control of flow is most commonly effected with gate valves. Most types of gate valve are unsuitable for regulating: erosion of the seat and disc occurs in the throttling position due to vibration of the disc ("chattering"). With some fluids, it may be desirable to use globe valves for on/off service, as they offer tighter closure. However, as the principal function of globe valves is regulation, they are described in 3.1.5.

**SOLID WEDGE GATE VALVE** has either a solid or flexible wedge disc. In addition to on/off service, these valves can be used for regulating, usually in sizes 6-inch and larger, but will chatter unless disc is fully guided throughout travel. Suitable for most fluids including steam, water, oil, air and gas. The flexible wedge was developed to overcome sticking on cooling in high-temperature service, and to minimize operating torque. The flexible wedge is not illustrated—it can be likened to two wheels set on a very short axle.

#### SOLID WEDGE GATE VALVE

(COURTESY WM. POWELL CO.)



**DOUBLE-DISC PARALLEL-SEATS GATE VALVE** has two parallel discs which are forced, on closure, against parallel seats by a 'spreader'. Used for liquids and gases at normal temperatures. Unsuitable for regulation. To prevent jamming, installation is usually vertical with handwheel up.

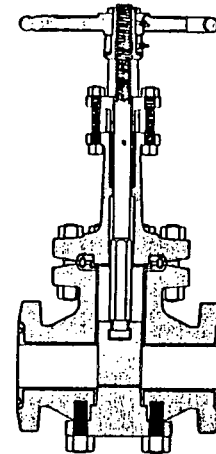
**DOUBLE-DISC (SPLIT-WEDGE) WEDGE GATE VALVE** Discs wedge against inclined seats without use of a spreader. Remarks for double-disc parallel seats gate valve apply, but smaller valves are made for steam service. Often, construction allows the discs to rotate, distributing wear.

**SINGLE-DISC SINGLE-SEAT GATE VALVE, or SLIDE VALVE**, is used for handling paper pulp slurry and other fibrous suspensions, and for low-pressure gases. Will not function properly with inflow on the seat side. Suitable for regulating flow if tight closure is not required.

**SINGLE-DISC PARALLEL-SEATS GATE VALVE** Unlike the single-seat slide valve, this valve affords closure with flow in either direction. Stresses on stem and bonnet are lower than with wedge-gate valves. Primarily used for liquid hydrocarbons and gases.

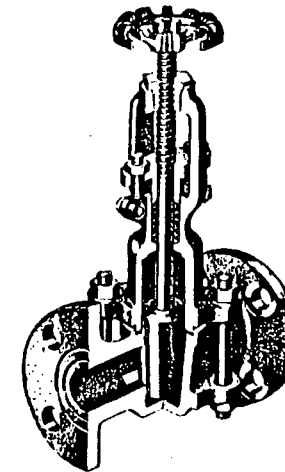
#### SINGLE-DISC PARALLEL-SEATS GATE VALVE

(COURTESY HENRY VOGT MACHINE CO.)



#### PLUG GATE VALVE

(COURTESY CRANE COMPANY)



**PLUG GATE VALVE** This valve has a round tapered disc which moves up and down. Suitable for throttling and full-flow use, but only available in the smaller sizes.

**PLUG VALVE** Mechanism is shown in chart 3.1, but the disc may be cylindrical as well as tapered. Advantages are compactness, and rotary 90-degree stem movement. The tapered plug tends to jam and requires a high operating torque: this is overcome to some extent by the use of a low-friction (teflon, etc.) seat, or by lubrication (with the drawback that the conveyed fluid is contaminated). The friction problem is also met by mechanisms raising the disc from the seat before rotating it, or by using the 'eccentric' design (see rotary-ball valve). Principal uses are for water, oils, slurries, and gases.

**LINE-BLIND VALVE** This is a positive shutoff device which basically consists of a flanged assembly sandwiching a spectacle-plate or blind. This valve is described and compared with other closures in 2.7.1.

#### VALVES MAINLY FOR REGULATING SERVICE

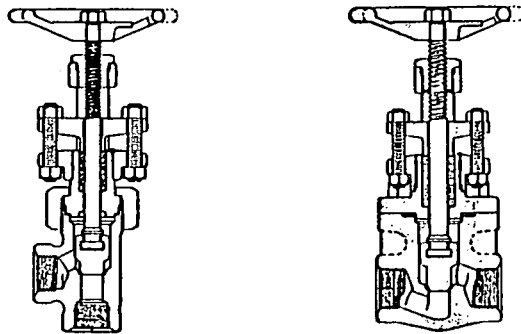
3.1.5

**GLOBE VALVE, STRAIGHT & ANGLE TYPE** These are the valves most used for regulating. For line sizes over 6-inch, choice of a valve for flow control tends to go to suitable gate or butterfly valves. For more satisfactory service, the direction of flow thru valve recommended by manufacturers is from stem to seat, to assist closure and to prevent the disc chattering against the seat in the throttling position. Flow should be from seat to stem side (1) if there is a hazard presented by the disc detaching from the stem thus closing the valve, or (2) if a composition disc is used, as this direction of flow then gives less wear.

**ANGLE VALVE** This is a globe valve with body ends at right angles, saving the use of a 90-degree elbow. However, the angles of piping are often subject to higher stresses than straight runs, which must be considered with this type of valve.

#### GLOBE VALVES

(COURTESY HENRY VOST MACHINE CO.)



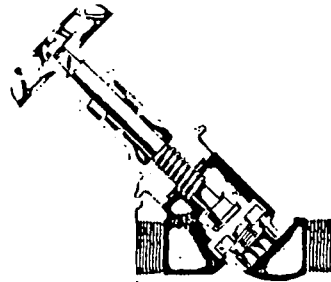
**REGULAR-DISC GLOBE VALVE** Unsuitable for close regulation as disc and seat have narrow (almost line) contact.

**PLUG-TYPE DISC GLOBE VALVE** Used for severe regulating service with gritty liquids, such as boiler feedwater, and for blow-off service. Less subject to wear under close regulation than the regular-seated valve.

**WYE-BODY GLOBE VALVE** has in-line ports and stem emerging at about 45 degrees; hence the 'Y'. Preferred for erosive fluids due to smoother flow pattern.

#### WYE-BODY GLOBE VALVE (Incorporating composition disc)

(COURTESY JENKINS BROS. VALVE MANUFACTURERS)



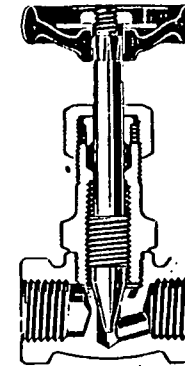
**COMPOSITION-DISC GLOBE VALVE** Suitable for coarse regulation and tight shutoff. Replaceable composition-disc construction is similar to that of a faucet. Grit will imbed in the soft disc preventing seat damage and ensuring good closure. Close regulating will rapidly damage the seat.

**DOUBLE-DISC GLOBE VALVE** features two discs bearing on separate seats spaced apart on a single shaft, which frees the operator from stresses set up by the conveyed fluid pressing into the valve. Principle is used on control valves and pressure regulators for steam and other gases. Tight shutoff is not ensured.

**NEEDLE VALVE** is a small valve used for flow control and for dosing liquids and gases. Resistance to flow is precisely controlled by a relatively large seat area and the adjustment afforded by fine threading of the stem.

#### NEEDLE VALVE

(COURTESY LUNKENHEIMER COMPANY)



**SQUEEZE VALVE** is well-suited to regulating the flow of difficult liquids, slurries and powders. Maximum closure is about 80%, which limits the range of regulation, unless the variation of this type of valve with a central core (seat) is used, offering full closure.

**PINCH VALVE** Also suited to regulating flow of difficult liquids, slurries and powders. Complete closure is possible but tends to rapidly wear the flexible tube, unless of special design.

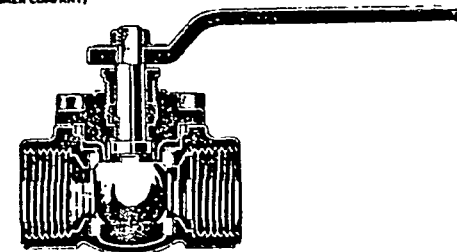
#### VALVES FOR BOTH REGULATING & ON/OFF SERVICE

3.1.6

**ROTARY-BALL VALVE** Advantages are low operating torque, availability in large sizes, compactness, rotary 90-degree stem movement, and 'in-line' replaceability of all wearing parts in some designs. Possible disadvantages are that fluid is trapped within the body (and within the disc on closure), and that compensation for wear is effected only by resilient material behind the seats: the latter problem is avoided in the single-seat 'eccentric' version, which has the ball slightly offset so that it presses into the seat, on closure. Principal uses are for water, oils, slurries, gases and vacuum. Valve is available with a ball having a shaped port for regulation.

#### ROTARY-BALL VALVE

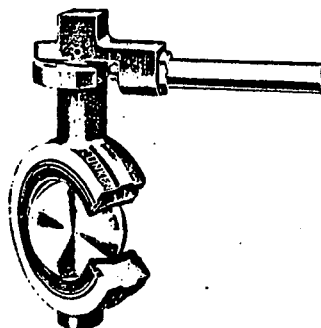
(COURTESY LUNKENHEIMER COMPANY)



**BUTTERFLY VALVE** offers the advantages of rotary stem movement (90 degrees or less), compactness, and absence of pocketing. It is available in all sizes, and can be produced in chemical-resistant and hygienic forms. The valves are used for gases, liquids, slurries, powders and vacuum. The usual resilient plastic seat has a temperature limitation, but tight closure at high temperatures is available with a version having a metal ring seal around the disc. If the valve is flanged, it may be held between flanges of any type. Slip-on and screwed flanges do not form a proper seal with some wafer forms of the valve, in which the resilient seat is extended to serve also as line gaskets.

#### **BUTTERFLY VALVE (Wafer type)**

(COURTESY LUNKENHEIMER COMPANY)



### **VALVES FOR CHECKING BACKFLOW**

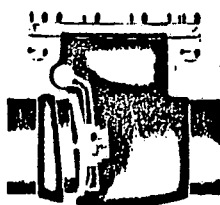
3.1.7

All valves in this category are designed to permit flow of liquid or gas in one direction and close if flow reverses.

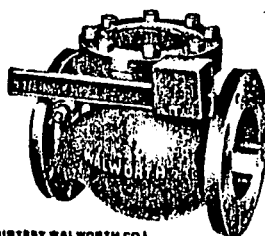
**SWING CHECK VALVE** The regular swing check valve is not suitable if there is frequent flow reversal as pounding and wearing of disc occurs. For gritty liquids a composition disc is advisable to reduce damage to the seat. May be mounted vertically with flow upward, or horizontally. Vertically-mounted valve has a tendency to remain open if the stream velocity changes slowly. An optional lever and outside weight may be offered either to assist closing or to counterbalance the disc in part, and allow opening by low-pressure fluid.

#### **SWING CHECK VALVES**

(COURTESY JENKINS BROS. - VALVE MANUFACTURERS)



Outside Lever & Weight  
for swing check valve



(COURTESY WALWORTH CO.)

**TILTING-DISC VALVE** Suitable where frequent flow reversal occurs. Valve closes rapidly with better closure and less slamming than the swing check valve, which it somewhat resembles. It has higher pressure drop with large

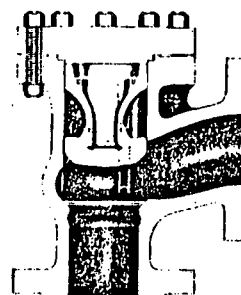
flow velocities and lower-pressure drop with small velocities than a comparable swing-check valve. May be installed vertically with flow upward, or horizontally. Disc movement can be controlled by an integral dashpot or snubber.

**LIFT-CHECK VALVE** resembles the piston-check valve. The disc is guided, but the dashpot feature is absent. Spring-loaded types can operate at any orientation, but unsprung valves have to be arranged so that the disc will close by gravity. Composition-disc valves are available for gritty liquids.

**PISTON-CHECK VALVE** Suitable where frequent change of direction of flow occurs as these valves are much less subject to pounding with pulsating flow due to the integral dash-pot. Spring-loaded types can operate at any orientation. Unsprung valves have to be orientated for gravity closure. Not suitable for gritty liquids.

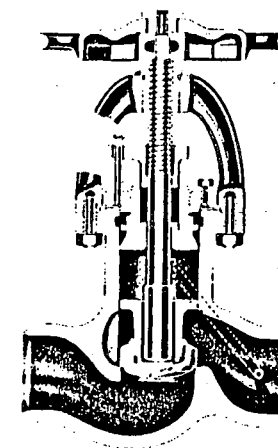
#### **PISTON-CHECK VALVE**

(COURTESY ROCKWELL MFG CO.)



#### **STOP CHECK VALVE**

(COURTESY ROCKWELL MFG CO.)



**STOP-CHECK VALVE** Principal example of use is in steam generation by multiple boilers, where a valve is inserted between each boiler and the main steam header. Basically, a check valve that optionally can be kept closed automatically or manually.

**BALL-CHECK VALVE** is suitable for most services. The valve can handle gases, vapors and liquids, including those forming gummy deposits. The ball seats by gravity and/or back pressure, and is free to rotate, which distributes wear and aids in keeping contacting surfaces clean.

**WAFER CHECK VALVE** effects closure by two semicircular 'doors', both hinged to a central post in a ring-shaped body which is installed between flanges. Frequently used for non-fouling liquids, as it is compact and of relatively low cost. A single disc type is also available.

**FOOT VALVE** Typical use is to maintain a head of water on the suction side of a sump pump. The valve is basically a lift-check valve with a strainer integrated.

### VALVES FOR SWITCHING FLOW

3.1.8

**MULTIPORT VALVE** Used largely on hydraulic and pneumatic control circuits and sometimes used directly in process piping, these valves have rotary-ball or plug-type discs with one or more ports arranged to switch flow.

**DIVERTING VALVE** Two types of 'diverting' valve are made. Both switch flow from a line into one of two outlets. One type is of wye pattern with a hinged disc at the junction which closes one of the two outlets, and is used to handle powders and other solids. The second type handles liquid only, and has no moving parts—flow is switched by two pneumatic control lines. It is available in sizes to 6-inch [9].

### VALVES FOR DISCHARGING

3.1.9

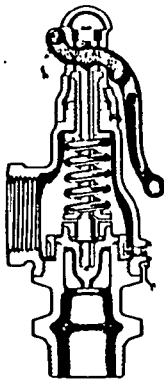
These valves allow removal of fluid from within a piping system either to atmosphere, to a drain, or to another piping system or vessel at a lower pressure. Operation is often automatic. Relief and safety valves, steam traps, and rupture discs are included in this section. Pressure-relieving valves are usually spring loaded, as those worked by lever and weight can be easily rendered inoperative by personnel. The first three valves are operated by system pressure, and are usually mounted directly onto the piping or vessel to be protected, in a vertical, upright position. Refer to the governing code for the application of these valves, including the need for an external lifting device (handlever, etc.).

**SAFETY VALVE** A rapid-opening (popping action) full-flow valve for air and other gases.

**RELIEF VALVE** Intended to relieve excess pressure in liquids, in situations where full-flow discharge is not required, when release of a small volume of liquid would rapidly lower pressure. Mounting is shown in figure 6.4.

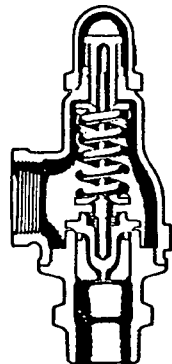
#### SAFETY VALVE

(COURTESY CRANE COMPANY)



#### RELIEF VALVE

(COURTESY CRANE COMPANY)

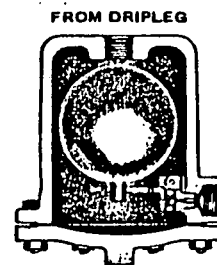


**SAFETY-RELIEF VALVE** Relieves excess pressure of either gas or liquid which may suddenly develop a vapor phase due to rapid and uncontrolled heating from chemical reaction in liquid-laden vessels. Refer to figure 6.4.

**BALL FLOAT VALVE** These automatic valves are used: (1) As air traps to remove water from air systems. (2) To remove air from liquid systems and act as vacuum breakers or breather valves. (3) To control liquid level in tanks. They are not intended to remove condensate.

#### BALL FLOAT VALVE

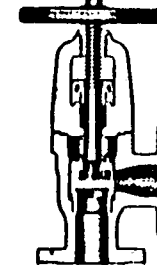
(For first use above)



WATER  
RELEASED

#### BLOWOFF VALVE

(COURTESY CRANE COMPANY)

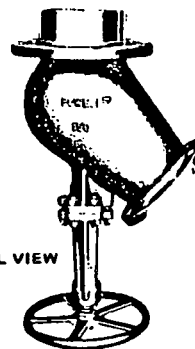


**BLOWOFF VALVE** A variety of globe valve conforming with boiler code requirements and especially designed for boiler blowoff service. Sometimes suitable also for blowdown service. Wye-pattern and angle types often used. Used to remove air and other gases from boilers, etc. Manually operated.

**FLUSH-BOTTOM TANK VALVE** Usually a globe type, designed to minimize pocketing, primarily for conveniently discharging liquid from the low point of a tank.

#### FLUSH-BOTTOM TANK VALVE (GLOBE TYPE)

(COURTESY WM. POWELL CO.)



EXTERNAL VIEW



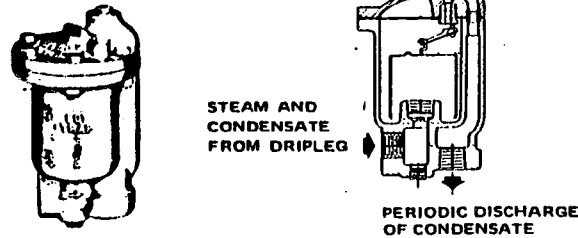
SECTIONAL VIEW

**RUPTURE DISC** A safety device designed to burst at a certain excess pressure and rapidly discharge gas or liquid from a system. Usually made in the form of a replaceable metal disc held between flanges. Disc may also be of graphite or, for lowest bursting pressures, plastic film.

**SAMPLING VALVE** A valve, usually of needle or globe pattern, placed in a branch line for the purpose of drawing off samples of process material thru the branch. Sampling from very high pressure lines is best done thru a double valved collecting vessel. A cooling arrangement may be needed for sampling from high-temperature lines.

**TRAP** An automatic valve for: (1) Discharging condensate, air and gases from steam lines without releasing steam. (2) Discharging water from air lines without releasing air—see 'Ball float valve', this section.

#### INVERTED-BUCKET TRAP (COURTESY ARMSTRONG MACHINE WORKS)



### CONTROL VALVES & PRESSURE REGULATORS

3.1.10

#### CONTROL VALVES

Control valves automatically regulate pressure and/or flow rate, and are available for any pressure. If there are different system pressures in a plant up to and including 300 PSIG, sometimes all control valves chosen will be rated at 300 PSI for interchangeability. However, if none of the system pressures exceeds 150 PSIG, this is not necessary. The control valve is usually chosen to be smaller than line size to avoid throttling and consequent rapid wear of the seat.

Globe-pattern valves are normally used for control, and their ends are usually flanged for ease of maintenance. The disc is moved by a hydraulic, pneumatic, electrical, or mechanical operator.

Figure 3.4 shows schematically how a control valve can be used to control rate of flow in a line. Flow rate is related to the pressure drop across the 'sensing element' (an orifice plate in this instance—see 6.7.5). The 'controller' receives the pressure signals, compares them with the pressure drop for the desired flow and, if the actual flow is different, adjusts the control valve to increase or decrease the flow.

Comparable arrangements to figure 3.4 can be devised to control any of numerous process variables—temperature, pressure, level and flow rate are the most common controlled variables.

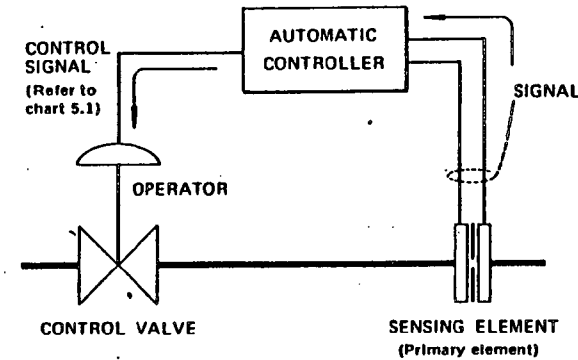
Control valves may be self-operating, and not require the addition of a controller, sensing element, etc. Pressure regulators are a common example of this type of valve, and chart 3.1 shows the principles of operation of a pressure regulator.

**PRESSURE REGULATOR** Control valve of globe type which adjusts downstream pressure of liquid or gas (including steam or vapors) to a lower desired value ('set pressure').

**BACK-PRESSURE REGULATOR** Control valve used to maintain upstream pressure in a system.

#### SCHEMATIC FOR A CONTROL VALVE ARRANGEMENT

FIGURE 3.4



### UNCLASSIFIED VALVES & TERMS

3.1.11

With few exceptions, the following are not special valve types different from those previously discussed, but are terms used to describe valves by service or function.

**BARSTOCK VALVE** Any valve having a body machined from solid metal (barstock). Usually needle or globe type.

**BIBB** A small valve with turned-down end, like a faucet.

**BLEED VALVE** Small valve provided for drawing off fluid.

**BLOCK VALVE** An on/off valve, nearly always a gate valve, placed in lines at battery limits.

**BLOWDOWN VALVE** Usually refers to a plug-type disc globe valve used for removing sludge and sedimentary matter from the bottom of boiler drums, vessels, driplegs, etc.

**BREATHING VALVE** A special self-acting valve installed on storage tanks, etc., to release vapor or gas on slight increase of internal pressure (in the region of ½ to 3 ounces per square inch).

**BYPASS VALVE** Any valve placed in a bypass arranged around another valve or equipment—see 6.1.3 under 'If there is no P&ID....' and figures 6.6 thru 6.11.

**DIAPHRAGM VALVE** Examples of true diaphragm valves, where the diaphragm closes off the flow, are shown in chart 3.1. These forms of diaphragm valve are popular for regulating the flow of slurries and corrosive fluids and for vacuum. The term 'diaphragm valve' is also applied to valves which have a diaphragm seal between stem and body, but these are better referred to as 'diaphragm seal' or 'packless' valves—see 3.1.2, under 'Seal'.

**DRAIN VALVE** A valve used for the purpose of draining liquids from a line or vessel. Selection of a drain valve, and the method of attachment, is influenced by the undesirability of pocketing the material being drained—this is important with slurries and liquids which are subject to: (1) Solidification on cooling or polymerization. (2) Decomposition.

**DRIP VALVE** A drain valve fitted to the bottom of a dripleg to permit blowdown.

3.1.8  
3.1.11

FIGURE  
3.4

**FLAP VALVE** A non-return valve having a hinged disc or rubber or leather flap, used for low-pressure lines.

**HEADER VALVE** An isolating valve installed in a branch where it joins a header.

**HOSE VALVE** A gate or globe valve having one of its ends externally threaded to one of the hose thread standards in use in the USA [12, p.62]. These valves are used for vehicular and firewater connections.

**ISOLATING VALVE** An on/off valve isolating a piece of equipment or a process from piping.

**KNIFE-EDGE VALVE** A single-disc single-seat gate valve (slide gate) with a knife-edged disc.

**MIXING VALVE** regulates the proportions of two inflows to produce a controlled outflow.

**NON-RETURN VALVE** Any type of stop-check valve—see 3.1.7.

**PAPER-STOCK VALVE** A single-disc single-seat gate valve (slide gate) with knife-edged or notched disc used to regulate flow of paper slurry or other fibrous slurry.

**PRIMARY VALVE** See 'Root valve', this section.

**REGULATING VALVE** Any valve used to adjust flow.

**ROOT VALVE** (1) A valve used to isolate a pressure element or instrument from a line or vessel. (2) A valve placed at the beginning of a branch from a header.

**SAMPLING VALVE** Small valve provided for drawing off fluid. See 3.1.9.

**SHUTOFF VALVE** An on/off valve placed in lines to or from equipment, for the purpose of stopping and starting flow.

**SLURRY VALVE** A knife-edge valve used to control flow of non-abrasive slurries.

**SPIRAL-SOCK VALVE** A valve used to control flow of powders by means of a twistable fabric tube or sock.

**STOP VALVE** An on/off valve, usually a globe valve.

**THROTTLING VALVE** Any valve used to closely regulate flow in the just-open position.

**VACUUM BREAKER** A special self-acting valve, or any valve suitable for vacuum service, operated manually or automatically, installed to admit gas (usually atmospheric air) into a vacuum or low-pressure space. Such valves are installed on high points of piping or vessels to permit draining, and sometimes to prevent siphoning.

**UNLOADING VALVE** See 3.2.2, under 'Unloading', and figure 6.23.

**QUICK-ACTING VALVE** Any on/off valve rapidly operable, either by manual lever, spring, or by piston, solenoid or lever with heat-fusible link releasing a weight which in falling operates the valve. Quick-acting valves are desirable in lines conveying flammable liquids. Unsuitable for water or for liquid service in general without a cushioning device (hydraulic accumulator, 'pulsation pot' or 'standpipe') to protect piping from shock. See 3.1.2, under 'Quick-acting operators for non-rotary valves'.

## PUMPS & COMPRESSORS

3.2

### PUMPS

3.2.1

#### REFERENCE

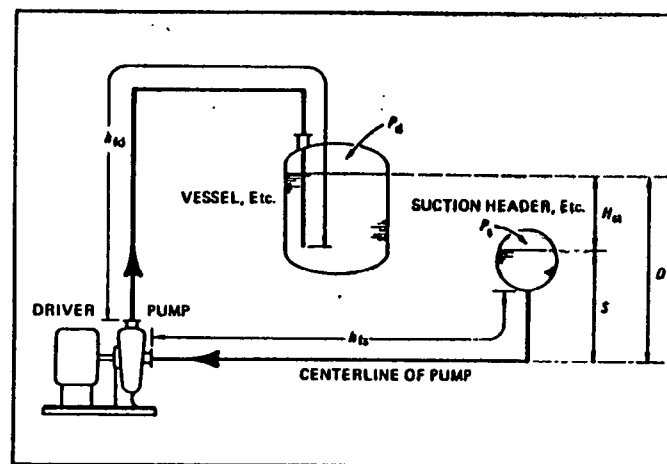
'Pumps & the chemical plant'. Thurflow C. 1965. Chemical Engineering reprint

#### DRIVERS

Electric motors are the most frequently used drivers. Larger pumps may be driven by steam-, gas-, or diesel-engines, or by turbines.

'HEADS' (PRESSURES) IN PUMP PIPING

FIGURE 3.6



#### NOTES

The total head,  $H$ , which must be provided by the pump in the arrangement shown, is:—

$$H = H_d - H_s = H_{st} + (H_{fd} + H_{fs}) + (P_d - P_s)$$

Heads may be expressed either all in absolute units or all in gage units, but not in mixed units. The various head terms in this equation are, with reference to the illustration:—

$H_d$  = total discharge head

$H_s$  = total suction head

$H_{st}$  = static head (differential) =  $D - S$

$H_{fd}$  = friction head loss in discharge piping, including exit loss (as liquid discharges into vessel, etc.) and loss at increaser located at pump outlet\*

$H_{fs}$  = friction head loss in suction piping, including entrance loss (as liquid enters line from header, etc.) and loss at reducer located at pump inlet\*

$P_d$  = pressure head above liquid level in discharge vessel or header

$P_s$  = pressure head above liquid level in suction header or vessel

NET POSITIVE SUCTION HEAD (NPSH)

'NPSH' is defined by:—  $S - H_{fs} + P_s - P_{vp}$ , where

$P_{vp}$  = vapor pressure of liquid at temperature of liquid at suction header, etc. Vapor pressures are given in absolute units

\*Table F-10 gives entrance loss, exit loss, flow resistance of reducers and swages, etc., expressed in equivalent lengths of pipe.



PUMP SELECTION GUIDE												
CHART 3.3												
CLASS OF MECHANISM	I. IMPELLOR			II. CHAMBER-CRANK TRAIN		III. CHAMBER-WHEEL TRAIN			IV. RECIPROCATING		V. MISCELLANEOUS	
BASIC PUMP TYPE	CENTRIFUGAL	PROPELLOR	TURBINE	VALE	MUTATOR	SPURGEAR	BENRENS	SCREW	PISTON	DIAPHRAGM	MOYMO	PERISTALTIC
OTHER RELATED TYPES OF PUMP	VOLUTE DIFFUSER		AXIAL FLOW TURBINE	CAM & PISTON, SHUTTLE-BLOCK, SWINGING VALE	MUTATING DISC	GEAR, STAR AND CRESCENT		TRIPLE SCREW	SWASH-PLATE, RADIAL, RAM		SINGLE SCREW	
BASIC FORM OF MECHANISM SHOWN SCHEMATICALLY (FLOW IS FROM LEFT TO RIGHT)												
FLOW RATE AT CONSTANT DRIVE SPEED	UNIFORM IF TOTAL HEAD UNCHANGED			SOME VARIATION	UNIFORM AT CONSTANT DRIVE SPEED				PULSATING UNDER ALL CONDITIONS		UNIFORM	NEARLY UNIFORM
DISCHARGE PRESSURE	LOW TO MEDIUM			LOW TO HIGH	LOW TO MEDIUM	MEDIUM	LOW TO HIGH	MEDIUM	LOW TO HIGH	LOW TO HIGH	LOW TO MEDIUM	LOW
TYPICAL FLUID HANDLED WITH APPROPRIATE CONSTRUCTION	CLEAN LIQUIDS	•	•	•	•	•	•	•	•	•	•	•
	OILS	•	•	•	•	•	•	•	•	•	•	•
	VISCOUS LIQUIDS	•	•	•	•	•	•	•	•	•	•	•
	SURRIES	•	•	•	•	•	•	•	•	•	•	•
	EMULSIONS	•	•	•	•	•	•	•	•	•	•	•
	PASTES	•	•	•	•	•	•	•	•	•	•	•
	LUMPS	•	•	•	•	•	•	•	•	•	•	•
	POWDERS	•	•	•	•	•	•	•	•	•	•	•

## TYPES OF PUMP

A pump is a device for moving a fluid from one place to another thru pipes or channels. Chart 3.3, a selection guide for pumps, puts various types of pump used industrially into five categories, based on operating principle. In common reference, the terms centrifugal, rotary, screw, and reciprocating are used. Chart 3.3 is not comprehensive; pumps utilizing other principles are in use.

About nine out of ten pumps used in industry are of centrifugal type.

The following information is given to enable an estimate to be made of required total head, pump size, capacity and horsepower for planning purposes. Data in the Guide permit estimating pressure drops and total head for pumped water systems; further information for calculating systems pumping other liquids may be found in the Chemical Engineer's Handbook [8], the Engineering Manual (McGraw-Hill), and the Mechanical Engineer's Handbook (McGraw-Hill).

## PRESSURES, or 'HEADS'

For pump calculations, pressure is often stated as a 'head' (height) of water --or of the liquid being pumped. Unless otherwise stated, pressures thus expressed may be assumed given in feet of water. Atmospheric pressure at sea level is equal to 14.7 PSIA, or 34 feet of water.

Figure 3.5 relates the total head supplied by a pump to various head losses in the piping.

## VELOCITY HEAD

Usually the liquid being pumped is stationary before entering the suction piping, and some power is absorbed in accelerating it to the suction line velocity. This causes a small 'velocity head' loss (usually about 1 ft) and may be found from table 3.2, which is applicable to liquid of any density, if the velocity head is read as feet of the liquid concerned.

## VELOCITY & VELOCITY HEAD

TABLE 3.2

VELOCITY (Ft/sec)	4	5	6	7	8	9	10	12	15
VELOCITY HEAD (Ft)	0.25	0.39	0.56	0.76	0.99	1.26	1.55	2.24	3.50

Flow rate, liquid velocity and cross-sectional area (at right angles to flow) are related by the formulas:

$$\text{Flow rate in cubic feet per second} = (v)(a)/(144)$$

$$\text{Flow rate in US gallons per minute} = (3.1169)(v)(a)$$

where:  $v$  = liquid velocity in feet per second

$a$  = cross-sectional area in square inches (table P-1)

## POWER CALCULATIONS

If S.G. = specific gravity of the pumped liquid,  $H$  = total head in feet of pumped liquid, and  $p$  = total head in PSI, then:

$$\text{Hydraulic horsepower} = \frac{(\text{GPM})(H)(\text{S.G.})}{3960} = \frac{(\text{GPM})(p)}{1714}$$

CHART 3.3

FIGURE 3.5

TABLE 3.2

The mechanical efficiency,  $e$ , of a pump is defined as the hydraulic horsepower (power transferred to the pumped liquid) divided by the brake horsepower (power applied to the driving shaft of the pump).

If the pump is driven by an electric motor which has a mechanical efficiency  $e_m$ , the electricity demand is:

$$\text{Kilowatt (KW)} = \frac{(\text{GPM})(H)(\text{S.G.})}{(5310)(e)(e_m)} = \frac{(\text{GPM})(p)}{(2299)(e)(e_m)}$$

Often, estimates of brake horsepower, electricity demand, etc., must be made without proper knowledge of the efficiencies. To obtain estimates, the mechanical efficiency of a centrifugal pump may be assumed to be 60%, and that of an electric motor 80%.

## COMPRESSORS, BLOWERS & FANS

3.2.2

### REFERENCES

'Compressed air and gas handbook'. Compressed Air and Gas Institute (New York) Revised 1966

'Compressor installation manual'. Atlas-Copco AB. 1966

Compressors are used to supply high-pressure air for plant use, to pressurize refrigerant vapors for cooling systems, to liquefy gases, etc. They are rated by their maximum output pressure and the number of cubic feet per minute of a gas handled at a specified speed or power, stated at 'standard conditions', 60 F and 14.7 PSIA (not at compressed volume). 60 F is accepted as standard temperature by the gas industry.

The term 'compressor' is usually reserved for machines developing high pressures in closed systems, and the terms 'blower' and 'fan' for machines working at low pressures in open-ended systems.

COMPRESSOR PRESSURE RANGES

TABLE 3.3

MACHINE	DISCHARGE PRESSURE RANGE
COMPRESSOR	15 thru 20,000 PSIG, and higher
BLOWER	1 thru 15 PSIG
FAN	Up to 1 PSIG (about 30 in. water)

### COMPRESSING IN STAGES

Gases (including air) can be compressed in one or more operations termed 'stages'. Each stage can handle a practicable increase in pressure—before temperature increase due to the compression necessitates cooling the gas. Cooling between stages is effected by passing the gas thru an intercooler. Staging permits high pressures, and lower discharge temperatures, with reduced stresses on the compressor.

## TYPES OF COMPRESSOR

**RECIPROCATING COMPRESSOR** Air or other gas is pressurized in cylinders by reciprocating pistons. If the compressor is lubricated, the outflow may be contaminated by oil. If an oil-free outflow is required, the pistons may be fitted with graphite or teflon piston rings. Flow is pulsating.

**ROTARY SCREW COMPRESSOR** Air or other gas enters pockets formed between mating rotors and a casing wall. The pockets rotate away from the inlet, taking the gas toward the discharge end. The rotors do not touch each other or the casing wall. Outflow is uncontaminated in the 'dry type' of machine, in which power is applied to both rotors thru external timing gears. In the 'wet type', power is applied to one rotor, and both rotors are separated by an oil film, which contaminates the discharge. Flow is uniform.

**ROTARY VANE COMPRESSOR** resembles the rotary vane pump shown in chart 3.3. Variation in the volume enclosed by adjacent vanes as they rotate produces compression. Ample lubrication is required, which may introduce contamination. Flow is uniform.

**ROTARY LOBE COMPRESSOR** consists of two synchronized lobed rotors turning within a casing, in the same way as the pump shown in chart 3.3 (under 'spurgear' type). The rotors do not touch each other or the casing. No lubrication is used within the casing, and the outflow is not contaminated. Flow is uniform. This machine is often referred to as a 'blower'.

**DYNAMIC COMPRESSORS** resemble gas turbines acting in reverse. Both axial-flow machines and centrifugal machines (with radial flow) are available. Centrifugal compressors commonly have either one or two stages. Axial compressors have at least two stages, but seldom more than 16 stages. The outflow is not contaminated. Flow is uniform.

**LIQUID RING COMPRESSOR** This type of compressor consists of a single multi-bladed rotor which turns within a casing of approximately elliptic cross section. A controlled volume of liquid in the casing is thrown to the casing wall with rotation of the vanes. This liquid serves both to compress and to seal. Inlet and outlet ports located in the hub communicate with the pockets formed between the vanes and the liquid ring. These compressors have special advantages: wet gases and liquid carryover including hydrocarbons which are troublesome with other compressors are easily handled. Additional cooling is seldom required. Condensable vapor can be recovered by using liquid similar to that in the ring. Flow is uniform.

### EQUIPMENT FOR COMPRESSORS

**INTERCOOLER** A heat exchanger used for cooling compressed gas between stages. Air must not be cooled below the dew point (at the higher pressure) as moisture will interfere with lubrication and cause wear in the next stage.

**AFTERCOOLER** A heat exchanger used for cooling gas after compression is completed. If air is being compressed, chilling permits removal of much of the moisture.

**DAMPENER or SNUBBER; VOLUME BOTTLE or SURGE DRUM** Reciprocating compressors create pulsations in the air or gas which may cause the

discharge and/or suction piping to resonate and damage the compressor or its valves. A dampener, or snubber, is a baffled vessel which smooths pulsations in flow. A volume bottle or surge drum has the same purpose, but lacks baffles. These devices are not normally part of the compressor package, and are often bought separately (with the compressor maker's recommendations). Large compressors may require an arrangement of 'choke tubes' (restrictions) and 'bottles' (vessels), conforming to a theoretical design and located near the compressor's outlet, upstream of the aftercooler.

The location of the following four items of equipment is shown in figure 6.23:

**SEPARATOR** (normally used only with air compressors) A water separator is often provided following the aftercooler, and, sometimes, also at the intake to a compressor having a long suction line, if water is likely to collect in the line. Each separator is provided with a drain to allow continuous removal of water.

**RECEIVER** Refer to 'Discharge (supply) lines' and 'Storing compressed air', this section.

**SILENCER** is used to suppress objectionable sound which may radiate from an air intake.

**FILTER** is provided in the suction line to an air compressor to collect particulate matter.

*The following information is given as a guide for engineering purposes*

#### LINE SIZES FOR AIR SUCTION & DISTRIBUTION

**SUCTION LINE** Suction lines and manifolds should be large enough to prevent excessive noise and starvation of the air supply. If the first compression stage is reciprocating, the suction line should allow a 10 to 23 ft/sec flow: if a single-stage reciprocating compressor is used, the intake flow should not be faster than 20 ft/sec. Dynamic compressors can operate with faster intake velocities, but 40 ft/sec is suggested as a maximum. The inlet reducer for a dynamic compressor should be placed close to the inlet nozzle.

**DISCHARGE (SUPPLY) LINES** are sized for 150 to 175% of average flow, depending on the number of outlets in use at any time. The pressure loss in a branch should be limited to 3 PSI. The pressure drop in a hose should not exceed 5 PSI. The pressure drop in distribution piping, from the compressor to the most remote part of the system, should not be greater than 5 PSI (not including hoses).

These suggested pressure drops may be used to select line sizes with the aid of table 3.5. From the required SCFM flow in the line to be sized, find the next higher flow in the table. Multiply the allowed pressure drop (PSI) in the line by 100 and divide by the length of the line in feet to obtain the PSI drop per 100 ft—find the next lower figure to this in the table, and read required line size.

Equipment drawing air at a high rate for a short period is best served by a receiver close to the point of maximum use—lines can then be sized on average demand. A minimum receiver size of double the SCF used in intermittent demand should limit the pressure drop at the end of the period of use to about 20% in the worst instances and keep it under 10% in most others.

COMPRESSOR CHARACTERISTICS

TABLE 3.4

COMPRESSOR TYPE	MAXIMUM OUTPUT PRESSURE (PSIG)	CONTAMINANT IN OUTPUT	INFLOW (CFM/HP)	ECONOMIC RANGE (Inflow CFM)
RECIPROCATING Lubricated Non-lubricated	35,000 700	OIL NONE	4, to 7	10,000
DYNAMIC Centrifugal Axial	4,000 90	NONE NONE	4 4½	500 to 110,000 5,000 to 13,000,000
ROTARY VANE	125	OIL	4	150 to 6,000
ROTARY LOBE	30	NONE		50,000
ROTARY SCREW NON-LUBED/LUBED	125	NONE/ OIL	4	30 to 150
LIQUID RING	75*	WATER or other	1.6 to 2.2	20 to 5,000

\* Figure applies to a two-stage machine

FLOW OF COMPRESSED AIR:  
PRESSURE DROPS OVER 100 Ft PIPE,  
WITH AIR ENTERING AT 100 PSIG\*  
(Adapted from data published by Ingersoll-Rand)

TABLE 3.5

FREE AIR INFLOW (SCFM)	NOMINAL PIPE SIZE (INCHES) — SCHEDULE 40 PIPE							
	¾	1	1½	2	2½	3	4	6
40	1.24	0.37						
70	3.77	1.05	0.12					
90	6.00	1.69	0.19					
100	7.53	2.09	0.24					
400		32.2	3.59	0.98	0.41	0.13		
700			10.8	2.92	1.19	0.38	0.10	
900			17.9	4.78	1.97	0.62	0.15	
1,000			22.0	5.90	2.43	0.76	0.19	
4,000						11.9	2.90	0.35
7,000							8.77	1.06
9,000							14.6	1.75
10,000							18.0	2.13
40,000								33.8

\* Pressure drop varies inversely as absolute pressure of entering air.

#### POWER CONSUMPTION

The power consumption of the different compressor types is characteristic. Table 3.4 gives the horsepower needed at an output pressure of 100 PSIG. Power consumption per CFM rises with rising output pressure. Air cooling adds 3-5% to power consumption (including fan drive). 'FAD' power consumption figures for compressors of 'average' power consumption are given. 'FAD' denotes 'free air delivered corresponding to standard cubic ft per minute (SCFM) or liters per minute measured as set out in ASME PTC9, BS 1571 or DIN 1945.'

3 .2.1  
.2.2

TABLES  
3.3-3.5

# SPECIFIC POWER CONSUMPTION (FAD)

PSIG		50	75	100	125
HP per 100 CFM INFLOW	SINGLE-STAGE	14	18	22	24
	TWO-STAGE	13	16	18	21

## COOLING-WATER REQUIREMENTS

Cooling-water demand is normally shown on the vendor's P&ID or data sheet. Most of the water demand is for the aftercooler (and intercooler, with a two-stage compressor). Jackets and lube oil may also require cooling. As a guide, 8 US gallons per hour are needed for each horsepower supplied to the compressor. If the final compression is 100 PSIG, the water demand will usually be about 2 US GPH per each SCFM inflow. These approximate demands are based on an 40 F temperature increase of the cooling water. Demand for cooling water increases slightly with relative humidity of the incoming air.

## QUANTITIES OF MOISTURE CONDENSED FROM COMPRESSED AIR

The following calculation (taken from the referenced Atlas Copco manual) is for a two-stage compressor, and is based on moisture content given in the table below:

**DATA:** Capacity of the compressor = 2225 SCFM  
 Temperature of the incoming air = 86 F  
 Relative humidity of the incoming air = 75%

Intercooler { Outlet temperature = 86 F  
 Air pressure = 25.3 PSIG, or 40 PSIA  
 Water separation efficiency = 80%

Aftercooler { Outlet air temperature = 86 F  
 Air pressure = 100 PSIG, or 115 PSIA  
 Water separation efficiency = 90%

## CALCULATIONS:

- From the table, weight of water vapor in 2225 SCFM air at 86 F and 75% RH =  $(0.00189)(2225)(0.75) = 3.15$  lb/min.
- Rate of removal of condensed water from intercooler, thru trap =  $(0.8)[3.15 - (0.00189)(2225)(14.7)/(40)] = 1.28$  lb/min., or  $(1.28)(60)/(8.33) = 9.2$  US GPH
- Rate of removal of condensed water from aftercooler, thru trap =  $(0.9)[3.15 - 1.28 - (0.00189)(2225)(14.7)/(115)] = 1.20$  lb/min., or  $(1.20)(60)/(8.33) = 8.6$  US GPH
- Total rate at which water is removed from both coolers =  $9.2 + 8.6 = 17.8$  US GPH

## MOISTURE CONTENT OF AIR AT 100% RH

TEMPERATURE (Degrees F)	14	32	50	68	86	104	122
MOISTURE ( $10^{-4}$ lb/ft <sup>3</sup> )	1.35	3.02	5.87	10.9	18.9	31.6	51.3

## UNLOADING (POSITIVE-DISPLACEMENT COMPRESSORS)

'Unloading' is the removal of the compression load from the running compressor. Compressors are unloaded at startup and for short periods when demand for gas falls off. Damage to the compressor's drive motor can result if full compression duties are applied suddenly.

If the vendor does not provide means of unloading the compressor, a manual or automatic bypass line should be provided between suction and discharge (on the compressor's side of any isolating valves)—see figure 6.23.

Provision should be made so that the discharge pressure cannot rise above a value which would damage the compressor or its driver. Automatic unloading will ensure this, and the control actions are listed in table 3.6.

## AUTOMATIC UNLOADING ACTIONS FOR COMPRESSORS

TABLE 3.6

COMPRESSOR	DISCHARGE PRESSURE	AUTOMATIC CONTROL ACTION
Not running	Low—reaches lower set value	Starts compressor unloaded, accelerates to normal speed, and brings on load
Running	High—reaches higher set value	Unloads compressor for a preset period
Idling	Low—reaches reload pressure before idling period is over	Reloads compressor
	Medium—idling period ends before reload pressure is reached	Switches off compressor

## STORING COMPRESSED AIR

A limited amount of compressed air or other gas can be stored in receivers. One or more receivers provided in the compressor's discharge piping also serve to suppress surges (which can be due to demand, as well as supply) to assist cooling, and to collect moisture. Receivers storing air or other gas are classed as pressure vessels—refer to 6.5.1.

**RECEIVER CONSTRUCTION** Usual construction is a long vertical cylinder with dished heads, supported on a pad. Water will collect in the base, and therefor a valved drain must be provided for manual blowdown. Collected water may freeze in cold climates. Feeding the warm air or gas at the base of the receiver may prevent freezing, but the inlet must be designed so that it cannot be closed by water if it does freeze.

**CAPACITY NEEDED** A simple rule to decide the total receiver volume is to divide the compressor rating in SCFM by ten to get the volume in cubic feet for the receiver. For example, if the compressor is designed to take 5500 cubic feet per minute, a receiver volume of about 550 cubic feet is adequate. This rule is considered suitable for outflow pressures up to about 125 PSIG and where the continuously running compressor is unloaded by automatic valves—see 'Unloading' above. An extensive piping system for distributing compressed air or other gas may have a capacity sufficiently large in itself to serve as a receiver.

## PROCESS EQUIPMENT

3.3

Process equipment is a term used to cover the many types of equipment used to perform one or more of these basic operations on the process material:

- (1) CHEMICAL REACTION
- (2) MIXING
- (3) SEPARATION
- (4) CHANGE OF PARTICLE SIZE
- (5) HEAT TRANSFER

Equipment manufacturers give all information necessary for installation and piping.

This section is a quick reference to the function of some items of equipment used in process work. In table 3.7, the function of the equipment is expressed in terms of the phase (solid, liquid or gas) of the process materials mixed. Examples: (1) A blender can mix two powders, and its function is tabulated as "S+S". (2) An agitator can be used to stir a liquid into another liquid—this function is tabulated "L+L". Another large and varied group of equipment achieves separations, and a similar method of tabulating function is used in table 3.8.

### CHEMICAL REACTION

3.3.1

Chemical reactions are carried out in a wide variety of specialized equipment, termed reactors, autoclaves, furnaces, etc. Reactions involving liquids, suspensions, and sometimes gases, are often performed in 'reaction vessels'. The vessel and its contents frequently have to be heated or cooled, and piping to a jacket or internal system of coils has to be arranged. If reaction takes place under pressure, the vessel may need to comply with the ASME Boiler and Pressure Vessel Code. Refer also to 8.5.1, under 'Pressure vessels', and to the standards listed in table 7.13.

### MIXING

3.3.2

A variety of equipment is made for mixing operations. The principal types of equipment are listed in table 3.7:

#### MIXING EQUIPMENT

TABLE 3.7

EQUIPMENT	PHASES MIXED
AGITATOR	S + L, L + L
BLENDER (TUMBLER TYPE)	S + S, S + L
EDUCTOR	L + L, L + G, G + G
MIXER (RIBBON, SCROLL, OR OTHER TYPE)	S + S, S + L
PROPORTIONING PUMP	L + L
PROPORTIONING VALVE	L + L
(G = GAS, L = LIQUID, S = SOLID)	

## SEPARATION

3.3.3

Equipment for separation is even more varied. Equipment separating solids on the basis of particle size or specific gravity alone are in general termed classifiers. The broader range of separation equipment separates phases (solid, liquid, gas) and some of the types used are listed in the table below:

#### SEPARATION EQUIPMENT

TABLE 3.8

EQUIPMENT	FEED MATERIAL	RETAINED MATERIAL	OUTFLOW MATERIAL
CENTRIFUGE	S + L	S	L
CONTINUOUS CENTRIFUGE	L(1) + L(2)	None	L(1), L(2), †
CYCLONE	S + G	None	G, S †
DEAERATOR	L + G	L	G
DEFOAMER	L + G	L	G
DISTILLATION COLUMN	L(1) + L(2)	L(1)	L(2) *
DRYER	S + L	S	L *
DRY SCREEN	S(1) + S(2)	S(1)	S(2)
EVAPORATOR	L + S	L + S	L *
	L(1) + L(2)	L(1)	L(2) *
FILTER PRESS	S + L	S	L
FLOTATION TANK	S + L	S	L
FRACTIONATION COLUMN	L(1) + L(2) + L(3) + etc.	None	L(1), L(2), L(3), etc.†
SCRUBBER	S + G	S	G
SETTLING TANK	S + L	S	L
STRIPPER	L(1) + L(2)	L(1)	L(2)

| † Separate flows | | \* Removed as vapor | |
| (G = GAS, L = LIQUID, S = SOLID, S(1), S(2), L(1), L(2), etc. = DIFFERENT SOLIDS OR LIQUIDS) | | | |

### CHANGE OF PARTICLE SIZE

3.3.4

Reduction of particle size is a common operation, and can be termed 'attrition'. Equipment used includes crushers, rod-, ball- and hammer-mills, and—to achieve the finest reductions—energy mills, which run on compressed air. Emulsions ('creams' or 'milks'), which are liquid-in-liquid dispersions, are stabilized by homogenizers, typically used on milk to reduce the size of the fat globules and thus prevent cream from separating.

Occasionally, particle or lump size of the product is increased. Equipment for agglomerating, pelletizing, etc., is used. Examples: tablets, sugar cubes, powdered beverage and food products.

### PROCESS HEAT TRANSFER

3.3.5

Adding and removing heat is a significant part of chemical processing. Heating or cooling of process material is accomplished with heat exchangers, jacketed vessels, or other heat transfer equipment. The project and piping groups specify the duty and mechanical arrangement, but the detail design is normally left to the manufacturer.

3.2.2  
3.5

TABLES  
3.6-3.8

The term 'heat exchanger' in chemical processing refers to an unfired vessel exchanging heat between two fluids which are kept separated. The commonest form of heat exchanger is the 'shell-and-tube' exchanger, consisting of a bundle of tubes held inside a 'shell' (the vessel part). One fluid passes inside the tubes, the other thru the space between the tubes and shell. Exchanged heat has to flow thru the tube walls. Refer to 6.8 ('Keeping process material at the right temperature') and to 6.6 for piping shell-and-tube heat exchangers.

Heat exchange with process material can take place in a variety of other equipment, such as condensers, evaporators, heaters, chillers, etc.

#### **MULTIFUNCTION EQUIPMENT**

#### **3.3.6**

Sometimes, items of equipment are designed to perform more than one of the functions listed at the beginning of 3.3.

Mixing and heating (or cooling) may be simultaneously carried out in mixers having blades provided with internal channels to carry hot (or cold) fluid.

Separation and attrition may be achieved in a single mill, designed to output particles of the required degree of fineness and recycle and regrind particles which are still too coarse.

# ORGANIZATION:

4.1  
1.2

## JOB RESPONSIBILITIES, DRAWING-OFFICE EQUIPMENT & PROCEDURES

### THE PIPING GROUP

4.1

Plant design is divided into several areas, each the responsibility of a 'design group'. Chart 4.1(a) shows the main groups of people cooperating on the plant design, and the types of drawings for which they are responsible. Other groups, involved with instrumentation, stress analysis, pipesupport, etc., contribute to the design at appropriate stages.

The personnel responsible for the piping design may be part of an engineering department's mechanical design group, or they may function as a separate section or department. For simplicity, this design group is referred to as the 'piping group', and its relationship with the organization and basic activities are indicated in chart 4.1(a).

Chart 4.1(c) shows the structure of a design group.

### RESPONSIBILITIES OF THE PIPING GROUP

4.1.1

The piping group produces designs in the form of drawings and model(s), showing equipment and piping.

The following are provided by the piping group as its contribution to the plant design:—

- (1) AN EQUIPMENT ARRANGEMENT DRAWING, USUALLY TERMED THE 'PLOT PLAN'
- (2) PIPING DESIGN (DRAWINGS OR MODEL)
- (3) PIPING DETAILS FOR FABRICATION AND CONSTRUCTION
- (4) REQUISITIONS FOR PURCHASE OF PIPING MATERIEL

### JOB FUNCTIONS

4.1.2

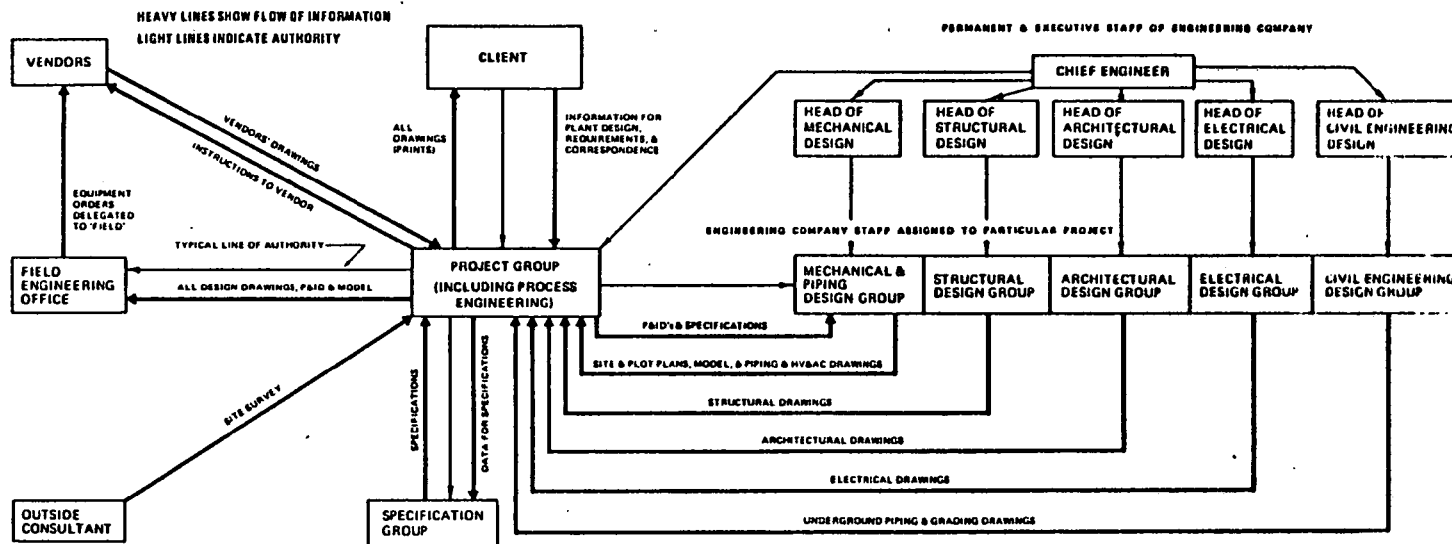
On joining a design office it is important that the new member knows what line of authority exists and to whom he is responsible. This is especially necessary when information is required and it saves the wrong people from being interrupted. Different companies will have different set-ups and different job titles. Chart 4.2 shows two typical lines of authority.

JOB	FUNCTIONS
<b>DESIGN SUPERVISOR</b>  <small>NOTE: The position of Chief Draftsman sometimes exists in large design Groups</small>	<ol style="list-style-type: none"><li>(1) RESPONSIBLE FOR ALL PERSONNEL IN GROUPS INCLUDING HIRING</li><li>(2) COORDINATING WITH OTHER GROUPS (AND THE CLIENT)</li><li>(3) OVERALL PLANNING AND SUPERVISING THE GROUP'S WORK</li><li>(4) LIAISON WITH PROJECT ENGINEER(S)</li></ol>
<b>GROUP LEADER</b>  <small>NOTE: On small projects, may also assume Design Supervisor's duties</small>	<ol style="list-style-type: none"><li>(1) SUPERVISING DESIGN &amp; DRAFTING IN AREA(S) ALLOCATED BY DESIGN SUPERVISOR</li><li>(2) ASSIGNING WORK TO DESIGNERS &amp; DRAFTSMEN</li><li>(3) RESPONSIBLE FOR PLOT PLANS, PLANT DESIGNS &amp; PRESENTATION &amp; COMPLETENESS OF FINISHED DRAWINGS</li><li>(4) COORDINATES MECHANICAL, STRUCTURAL, ELECTRICAL, AND CIVIL DETAILS FROM OTHER GROUPS</li><li>(5) CHECKING &amp; MARKING VENDORS' DRAWINGS</li><li>(6) OBTAINING INFORMATION FOR MEMBERS OF THE GROUP</li><li>(7) ESTABLISHING THE NUMBER OF DRAWINGS REQUIRED FOR EACH JOB (DRAWING CONTROL OR REGISTER)—SEE INDEX</li><li>(8) ASSIGNING TITLES FOR EACH DRAWING AND MAINTAINING UP-TO-DATE DRAWING CONTROL OR REGISTER OF DRAWINGS, CHARTS, GRAPHS, AND SKETCHES FOR EACH CURRENT PROJECT</li><li>(9) ESTABLISHING A DESIGN GROUP FILING SYSTEM FOR ALL INCOMING &amp; OUTGOING PAPERWORK</li><li>(10) KEEPING A CURRENT MANHOURLY SCHEDULE AND RECORD OF MANHOURS WORKED</li><li>(11) REQUISITIONING VIA PURCHASING DEPARTMENT ALL PIPING MATERIALS</li></ol>
<b>CHECKER</b>	<ol style="list-style-type: none"><li>(1) CHECKING DESIGNERS' AND DRAFTSMEN'S DESIGNS AND DETAILS FOR DIMENSIONAL ACCURACY AND CONFORMITY WITH SPECIFICATIONS, P&amp;ID's, VENDORS' DRAWINGS, ETC.</li><li>(2) IF AGREED WITH THE DESIGNER &amp;/OR GROUP LEADER, MAY MAKE IMPROVEMENTS AND ALTERATIONS TO THE DESIGN</li></ol>
<b>DESIGNER</b>	<ol style="list-style-type: none"><li>(1) PRODUCING STUDIES AND LAYOUTS OF EQUIPMENT AND PIPING WHICH MUST BE ECONOMIC, SAFE, OPERABLE AND EASILY MAINTAINED</li><li>(2) MAKING ANY NECESSARY ADDITIONAL CALCULATIONS FOR THE DESIGN</li><li>(3) SUPERVISING DRAFTSMEN</li></ol>
<b>DRAFTSMAN</b>	<p>MINIMUM RESPONSIBILITIES ARE:—</p> <ol style="list-style-type: none"><li>(1) PRODUCING DETAILED DRAWINGS FROM DESIGNERS' OR GROUP LEADERS' SCHEMES OR SKETCHES</li><li>(2) SECONDARY DESIGN WORK</li><li>(3) ACQUAINTING HIMSELF WITH THE RECORDS, FILES, INFORMATION SHEETS AND COMPANY PRACTICES RELATING TO THE PROJECT</li></ol>

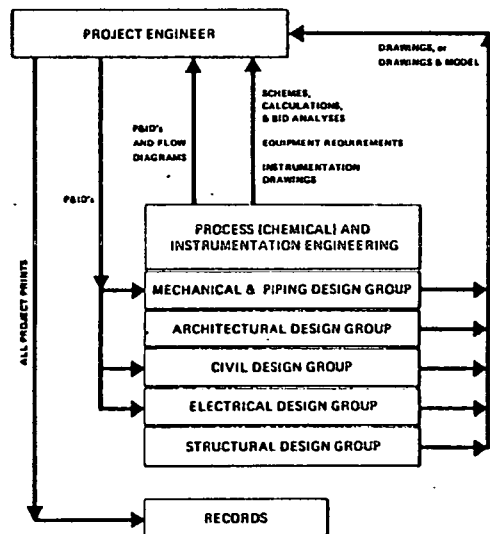
# OFFICE ORGANIZATION

## CHART 4.1

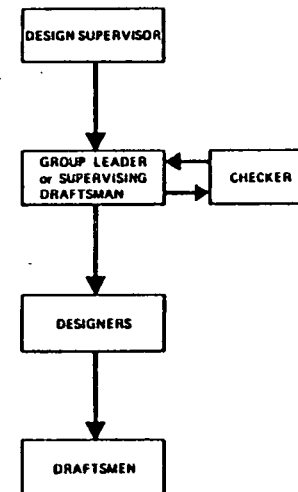
### (a) PROJECT ORGANIZATION



### (b) PROJECT & DESIGN GROUPS SHOWING FLOW OF INFORMATION



### (c) DESIGN GROUP SHOWING LINES OF AUTHORITY





The following information is required by the piping group:—

FROM THE PROJECT GROUP	(1)	'JOB SCOPE' DOCUMENT, WHICH DEFINES PROCEDURES TO BE USED IN PREPARING DESIGN SKETCHES AND DIAGRAMS
	(2)	PIPING & INSTRUMENTATION DIAGRAM (P&ID—SEE 5.2.4)
	(3)	LIST OF MAJOR EQUIPMENT (EQUIPMENT INDEX), SPECIAL EQUIPMENT AND MATERIALS OF FABRICATION
	(4)	LINE DESIGNATION SHEETS OR TABLES, INCLUDING ASSIGNATION OF LINE NUMBERS—SEE 4.2.3 AND 5.2.5
	(5)	SPECIFICATIONS FOR MATERIALS USED IN PIPING SYSTEMS—SEE 4.2.1
	(6)	SCHEDULE OF COMPLETION DATES (UPDATED ON FED-BACK INFORMATION)
	(7)	CONTROLS (METHODS OF WORKING, ETC.) TO BE ADOPTED FOR EXPEDITING THE JOB
FROM OTHER GROUPS	(8)	DRAWINGS—SEE 5.2.7
FROM SUPPLIERS	(9)	VENDORS' PRINTS—SEE 5.2.7

## SPECIFICATIONS

4.2.1

These consist of separate specifications for plant layout, piping materials, supporting, fabrication, insulation, welding, erection, painting and testing. The piping designer is mostly concerned with plant layout and material specifications, which detail the design requirements and materials for pipe, flanges, fittings, valves, etc., to be used for the particular project.

The piping materials specification usually has an index to the various services or processes. The part of the specification dealing with a particular service can be identified from the piping drawing line number or P&ID line number—see 5.2.4 under 'Flow lines'. All piping specifications must be strictly adhered to as they are compiled from information supplied by the project group. Although the fittings, etc., described in the Guide are those most frequently used, they will not necessarily be seen in every piping specification.

On some projects (such as 'revamp' work) where there is no specification, the designer may be responsible for selecting materials and hardware, and it is important to give sufficient information to specify the hardware in all essential details. Non-standard items are often listed by the item number and/or model specification for ordering taken from the catalog of the particular manufacturer.

## LIST OF EQUIPMENT, or EQUIPMENT INDEX

4.2.2

This shows, for each item of equipment, the equipment number, equipment title, and status—that is whether the item has been approved, ordered, and whether certified vendor's prints have been received.

These sheets contain tabulated data showing nominal pipe size, material specification, design and operating conditions. Line numbers are assigned in sequence of flow, and a separate sheet is prepared for each conveyed fluid—see 5.2.5.

## DRAWING CONTROL (REGISTER)

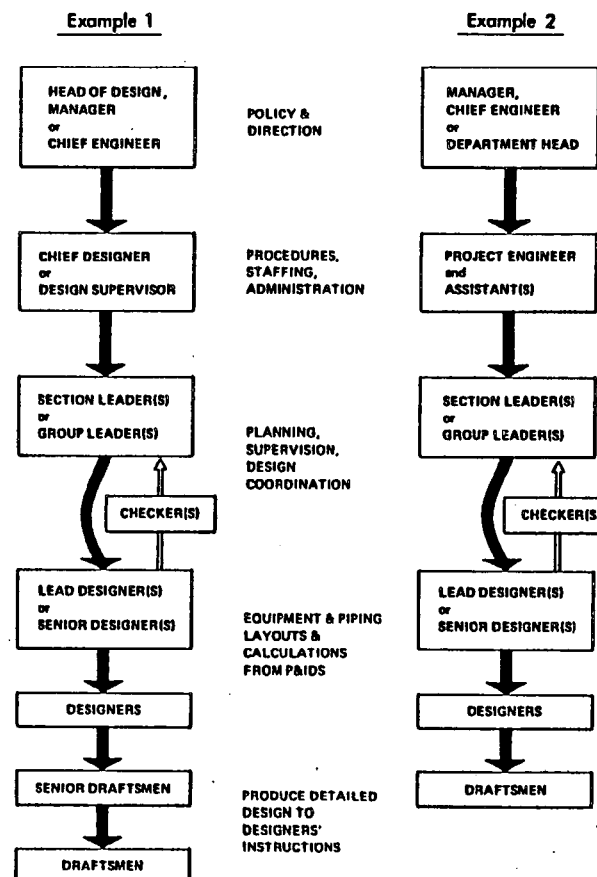
4.2.4

A drawing number relates the drawing to the project, and may be coded to show such information as project (or 'job') number, area of plant, and originating group (which may be indicated 'M' for mechanical, etc.). Figure 5.15 shows a number identifying part of a piping system.

The drawing control shows the drawing number, title, and progress toward completion. The status of revision and issues is shown—see 5.4.3. The drawing control is kept up-to-date by the group leader.

## DESIGN GROUP—TWO TYPICAL LINES OF AUTHORITY

CHART 4.2



CHARTS  
4.1 & 4.2

There are two types of drawings to file—those produced by the group and those received by the group. The former are filed in numerical order under plant or unit number in the drawing office on a 'stick file' or in a drawer—see 4.4.10. The filing of the latter, 'foreign', prints is often poorly done, causing time to be wasted and information to be lost. These prints are commonly filed by equipment index number, placing all information connected with that item of equipment in the one file.

A suggested method for filing these incoming prints is illustrated in chart 4.3, which cross-references process, function, or area with the group originating the drawing, and with associated vessels, equipment, etc. All correspondence between the project and design groups, client, vendors, and field would be filed under 'zero', as shown.

## MATERIALS & TOOLS FOR THE DRAFTING ROOM 4.4

### PAPER 4.4.1

**TRACING PAPER** is used for all drawings. It has to be translucent to the light used in copying machines (see below). The cheapest paper used is rag vellum. Linen is expensive but still used for important work, 'though largely supplanted by plastic film such as mylar, which is very durable. Papers can be supplied printed with border and title block and with a 'fade out' ruled grid on the reverse side. 'Isometric' sheets with fade out 30-degree grid are available for drawing isos.

Tracings must be carefully handled, avoiding crumpling, folding, punching, tearing and heavy erasing. If torn, the tear must be repaired with 'Magic tape' or equivalent—not with regular 'Scotch tape', which will show on prints.

ANSI Y14.1 defines the following drawing-sheet sizes (in inches): (A) 8½x11, or 9x12. (B) 11x17, or 12x18. (C) 17x22, or 18x24. (D) 22x34, or 24x36. (E) 34x44, or 36x48.

**PAPERS FOR COPYING MACHINES** Photosensitive paper is used for making prints for checking, issuing and filing purposes. 'Sepia' photocopying paper (Ozalid Company, etc.) gives brown positive prints which may be amended with pencil or ink, and the revision used as an original for photocopying in a diazo machine. Sepias may also be used to give a faint background print for drawing other work over, such as ducting or pipe supports. The quality of sepia prints is not good. Positive photocopies of superior quality are made on clear plastic film, which may have either continuous emulsion to give heavy copies, or screened emulsion to yield faint background prints (emulsion should preferably be water-removable).

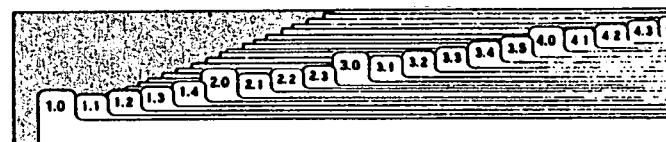
### LEADS & PENCILS 4.4.2

Pencil leads used in the drawing office are available in the following grades, beginning with the softest: B (used for shading), HB (usually used for writing only), F (usually softest grade used for drafting), H (grade most often used for drafting), 2H (used for drawing thinner lines such as dimension lines), 3H and 4H (used for faint lines for layout or background). Softer penciling is prone

UNIT OR AREA		0	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
UNIT OR AREA	CORRESPONDENCE																	
	MECHANICAL																	
	PIPING																	
	ELECTRICAL																	
	CIVIL																	
	STRUCTURAL																	
	ARCHITECTURAL																	
	INSTRUMENTATION																	
	PUMPS																	
	VESSELS																	
	TANKS																	
	EXCHANGERS																	
	CONDENSERS																	
	SEPARATORS																	
	CONVEYORS																	
1	COMPRESSED AIR																	
2	COOLING WATER																	
3	FLARESTACK																	
4	FUEL OIL																	
5	SOLVENTS																	
6	STEAM SYSTEM																	
7	VENTILATION - OFFICES																	
8	VENTILATION - PROCESS AREA																	
9																		
10																		

Paperwork classified according to a system of this type may be located in a filing cabinet fitted with numbered dividers as shown:—

STANDARD DIVIDERS FOR FILING CABINET



to smearing on handling. Grades harder than 3H tend to cut paper so that lines are difficult to erase. For plastic drafting films, special pencils are available and are better than HB and H leads for these films. Conventional leads are 2mm in diameter and require frequent repointing. 0.5mm and 0.3mm leads speed work, as they need no repointing. Flat leads, about 0.5mm x 2mm, are also available.

Clutch pencils (lead holders) which are commonly used, use metal chucks to grip the lead. Holders for the thinner 0.5mm and 0.3mm leads have a push-button advance.

### SCALES

### 4.4.3

The architect's scale is used for piping drawings, and is divided into fractions of an inch to one foot—for example, 3/8 inch per foot. The engineer's scale is used to draw site plans, etc., and is divided into one inch per stated number of feet, such as 1 inch per 30 feet.

Several types of eraser and erasing methods are available—use of each is given in table 4.1: Rubber in various hardnesses from pure gum rubber (artgum) for soft penciling and cleaning lead smears, to hard rubber for hard penciling and ink; 'plastic' is cleaner to use, as it has less tendency to absorb graphite; 'magic rub' for erasing pencil from plastic films. Most types of eraser are available for use with electric erasing machines.

An erasing shield is a thin metal plate with holes of various shapes and sizes so that parts of the drawing not to be erased may be protected.

ERASING GUIDE

TABLE 4.1

MATERIAL	MEDIUM	SOFT PENCIL	HARD PENCIL	INDIAN INK	PHOTOGRAPHIC BACKGROUND
TRACING PAPER, or LINEN		SRE, or artgum	HRE, or SRE	IHRE	—
SEPIA (OZALID), or PHOTOCOPY PAPER (PHOTOSTAT)		SRE	HRE, or SRE	Blade, or IHRE	Bleach *
PLASTIC FILM		Wet PE	Wet PE	Wet PE, or Blade	Wet PE, or Bleach*
KEY: E = eraser, SR = soft rubber, HR = hard rubber, I = Ink, P = plastic. Chemical bleach for removing black photographic silver deposit					

## CLEANING POWDER

4.4.5

Fine rubber granules are supplied in 'salt-shaker' drums. Sprinkled on a drawing, these granules reduce smearing of pencil lines during working. The use of cleaning powder is especially helpful when using a teesquare. The powder is brushed off after use.

## LETTERING AIDS

4.4.6

Title blocks, notes, and subtitles on drawings or sections should be in capitals. Capitals, either upright or sloped, are preferred. Pencilled lettering is normally used. Where ink work is required on drawings for photography, charts, reports, etc., ink stylus pens (Technos, Rapidograph, etc.) are available for stencil lettering (and for line drawing in place of ruling pens). The Leroy equipment is also used for inked lettering. Skeleton lettering templates are used for lettering section keys. The parallel line spacer is a small, inexpensive tool useful for ruling guide lines for lettering.

As alternatives to hand-inked lettering, special typewriters such as the Vari-typer can either print directly on the drawing or onto adhesive-backed transparent film which is later positioned on the drawing. Adhesive or transferable letters and numbers are available in sheets, and special patterns and panels can be supplied in order for title blocks or detailing, symbolism, abbreviations, special notes, etc. Self-adhesive tapes are somewhat limited in appli-

cation, but are useful for making drawings for photographic reproduction, such as panel boards, charts, and special reports—see 4.4.13, under 'Photographic layouts'.

## TEMPLATES

4.4.7

Templates having circular and rectangular openings are common. Orthogonal and isometric drafting templates are available for making process piping drawings and flow diagrams. These piping templates give the outlines for ANSI valves, flanges, fittings and pipe diameters to 3/8 inch per foot, or 1/4-inch per foot.

## MACHINES

4.4.8

The first two machines are usually used in drawing offices in place of the slower teesquare:

**DRAFTING MACHINE** Articulated rods allow parallel movement of a pair of rules set at right angles. The rules are set on a protractor, and their angle on the board may be altered. The protractor has 15-degree clickstops and vernier scale.

**PARALLEL RULE, or SLIDER**, permits drawing of long horizontal lines only, and is used with a fixed or adjustable triangle.

**PLANIMETER** A portable machine for measuring areas. When set to the scale of the drawing, the planimeter will measure areas of any shape.

**PANTOGRAPH** System of articulated rods permitting reduction or enlargement of a drawing by hand. Application is limited.

## LIGHT BOX

4.4.9

A light box has a translucent glass or plastic working surface fitted underneath with electric lights. The drawing to be traced is placed on the illuminated surface.

## FILING METHODS

4.4.10

Original drawings are best filed flat in shallow drawers. Prints filed in the drawing office are usually retained on a 'stick', which is a clamp for holding several sheets. Sticks are housed in a special rack or cabinet.

Original drawings will eventually create a storage problem, as it is inadvisable to scrap them. If these drawings are not sent to an archive, after a period of about three years they are photographed to a reduced scale for filing, and only the film is retained. Equipment is available for reading such films, or large photographic prints can be made.

4.3

CHART  
4.3TABLE  
4.1

'Diazo' or 'dye-line' processes reproduce to the same scale as the original drawing as a positive copy or print. Bruning and Ozalid machines are often employed. The drawing that is to be copied must be on tracing paper, linen or film, and the copy is made on light-sensitive papers or films. The older reversed-tone 'blue-print' is no longer in use.

#### SCALED PLANT MODELS

#### 4.4.12

Plant models are often used in designing large installations involving much piping. When design of the plant is completed, the model is sent to the site as the basis of construction in the place of orthographic drawings. Some engineering companies strongly advocate their use, which necessitates maintaining a model shop and retaining trained personnel. Scaled model piping components are available in a wide range of sizes. The following color coding may be used on models:—

PIPING . . . . .	YELLOW, RED or BLUE
EQUIPMENT . . . . .	GREY
INSTRUMENTS . . . . .	ORANGE
ELECTRICAL . . . . .	GREEN

#### ADVANTAGES

- Available routes for piping are easily seen
- Interferences are easily avoided
- Piping plan and elevation drawings can be eliminated; only the model, plot plan, P&ID's, and piping fabrication drawings (isos) are required
- The model can be photographed — see 4.4.13. 'Wire-and-disc' construction, where the disc shows pipe diameter, makes photographing easier.
- Provides a superior visual aid for conferences, for construction crews and for training plant personnel

#### DISADVANTAGES

- Duplication of the model is expensive
- The model is not easily portable and is liable to damage during transportation
- Changes are not recorded in the model itself

#### PHOTOGRAPHIC AIDS

#### 4.4.13

##### 'DRAWINGS' FROM THE MODEL

The lack of portability of a scaled plant model can be partially overcome by photographing it. To do this it must be designed so that it can be taken apart easily. Photographs can be made to correspond closely to the regular plan, elevation and isometric projections by photographing the model from 40 ft or more away with long focal length lenses—'vanishing points' (converging lines) in the picture are effectively eliminated.

The negative is projected through a contact screen and a print made on 'reproducible' film. Dimensions, notes, etc., are added to the reproducible film which can be printed by a diazo process—see 4.4.11. These prints are used as working drawings, and distributed to those needing information.

#### REVAMP WORK FOR EXISTING PLANTS

A polaroid camera can be used to supply views of the plant to the design office. Filed drawings of the plant do not always include alterations, and the photographs may show unrecorded changes.



Photographs of sections of a plant can be combined with drawings to facilitate installation of new equipment, or to make further changes to the existing plant. To do this, photographs are taken of the required views, using a camera fitted with a wide-angle lens (to obtain a wider view).

The negatives obtained are printed onto screened positive films which are attached to the back of a clear plastic drawing sheet. Alterations to the piping system are then drawn on the front face of this sheet, linking the photographs as desired. Reproductions of the composite drawing are made in the usual way by diazo process.

Alternately, positives may be marked directly for minor changes or instructions to the field.

#### PHOTOGRAPHIC LAYOUTS

The following technique produces equipment layout 'drawings', and is especially useful for areas where method study or investigational reports are required.

First, equipment outlines are produced to scale on photographic film, either in the regular way or by xerography. Next, a drawing-sized sheet of clear film is laid on a white backing sheet having a correctly-scaled grid marked on it.

The building outline and other features can be put onto the film using the variety of printed transparent tapes and decals available. The pieces of film with equipment outlines may then be positioned with clear tape, and any other parts of the 'drawing' completed. Alterations to the layout may be rapidly made with this technique, which photographs well for reports, and allows prints to be made in the usual ways for marking and comment. The film layout should be covered with an acetate or other protective sheet before insertion in a copying machine.

#### REDUCTION BY PHOTOGRAPHY

It is frequently required to include reproductions of diagrams and drawings in reports, etc. Photographic reduction to less than half-size (on lengths) is not recommended because normal-sized printing and details may not be legible. A graphic scale should be included on drawings to be reduced—see chart 5.8.

PROCESS & PIPING DRAWINGS  
(CONTENT, SYMBOLS, & DIMENSIONING)

PIPING SYMBOLS 5.1

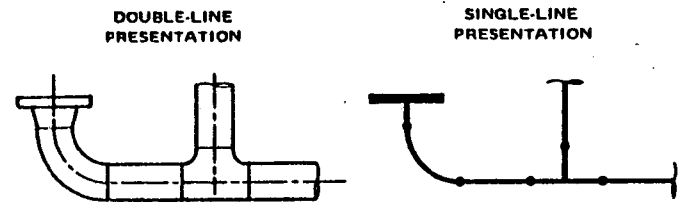
REFERENCE

'Dictionary of mechanical engineering abbreviations, signs & symbols'.  
Polon D. D. (Ed.) 1967 (Odessey)

SHOWING PIPE & JOINTS ON PIPING DRAWINGS 5.1.1

Most companies now represent piping (arrangements) by single lines. Pipe and flanges are sometimes drawn partially 'double line' to display clearances.

In double-line drawing, valves are shown by the symbols in chart 5.6 (refer to the panel 'Drafting valves'). Double-line representation is not used for entire piping arrangements, as it is very time-consuming, difficult to read, and not justified technically.



In presenting piping 'single line' on piping drawings, only the centerline of the pipe is drawn, using a solid line (see chart 5.1), and the line size is written. Flanges are shown as thick lines drawn to the scaled outside diameter of the flange. Valves are shown by special symbols drawn to scale. Pumps are shown by drawing the pads on which they rest, and their nozzles: figure 6.21 illustrates this simplified presentation. Equipment and vessels are shown by drawing their nozzles, outlines, and supporting pads.

If there is a piping specification, it is not necessary to indicate welded or screwed joints, except to remove ambiguities—for example, to differentiate between a tee and a stub-in. In most current practice, the symbols for screwed joints and socket welds are normally omitted, although butt welds are often shown.

The ways of showing joints set out in the standard ANSI Z32.2.3 (1949, re-affirmed 1953) are not current industrial practice. The standard's butt-weld symbol as shown in table 5.1 is now used to indicate a butt-weld to be made 'in the field' ('field weld'). The standard will be renumbered in the 'Y' series.

SHOWING NON-FLANGED JOINTS AT ELBOWS TABLE 5.1






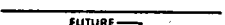
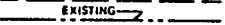





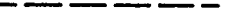


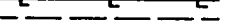



	BUTT WELD	SOCKET WELD	SCREWED JOINT
SIMPLIFIED PRACTICE *			
CONVENTIONAL PRACTICE			
ANSI Z32.2.3 (Not current practice)			

\*The joint symbol may be omitted if the type of joint is determined by a piping specification. It is usually preferred to use the dot weld symbol to make the type of construction clear: for example, to distinguish between a tee and a stub-in.

TABLE 5.1

## LINE SYMBOLS WHICH MAY BE USED ON ALL DRAWINGS 5.1.2

Chart 5.1 shows commonly accepted ways of drawing various lines. Many other line symbols have been devised but most of these are not readily recognized, and it is better to state in words the function of special lines, particularly on process flow diagrams and P&ID's. The designer or draftsman should use his current employer's symbols.

SYMBOLS FOR LINES	
CHART 5.1	
LINE SYMBOLS WHICH MAY BE USED ON P&ID's, PROCESS FLOW DIAGRAMS & PIPING DRAWINGS	
LINE	SYMBOL
<b>PIPING DRAWINGS (PLANS, ELEVATIONS, ISOs AND SPOOL DRAWINGS)</b> MATCHLINE OUTLINES OF BUILDINGS, UNITS, ETC. CENTERLINE SINGLE-LINE PIPING PIPING UNDERGROUND, OR OBSCURED BY EQUIPMENT, WALL, ETC. FUTURE PIPING EXISTING PIPING EQUIPMENT OUTLINES, DIMENSION LINES, DOUBLE-LINE PIPING FUTURE EQUIPMENT EXISTING EQUIPMENT	         
<b>P&amp;ID's AND PROCESS FLOW DIAGRAMS</b> PRIMARY PROCESS, SERVICE OR UTILITY PRIMARY PROCESS, SERVICE OR UTILITY, UNDERGROUND SECONDARY PROCESS, SERVICE OR UTILITY SECONDARY PROCESS, SERVICE OR UTILITY, UNDERGROUND	   
<b>SIGNAL (INSTRUMENT) LINES</b> INSTRUMENT AIR (PNEUMATIC SIGNAL) INSTRUMENT LIQUID (HYDRAULIC SIGNAL) ELECTRIC ELECTROMAGNETIC* OR SONIC INSTRUMENT CAPILLARY TUBING * RADIATION: LIGHT, HEAT, RADIO WAVE, ETC.	    

## VALVE & EQUIPMENT SYMBOLS FOR P&ID's & PROCESS FLOW DIAGRAMS 5.1.3

Practice in showing equipment is not uniform. Chart 5.2 is based on ANSI Y32.11-1961, and applies to P&ID's and process flow diagrams.

## REPRESENTING PIPING ON PIPING DRAWINGS 5.1.4

Charts 5.3-6 show symbols used in butt-welded, screwed and socket-welded systems. The various aspects of the fitting, valve, etc., are given. These symbols are based on conventional practice rather than the ANSI standard Z32.2.3, titled 'Graphic symbols for pipe fittings, valves and piping'.

## REPRESENTING VALVES ON PIPING DRAWINGS 5.1.5

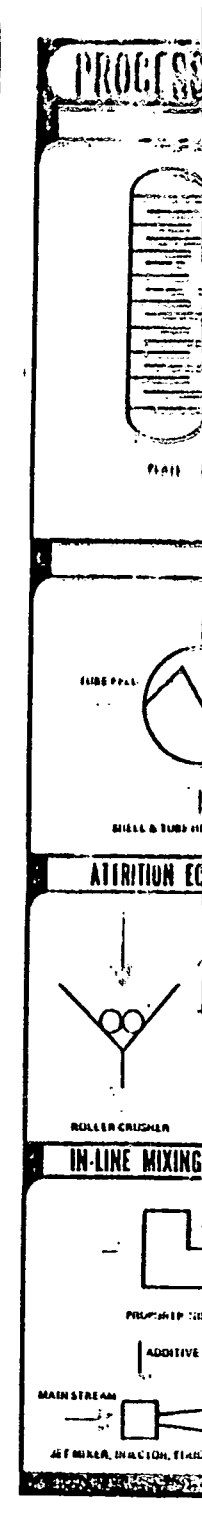
Chart 5.6 shows ways of denoting valves, including stems, handwheels and other operators. The symbols are based on ANSI Z32.2.3, but more valve types are covered and the presentation is up-dated. Valve handwheels should to be drawn to scale with valve stem shown fully extended.

## MISCELLANEOUS SYMBOLS FOR PIPING DRAWINGS 5.1.6

Symbols that are shown in a similar way in all systems are collected in chart 5.7.

## GENERAL ENGINEERING SYMBOLS 5.1.7

Chart 5.8 gives some symbols, signs, etc., which are used generally and are likely to be found or needed on piping drawings.

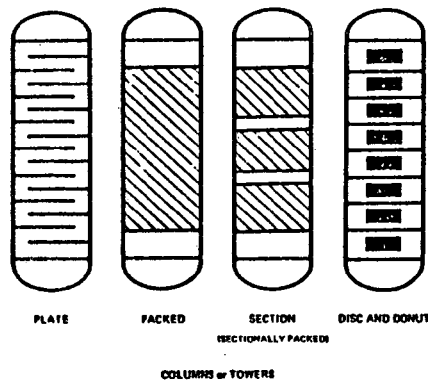


# PROCESS EQUIPMENT SYMBOLS

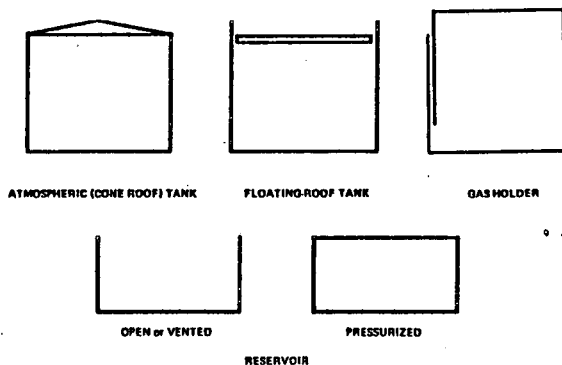
CHART 5.2A

5

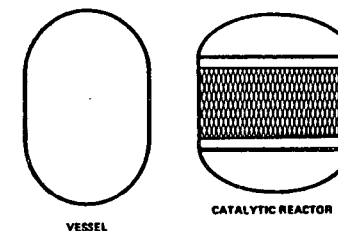
## COLUMNS



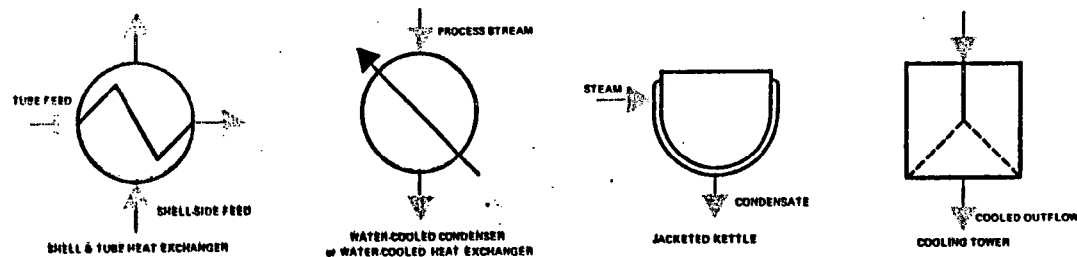
## TANKS & RESERVOIRS



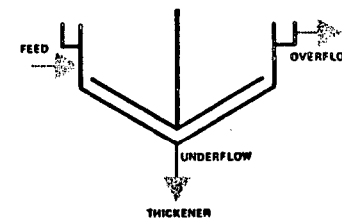
## VESSELS



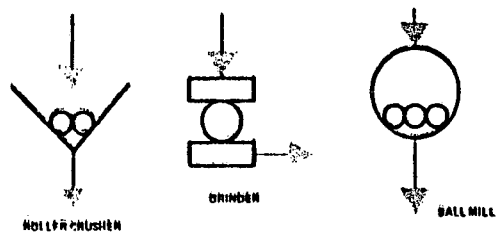
## HEAT-EXCHANGE EQUIPMENT



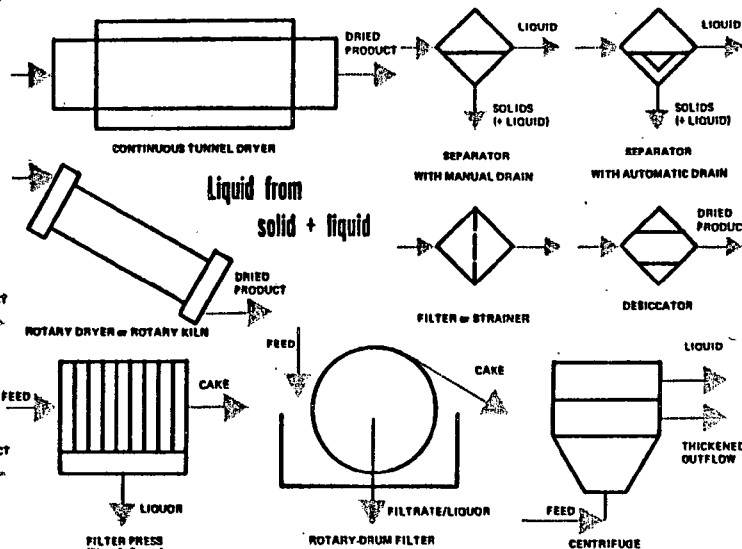
## THICKENER or CLARIFIER



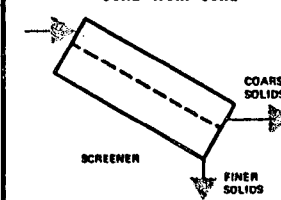
## ATTRITION EQUIPMENT (Mills, grinders, etc.)



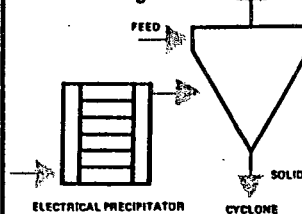
## SEPARATION EQUIPMENT



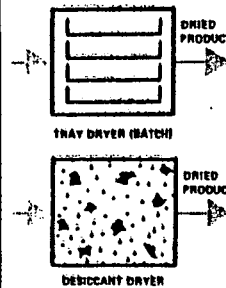
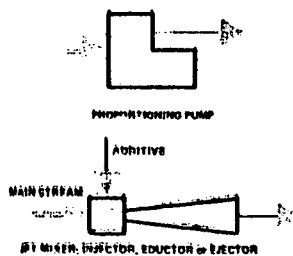
## Solid from solid



## Solid from solid + gas



## IN-LINE MIXING EQUIPMENT



CHARTS  
5.1 & 5.2A

# PROCESS EQUIPMENT SYMBOLS

CHART 6.2B

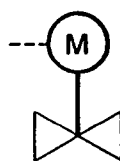
## VALVES



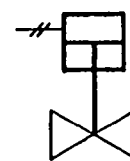
### VALVES (GENERAL)

Special types of valve may be indicated by the symbols given in chart 6.8

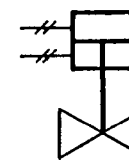
## VALVE OPERATORS (ISA 55.1)



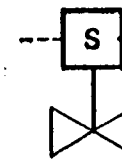
ROTARY MOTOR  
(Electric Signal)



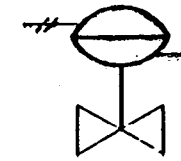
SINGLE-ACTING  
CYLINDER



DOUBLE-ACTING  
CYLINDER

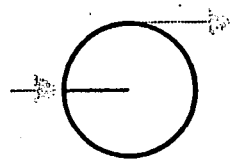


SOLENOID

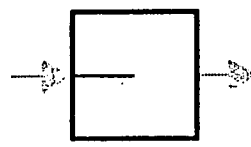


DIAPHRAGM  
(Pressure-Balanced)

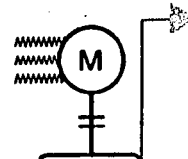
## PUMPS, COMPRESSOR, BLOWER, & FAN



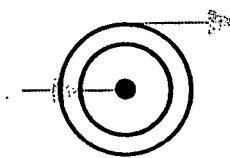
CENTRIFUGAL PUMP



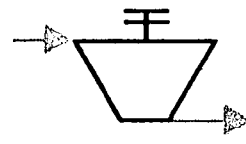
RECIPROCATING PUMP



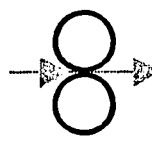
SUMP PUMP & MOTOR



BLOWER or FAN

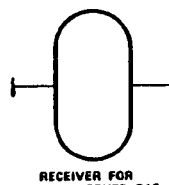


TURBINE COMPRESSOR



ROTARY PUMP

## RECEIVER



RECEIVER FOR  
AIR or OTHER GAS

## DRAIN

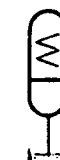


VISIBLE DRAIN

## ACCUMULATORS



GENERAL  
SYMBOL



SPRING-LOADED  
TYPE



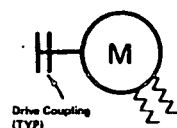
GAS-CHARGED  
TYPE



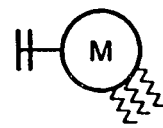
WEIGHTED  
TYPE

THESE SYMBOLS CAN BE USED FOR HYDRAULIC OR PNEUMATIC ACCUMULATORS USED TO SMOOTH THE PULSATING OUTPUT FROM PUMPS AND COMPRESSORS OR TO ACT AS RESERVOIRS FOR VARIABLE DEMANDS

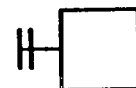
## DRIVERS



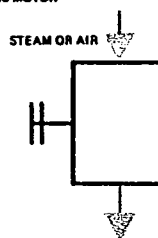
2-PHASE ELECTRIC MOTOR



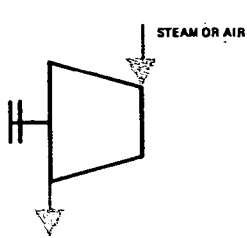
3-PHASE ELECTRIC MOTOR



ENGINE DRIVER

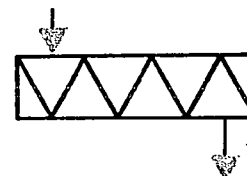


STEAM or AIR-PISTON DRIVER



TURBINE DRIVER

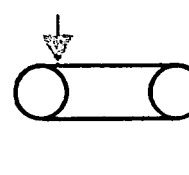
## CONVEYORS



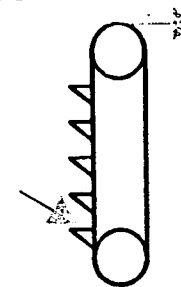
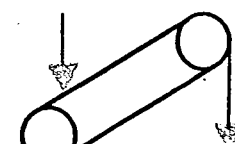
SCREW CONVEYOR



ROLLER CONVEYOR



BELTS or SHAKERS



BUCKET or FLIGHT CONVEYOR

SYMBOL

NAME OF ITEM

UNION (Gate Valve)

PIPE WELD

BLIND FLANGE

CAP

COUPLING,  
FULL or HALF

ELBOW

ELBOW, 90°, LR

ELBOW, 90°, SR

ELBOW, 45°

TEE

EXPANDER FLANGE

FIELD WELD

FULL COUPLING  
HALF COUPLING

NOSE

PIPE COUPLING



## SYMBOLS FOR BUTT-WELDED SYSTEMS

## CHART 5.3

## NOTE

IN CHARTS 5.3 THRU 5.5, THE SYMBOL IS SHOWN IN HEAVY LINE. LIGHTER LINES SHOW CONNECTED PIPE, AND ARE NOT A PART OF THE SYMBOL.

NAME OF ITEM	END VIEW	SIDE VIEW	END VIEW	NAME OF ITEM	END VIEW	SIDE VIEW	END VIEW	NAME OF ITEM	END VIEW	SIDE VIEW	END VIEW
BEND (State Radius)				LAP JOINT FLANGE & STUB				RETURN			
BUTT WELD				LATERAL				SOCKET	SHOW AS 'WELDOLET'—THIS CHART		
BLIND FLANGE				LATROLET				SLIP-ON FLANGE			
CAP				MITER	SEE END OF THIS CHART			STUB-IN			
COUPLING, FULL or HALF				NIPOLET				SWAGE, CONCENTRIC	TOP VIEW 		
CROSS				PIPE				ECCENTRIC STATE WHETHER TOP OR BOTTOM IS 'FLAT'			
ELBOW, 90°, LN				REDUCER, CONCENTRIC	TOP VIEW 			SWEETPOLET			
ELBOW, 90°, BR				ECCENTRIC STATE WHETHER TOP OR BOTTOM IS 'FLAT'				THREDOLET	SHOW AS 'WELDOLET'—THIS CHART		
ELBOW, 45°				REDUCING FLANGE				TEE			
FLROLET			TOP VIEW 	REDUCING ELBOW				WELDING-NECK FLANGE			
EXPANDER FLANGE				REINFORCEMENTS				WELDOLET			
FIELD WELD				SADDLE				2-PIECE MITER			
FULL COUPLING	SEE 'COUPLING' THIS CHART			WRAPAROUND SADDLE				3-PIECE MITER			
HALF COUPLING											
HOSE											
HOSE COUPLING											

# SYMBOLS FOR SCREWED SYSTEMS

CHART 5.4

NAME OF ITEM	END VIEW	SIDE VIEW	END VIEW
CAP			
COUPLING, FULL- & HALF-	SHOW FOR BRANCH CONNECTIONS ONLY—SEE 'COUPLING' IN CHART 5.3		
CROSS			
ELBOW, 90°			
ELBOW, 45°			
FLANGE			
HOSE			
HOSE CONNECTION			
PIPE			
PLUG			
REDUCER			
RETURN <small>Only malleable-iron and cast-iron returns are available. For forged-steel systems, combine forged-steel elbows.</small>			
SEAL WELD	SHOW BY NOTING 'SEAL WELD'		
SWAGE, CONCENTRIC	TOP VIEW		
ECCENTRIC <small>STATE WHETHER TOP OR BOTTOM IS 'FLAT'</small>			
TEE, STRAIGHT or REDUCING			
THREDOLET	SHOW AS 'WELDOLET'—CHART 5.3		
UNION			

# SYMBOLS FOR SOCKET-WELDED SYSTEMS

CHART 5.5

NAME OF ITEM	END VIEW	SIDE VIEW	END VIEW
CAP			
COUPLING, FULL- & HALF-	SHOW FOR BRANCH CONNECTIONS ONLY—SEE 'COUPLING' IN CHART 5.3		
CROSS			
ELBOLET	SEE 'ELBOLET'—CHART 5.3		
ELBOW, 90°			
ELBOW, 45°			
FLANGE			
HOSE			
PIPE			
REDUCER,			
RETURN	NO SOCKET-WELDING FORGED-STEEL FITTING IS AVAILABLE. IF A 180-DEGREE RETURN IS REQUIRED, IT MAY BE MADE USING A BUTT-WELDING RETURN, OR TWO SOCKET-WELDING ELBOWS WITH NIPPLE BETWEEN.		
SOCKOLET	SHOW AS 'WELDOLET'—CHART 5.3		
SWAGE, CONCENTRIC	TOP VIEW		
ECCENTRIC <small>STATE WHETHER TOP OR BOTTOM IS 'FLAT'</small>			
TEE, STRAIGHT or REDUCING			
UNION			

# DRAFTING VALVES

CHART 5.6 GIVES THE BASIC SYMBOLS FOR VALVES. THESE BASIC SYMBOLS ARE USED OR ADAPTED AS FOLLOWS:

## P & I D's

USE THE RELEVANT VALVE SYMBOL TO SHOW THE TYPE OF VALVE. DRAW MOST SYMBOLS 1/4 IN. LONG. MANUAL OPERATIONS ARE NOT SHOWN.

## PIPING DRAWINGS

OPERATOR IS SHOWN IF IMPORTANT

### (1) SCREWED VALVES

USE THE BASIC VALVE SYMBOL. DRAW THE LENGTH OF THE VALVE TO SCALE.

### (2) SOCKET-ENDED VALVES

IF THE PROJECT HAS A PIPING SPECIFICATION, USE THE BASIC VALVE SYMBOL. IF NOT, SHOW SOCKET ENDS TO THE VALVES:

VALVE WITH:	Sockets both ends	Sockets one end, other end flange
SYMBOL EXAMPLE		

DRAW THE LENGTH OF THE BASIC VALVE SYMBOL TO SCALE OVER SOCKET ENDS.

### (3) FLANGED VALVES

USE THE BASIC VALVE SYMBOL, WITH OPERATOR, AND SHOW MATING FLANGES AS DETAILED BELOW:

SINGLE-LINE	DOUBLE-LINE
<b>1. Drawing the symbol</b> 	
<b>2. Dimensioning nonstandard valves</b> Refer to 5.3.3, under 'Dimensioning to valves' 	

(d) Draw this length to scale (overall length of valve without gasket) but place arrowheads on the drawing as shown. This convention ensures that:  
 (1) The line will be made to the correct length.  
 (2) The fabricator will be reminded to allow for gaskets.

# SYMBOLS FOR VALVES AND VALVE OPERATORS

## CHART 5.6

TYPE OF VALVE	SIDE VIEW	TOP VIEW	TYPE OF VALVE	SIDE VIEW	TOP VIEW	TYPE OF VALVE	SIDE VIEW	TOP VIEW		
ANGLE COCK			(a) LINE-BLIND VALVE (Using spectacle plate) (b) LINE BLIND (Shown between flanges)	(a)	(b)	VACUUM BREAKER (or Breather)				
BALL, ROTARY			NEEDLE			WYE-PATTERN GLOBE				
BUTTERFLY			PINCH	USE 'SQUEEZE VALVE' SYMBOL		3-WAY				
CHECK (SWING) <i>Position of dot here shows flow from left to right</i>			PLUG			4-WAY				
COCK	SEE 'PLUG VALVE'		'QUICK OPENING'			OPERATOR	SIDE VIEW	END VIEW	TOP VIEW	
CONTROL				RELIEF			SPUR GEAR			
DIAPHRAGM				SAFETY			BEVEL GEAR			
FLUSH-BOTTOM TANK VALVE			SAFETY-RELIEF			CHAIN WHEEL				
GATE			STOP CHECK			CHAIN WRENCH				
GLOBE			SQUEEZE							
			TRAP							

THIS CHART GIVES THE BASIC VALVE SYMBOL WHICH IS USED ON P&ID's AND FLOW DIAGRAMS.  
ADAPTATION OF THE SYMBOLS TO PIPING DRAWINGS IS EXPLAINED ON THE FACING PAGE.

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THIS CHART GIVES THE BASIC VALVE SYMBOL WHICH IS USED ON P&ID'S AND FLOW DIAGRAMS.  
ADAPTATION OF THE SYMBOLS TO PIPING DRAWINGS IS EXPLAINED ON THE FACING PAGE.

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CHARTS  
5.4-5.6

# MISCELLANEOUS SYMBOLS FOR PIPING DRAWINGS

CHART 6.7

NAME OF ITEM	SYMBOL	NAME OF ITEM	SYMBOL	NAME OF ITEM	SYMBOL
BLEED RING		JACKETED PIPE WITH INSULATION		TRAP	
CONTROL STATION (in Plan View)		ORIFICE FLANGE ASSEMBLY		VENT (for line)	
DRAIN or HUB (in floor)		PERSONNEL PROTECTION (Protective use of insulation)		VENT FOR TANK	
DRAIN (for line)		QUICK CONNECTORS		<b>PIPE SUPPORT SYMBOLS</b>	
EDUCTOR		REMOVABLE SPOOL		SUPPORT	SYMBOL
EJECTOR		RUPTURE DISC		ANCHOR	
ELECTRIC TRACING		SCREEN Conical, Mounted between Flanges		GUIDE	
EXHAUST HEAD (for steam)		SCREEN Flat, Mounted between Flanges		SHOE	
EXPANSION JOINT		STEAM TRACING		HANGER	
FLAME ARRESTOR		STRAINER, WYE TYPE		SPRING HANGER	
FLEXIBLE COUPLING				FLOOR SUPPORT	
HOSE				SPRING SUPPORT	
INSULATION					

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# GENERAL SYMBOLS FOR ENGINEERING DRAWINGS

CHART 5.8

5

SYMBOL	DESCRIPTION	SYMBOL	DESCRIPTION
	<p>NORTH ARROWS.</p> <p>(1) FOR PLANS AND ELEVATIONS</p> <p>(2) FOR ISOMETRIC DRAWINGS</p>		<p>'CONSTRUCTION HOLD' MARKING. IF SUFFICIENT INFORMATION IS NOT AVAILABLE TO FINALIZE PART OF THE DESIGN, THE 'HOLD' MARKING IS USED TO INSTRUCT THE CONTRACTOR TO AWAIT A LATER REVISION OF THE DRAWING BEFORE STARTING THE WORK IN QUESTION</p>
	<p>GRAPHIC SCALE REQUIRED ON DRAWINGS LIKELY TO BE CHANGED IN SIZE PHOTOGRAPHICALLY FOR REPORTS, etc.</p>		<p>REVISION TRIANGLE. THE LATEST REVISION NUMBER OF THE DRAWING IS SHOWN WITHIN THE TRIANGLE WHICH IS ENCIRCLED ON THE REAR OF THE SHEET. ALL REVISION TRIANGLES REMAIN ON THE DRAWING, BUT ENCIRCLED OF THE PREVIOUS TRIANGLE IS ERASED</p>
	<p>SYMBOL LOCATING AXES OF REFERENCE: INTERSECTION OF ORDINATES (COORDINATE POINT)</p>		<p>OPENINGS.</p> <p>(1) OPENING WHICH MAY BE COVERED. (ARCH. AND H&amp;V DRAWINGS)</p> <p>(2) HOLE. (ARCH.)</p>
	<p>TYPICAL SECTION INDICATORS. LETTERS 'I' AND 'O' SHOULD NOT BE USED TO AVOID CONFUSION WITH NUMERALS '1' AND '0'. IF MORE THAN 24 SECTIONS ARE NEEDED, USE COMBINATIONS OF LETTERS AND NUMERALS. SHOW NUMBER OF THE DRAWING ON WHICH SECTION WILL APPEAR</p>		<p>STRUCTURAL STEEL SECTIONS:</p> <p>(1) ANGLE. (2) CHANNEL. (3) I-BEAM</p>
	<p>CENTERLINE SYMBOL</p>		<p>ELEVATION SYMBOLS FOR RAILING</p>
	<p>DIMENSION LINE SYMBOL USED TO SHOW A DIMENSION NOT TO SCALE</p>		<p>DISCONTINUED VIEWS:</p> <p>(1) PIPE, ROUND SHAFT, etc.</p> <p>(2) SLAB, SQUARE BAR, etc.</p> <p>(3) VESSEL, EQUIPMENT, etc.</p> <p>(Also used to terminate drawing)</p>
	<p>'FITTING MAKEUP' SYMBOL (NOT PREFERRED - SEE 5.3.3, UNDER 'FITTING MAKEUP')</p>		<p>SCREWTHREAD SYMBOLS</p>
	<p>INSTRUMENT BALLOON, USUALLY DRAWN 7/16-INCH DIAMETER ON P&amp;ID's AND PIPING DRAWINGS (TO 3/8 IN. PER FT SCALE)</p>		<p>CHAIN SYMBOL</p>

CHARTS  
5.7 & 5.8

SHADINGS		THESE SHADINGS ARE USED FOR SHOWING MATERIALS AND SECTIONS OF SOLIDS					
GRADE or EARTH	SOLID MATERIAL (and pipe cross section)	STEEL	CONCRETE	BRICK & STONE MASONRY	WOOD	CHECKER PLATE (Use 30° lines)	GRATING

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# WELDING SYMBOLS (AMERICAN WELDING SOCIETY)

REPRODUCED WITH PERMISSION OF  
THE AMERICAN WELDING SOCIETY

CHART 5.9

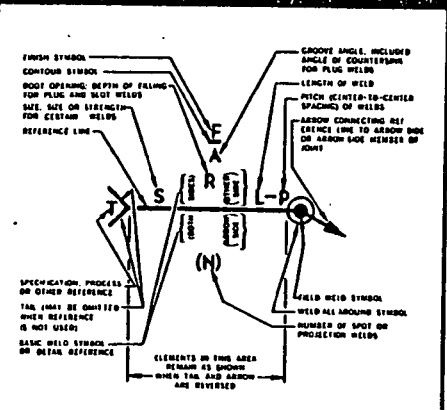
## Basic Weld Symbols and Their Location Significance

LOCATION SIGNIFICANCE	FILLET	PLUG OR SLOT	SPOT OR PROJECTION	SEAM	FLASH OR SURFACE	GROOVE	BACK OR BAKING	SURFACING	FLANGE	ARC BEAM OR ART SPOT	WELDABLE SPOT	PROJECTION	WELDABLE SPOT	FLASH OR SURFACE
ARROW SIDE														
OTHER SIDE														
BOTH SIDES														
NO "ARROW SIDE" OR "OTHER SIDE" SIGNIFICANCE														

## Supplementary Symbols

WELD ALL AROUND	FIELD WELD	MELT-THRU	CONTOUR
			FLUSH CONVEX CONCAVE

## Location of Elements of a Welding Symbol



## Typical Welding Symbols

<b>BACK OR BAKING WELD SYMBOL</b>  NOT APPLICABLE SINGLE GROOVE WELD SYMBOL	<b>SINGLE-V-GROOVE WELDING SYMBOL INDICATING ROOT PENETRATION</b>  DEPTH OF CHAMFERING PLUS ROOT PENETRATION, GROOVE ANGLE	<b>PROJECTION WELDING SYMBOL</b>  DEPTH OF PROJECTION, PROJECTION WELDING SYMBOL
<b>SURFACING WELD SYMBOL INDICATING BUILT-UP SURFACE</b>  SIZE (HEIGHT OF DEPOSIT), SURFACING INDICATES NO SPECIFIC HEIGHT SHOWN	<b>DOUBLE-BEVEL-GROOVE WELDING SYMBOL</b>  DIVISION OF SIZE INDICATOR INDICATES A TOTAL DEPTH OF CHAMFERING (EQUAL TO THEORETICAL BEVELS)	<b>SEAM WELDING SYMBOL</b>  LENGTH OF WELD, SEAM WELDING SYMBOL
<b>DOUBLE FILLET WELDING SYMBOL</b>  SIZE (LENGTH OF LEG), SPECIFICATION, PROCESS OR OTHER REFERENCE	<b>WELDING SYMBOLS FOR COMBINED WELDS</b>  PITCH (DISTANCE BETWEEN CENTERS OF WELDS), DEPTH OF FILLING IN INCLUDED ANGLE OF CONTOURING, SURFACING INDICATES FILLING IS COMPLETE	<b>FLASH OR UPSET WELDING SYMBOL</b>  FLASH OR UPSET WELDING SYMBOL
<b>CHAIN INTERMITTENT FILLET-WELDING SYMBOL</b>  SIZE (LENGTH OF LEG), PITCH (DISTANCE BETWEEN CENTERS OF INCREMENTS)	<b>PLUG WELDING SYMBOL</b>  PITCH (DISTANCE BETWEEN CENTERS OF WELDS), DEPTH OF FILLING IN INCLUDED ANGLE OF CONTOURING, SURFACING INDICATES FILLING IS COMPLETE	<b>SQUARE-GROOVE WELDING SYMBOL</b>  DIVISION OF SIZE INDICATOR INDICATES A TOTAL DEPTH OF CHAMFERING (EQUAL TO THEORETICAL BEVELS)
<b>STAGGERED INTERMITTENT FILLET-WELDING SYMBOL</b>  SIZE (LENGTH OF LEG), PITCH (DISTANCE BETWEEN CENTERS OF INCREMENTS), LENGTH OF INCREMENTS	<b>SLOT WELDING SYMBOL</b>  DEPTH OF FILLING IN INCLUDED ANGLE OF CONTOURING, SURFACING INDICATES FILLING IS COMPLETE	<b>FLARE-V-GROOVE AND FLARE-BEVEL GROOVE WELDING SYMBOLS</b>  DEPTH OF CHAMFERING PLUS ROOT PENETRATION, GROOVE ANGLE
<b>SINGLE-V-GROOVE WELDING SYMBOL</b>  SIZE (DEPTH OF CHAMFERING), DIVISION INDICATES DEPTH OF CHAMFERING (EQUAL TO THEORETICAL BEVELS), ROOT OPENING, GROOVE ANGLE	<b>SPOT WELDING SYMBOL</b>  PITCH (DISTANCE BETWEEN CENTERS OF WELDS), DEPTH OF FILLING IN INCLUDED ANGLE OF CONTOURING, SURFACING INDICATES FILLING IS COMPLETE	<b>EDGE-FLANGE AND CORNER-FLANGE WELDING SYMBOLS</b>  DEPTH OF CHAMFERING PLUS ROOT PENETRATION, GROOVE ANGLE

## Supplementary Symbols Used with Welding Symbols

<b>WELD-ALL-AROUND SYMBOL</b>  WELD ALL AROUND SYMBOL INDICATES THAT WELD EXTENDS COMPLETELY AROUND THE JOINT	<b>FIELD WELD SYMBOL</b>  FIELD WELD SYMBOL INDICATES THAT WELD IS TO BE MADE AT A PLACE OTHER THAN THAT OF INITIAL CONSTRUCTION	<b>MELT-THRU SYMBOL</b>  MELT-THRU SYMBOL IS NOT DIMENSIONED (EXCEPT HEIGHT)	<b>FLUSH CONTOUR SYMBOL</b>  FLUSH CONTOUR SYMBOL INDICATES FACE OF WELD TO BE MADE FLUSH WITH SURFACING INDICATES WELD TO BE SPILLED FLUSH WITHOUT SUBSEQUENT FINISHING	<b>CONVEX CONTOUR SYMBOL</b>  CONTOUR SYMBOL INDICATES FACE OF WELD TO BE FINISHED TO CONTOUR SHOWN
---	--	--	--	---

## Basic Joints—Identification of Arrow Side and Other Side of Joint and Arrow-Side and Other-Side Member of Joint

<b>BUTT JOINT</b>  ARROW SIDE OF JOINT, OTHER SIDE OF JOINT	<b>CORNER JOINT</b>  ARROW SIDE OF JOINT, OTHER SIDE OF JOINT	<b>TEE JOINT</b>  ARROW SIDE OF JOINT, OTHER SIDE OF JOINT	<b>LAP JOINT</b>  ARROW SIDE OF JOINT, OTHER SIDE OF JOINT	<b>EDGE JOINT</b>  ARROW SIDE OF JOINT, OTHER SIDE OF JOINT
---	---	--	--	---

## DESIGNATION OF WELDING PROCESSES BY LETTERS

CMA Carbon Arc Welding CW Cold Chisel D Diffusion Welding E Electroslag Welding F Fusion Welding G Gas Welding H Hot Chisel I Induction Welding J Jet Welding K Laser Beam Welding L Laser Beam Welding M Microwave Welding N Non-Fusion Welding O Other Welding P Plasma Arc Welding Q Quenching R Resistance Welding S Seam Welding T Thermal Welding U Ultrasonic Welding V Vacuum Welding W Wire Arc Welding X X-ray Welding Y Y-joint Welding Z Zonal Welding	CA Cold Chisel CW Cold Chisel D Diffusion E Electroslag F Fusion G Gas H Hot Chisel I Induction J Jet K Laser Beam L Laser Beam M Microwave N Non-Fusion O Other P Plasma Arc Q Quenching R Resistance S Seam T Thermal U Ultrasonic V Vacuum W Wire Arc X X-ray Y Y-joint Z Zonal
--	--

## DESIGNATION OF CUTTING PROCESSES BY LETTERS

A Air Carbon Arc Cutting B Burn C Cold Chisel D Diffusion E Electroslag F Fusion G Gas H Hot Chisel I Induction J Jet K Laser Beam L Laser Beam M Microwave N Non-Fusion O Other P Plasma Arc Q Quenching R Resistance S Seam T Thermal U Ultrasonic V Vacuum W Wire Arc X X-ray Y Y-joint Z Zonal	A Air Carbon Arc B Burn C Cold Chisel D Diffusion E Electroslag F Fusion G Gas H Hot Chisel I Induction J Jet K Laser Beam L Laser Beam M Microwave N Non-Fusion O Other P Plasma Arc Q Quenching R Resistance S Seam T Thermal U Ultrasonic V Vacuum W Wire Arc X X-ray Y Y-joint Z Zonal
---	---

NONPREFERRED SYMBOLS;  
USE PREFERRED SYMBOL WITH PROCESS REFERENCE IN THE TAIL

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AWS A 11.10

## SYMBOLS FOR WELDING DETAILS

5.1.8

Standard welding symbols are published by the American Welding Society. These symbols should be used as necessary on details of attachments, vessels, piping supports, etc. The practice of writing on drawings instructions such as 'TO BE WELDED THROUGHOUT', or 'TO BE COMPLETELY WELDED' transfers the design responsibility for all attachments and connections from the designer to the welder, which the Society considers to be a dangerous and uneconomic practice.

The 'welding symbol' devised by the American Welding Society has eight elements. Not all of these elements are necessarily needed by piping designers. The assembled welding symbol which gives the welder all the necessary instruction, and locations of its elements, is shown in chart 5.9. The elements are:

- REFERENCE LINE
- ARROW
- BASIC WELD SYMBOLS
- DIMENSIONS & OTHER DATA
- SUPPLEMENTARY SYMBOLS
- FINISH SYMBOLS
- TAIL
- SPECIFICATIONS, PROCESS or OTHER REFERENCE

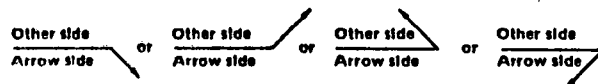
The following is a quick guide to the scheme. Full current details will be found in the 1968 revision of 'Standard Welding Symbols' available from the American Welding Society.

### ASSEMBLING THE WELDING SYMBOL

Reference line and arrow: The symbol begins with a reference line and arrow pointing to the joint where the weld is to be made. The reference line has two 'sides': 'other side' (above the line) and 'arrow side' (below the line)—refer to the following examples and to chart 5.9.

#### BASIC WELDING ARROW

FIGURE 5.1



#### BASIC WELDING SYMBOLS

##### (a) The weld symbol

FILLET	BACK, or BACKING	PLUG or SLOT	SPOT, or PROJECTION	SEAM	EDGE FLANGE	CORNER FLANGE

##### (b) The groove symbol

SQUARE	V	BEVEL	V	J	FLARE-V	FLARE-BEVEL

## EXAMPLE USE OF THE FILLET WELD SYMBOL

If a continuous fillet weld is needed, like this:



the fillet weld symbol is placed on the 'arrow side' of the reference line, thus:



If the weld is required on the far side from the arrow, thus:



the weld symbol is shown on the 'other side' of the reference line:



If a continuous fillet weld is needed on both sides of the joint,



the fillet weld symbol is placed on both sides of the reference line:



## EXAMPLE USE OF THE BEVEL GROOVE SYMBOL

If a bevel groove is required, like this:



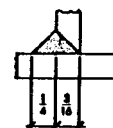
The 'groove' symbol for a bevel is shown, with the fillet weld symbol, and a break is made in the arrow toward the member to be beveled, thus:



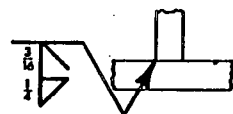
Only the bevel and 'J' groove symbols require a break in the arrow—see chart 5.9.

## DIMENSIONING THE WELD CROSS SECTION

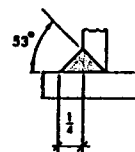
Suppose the weld is required to be 1/4 inch in size, and the bevel is to be 3/16 inch deep:



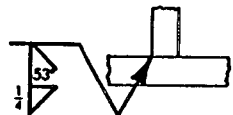
These dimensions are shown to the left of the weld symbol:



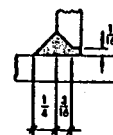
Alternatively, the bevel can be expressed in degrees of arc:



and be indicated thus on the symbol:



If a root gap is required, thus:



the symbol is:



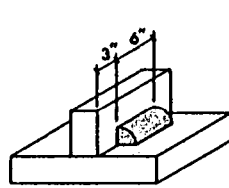
5.1.8

CHART 5.9

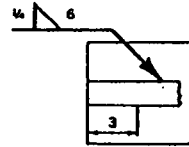
FIGURE 5.1

## DIMENSIONING THE LENGTH OF THE WELD

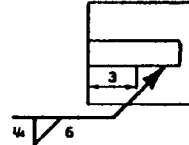
Going back to the fillet weld joint without a bevel, if the weld needs to be 1/4-inch in size and 6 inches long, like this:



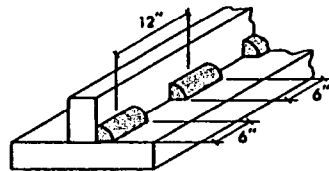
the weld symbol may be drawn:



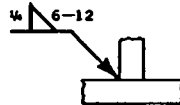
alternately:



If a series of 6-inch long welds is required with 6-inch gaps between them (that is, the pitch of the welds is 12 inches), thus:



the symbol is:

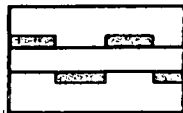


alternately:

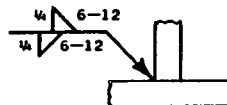


If these welds are required staggered on both sides—

like this:



the symbol is:



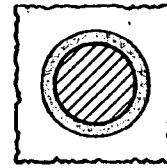
## SUPPLEMENTARY SYMBOLS

These symbols give instructions for making the weld and define the required contour:

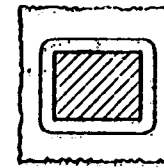
WELD ALL AROUND	FIELD WELD	MELT-THRU	CONTOUR		
			FLUSH	CONVEX	CONCAVE

Going back to the example of a simple fillet weld, if the weld is required all around a member,

like this:



or like this:



it is shown in this way:



If this same 'all around' weld has to be made in the field, it is shown thus:



The contour of the weld is shown by a contour symbol on the weld symbol:

FLUSH CONTOUR

CONVEX CONTOUR

CONCAVE CONTOUR

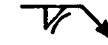
like this:



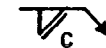
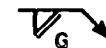
like this:



or:



The method of finishing the weld contour is indicated by adding a finish notation letter, thus,



where M = machining, G = grinding, and C = chipping.

## FULL WELDING SYMBOL

Occasionally it is necessary to give other instructions in the welding symbol. The symbol can be elaborated for this as shown in 'Location of elements of a welding symbol' in chart 5.9.

Chart 5.9, reproduced by permission of the American Welding Society, summarizes and amplifies the explanations of this section.



All information for constructing piping systems is contained in drawings, apart from the specifications, and the possible use of a model and photographs.

THE MAIN PURPOSE OF A DRAWING IS TO COMMUNICATE INFORMATION IN A SIMPLE AND EXPLICIT WAY.

#### PROCESS & PIPING DRAWINGS GROW FROM THE SCHEMATIC DIAGRAM

5.2.1

To design process piping, three types of drawing are developed in sequence from the schematic diagram (or 'schematic') prepared by the process engineer.

These three types of drawing are, in order of development:—

- (1) FLOW DIAGRAM (PROCESS, or SERVICE)
- (2) PIPING AND INSTRUMENTATION DIAGRAM, or 'P&ID'
- (3) PIPING DRAWING

#### EXAMPLE DIAGRAMS

Figure 5.2 shows a simple example of a 'schematic'. A solvent recovery system is used as an example. Based on the schematic diagram of figure 5.2, a developed process flow diagram is shown in figure 5.3. From this flow diagram, the P&ID (figure 5.4) is evolved.

As far as practicable, the flow of material(s) should be from left to right. Incoming flows should be arrowed and described down the left-hand edge of the drawing, and exiting flows arrowed and described at the right of the drawing, without intruding into the space over the title block.

Information normally included on the process drawings is detailed in sections 5.2.2 thru 5.2.4. Flow diagrams and P&ID's each have their own functions and should show only that information relevant to their functions, as set out in 5.2.3 and 5.2.4. Extraneous information such as piping, structural and mechanical notes should not be included, unless essential to the process.

#### SECURITY

A real or supposed need for industrial or national security may restrict information appearing on drawings. Instead of naming chemicals, indeterminate or traditional terms such as 'sweet water', 'brine', 'leach acid', 'chemical B', may be used. Data important to the reactions such as temperatures, pressures and flow rates may be withheld. Sometimes certain key drawings are locked away when not in use.

Commonly referred to as a 'schematic', this diagram shows paths of flow by single lines, and operations or process equipment are represented by simple figures such as rectangles and circles. Notes on the process will often be included.

The diagram is not to scale, but relationships between equipment and piping with regard to the process are shown. The desired spatial arrangement of equipment and piping may be broadly indicated. Usually, the schematic is not used after the initial planning stage, but serves to develop the process flow diagram which then becomes the primary reference.

#### FLOW DIAGRAM

5.2.3

This is an unscaled drawing describing the process. It is also referred to as a 'flow sheet'.

It should state the materials to be conveyed by the piping, conveyors, etc., and specify their rates of flow and other information such as temperature and pressure, where of interest. This information may be 'flagged' (on lines) within the diagram or be tabulated on a separate panel—such a panel is shown at the bottom left of figure 5.3.

#### LAYOUT OF THE FLOW DIAGRAM

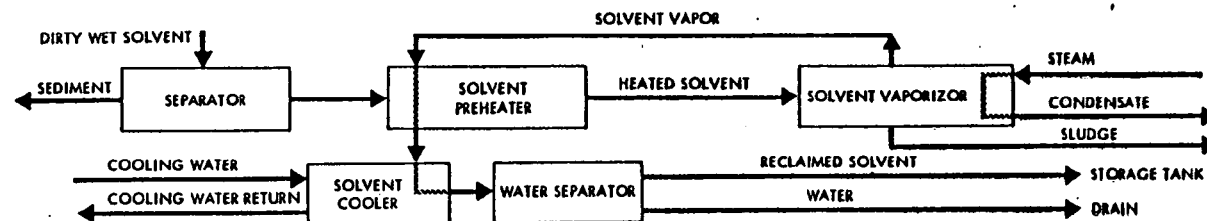
Whether a flow diagram is to be in elevation or plan view should depend on how the P&ID is to be presented. To easily relate the two drawings, both should be presented in the same view. Elevations are suitable for simple systems arranged vertically. Installations covering large horizontal areas are best shown in plan view.

Normally, a separate flow diagram is prepared for each plant process. If a single sheet would be too crowded, two or more sheets may be used. For simple processes, more than one may be shown on a sheet. Process lines should have the rate and direction of flow, and other required data, noted. Main process flows should preferably be shown going from the left of the sheet to the right. Line sizes are normally not shown on a flow diagram. Critical internal parts of vessels and other items essential to the process should be indicated.

All factors considered, it is advisable to write equipment titles *either near the top or near the bottom of the sheet*, either directly above or below the equipment symbol. Sometimes it may be directed that all pumps be drawn at a common level near the bottom of the sheet, although this practice may lead to a complex-looking drawing. Particularly with flow diagrams, simplicity in presentation is of prime importance.

# SCHEMATIC DIAGRAM

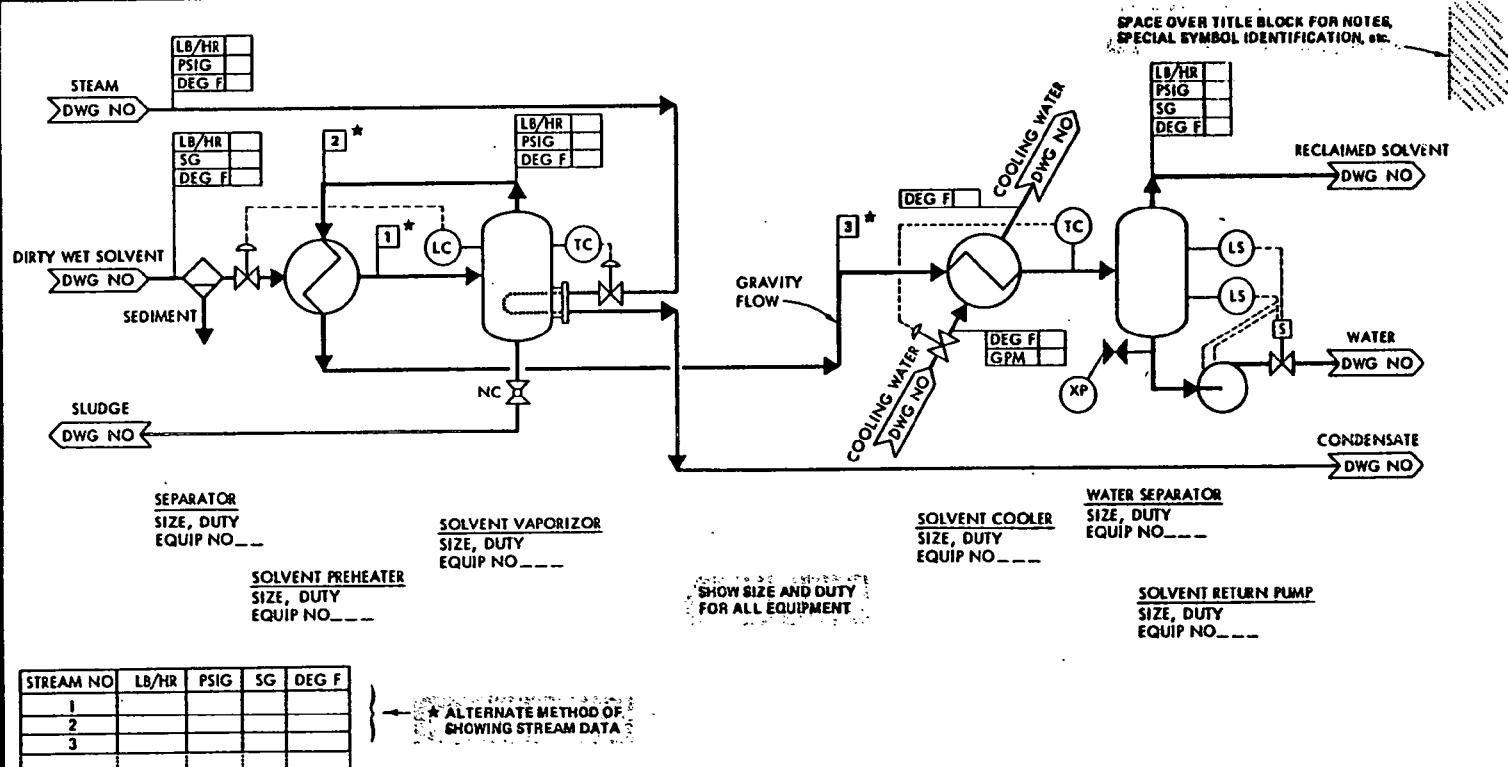
FIGURE 5.2



# PROCESS FLOW DIAGRAM

THIS DIAGRAM SHOWS THE MANNER OF PRESENTATION ONLY—A WORKING DRAWING WOULD BE DEVELOPED TO INCLUDE MORE INFORMATION

FIGURE 5.3

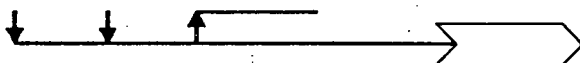


## FLOW LINES

Directions of flow within the diagram are shown by solid arrowheads. The use of arrowheads at all junctions and corners aids the rapid reading of the diagram. The number of crossings can be minimized by good arrangement. Suitable line thicknesses are shown at full size in chart 5.1. For photographic reduction, lines should be spaced not closer than 3/8 inch.

Process and service streams entering or leaving the flow diagram are shown by large hollow arrowheads, with the conveyed fluid written over and the continuation sheet number within the arrowhead, as in figure 5.3.

## ARROWS ON FLOW DIAGRAMS



## SHOWING VALVES ON THE FLOW DIAGRAM

Instrument-controlled and manual valves which are necessary to the process are shown. The following valves are shown if required by a governing code or regulation, or if they are essential to the process: isolating, bypassing, venting, draining, sampling, and valves used for purging, steamout, etc., for relieving excess pressure of gases or liquids (including rupture discs), breather valves and vacuum breakers.

## SHOW ONLY SPECIAL FITTINGS

Piping fittings, strainers, and flame arrestors should not be shown unless of special importance to the process.

## ESSENTIAL INSTRUMENTATION

Only instrumentation essential to process control should be shown. Simplified representation is suitable. For example, only instruments such as controllers and indicators need be shown; items not essential to the drawing (transmitters, for example) may be omitted.

## EQUIPMENT DATA

Capacities of equipment should be shown. Equipment should be drawn schematically, using equipment symbols, and where feasible should be drawn in proportion to the actual sizes of the items. Equipment symbols should neither dominate the drawing, nor be too small for clear understanding.

## STANDBY & PARALLELED EQUIPMENT

Standby equipment is not normally drawn. If identical units of equipment are provided for paralleled operation (that is, all units on stream), only one unit need normally be drawn. Paralleled or standby units should be indicated by noting the equipment number and the service function ('STANDBY' or 'PARALLEL OP').

It is advisable to draw equipment that is operated cyclically. For example, with filter presses operated in parallel, one may be shown on-stream, and the second press for alternate operation.

## PROCESS DATA FOR EQUIPMENT

The basic process information required for designing and operating major items of equipment should be shown. This information is best placed immediately below the title of the equipment.

## IDENTIFYING EQUIPMENT

Different types of equipment may be referred to by a classification letter (or letters). There is no generally accepted coding — each company has its own scheme if any standardization is made at all. Equipment classed under a certain letter is numbered in sequence from '1' upward. If a new installation is made in an existing plant, the method of numbering may follow previous practice for the plant.

Also, it is useful to divide the plant and open part of the site as necessary into areas, giving each a code number. An area number can be made the first part of an equipment number. For example, if a heat exchanger is the 53rd item of equipment listed under the classification letter 'E', located in area '1', (see 'Key plan' in 5.2.7) the exchanger's equipment number can be 1-E-53.

Each item of equipment should bear the same number on all drawings, diagrams and listings. Standby or identical equipment, if in the same service, may be identified by adding the letters, A, B, C, and so on, to the same equipment identification letter and number. For example, a heat exchanger and its standby may be designated 1-E-53A, and 1-E-53B.

## SERVICES ON PROCESS FLOW DIAGRAMS

Systems for providing services should not be shown. However, the type of service, flow rates, temperatures and pressures should be noted at consumption rates corresponding to the material balance—usually shown by a 'flag' to the line—see figure 5.3.

## DISPOSAL OF WASTES

The routes of disposal for all waste streams should be indicated. For example, arrows or drain symbols may be labelled with destination, such as 'chemical sewer' or 'drips recovery system'. In some instances the disposal or waste-treatment system may be detailed on one or more separate sheets. See 6.13 where 'effluent' is discussed.

## MATERIAL BALANCE

The process material balance can be tabulated on separate 8½ x 11-inch sheets, or along the bottom of the process flow diagram.

This drawing is commonly referred to as the 'P&ID'. Its object is to indicate all process and service lines, instruments and controls, equipment, and data necessary for the design groups. The process flow diagram is the primary source of information for developing the P&ID. Symbols suitable for P&ID's are given in charts 5.1 thru 5.7.

The P&ID should define piping, equipment and instrumentation well enough for cost estimation and for subsequent design, construction, operation and modification of the process. Material balance data, flow rates, temperatures, pressures, etc., and piping fitting details are not shown, and purely mechanical piping details such as elbows, joints and unions are inappropriate to P&ID's.

#### INTERCONNECTING P&ID

This drawing shows process and service lines between buildings and units, etc., and serves to link the P&ID's for the individual processes, units or buildings. Like any P&ID, the drawing is not to scale. It resembles the layout of the site plan, which enables line sizes and branching points from headers to be established, and assists in planning pipeways.

#### P&ID LAYOUT

The layout of the P&ID should resemble as far as practicable that of the process flow diagram. The process relationship of equipment should correspond exactly. Often it is useful to draw equipment in proportion vertically, but to reduce horizontal dimensions to save space and allow room for flow lines between equipment. Crowding information is a common drafting fault — it is desirable to space generously, as, more often than not, revisions add information. On an elevational P&ID, a base line indicating grade or first-floor level can be shown. Critical elevations are noted.

For revision purposes, a P&ID is best made on a drawing sheet having a grid system—this is a sheet having letters along one border and numbers along the adjacent border. Thus, references such as 'A6', 'B5', etc., can be given to an area where a change has been made. (A grid system is applicable to P&ID's more complicated than the simple example of figure 5.4.)

#### DRAFTING GUIDELINES FOR P&ID's

- Suitable line thicknesses are shown at full size in chart 5.1
- Crossing lines must not touch—break lines going in one direction only. Break instrument lines crossing process and service lines
- Keep parallel lines at least 3/8 inch apart
- Preferably draw all valves the same size—1/4-inch long is suitable—as this retains legibility for photographic reduction. Instrument isolating valves and drain valves can be drawn smaller, if desired
- Draw instrument identification balloons 7/16th-inch diameter—see 5.5
- Draw trap symbols 3/8th-inch square

#### FLOW LINES ON P&ID's

All flow lines and interconnections should be shown on P&ID's. Every line should show direction of flow, and be labeled to show the area of project, conveyed fluid, line size, piping material or specification code number (company code), and number of the line. This information is shown in the 'line number'.

**EXAMPLE LINE NUMBER:** **74|BZ|6|412|23** may denote the 23rd line in area 74, a 6-inch pipe to company specification 412. 'BZ' identifies the conveyed fluid.

This type of full designation for a flow line need not be used, provided identification is adequate.

Piping drawings use the line numbering of the P&ID, and the following points apply to piping drawings as well as P&ID's.

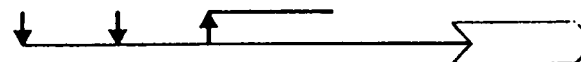
- For a continuous line, retain the same number of line (such as 23 in the example) as the line goes thru valves, strainers, small filters, venturis, traps, orifice flanges and small equipment generally
- Change the number of a line terminating at a major item of equipment such as a tank, pressure vessel, mixer, or any equipment carrying an individual equipment number
- Allocate new numbers to branches
- For a system of lines carrying the same material, allocate sequential numbers to lines, beginning with '1' for each system



As with the process flow diagram, directions of flow within the drawing are shown by solid arrows placed at every junction, and all corners except where changes of direction occur closely together. Corners should be square. The number of crossings should be kept minimal by good arrangement.

Process and service streams entering or leaving the process are noted by hollow arrows with the name of the conveyed fluid written over the arrowhead and the continuation sheet number within it. No process flow data will normally be shown on a P&ID.

#### FLOW LINES ON P&ID's



#### NOTES FOR LINES

Special points for design and operating procedures are noted—such as lines which need to be sloped for gravity flow, lines which need careful cleaning before startup, etc.

## P&ID SHOWS ALL EQUIPMENT & SPECIAL ITEMS

The P&ID should show all major equipment and information that is relevant to the process, such as equipment names, equipment numbers, the sizes, ratings, capacities, and/or duties of equipment, and instrumentation.

Standby and paralleled equipment is shown, including all connected lines. Equipment numbers and service functions ('STANDBY' or 'PARALLEL OP') are noted.

'Future' equipment, together with the equipment that will service it, is shown in broken outline, and labeled. Blind-flange terminations to accommodate future piping should be indicated on headers and branches. 'Future' additions are usually not anticipated beyond a 5-year period.

Pressure ratings for equipment are noted if the rating is different from the piping system. A 'typical' note may be used to describe multiple pieces of identical equipment in the same service, but all equipment numbers are written.

## CLOSURES

Temporary closures for process operation or personnel protection are shown.

## SEPARATORS, SCREENS & STRAINERS

These items should be shown upstream of equipment and processes needing protection, and are discussed in 2.10.

## STEAM TRAPS ON THE P&ID

If the locations of traps are known they are indicated. For example, the trap required upstream of a pressure-reducing station feeding a steam turbine should be shown.

Steam traps on steam piping are not otherwise indicated, as these trap positions are determined when making the piping drawings. They can be added later to the P&ID if desired, after the piping drawings have been completed.

## DRIPLEGS

Driplegs are not shown.

## VENTS & DRAINS

Vents and drains on high and low points of lines respectively, to be used for hydrostatic testing, are not shown, as they are established on the piping arrangement drawings. Process vents and drains are shown.

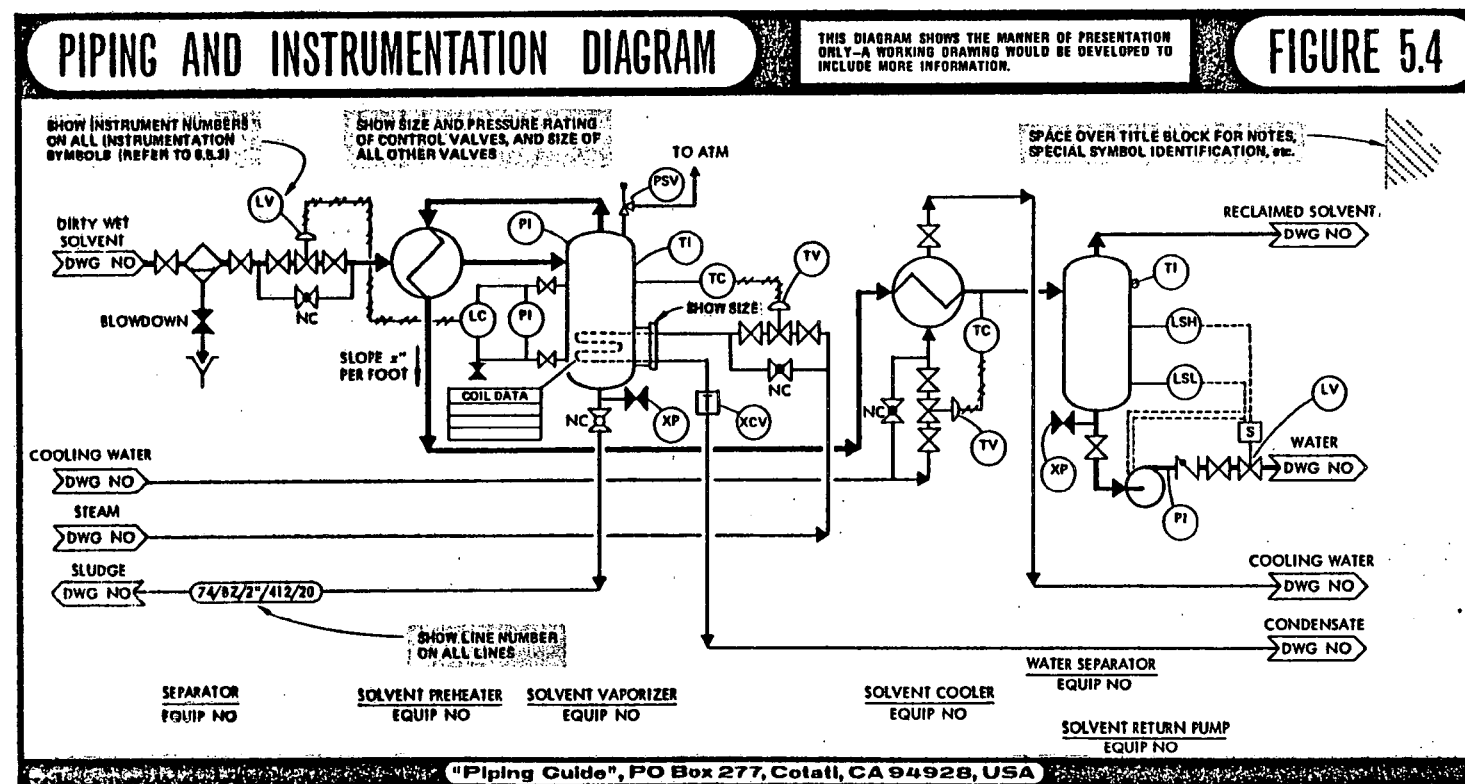


FIGURE 5.4

## VALVES ON THE P&ID

- Show and tag process and service valves with size and identifying number if applicable. Give pressure rating if different from line specification
- Indicate any valves that have to be locked open or locked closed
- Indicate powered operators

## SHOWING INSTRUMENTATION ON THE P&ID

Signal-lead drafting symbols shown in chart 5.1 may be used, and the ISA scheme for designating instrumentation is described in 5.5. Details of instrument piping and conduit are usually shown on separate instrument installation drawings.

- Show all instrumentation on the P&ID, for and including these items: element or sensor, signal lead, orifice flange assembly, transmitter, controller, vacuum breaker, flame arrestor, level gage, sight glass, flow indicator, relief valve, rupture disc, safety valve. The last three items may be tagged with set pressure(s) also
- Indicate local- or board-mounting of instruments by the symbol—refer to the labeling scheme in 5.5.4

## INSULATION & TRACING

Insulation on piping and equipment is shown, together with the thickness required. Tracing requirements are indicated. Refer to 6.8.

## CONTROL STATIONS

Control stations are discussed in 6.1.4. Control valves are indicated by pressure rating, instrument identifying number and size—see figure 5.15, for example.

## P&ID SHOWS HOW WASTES ARE HANDLED

Drains, funnels, relief valves and other equipment handling wastes are shown on the P&ID. If an extensive system or waste-treatment facility is involved, it should be shown on a separate P&ID. Wastes and effluents are discussed in 6.13.

## SERVICE SYSTEMS MAY HAVE THEIR OWN P&ID

Process equipment may be provided with various services, such as steam for heating, water or refrigerant for cooling, or air for oxidizing. Plant or equipment providing these services is usually described on separate 'service P&ID's'. A service line such as a steam line entering a process P&ID is given a 'hollow arrow' line designation taken from the service P&ID. Returning service lines are designated in the same way. Refer to figure 5.4.

## UTILITY STATIONS

Stations providing steam, compressed air, and water, are shown. Refer to 6.1.5.

## LINE DESIGNATION SHEETS OR TABLES

5.2.5

These sheets are tabulated lists of lines and information about them. The numbers of the lines are usually listed at the right of the sheet. Other columns list line size, material of construction (using company's specification code, if there is one), conveyed fluid, pressure, temperature, flow rate, test pressure, insulation or jacketing (if required), and connected lines (which will usually be branches).

The sheets are compiled and kept up-to-date by the project group, taking all the information from the P&ID. Copies are supplied to the piping group for reference.

On small projects involving only a few lines line designation sheets may not be used. It is useful to add a note on the P&ID stating the numbers of the last line and last valve used.

## VIEWS USED FOR PIPING DRAWINGS

5.2.6

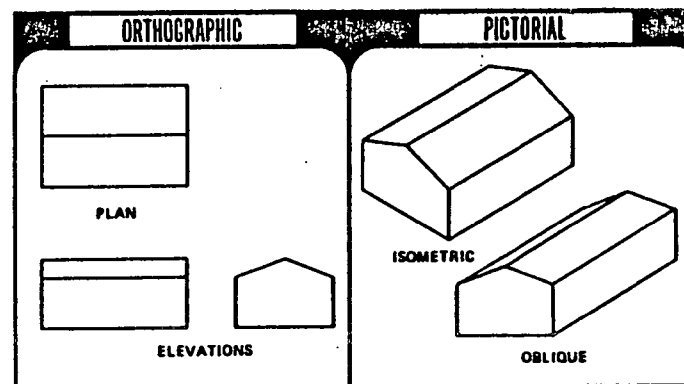
Two types of view are used:

- (1) ORTHOGRAPHIC — PLANS AND ELEVATIONS
- (2) PICTORIAL — ISOMETRIC VIEW AND OBLIQUE PRESENTATION

Figure 5.5 shows how a building would appear in these different views.

## PRESENTATIONS USED IN PIPING DRAWINGS

FIGURE 5.6



## PLANS & ELEVATIONS

Plan views are more common than elevational views. Piping layout is developed in plan view, and elevational views and section details are added for clarity where necessary.

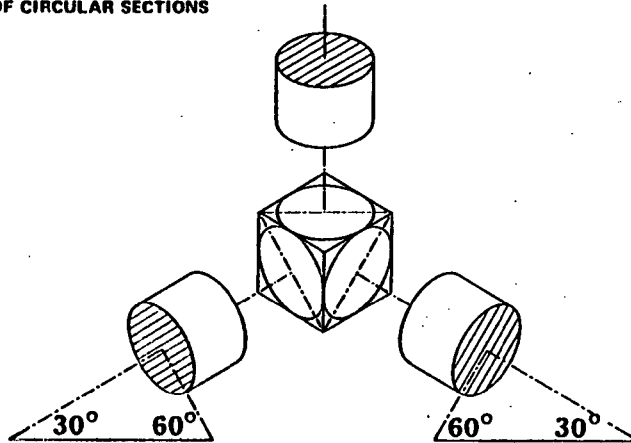
## PICTORIAL VIEWS

In complex piping systems, where orthographic views may not easily illustrate the design, pictorial presentation can be used for clarity. In either isometric or oblique presentations, lines not horizontal or vertical on the drawing are usually drawn at 30 degrees to the horizontal.

Oblique presentation has the advantage that it can be distorted or expanded to show areas of a plant, etc. more clearly than an isometric view. It is not commonly used, but can be useful for diagrammatic work.

Figure 5.6 illustrates how circular shapes viewed at different angles are approximated by means of a 35-degree ellipse template. Isometric templates for valves, etc., are available and neat drawings can be rapidly produced with them. Orthographic and isometric templates can be used to produce an oblique presentation.

**ISOMETRIC PRESENTATION OF CIRCULAR SECTIONS**



**FIGURE 5.6**

## PLAN, ELEVATION, ISOMETRIC & OBLIQUE PRESENTATIONS OF A PIPING SYSTEM

5.2.4  
5.2.7

Figure 5.7 is used to show the presentations used in drafting. Isometric and oblique drawings both clearly show the piping arrangement, but the plan view fails to show the bypass loop and valve, and the supplementary elevation is needed.

### PIPING DRAWINGS ARE BASED ON OTHER DRAWINGS

5.2.7

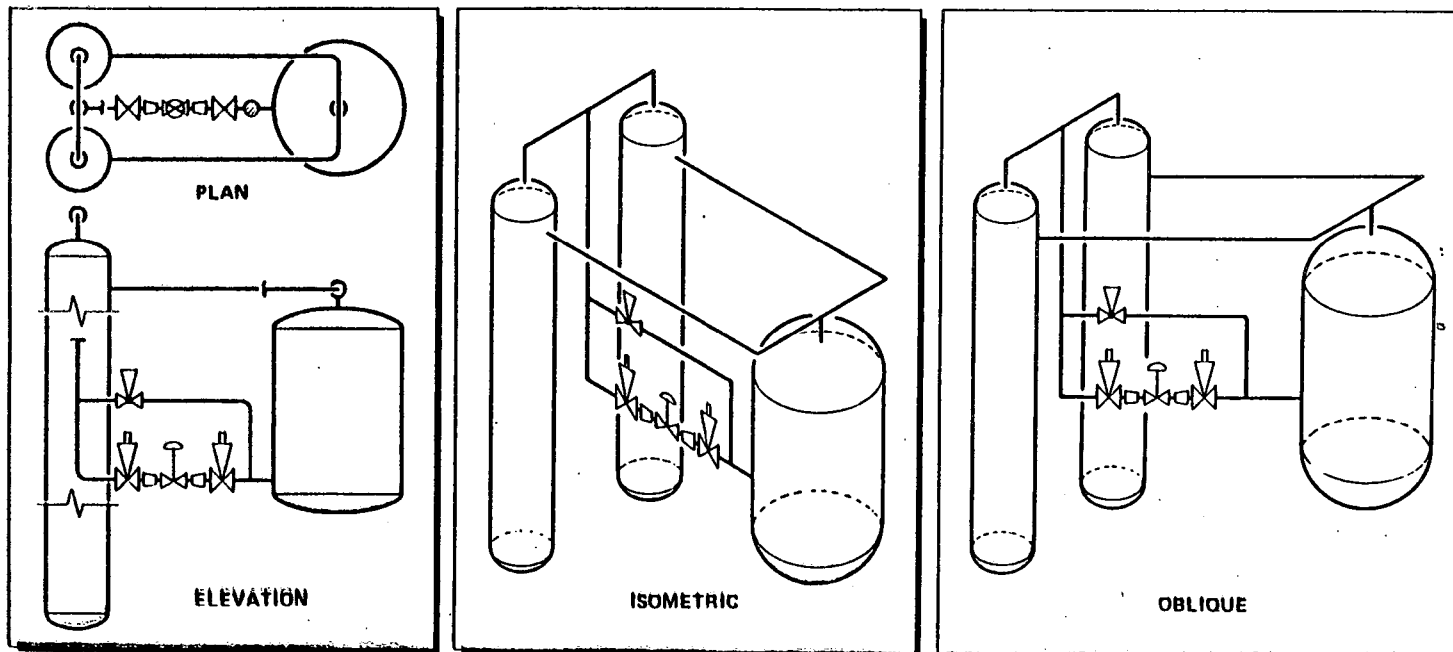
The purpose of piping drawings is to supply detailed information to enable a plant to be built. Prior to making piping drawings, the site plan and equipment arrangement drawings are prepared, and from these two drawings the plot plan is derived. These three drawings are used as the basis for developing the piping drawings.

#### SITE PLAN

The piping group produces a 'site plan' to a small scale (1 inch to 30 or 100 ft for example). It shows the whole site including the boundaries, roads, railroad spurs, pavement, buildings, process plant areas, large structures, storage areas, effluent ponds, waste disposal, shipping and loading areas. 'True' (geographic) and 'assumed' or 'plant' north are marked and their angular separation shown—see figure 5.11.

**PIPING ARRANGEMENT IN DIFFERENT PRESENTATIONS**

**FIGURE 5.7**



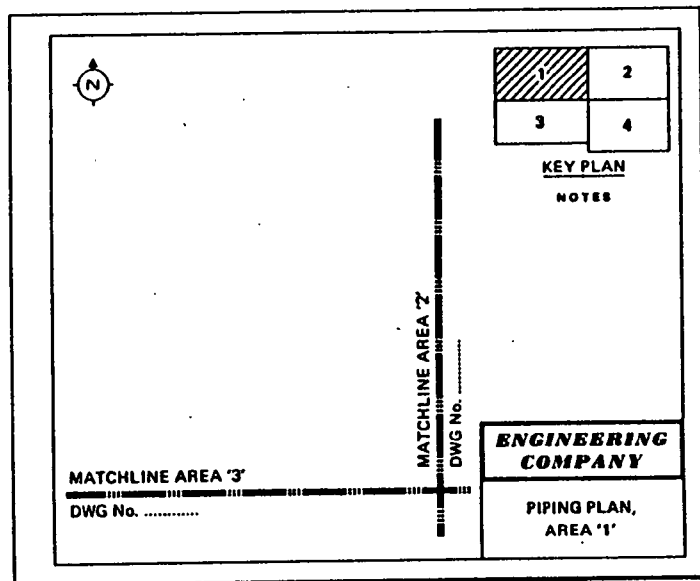
**FIGURES 5.5-5.7**

## KEY PLAN

A 'key plan' is produced by adapting the site plan, dividing the area of the site into smaller areas identified by key letters or numbers. A small simplified inset of the key plan is added to plot plans, and may be added to piping and other drawings for reference purposes. The subject area of the particular drawing is hatched or shaded, as shown in figure 5.8.

DRAWING SHEET SHOWING KEY PLAN & MATCHLINE

FIGURE 5.8



## EQUIPMENT ARRANGEMENT DRAWING

Under project group supervision, the piping group usually makes several viable arrangements of equipment, seeking an optimal design that satisfies process requirements. Often, preliminary piping studies are necessary in order to establish equipment coordinates.

A design aid for positioning equipment is to cut out scaled outlines of equipment from stiff paper, which can be moved about on a plan view of the area involved. (If multiple units of the same type are to be used, xeroxing the equipment outlines is faster.) Another method which is useful for areas where method study or investigational reports are needed is described in 4.4.13 under 'Photographic layouts'.

## PLOT PLAN

When the equipment arrangement drawings are approved, they are developed into 'plot plans' by the addition of dimensions and coordinates to locate all major items of equipment and structures.

North and east coordinates of the extremities of buildings, and centerlines of steelwork or other architectural constructions should be shown on the plot plan, preferably at the west and south ends of the installation. Both 'plant north' and true north should be shown—see figure 5.11.

Equipment coordinates are usually given to the centerlines. Coordinates for pumps are given to the centerline of the pump shaft and either to the face of the pump foundation, or to the centerline of the discharge port.

Up-dated copies of the above drawings are sent to the civil, structural and electrical or other groups involved in the design, to inform them of requirements as the design develops.

## VESSEL DRAWINGS

When the equipment arrangement has been approved and the piping arrangement determined, small dimensioned drawings of process vessels are made (on sheets 8½ x 11 or 11 x 17 inches) in order to fix nozzles and their orientations, manholes, ladders, etc. These drawings are then sent to the vendor who makes the shop detail drawings, which are examined by the project engineer and sent to the piping group for checking and approval. Vessel drawings need not be to scale. (Figure 5.14 is an example vessel drawing.)

## DRAWINGS FROM OTHER SOURCES

Piping drawings should be correlated with the following drawings from other design groups and from vendors. Points to be checked are listed:

### Architectural drawings:

- Outlines of walls or sidings, indicating thickness
- Floor penetrations for stairways, lifts, elevators, ducts, drains, etc.
- Positions of doors and windows

### Civil engineering drawings:

- Foundations, underground piping, drains, etc.

### Structural-steel drawings:

- Positions of steel columns supporting next higher floor level
- Supporting structures such as overhead cranes, monorails, platforms or beams
- Wall bracing, where pipes may be taken thru walls

### Heating, ventilating & air-conditioning (HVAC) drawings:

- Paths of ducting and rising ducts, fan room, plenums, space heaters, etc.

### Electrical drawings:

- Positions of motor control centers, switchgear, junction boxes and control panels
- Major conduit or wiring runs (including buried runs)
- Positions of lights

### Instrumentation drawings:

- Instrument panel and console locations

### Vendors' drawings:

- Dimensions of equipment
- Positions of nozzles, flange type and pressure rating, instruments, etc.

### Mechanical drawings:

- Positions and dimensions of mechanical equipment such as conveyors, chutes, etc.
- Piped services needed for mechanical equipment.



Process equipment and piping systems have priority. Drawings listed on the preceding page must be reviewed for compatibility with the developing piping design.

Pertinent background details (drawn faintly) from these drawings help to avoid interferences. Omission of such detail from the piping drawing often leads to the subsequent discovery that pipe has been routed thru a brace, stairway, doorway, foundation, duct, mechanical equipment, motor control center, fire fighting equipment, etc.

Completed piping drawings will also show spool numbers, if this part of the job is not subcontracted – see 5.2.9. Electrical and instrument cables are not shown on piping drawings, but trays to hold the cables are indicated—for example, see figure 6.3, point (8).

It is not always possible for the piping drawing to follow exactly the logical arrangement of the P&ID. Sometimes lines must be routed with different junction sequence, and line numbers may be changed. During the preliminary piping studies, economies and practicable improvements may be found, and the P&ID may be modified to take these into account. However, it is not the piping designer's job to seek ways to change the P&ID.

### SCALE

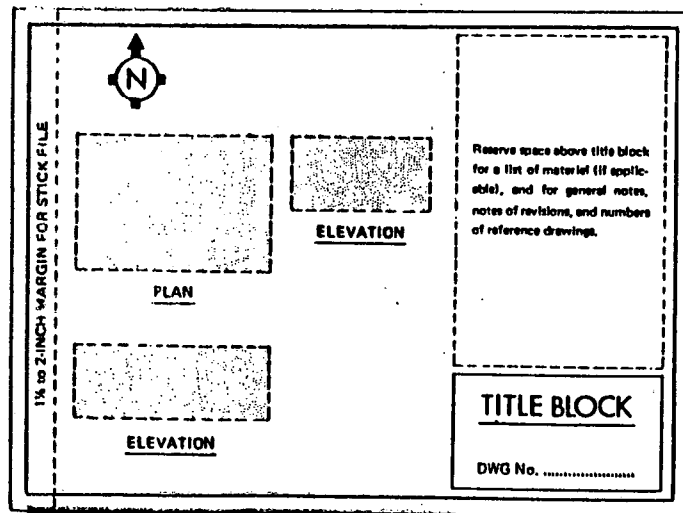
Piping is arranged in plan view, usually to 3/8 in./ft scale.

### ALLOCATING SPACE ON THE SHEET

- Obtain the drawing number and fill in the title block at the bottom right corner of the sheet

### ALLOCATING SPACE ON A DRAWING SHEET

FIGURE 5.9



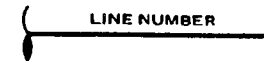
- On non-standard sheets, leave a 1½- to 2-inch margin at the left edge of the sheet, to allow filing on a 'stick'. Standard drawing sheets usually have this margin
- On drawings showing a plan view, place a north arrow at the top left corner of the sheet to indicate plant north—see figure 5.11
- Do not draw in the area above the title block, as this space is allocated to the bill of material, or to general notes, brief descriptions of changes, and the titles and numbers of reference drawings
- If plans and elevations are small enough to go on the same sheet, draw the plan at the upper left side of the sheet and elevations to the right and bottom of it, as shown in figure 5.9

### BACKGROUND DETAIL

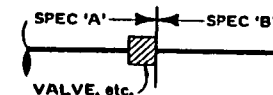
- Show background detail as discussed in 5.2.8 under 'Piping drawings'. It is sometimes convenient to draw outlines on the reverse side of the drawing sheet
- After background details have been determined, it is best to make a print on which nozzles on vessels, pumps, etc., to be piped can be marked in red pencil. Utility stations can also be established. This will indicate areas of major usage and the most convenient locations for the headers. Obviously, at times there will be a number of alternate routes offering comparable advantages

### PROCESS & SERVICE LINES ON PIPING DRAWINGS

- Take line numbers from the P&ID. Refer to 5.2.4 under 'Flow lines on P&ID's' for information on numbering lines. Include line numbers on all views, and arrowheads showing direction of flow
- Draw all pipe 'single line' unless special instructions have been given for drawing 'double line'. Chart 5.1 gives line thicknesses (full size)
- Line numbers are shown against lines, thus:



- Take lines continued on another sheet to a matchline, and there code with line numbers only. Show the continuation sheet numbers on matchlines—see figure 5.8
- Show where changes in line material specification occur. The change is usually indicated immediately downstream of a flange of a valve or equipment



- Show a definite break in a line crossing behind another line—see 'Rolled ell', under 'Plan view piping drawings', this section

- If pipe sleeves are required thru floors, indicate where they are needed and inform the group leader for transmitting this information to the group(s) concerned
- Indicate insulation, and show whether lines are electrically or steam traced—see chart 5.7

#### FITTINGS, FLANGES, VALVES & PUMPS ON PIPING DRAWINGS

- The following items should be labeled in one view only: tees and ells rolled at 45 degrees (see example, this page), short-radius ell, reducing ell, eccentric reducer and eccentric swage (note on plan views whether 'top flat' or 'bottom flat'), concentric reducer, concentric swage, non-standard or companion flange, reducing tee, special items of unusual material, of pressure rating different from that of the system, etc. Refer to charts 5.3, 5.4 and 5.5 for symbol usage
- Draw the outside diameters of flanges to scale
- Show valve identification number from P&ID
- Label control valves to show: size, pressure rating, dimension over flanges, and valve instrument number, from the P&ID—see figure 5.15
- Draw valve handwheels to scale with valve stem fully extended
- If a valve is chain-operated, note distance of chain from operating floor, which for safety should be approximately 3 ft
- For pumps, show outline of foundation and nozzles

#### DRIPLEGS & STEAM TRAPS

Driplegs are indicated on relevant piping drawing plan views. Unless identical, a separate detail is drawn for each dripleg. The trap is indicated on the dripleg piping by a symbol, and referred to a separate trap detail or data sheet. The trap detail drawing should show all necessary valves, strainers, unions, etc., required at the trap—see figures 6.43 and 6.44.

The piping shown on the dripleg details should indicate whether condensate is to be taken to a header for re-use, or run to waste. The design notes in 6.10.5 discuss dripleg details for steam lines in which condensate forms continuously. Refer to 6.10.9 also.

#### INSTRUMENTS & CONNECTIONS ON PIPING DRAWINGS

- Show location for each instrument connection with encircled instrument number taken from the P&ID. Refer to 5.5.3 and chart 6.2
- Show similar isolating valve arrangements on instrument connections as 'typical' detail, unless covered by standard company detail sheet

#### VENTS & DRAINS

Refer to 6.11 and figure 6.47.

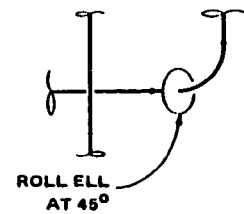
#### PIPE SUPPORTS

Refer to 6.2.2, and chart 5.7. for symbols.

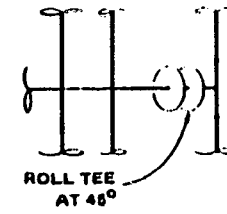
#### PLAN VIEW PIPING DRAWINGS

- Draw plan views for each floor of the plant. These views should show what the layout will look like between adjacent floors, viewed from above, or at the elevation thru which the plan view is cut
- If the plan view will not fit on one sheet, present it on two or more sheets, using matchlines to link the drawings. See figure 5.8
- Note the elevation below which a plan view is shown—for example, 'PLAN BELOW ELEVATION 15'-0" '. For clarity, both elevations can be stated: 'PLAN BETWEEN ELEVATIONS 30'-0" & 15'-0" '
- If a tee or elbow is 'rolled' at 45 degrees, note as shown in the view where the fitting is rolled out of the plane of the drawing sheet

'ROLLED' ELL



'ROLLED' TEE



- Figure 5.10 shows how lines can be broken to give sufficient information without drawing other views
- Indicate required field welds

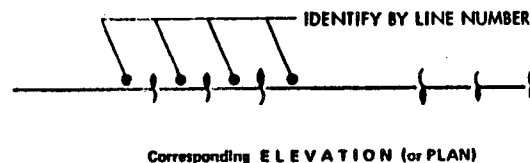
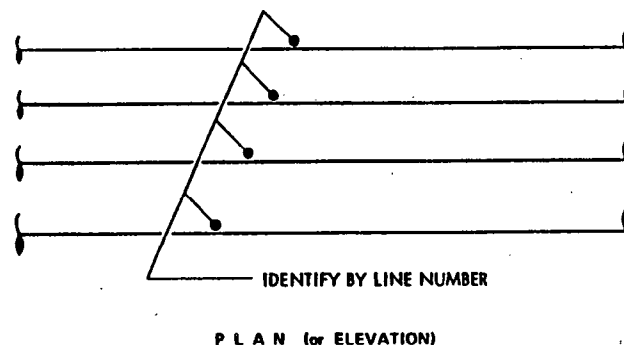
#### ELEVATIONS (SECTIONS) & DETAILS

- Draw elevations and details to clarify complex piping or piping hidden in the plan view
- Do not draw detail that can be described by a note
- Show only as many sections as necessary. A section does not have to be a complete cross section of the plan
- Draw to a large scale any part needing fuller detail. Enlarged details are preferably drawn in available space on elevational drawings, and should be cross-referenced by the applicable detail and drawing number(s)
- Identify sections indicated on plan views by letters (see chart 5.8) and details by numbers. Letters I and O are not used as this can lead to confusion with numerals. If more than twentyfour sections are needed the letter identification can be broken down thus: A1-A1, A2-A2, B4-B4, ..... and so on
- Do not section plan views looking toward the bottom of the drawing sheet

- Figure 5.10 shows how to break lines to give sufficient information whilst avoiding drawing another view or section

#### SHOWING 'HIDDEN' LINES ON PIPING DRAWINGS

FIGURE 5.10



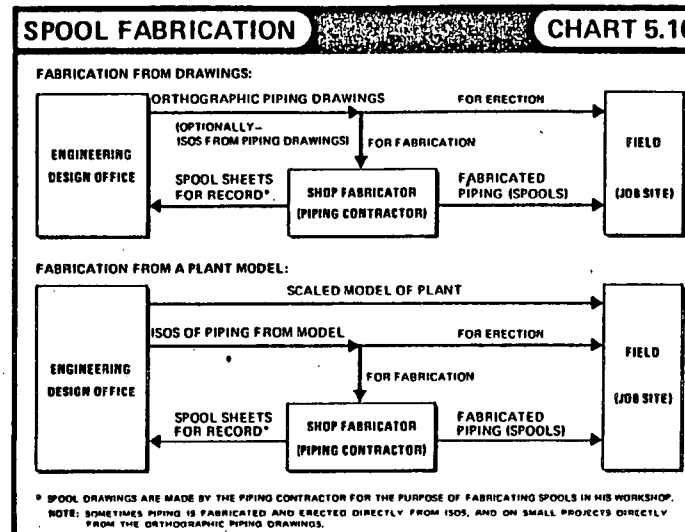
#### PIPING FABRICATION DRAWINGS—'ISOS' & 'SPOOLS'

5.2.9

The two most common methods for producing piping designs for a plant are by making either plan and elevation drawings, or by constructing a scaled model. For fabricating welded piping, plans and elevations are sent directly to a subcontractor, usually referred to as a 'shop fabricator'—if a model is used, isometric drawings (referred to as 'isos') are sent instead.

Isometric views are commonly used in prefabricating parts of butt-welded piping systems. Isos showing the piping to be prefabricated are sent to the shop fabricator. Figure 5.15 is an example of such an iso.

The prefabricated parts of the piping system are termed 'spools', described under 'Spools', this section. The piping group either produces isos showing the required spools, or marks the piping to be spooled on plans and elevations, depending on whether or not a model is used (as shown in chart 5.10). From these drawings, the subcontractor makes detail drawings termed 'spool sheets'. Figure 5.17 is an example spool sheet.



#### ISOMETRIC DRAWINGS, or 'ISOS'

An iso usually shows a complete line from one piece of equipment to another—see figure 5.15. It gives all information necessary for fabrication and erection of piping.

Isos are usually drawn freehand, but the various runs of pipe, fittings and valves should be roughly in proportion for easy understanding. Any one line (that is, all the piping with the same line number) should be drawn on the minimum number of iso sheets. If continuation sheets are needed, break the line at natural breakpoints such as flanges (except orifice flanges), welds at fittings, or field welds required for installation.

Items and information to be shown on an iso include:

- North arrow (plant north)
- Dimensions and angles
- Reference number of plan drawing from which iso is made (unless model is used), line number, direction of flow, insulation and tracing
- Equipment numbers and locations of equipment (by centerlines)
- Identify all items by use of an understood symbol, and amplify by a description, as necessary
- Give details of any flanged nozzles on equipment to which piping has to be connected, if the flange is different from the specification for the connected piping
- Size and type of every valve
- Size, pressure rating and instrument number of control valves
- Number, location and orientation for each instrument connection

5.2.8  
5.2.9

CHART  
5.10

FIGURE  
5.10

- Shop and field welds. Indicate limits of shop and field fabrication
- Iso sheet continuation numbers
- Unions required for installation and maintenance purposes
- On screwed and socket-welded assemblies, valve handwheel positions need not be shown
- Materials of construction
- Locations of vents, drains, and traps
- Locations of supports, identified by pipesupport number

The following information may also be given:

- Requirements for stress relieving, seal welding, pickling, lining, coating, or other special treatment of the line

Drawing style to be followed is shown in the example iso, figure 5.15, which displays some of the above points, and gives others as shaded notes. An iso may show more than one spool.

## SPOOLS

A spool is an assembly of fittings, flanges and pipe that may be prefabricated. It does not include bolts, gaskets, valves or instruments. Straight mill-run lengths of pipe over 20 ft are usually not included in a spool, as such lengths may be welded in the system on erection (on the iso, this is indicated by noting the length, and stating 'BY FIELD').

The size of a spool is limited by the fabricator's available means of transportation, and a spool is usually contained within a space of dimensions 40 ft x 10 ft x 8 ft. The maximum permissible dimensions may be obtained from the fabricator.

## FIELD-FABRICATED SPOOLS

Some States in the USA have a trades agreement that 2-inch and smaller carbon-steel piping must be fabricated at the site. This rule is sometimes extended to piping larger than 2-inch.

## SHOP-FABRICATED SPOOLS

All alloy spools, and spools with 3 or more welds made from 3-inch (occasionally 4-inch) and larger carbon-steel pipe are normally 'shop-fabricated'. This is, fabricated in the shop fabricator's workshop, either at his plant or at the site. Spools with fewer welds are usually made in the field.

Large-diameter piping, being more difficult to handle, often necessitates the use of jigs and templates, and is more economically produced in a workshop.

## SPOOL SHEETS

A spool sheet is an orthographic drawing of a spool made by the piping contractor either from plans and elevations, or from an iso—see chart 5.10.

Each spool sheet shows only one type of spool, and:—

- (1) Instructs the welder for fabricating the spool
- (2) Lists the cut lengths of pipe, fittings and flanges, etc. needed to make the spool
- (3) Gives materials of construction, and any special treatment of the finished piping
- (4) Indicates how many spools of the same type are required

## NUMBERING ISOS, SPOOL SHEETS, & SPOOLS

Spool numbers are allocated by the piping group, and appear on all piping drawings. Various methods of numbering can be used as long as identification is easily made. A suggested method follows:—

Iso sheets can be identified by the line number of the section of line that is shown, followed by a sequential number. For example, the fourth iso sheet showing a spool to be part of a line numbered 74/BZ/6/412/23 could be identified: 74/BZ/6/412/23—4.



Both the spool and the spool sheet can be identified by number or letter using the iso sheet number as a prefix. For example, the numbering of spool sheets relating to iso sheet 74/BZ/6/412/23—4 could be

74/BZ/6/412/23—4—1, 74/BZ/6/412/23—4—2, ..... etc.,  
or 74/BZ/6/412/23—4—A, 74/BZ/6/412/23—4—B, ..... etc.

The full line number need not be used if a shorter form would suffice for identification.

Spool numbers are also referred to as 'mark numbers'. They are shown on isos and on the following:—

- (1) Spool sheets—as the sheet number
- (2) The fabricated spool—so it can be related to drawings or isos
- (3) Piping drawings—plans and elevations

## DIMENSIONING

5.3

### DIMENSIONING FROM REFERENCE POINTS

5.3.1

#### HORIZONTAL REFERENCE

When a proposed plant site is surveyed, a geographic reference point is utilized from which measurements to boundaries, roads, buildings, tanks, etc., can be made. The geographic reference point chosen is usually an officially-established one.

The lines of latitude and longitude which define the geographic reference point are not used, as a 'plant north' (see figure 5.11) is established, parallel to structural steelwork. The direction closest to true north is chosen for the 'plant north'.

The coordinates of the southwest corner of the plant in figure 5.11, as referred to 'plant north', are N 110.00 and E 200.00.

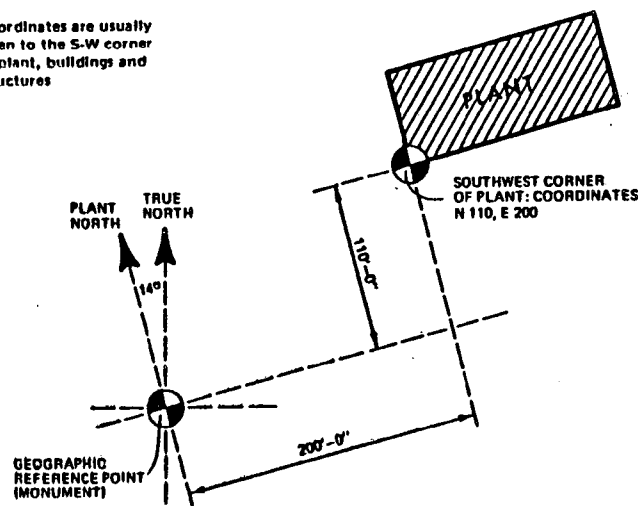
Sometimes coordinates such as those above may be written N 1+10 and E 2+00. The first coordinate is read as "one hundred plus 10 ft north" and the second as "two hundred plus zero ft east". This is a system used for traverse survey, and is more correctly applied to highways, railroads, etc.

Coordinates are used to locate tanks, vessels, major equipment and structural steel. In the open, these items are located directly with respect to a geographic reference point, but in buildings and structures, can be dimensioned from the building steel.

#### HORIZONTAL REFERENCE

FIGURE 5.11

Coordinates are usually given to the S-W corner of plant, buildings and structures



The US Department of Commerce's Coast and Geodetic Survey has established a large number of references for latitude and longitude, and for elevations above sea level. These are termed 'geodetic control stations'.

Control stations for horizontal reference (latitude and longitude) are referred to as 'triangulation stations' or 'traverse stations', etc. Control stations for vertical reference are referred to as 'benchmarks'. Latitude and longitude have not been established for all benchmarks.

A geodetic control station is marked with a metal disc showing identity and date of establishment. To provide stable locations for the discs, they are set into tops of 'monuments', mounted in holes drilled in bedrock or large firmly-imbedded boulders, or affixed to a solid structure, such as a building, bridge, etc.

The geographic positions of these stations can be obtained from the Director, US Coast and Geodetic Survey, Rockville, Maryland 20852.

#### VERTICAL REFERENCE

Before any building or erecting begins, the site is leveled ('graded') with earth-moving equipment. The ground is made as flat as practicable, and after leveling is termed 'finished grade'.

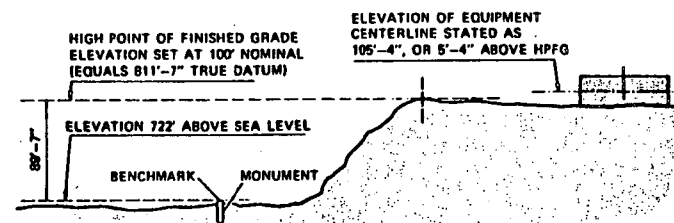
The highest graded point is termed the 'high point of finished grade', (HPFG), and the horizontal plane passing thru it is made the vertical reference plane or 'datum' from which plant elevations are given. Figure 5.12 shows that this horizontal plane is given a 'false' or nominal elevation, usually 100 ft, and is not referred to mean sea level.

The 100 ft nominal elevation ensures that foundations, basements, buried pipes and tanks, etc., will have positive elevations. 'Minus' elevations, which would be a nuisance, are thus avoided.

Large plants may have several areas, each having its own high point of finished grade. Nominal grade elevation is measured from a benchmark, as illustrated in figure 5.12.

#### VERTICAL REFERENCE

FIGURE 5.12



#### DIMENSIONING PIPING DRAWINGS

5.3.2

#### DRAWING DIMENSIONS—& TOLERANCES MAINTAINED IN ERECTED PIPING

**On plot:** Dimensions on piping drawings are normally maintained within the limits of plus or minus 1/16th inch. How this tolerance is met does not concern the designer. Any necessary allowances to ensure that dimensions are maintained are made by the fabricator and erector (contractor).

**Off plot:** Dimensions are maintained as closely as practicable by the erector.

#### WHICH DIMENSIONS SHOULD BE SHOWN?

Sufficient dimensions should be given for positioning equipment, for fabricating spools and for erecting piping. Duplication of dimensions in different views should be avoided, as this may easily lead to error if alterations are made.

Basically the dimensions to show are:

TYPE OF DIMENSION		EXAMPLES
1	REFERENCE LINE* TO CENTERLINE	VESSELS PUMPS EQUIPMENT LINES
2	CENTERLINE TO CENTERLINE	LINES STANDARD VALVES
3	CENTERLINE TO FLANGE FACE †	NOZZLES ON { VESSELS PUMPS EQUIPMENT
4	FLANGE FACE TO FLANGE FACE †	NON-STANDARD { VALVES EQUIPMENT METERS INSTRUMENTS
• REFERENCE LINE CAN BE EITHER AN ORDINATE (LINE OF LATITUDE OR LONGITUDE) OR A CENTERLINE OF BUILDING STEEL		
† IT IS NECESSARY TO SHOW THESE DIMENSIONS FOR ITEMS LACKING STANDARD DIMENSIONS (DEFINED BY ANY RECOGNIZED STANDARD)		

Figure 5.13 illustrates the use of these types of dimensions.

PLAN VIEW DIMENSIONS

Plan views convey most of the dimensional information, and may also show dimensions for elevations in the absence of an elevational view or section.

EXAMPLE DIMENSIONS FOR PLAN VIEW

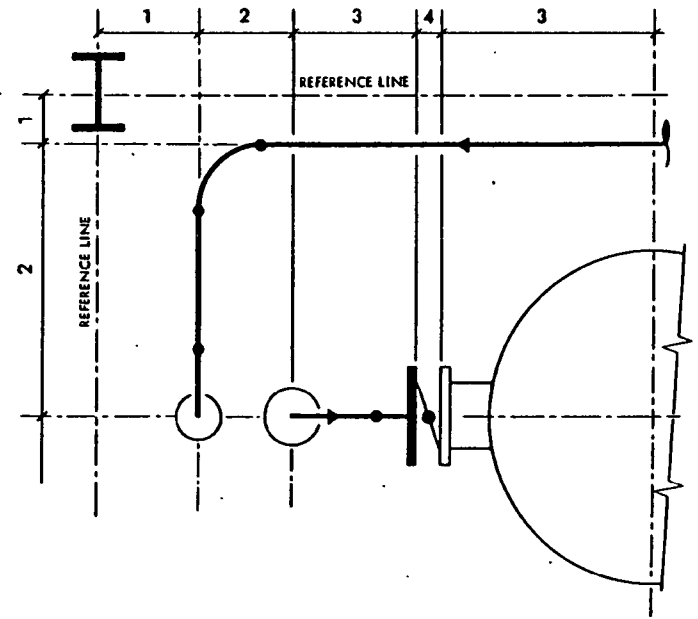
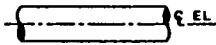

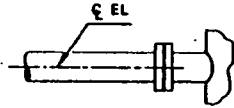
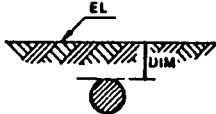


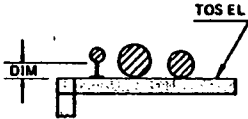
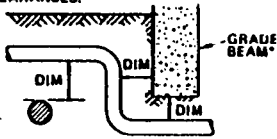



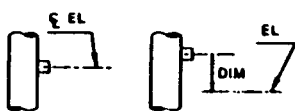


FIGURE 5.13

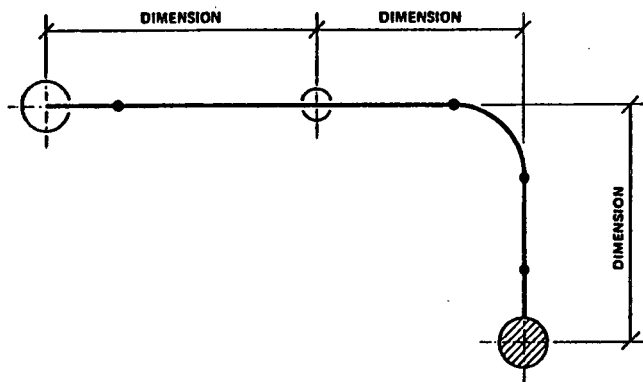
VERTICAL VIEW ELEVATIONS & DIMENSIONS

On piping drawings, elevations may be given as in table 5.2.

SHOWING ELEVATIONS		TABLE 5.2	
PIPE-GENERAL		BURIED PIPE	
SINGLE PIPE: SHOW CENTERLINE ELEVATION		BURIED LINES (IN A TRENCH): SHOW ELEVATION OF BOTTOMS OF PIPES	
SINGLE PIPE TO NOZZLE: SHOW CENTERLINE ELEVATION OF PIPE AT NOZZLE		FOR MINIMUM COVER, REFER TOP OF PIPE TO GRADE ELEVATION:	
SEVERAL PIPES SHARING A COMMON SUPPORT: SHOW ELEVATION OF BOTTOMS OF PIPES		DRAINS AND SEWERS: SHOW 'INVERT ELEVATION' (IE)	
SEVERAL PIPES ON A PIPERACK: SHOW 'TOP OF SUPPORT' ELEVATION		CLEARANCES:	
MISCELLANEOUS ELEVATIONS		*PIPES MAY BE RUN UNDER GRADE BEAMS OF BUILDINGS, BUT NOT UNDER FOUNDATIONS.	
FINISHED FLOOR: SHOW ELEVATION OF HIGH POINT OF FLOOR		VERTICAL NOZZLE: SHOW ELEVATION OF FLANGE FACE	
FOUNDATION: SHOW 'TOP OF CONCRETE', INCLUDING GROUT		INSTRUMENT POINT: SHOW ELEVATION OF CONNECTION CENTERLINE, or DIMENSION FROM NEAREST RELEVANT ELEVATION	
SHOE: DIMENSION AS SHOWN IN THE PIPERACK SKETCH ABOVE			

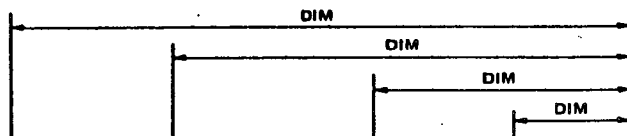
## GUIDELINES FOR DIMENSIONING ALL PIPING DRAWINGS 5.3.3

- Show all key dimensions, including elevations and coordinates
- Show dimensions outside of the drawn view unless unavoidable — do not clutter the picture
- Draw dimension lines unbroken with a fine line. Write the dimension just above a horizontal line. Write the dimension of a vertical line sideways, preferably at the left. It is usual to terminate the line with arrowheads, and these are preferable for isos. The oblique dashes shown are quicker and are suitable for plans and elevations, especially if the dimensions are cramped

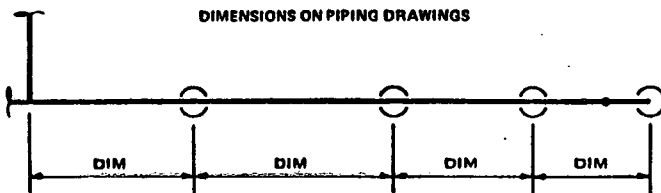


- If a series of dimensions is to be shown, string them together as shown in the sketch. (Do not dimension from a common reference line as in machine drawing.) Show the overall dimension of the string of dimensions if this dimension will be of repeated interest

DIMENSIONS ON MACHINE DRAWINGS



DIMENSIONS ON PIPING DRAWINGS



- Do not omit a significant dimension other than 'fitting makeup', even though it may be easily calculated — see 'fitting makeup', this section

- Most piping under 2-inch is screwed or socket-welded and assembled at the site (field run). Therefore, give only those dimensions necessary to route such piping clear of equipment, other obstructions, and thru walls, and to locate only those items whose safe positioning or accessibility is important to the process
- Most lengths will be stated to the nearest sixteenth of an inch. Dimensions which cannot or need not be stated to this precision are shown with a plus-or-minus sign: 8'-7"±, 15'-3"±, etc.
- Dimensions under two feet are usually marked in inches, and those over two feet in feet and inches. Some companies prefer to mark all dimensions over one foot in feet and inches
- Attempt to round off non-critical dimensions to whole feet and inches. Reserve fractions of inches for dimensions requiring this precision

## PLANS & ELEVATIONS—GENERAL DIMENSIONING POINTS

- Reserve horizontal dimensions for the plan view
- Underline all out-of-scale dimensions, or show as in chart 5.8
- If a certain piping arrangement is repeated on the same drawing, it is sufficient to dimension the piping in one instance and note the other appearances as 'TYP' (typical). This situation occurs where similar pumps are connected to a common header. For another example, see the pump base in figure 6.17
- Do not duplicate dimensions. Do not repeat them in different views

## DIMENSIONING TO JOINTS

- Do not terminate dimensions at a welded or screwed joint
- Unless necessary, do not dimension to unions, in-line couplings or any other items that are not critical to construction or operation of the piping
- Where flanges meet it is usual to show a small gap between dimension lines to indicate the gasket. Gaskets should be covered in the piping specification, with gasket type and thickness stated. Refer to the panel 'Drafting valves', preceding chart 5.6.

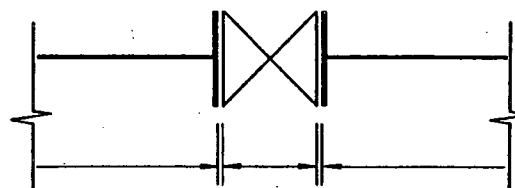


FIGURE 5.13

- As nearly all flanged joints have gaskets, a time-saving procedure is to note flanged joints without gaskets (for example, see 3.1.6 under 'Butterfly valve'). The fabricator and erector can be alerted to the need for gaskets elsewhere by a general note on all piping drawings:

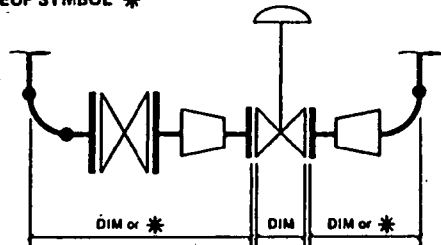
"GASKETS AS SPECIFICATION EXCEPT AS NOTED"

TABLE 5.2

## FITTING MAKEUP

If a number of items of standard dimensions are grouped together it is unnecessary to dimension each item, as the fabricator knows the sizes of standard fittings and equipment. It is necessary, however, to indicate that the overall dimension is 'fitting makeup' by the special cross symbol, or preferably by writing the overall dimension. Any non-standard item inserted between standard items should be dimensioned.

## FITTING MAKEUP SYMBOL \*



## DIMENSIONING TO VALVES

- Locate flanged and welding-end valves with ANSI standard dimensions by dimensioning to their centers. Most gate and globe valves are standard—see table V-1
- Dimension non-standard flanged valves as shown in the panel opposite chart 5.6. Although a standard exists for control valves, face-to-face dimensions are usually given, as it is possible to obtain them in non-standard sizes
- Standard flanged check valves need not be dimensioned, but if location is important, dimension to the flange face(s)
- Non-flanged valves are dimensioned to their centers or stems

## DIMENSIONING TO NOZZLES ON VESSELS & EQUIPMENT

- In plan view, a nozzle is dimensioned to its face from the centerline of the equipment it is on
- In elevation, a nozzle's centerline is either given its own elevation or is dimensioned from another reference. In the absence of an elevational view, nozzle elevations can be shown on the plan view

## DIMENSIONING ISOS

5.3.4

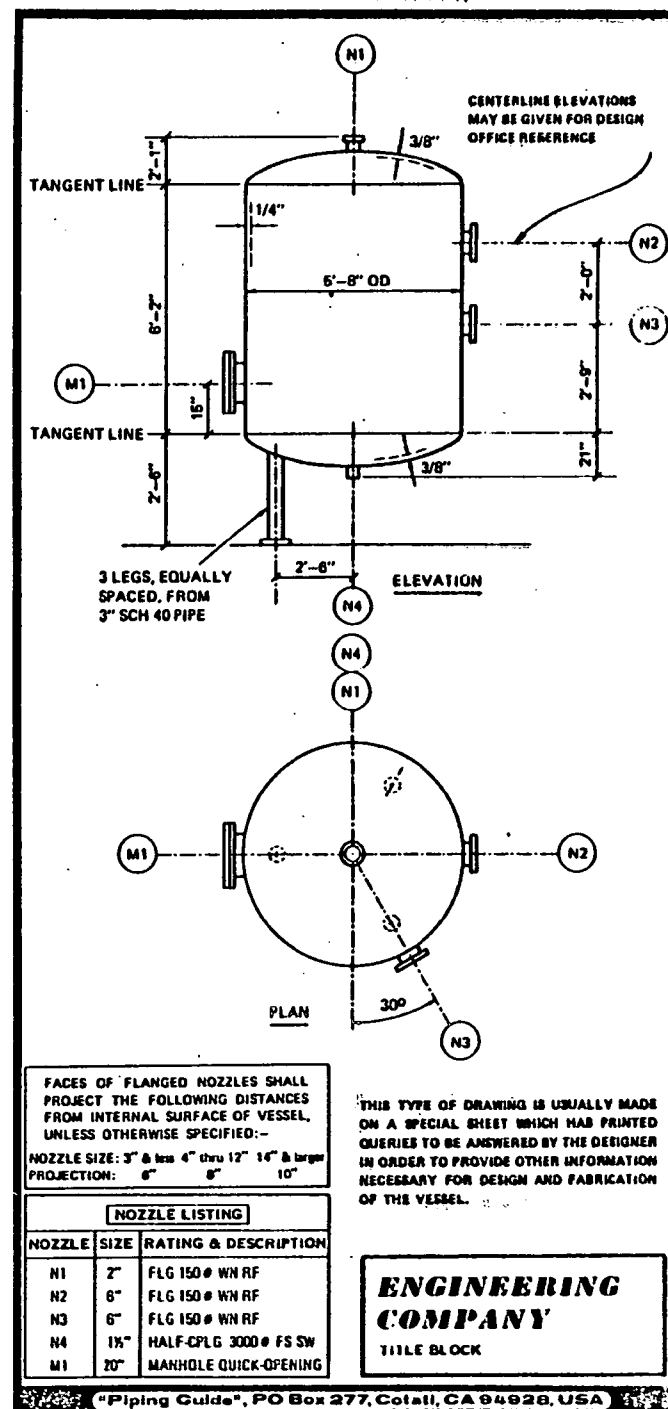
In order to clearly show all dimensions, the best aspect of the piping must be determined. Freedom to extend lines and spread the piping without regard to scale is a great help in showing isometric dimensions. The basic dimensions set out in 5.3.2, 5.3.3, and the guidelines in 5.2.9 apply.

Figure 5.15 illustrates the main requirements of an isometric drawing, and includes a dimensioned offset. Figure 5.16 shows how other offsets are dimensioned.

- Dimension in the same way as plans and elevations
- Give sufficient dimensions for the fabricator to make the spool drawings—see figure 5.17

EXAMPLE VESSEL DRAWING SHOWING DIMENSIONS REQUIRED BY VENDOR (Refer to 5.2.7)

FIGURE 5.14

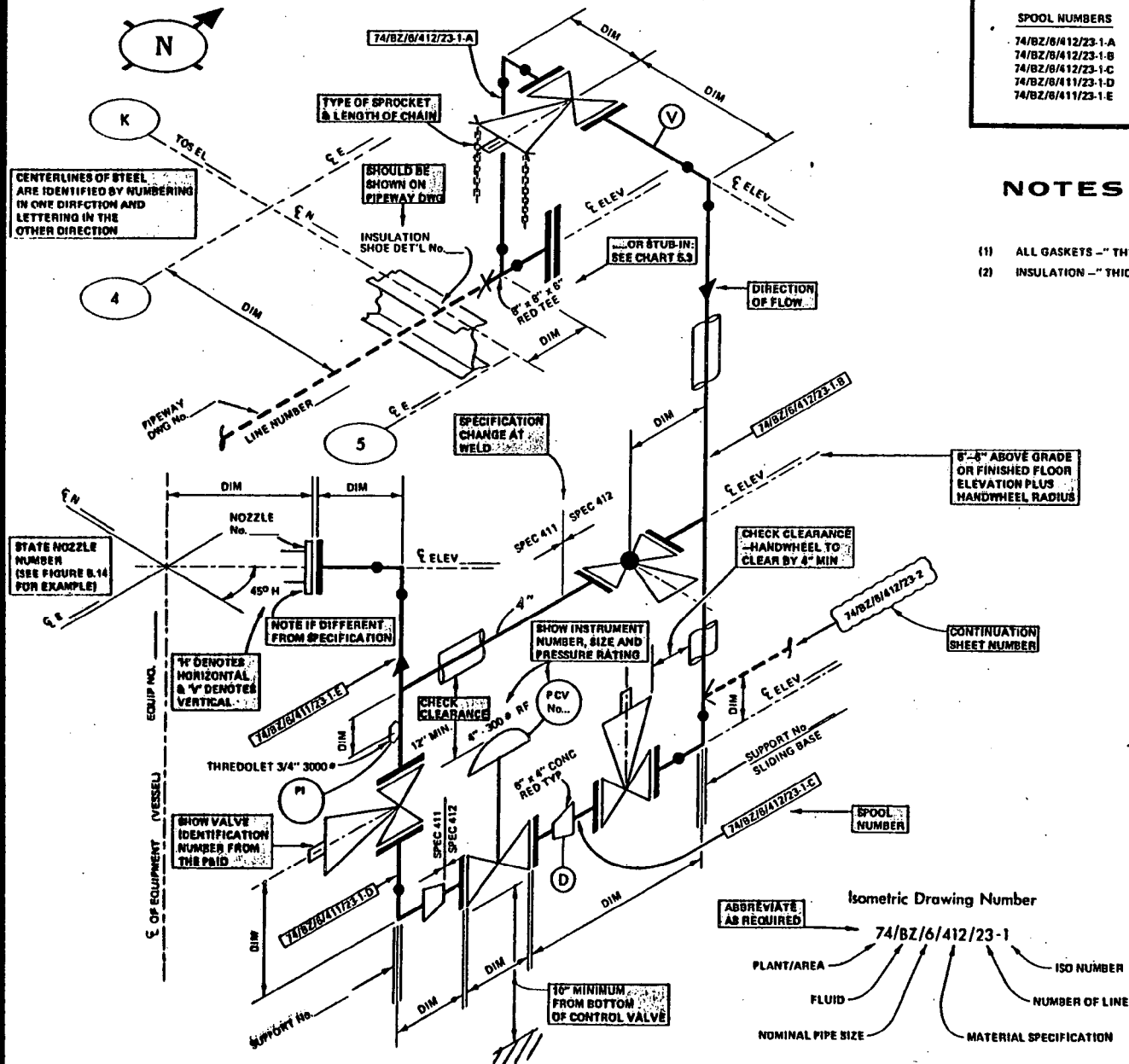




# EXAMPLE 'ISO'

# FIGURE 5.15

5.3.3  
5.3.4



FIGURES  
5.14 & 5.15

# HOW TO SHOW OFFSETS ON ISOS

(Chart M-1 gives a formula for calculating the compound angle)

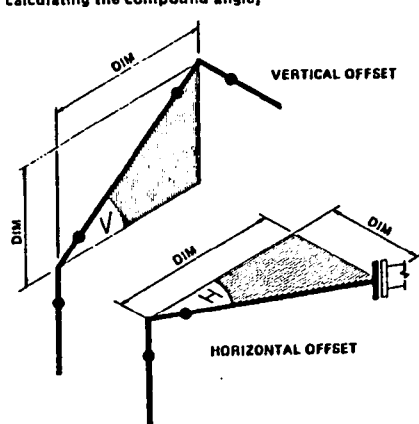


FIGURE 5.16

# DIMENSIONING SPOOLS (WELDED ASSEMBLIES)

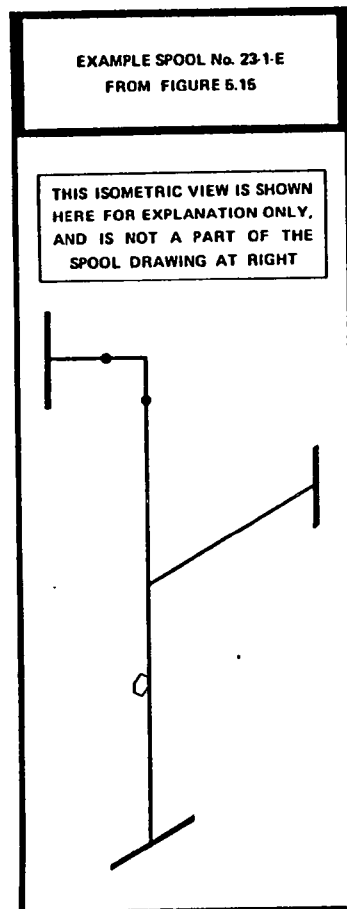
6.3.6

Allowance for weld spacing (root gap) is a shop set-up problem and should not be considered in making assembly drawings or detailed sketches. The Pipe Fabrication Institute recommends that an overall dimension is shown which is the sum of the nominal dimensions of the component parts.

A spool sheet deals with only one design of spool, and shows complete dimensional detail, lists material for making the spool, and specifies how many spools of that type are required. Figure 5.17 shows how a spool from figure 5.15 would be dimensioned.

EXAMPLE SPOOL SHEET

FIGURE 5.17



LIST OF MATERIAL			
ITEM	QTY	DESCRIPTION	MATERIAL OR REQ. NO
PIPE			
1	1	6" x 3'-10 5/8" SCH 40	A-53B
2	1	8" x 11 5/8" SCH 40	A-53B
3	1	4" x 3' 0 3/16" SCH 40	A-53B
FITTINGS			
4	1	LRELL 6" STD BW	A-234
FLANGES			
5	1	4" 300# SO	A-181 GR 1
6	2	6" 150# SO	A-181 GR 1
OTHER			
7	1	THREDOLET 3/4" 300#	A-105 GR II
ENGINEERING CO.			

REVISION	3	2	1	0
3				ISSUED FOR CONSTN.
2				
1				
0				

REFERENCE DRAWINGS (PLAN DRAWING NO. SHOWING SPOOL)			JOB NO.	ISOMETRIC REFERENCE NO.	SPOOL NO.	REV NO
DRAWN:	CHECKED:	APPROVED:	DATE:	74/82/6/412/73-1	23 1-E	0

## CHECKING & ISSUING DRAWINGS

5.4

### RESPONSIBILITIES

5.4.1

P&ID's, process flow diagrams and line designation sheets are checked by engineers in the project group.

Except for spool drawings, all piping drawings are checked by the piping group.

Orthographic spool drawings produced by the piping fabricator are not usually checked by the piping group, except for 'critical' spools, such as spools for overseas shipment and intricate spools.

Usually an experienced designer within the piping group is given the task of checking. Some companies employ persons specifically as design checkers.

The checker's responsibilities are set out in 4.1.2.

### CHECKING PIPING DRAWINGS

5.4.2

Prints of drawings are checked and corrected by marking with colored pencils. Areas to be corrected on the drawing are usually marked in red on the print. Correct areas and dimensions are usually marked in yellow.

Checked drawings to be changed should be returned to their originator whenever possible, for amendment. A new print is supplied to the checker with the original 'marked up' print for 'backchecking'.

### ISSUING DRAWINGS

5.4.3

Areas of a drawing awaiting further information or decision are ringed clearly on the reverse side and labeled 'HOLD'—refer to chart 5.8. (A black, red, or yellow china marker is suitable for film with a slick finish on the reverse side.)

Changes or revisions are indicated on the fronts of the sheets by a small triangle in the area of the revision. The revision number is marked inside the triangle, noted above the title block (or in an allocated panel) with a description of the revision, required initials, and date. The revision number may be part of the drawing number, or it may follow the drawing number (preferred method—see figure 5.17). The drawing as first issued is numbered the 'zero' revision.

A drawing is issued in three stages. The first issue is 'FOR APPROVAL', by management or client. The second issue is 'FOR CONSTRUCTION BID', when vendors are invited to bid for equipment and work contracts. The third issue is 'FOR CONSTRUCTION' following awarding of all purchase orders and contracts. Drawings may be reissued at each stage if significant changes are made. Minor changes may be made after the third stage (by agreement on cost and extent of work) but major changes may involve all three stages of issue.

## CHECKING PIPING DRAWINGS (PLANS, ELEVATIONS, & ISOS)

5.4.4

5.3.4  
4.4

Points to be checked on all piping drawings include the following:

- Title of drawing
- Number of issue, and revision number
- Orientation: North arrow against plot plan
- Inclusion of graphic scale (if drawing is to be photographically reduced)
- Equipment numbers and their appearance on piping drawings
- That correct identification appears on all lines in all views
- Line material specification changes
- Agreement with specifications and agreement with other drawings
- That the drawing includes reference number(s) and title(s) to any other relevant drawings
- That all dimensions are correct
- Agreement with certified vendors' drawings for dimensions, nozzle orientation, manholes and ladders
- That face-to-face dimensions and pressure ratings are shown for all non-standard flanged items
- Location and identification of instrument connections
- Provision of line vents, drains, traps, and tracing. Check that vents are at all high points and drains at all low points of lines for hydrostatic test. Driplegs should be indicated and detailed. Traps should be identified, and piping detailed
- The following items should be labeled in one view only: tees and ells rolled at 45 degrees (see example in 5.2.8), short-radius ell, reducing ell, eccentric reducer and eccentric swage (note on plan views whether 'top flat' or 'bottom flat'), concentric reducer, concentric swage, non-standard or companion flange, reducing tee, special items of unusual material, of pressure rating different from that of the system, etc. Refer to charts 5.3, 5.4 and 5.5 for symbol usage
- That insulation has been shown as required by the P&ID
- Pipe support locations with support numbers
- That all anchors, dummy legs and welded supports are shown
- That the stress group's requirements have been met
- That all field welds are shown
- Correctness of scale
- Coordinates of equipment against plot plan
- Piping arrangement against P&ID requirements
- Possible interferences
- Adequacy of clearances of piping from steelwork, doors, windows and braces, ductwork, equipment and major electric apparatus, including control consoles, cables from motor control centers (MCC's), and fire-fighting equipment. Check accessibility for operation and maintenance

FIGURES  
5.16 & 5.17

- That floor and wall penetrations are shown correctly
- Accessibility for operation and maintenance, and that adequate man-holes, hatches, covers, dropout and handling areas, etc. have been provided
- Foundation drawings with vendors' equipment requirements
- List of materiel, if any. Listed items should be identified once, either on the plan or the elevation drawings
- That section letters agree with the section markings on the plan view
- That drawings include necessary matchline information
- Appearance of necessary continuation sheet number(s)
- That spool numbers appear correctly
- Presence of all required signatures

This further point should be checked on isos:

- Agreement with model

These further points should be checked on spool sheets:

- That materiel is completely listed and described
- That the required number of spools of identical type is noted

## INSTRUMENTATION (As shown on P&ID's)

5.5

This section briefly describes the purposes of instruments and explains how instrumentation may be read from P&ID's. Piping drawings will *also* show the connection (coupling, etc.) to line or vessel. However, piping drawings should show only instruments connected to (or located in) piping and vessels. The only purpose in adding instrumentation to a piping drawing is to identify the connection, orifice plate or equipment to be installed on or in the piping, and to correlate the piping drawing to the P&ID.

### INSTRUMENT FUNCTION ONLY IS SHOWN

5.5.1

Instrumentation is shown on process diagrams and piping drawings by symbols. The *functions* of instruments are shown, not the instruments. Only the primary connection to a vessel or line, or devices installed in a line (such as orifice plates and control valves) are indicated on piping drawings.

There is some uniformity, among the larger companies at least, in the way in which instrumentation is shown. There is a willingness to adopt the recommendations of the Instrument Society of America, but adherence is not always complete. The ISA revised its standard S5.1, titled 'Instrumentation symbols and identification', in 1968.

Compliance with the ISA scheme is to some extent international. This is beneficial when drawings go from one country to another, as there is then no difficulty in understanding the instrumentation.

## INSTRUMENT FUNCTIONS

5.5.2

Although instruments are used for many purposes, their basic functions are few in number:

- (1) *To sense* a 'condition' of the process material, most commonly its pressure, temperature, flow rate or level. These 'conditions' are termed process variables. The piece of equipment that does the sensing is termed a 'primary element', 'sensor', or 'detector'.
- (2) *To transmit* a measure of the process variable from a primary element.
- (3) *To indicate* a measure of a process variable to the plant operator, by showing the measured value by a dial and pointer, pen and paper roll or digital display. Another form of indicator is an alarm which gives audible or visual warning when a process variable such as temperature approaches an unsafe or undesired value.
- (4) *To record* the measure of a process variable. Most recorders are electrically-operated pen-and-paper-roll types which record either the instantaneous value or the average over a time period.
- (5) *To control* the process variable. An instrument initiating this function is termed a 'controller'. A controller sustains or changes the value of the process variable by actuating a 'final control element' (this element is usually a valve, in process piping).

Many instruments combine two or more of these five functions, and may also have mechanical parts integrated — the commonest example of this is the self-contained control valve (see 3.1.10, under 'Pressure regulator', and chart 3.1).

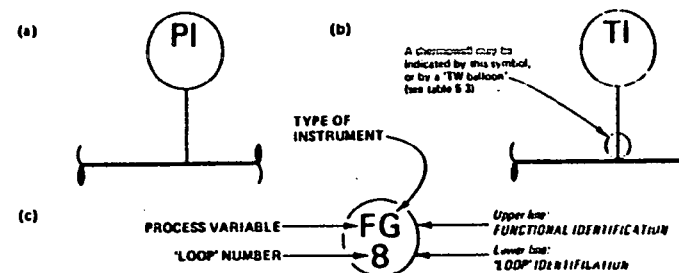
## HOW INSTRUMENTATION IS IDENTIFIED

5.5.3

The most-used instruments are pressure and temperature gages ('indicators') and are shown as in figure 5.18 (a) and (b). An example 'instrument identification number' (or 'tag number') is shown in figure 5.18 (c). The balloon around the number is usually drawn 7/16-inch diameter.

### INSTRUMENT IDENTIFICATION NUMBERS

FIGURE 5.18



In figure 5.18, 'P', 'T', and 'F' denote process variables pressure, temperature, and flow respectively. 'I' and 'G' show the type of instrument; indicator and gage respectively. Table 5.3 gives other letters denoting process variable, type of instrument, etc. The number '8', labeled 'loop number', is an example sequential number (allocated by an instrumentation engineer).

A horizontal line in the ISA balloon shows that the instrument performing the function is to be 'board mounted' in a console, etc. Absence of this line shows 'local mounting', in or near the piping, vessel, etc.

## BOARD MOUNTING



## LOCAL MOUNTING



The ISA scheme shows instrument functions, not instruments. However, a multiple-function instrument can be indicated by drawing the balloons showing the separate functions so that the circles touch.

Sometimes, a multiple-function instrument will be indicated by a single balloon symbol, with a function identification, such as 'TRC' for a temperature recorder-controller. This practice is not preferred—it is better to draw (in this example) separate 'TR' and 'TC' balloons, touching.

## INTERCONNECTED INSTRUMENTS ('LOOPS')

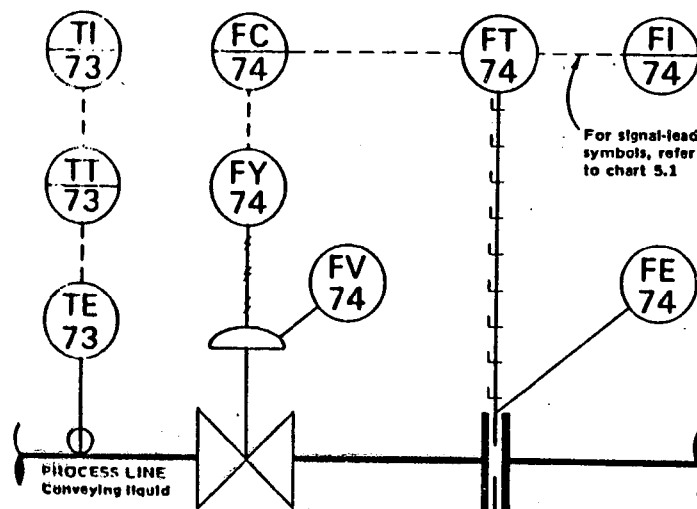
5.5.5

The ISA standard uses the term 'loop' to describe an interconnected group of instruments, which is not necessarily a closed-loop arrangement: that is, instrumentation used in a feedback (or feedforward) arrangement.

If several instruments are interconnected, they may be all allocated the same number for 'loop' identification. Figure 5.19 shows a process line served by one group of instruments (loop number 73) to sense, transmit and indicate temperature, and a second group (loop number 74) to sense, transmit, indicate, record and control flow rate.

EXAMPLE INSTRUMENT 'LOOPS'

FIGURE 5.19



For signal-lead symbols, refer to chart 5.1

## SIGNAL LEADS

5.5.6

Elements, transmitters, recorders, indicators and controllers communicate with each other by means of signal leads — which are represented by lines on the drawing. The signal can be a voltage, the pressure of a fluid, etc.—these are the most common signals.

Symbols for instrument signal leads are given in chart 5.1.

## INSTRUMENTATION CODING : ISA CODING

TABLE 5.3

PROCESS VARIABLE		TYPE OF INSTRUMENT	
ANALYSIS	A	ALARM	A
CHEMICAL COMPOSITION	A	USER'S CHOICE	B
BURNER FLAME	B	CONTROLLER	C
ELECTRICAL CONDUCTIVITY	C	CONTROL VALVE	CV
DENSITY	D	TRAP	CV
SPECIFIC GRAVITY	D	PRIMARY ELEMENT	E
FLOW RATE	F	GLASS (Sight glass)	G
LENGTH (Thickness, etc.)	G	INDICATOR	I
CURRENT (Electric)	I	CONTROL STATION	K
LEVEL	L	PILOT LIGHT	L
HUMIDITY	M	USER'S CHOICE	N
MOISTURE	M	ORIFICE	O
USER'S CHOICE	N	TEST POINT	P
USER'S CHOICE	O	RECORDER	R
PRESSURE	P	SWITCH	S
VACUUM	P	TRANSMITTER	T
RADIOACTIVITY	R	MULTIFUNCTION	U
SPEED (or Frequency)	S	VALVE	V
TEMPERATURE	T	DAMPER	V
MULTIVARIABLE	U	RUPTURE DISC	V
VISCOSITY	V	WELL	W
FORCE	W	UNCLASSIFIED	X
WEIGHT	W	RELAY	Y
UNCLASSIFIED	X	DRIVER	Z
USER'S CHOICE	Y	ACTUATOR	Z

QUALIFYING LETTER AFTER THE 'PROCESS VARIABLE' LETTER	
DIFFERENTIAL . . . D	THE QUALIFYING LETTER IS USED:— When the difference between two values of the process variable is involved
TOTAL . . . . . Q	When the process variable is to be summed over a period of time. For example, flow rate can be summed to give total volume
RATIO . . . . . F	When the ratio of two values of the process variable is involved
SAFETY ITEM . . . S	To denote an item such as a relief valve or rupture disc
'HAND' . . . . . H	To denote a hand-operated or hand-started item

QUALIFYING LETTER AFTER THE 'TYPE OF INSTRUMENT' LETTER	
HIGH . . . . . H	To denote instrument action on 'high' set value of the process variable
INTERMEDIATE. . . M	To denote instrument action on 'intermediate' set value of the process variable
LOW . . . . . L	To denote instrument action on 'low' set value of the process variable

FIGURES  
5.18 & 5.19TABLE  
5.3

## LISTING PIPING MATERIEL ON DRAWINGS

5.6

In the engineering construction industry, it is usual for piping components to be given a code number which appears in the piping specification. In companies not primarily engaged in plant construction, materiel is frequently listed on drawings.

### DIFFERENT FORMS OF LIST

5.6.1

This list is usually titled 'list of materiel', or preferably, 'list of material', as items of hardware are referred to. 'Parts list' and 'Bill of materiel' are alternate headings.

Either a separate list can be made for materiel on several drawings, or each drawing sheet can include a list for items on the particular drawing. Lists on drawings are written in the space above the title block. Column headings normally used for the list are:

LIST OF MATERIEL			
ITEM NUMBER	QUANTITY	DESCRIPTION	REMARK, REQUISITION NUMBER, OR COMPANY CODE

### SUGGESTED LISTING SCHEME

5.6.2

Vessels, pumps, machinery and instruments are normally listed separately from piping hardware. However, it is not uncommon, on small projects or revamp work, to list all materiel on a drawing.

### CLASSIFICATION FOR PIPING COMPONENTS

CHART 5.11

CLASS	INTENDED DUTY OF HARDWARE WITH RESPECT TO FLUID		EXAMPLE HARDWARE
I	CONVEYANCE: To provide a path for fluid flow		Pipe, fittings, ordinary flanges, bolt and gasket sets
II	FLOW CONTROL: To produce a large change in flow rate or pressure of fluid	(A) Non-powered	In-line valve, orifice plate, venturi
		(B) Powered	Pump, ejector
III	SEPARATION: To remove material by mechanical means from the fluid		Steam trap, discharge valve, safety or relief valve, screen, strainer
IV	HEATING OR COOLING: To change the temperature of the fluid by adding or removing heat		Jacketed pipe, tracer
V	MEASUREMENT: To measure a variable of the fluid, such as flow rate, temperature, pressure, density, viscosity, turbidity, color		Gages (all types), thermometers (all types), flow meter, densitometer, sensor housing (such as a thermowell) and other special fittings for instruments
VI	NONE: Ancillary hardware		Insulation, reinforcement, hanger, support

Haphazard listing of items makes reference troublesome. The scheme suggested in chart 5.11 is based on the duty of the hardware and can be extended to listing equipment if desired. Items of higher pressure rating and larger size can be listed first within each class.

### LISTING SPECIFIC ITEMS

5.6.3

Under the heading DESCRIPTION, usually the size of the item is stated first. A typical order is: SIZE (in inches), RATING (pressure, schedule number, etc.) NAME (of item), MATERIAL (ASTM or other material specification), and FEATURE (design feature).

Descriptions are best headed by the NAME of the item, followed by the SIZE, RATING, FEATURE(S), and MATERIAL. Materiel listings are now often handled by data-processing machines, and heading a description by the name of the item is of assistance in handling the data. The description for 'pipe' is detailed.

### EXAMPLE LISTING FOR PIPE

- NAME: State 'PIPE'
- SIZE: Specify nominal pipe size. See 2.1.3 and table P-1
- RATING: Specify wall thickness as either a schedule number, a manufacturers' weight, etc. See table P-1. SCH=schedule, STD= standard, XS= extra-strong, XXS= double-extra-strong, L= light, API= American Petroleum Institute.
- FEATURE: Specify design feature(s) unless covered by a pipe specification for the project.  
Pipe is available seamless or with a welded seam—examples of designations are: SMLS = seamless, FBW = furnace-butt-welded, ERW = electric-resistance-welded GALV = galvanized. Specify ends: T&C = threaded and coupled, BE = beveled end, PE = plain end.
- MATERIAL: Carbon-steel pipe is often ordered to ASTM A53 or A106, Grade A or B. Other specifications are given in tables 7.4 and 2.1.

### POINTS TO CHECK WHEN MAKING THE LIST

5.6.4

- See that all items in the list have been given a sequential item number
- Label the items appearing on the piping drawings with the item number from the list. Write the item number in a circle with a fine line or arrow pointing to the item on the drawing. Each item in the list of materiel is indicated in this way once on the plan or elevational piping drawings
- Verify that all data on the list agree with:
  - Requirements set out in piping drawings
  - Available hardware in the manufacturers' catalogs

# DESIGN:

6	.1 .1.1
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## ARRANGEMENT, SUPPORT, INSULATION, HEATING, VENTING & DRAINING OF PIPING SYSTEMS, VESSELS, & EQUIPMENT

### ARRANGING PIPING

6.1

#### GUIDELINES & NOTES

6.1.1

*Simple arrangements and short lines minimize pressure drops and lower pumping costs.*

Designing piping so that the arrangement is 'flexible' reduces stresses due to mechanical or thermal movement—refer to figure 6.1 and 'Stresses on piping', this section.

Inside buildings, piping is usually arranged parallel to building steelwork to simplify supporting and improve appearance.

Outside buildings, piping can be arranged: (1) On piperacks. (2) Near grade on sleepers. (3) In trenches. (4) Vertically against steelwork or large items of equipment.

#### PIPING ARRANGEMENT

- Use standard available items wherever possible
- Do not use miters unless directed to do so
- Do not run piping under foundations. (Pipes may be run under grade beams)
- Piping may have to go thru concrete floors or walls. Establish these points of penetration as early as possible and inform the group concerned (architectural or civil) to avoid cutting existing reinforcing bars
- Preferably lay piping such as lines to outside storage, loading and receiving facilities, at grade on pipe sleepers (see figure 6.3) if there is no possibility of future roads or site development

- Avoid burying steam lines that pocket, due to the difficulty of collecting condensate. Steam lines may be run below grade in trenches provided with covers or (for short runs) in sleeves
- Lines that are usually buried include drains and lines bringing in water or gas. Where long cold winters freeze the soil, burying lines below the frost line may avoid the freezing of water and solutions, saving the expense of tracing long horizontal parts of the lines
- Include removable flanged spools to aid maintenance, especially at pumps, turbines, and other equipment that will have to be removed for overhaul
- Take gas and vapor branch lines from tops of headers where it is necessary to reduce the chance of drawing off condensate (if present) or sediment which may damage rotating equipment
- Avoid pocketing lines—arrange piping so that lines drain back into equipment or into lines that can be drained
- Vent all high points and drain all low points on lines — see figure 6.47. Indicate vents and drains using symbols in chart 5.7. Carefully-placed drains and valved vents permit lines to be easily drained or purged during shutdown periods: this is especially important in freezing climates and can reduce winterizing costs

#### ARRANGE FOR SUPPORTING

- Group lines in pipeways, where practicable
- Support piping from overhead, in preference to underneath
- Run piping beneath platforms, rather than over them

#### REMOVING EQUIPMENT & CLEANING LINES

- Provide union- and flanged joints as necessary, and in addition use crosses instead of elbows, to permit removing material that may solidify

CHART 5.11
---------------

## CLEARANCES & ACCESS

- Route piping to obtain adequate clearance for maintaining and removing equipment
- Locate within reach, or make accessible, all equipment subject to periodic operation or inspection – with special reference to check valves, pressure relief valves, traps, strainers and instruments
- Take care to not obstruct access ways – doorways, escape panels, truckways, walkways, lifting wells, etc.
- Position equipment with adequate clearance for operation and maintenance. Clearances often adopted are given in table 6.1. In some circumstances, these clearances may be inadequate—for example, with shell-and-tube heat exchangers, space must be provided to permit withdrawal of the tubes from the shell

CLEARANCES & DIMENSIONS*		TABLE 6.1
<b>MINIMUM CLEARANCES</b>		
<b>HORIZONTAL CLEARANCES:</b>	Operating space around equipment †	2ft 6in.
	Centerline of railroad to nearest obstruction: (1) Straight track	8ft 6in.
	(2) Curved track	9ft 6in.
	Manhole to railing or obstruction	3ft 0in.
<b>VERTICAL CLEARANCES:</b>	Over walkway, platform, or operating area	6ft 6in.
	Over stairway	7ft 0in.
	Over high point of plant roadway:	
	(1) Minor roadway	17ft 0in.
	(2) Major roadway	20ft 0in.
	Over railroad from top of rail	22ft 6in.
<b>MINIMUM HORIZONTAL DIMENSIONS</b>		
	Width of walkway at floor level	3ft 0in.
	Width of elevated walkway or stairway	2ft 6in.
	Width of rung of fixed ladder See chart P-2.	16in.
	Width of way for forklift truck	8ft 0in.
<b>VERTICAL DIMENSIONS</b>		
	Railing. Top of floor, platform, or stair, to: (1) Lower rail	1ft 9in.
	(2) Upper rail	3ft 6in.
	Manhole centerline to floor	3ft 0in.
	Valves: See table 6.2 and chart P-2.	
<small>*In laying out a plant, reference should be made to the Federal "Occupational safety and health standard", 1971, US Department of Labor (which may give smaller dimensions than above), to the Uniform Building Code, and to regulations by individual States. For tank spacings, refer to table 6.11, to the NFPA "National fire codes" (volume 1, etc.), to the API Standard 2510 for LPG installations, and to the Oil Insurance Association's standards for minimum spacings, No. 63 (1964).          †Equipment such as heat exchangers, compressors and turbines will require additional clearance. Check manufacturers' drawings to determine particular space requirements. Refer to figure 6.33 and table 6.6 for spacing heat exchangers.</small>		

- Establish sufficient headroom for ductwork, essential electrical runs, and at least two elevations for pipe run north-south and east-west (based on clearance of largest lines, steelwork, ductwork, etc.—see figure 6.49)
- Elevations of lines are usually changed when changing horizontal direction where lines are grouped together or are in a congested area, so as not to block space where future lines may have to be routed

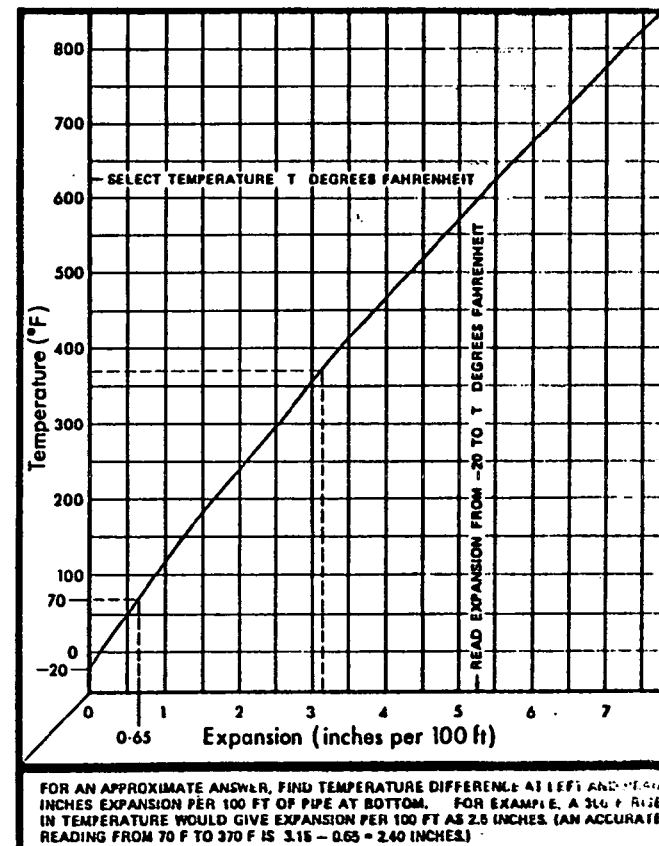
- Stagger flanges, with 12-inch minimum clearance from supporting steel
- Keep field welds and other joints at least 3 inches from supporting steel, building siding or other obstruction. Allow room for the joint to be made
- Allow room for loops and other pipe arrangements to cope with expansion by early consultation with staff concerned with pipe stressing. Notify the structural group of any additional steel required to support such loops

## THERMAL MOVEMENT

Maximum and minimum lengths of a pipe run will correspond to the temperature extremes to which it is subjected. The amount of expansion or shrinkage in steel per degree change in temperature ('coefficient of expansion') is approximately the same – that is, the expansion from 40F to 41F is about the same as from 132 F to 133 F, or from 179 F to 180 F, etc. Chart 6.1 gives changes in line length for changes in temperature.

EXPANSION OF CARBON-STEEL PIPE

CHART 6.1





FLEXIBILITY		FIGURE 6.1
RIGID	FLEXIBLE	
		In current practice, loops are made from straight pipe and elbows in nearly all circumstances. The legs perpendicular to the run give flexibility.
		On piperacks, arrange lines subject to thermal movement to one side with larger lines outermost so that larger loops can be provided for them, and so that all loops can be made over the piperack to save space.
		Offsetting the run gives flexibility which increases with the length of the offset
		Rigid connections between tanks and vessels or other connected equipment are to be avoided if: (1) There is likely to be large changes in temperature due to the process or to climate (2) The tanks or equipment are placed in the open on separate foundations which are liable to settle
		In both arrangements, the pump is used to circulate liquid in the tanks or vessels. The flexible arrangement reduces stresses on nozzles and also permits access between the units.
SOME FLEXIBILITY	MORE FLEXIBILITY	
		In turning corners, an offset limb gives a limited flexibility to the piping. The longer the offset, the greater the flexibility.
		The extra limb in the more flexible arrangement allows greater thermal movement between branch and run.
		These are two arrangements using a loop at a corner. Greater flexibility is gained by making one of the runs form one limb of the loop—this arrangement also saves an elbow and two welds.

"Piping Guide", PO Box 277, Cotati, CA 94928, USA

## STRESSES ON PIPING

**THERMAL STRESSES** Changes in temperature of piping, due either to change in temperature of the environment or of the conveyed fluid, cause changes in length of the piping. This expansion or contraction in turn causes strains in piping, supports and attached equipment.

**SETTLEMENT STRAINS** Foundations of large tanks and heavy equipment may settle or tilt slightly in the course of time. Connected piping and equipment not on a common foundation will be stressed by the displacement.

References [12, p.388] and [33, p.247] give methods for calculating working pressures, stresses and strength of pipe.

## FLEXIBILITY IN PIPING

To reduce strains in piping caused by substantial thermal movement, flexible and expansion joints may be used. However, the use of these joints may be minimized by arranging piping in a flexible manner, as illustrated in figure 6.1. Pipe can flex in a direction perpendicular to its length: thus, the longer an offset, or the deeper a loop, the more flexibility is gained.

## COLD SPRING

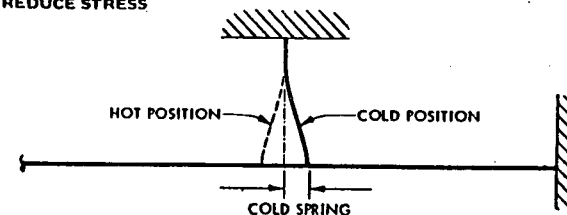
Cold springing of lines should be avoided if an alternate method can be used. A line may be cold sprung to reduce the amplitude of movement from thermal expansion or contraction in order: (a) To reduce stress on connections. (b) To avoid an interference.

Figure 6.2 schematically illustrates the use of cold springing for both purposes. Cold springing in example (a) consists of making the branch in the indicated cold position, which divides thermal movement between the cold and hot positions. In example (b) the cold spring is made equal to the thermal movement.

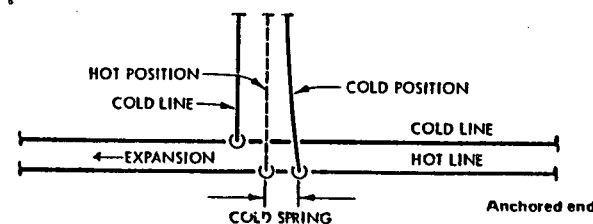
## COLD SPRINGING

FIGURE 6.2

### (a) TO REDUCE STRESS



### (b) TO AVOID AN INTERFERENCE



6.1.1

CHART  
6.1

FIGURES  
6.1-6.2

TABLE  
6.1

In the following example, cold springing is employed solely to reduce a stress:

A long pipe connected by a 90-degree elbow and flange to a nozzle may on heating expand so that it imposes a load on the nozzle in excess of that recommended. Assume that piping to the nozzle has been installed at ambient temperature, and that the pipe expands 0.75 inch when hot material flows thru it, putting a lateral (sideways) load of 600 lb on the nozzle.

If the pipe had 0.375 inch of its length removed before connection, the room-temperature lateral load on the nozzle would be about 300 lb (instead of zero), and the hot load would be reduced to about 300 lb.

The fraction of the expansion taken up can be varied. A cold spring of 50% of the expansion between the temperature extremes gives the most benefit in reducing stress. Cold springing is not recommended if an alternate solution can be used. Refer to chapter 3 of the Code for Pressure Piping, ANSI B 31.1-1955, or p.28 of the later version, ANSI B31.1.0-1967.

#### RESISTANCE OF PIPING TO FLOW

All piping has resistance to flow. The smaller the flow cross section and the more abrupt the change in direction of flow, the greater is the resistance and loss of pressure. For a particular line size the resistance is proportional to the length of pipe, and the resistance of fittings, valves, etc. may be expressed as a length of pipe having the same resistance to flow. Table F-10 gives such equivalent lengths of pipe for fittings, valves, etc.

Table F-11 gives pressure drops for water flowing thru SCH 40 pipe at various rates. Charts to determine the economic size (NPS) of piping are given in the Chemical Engineer's Handbook [8], and on page 134 of reference [20].

#### SLIDERULE FOR FLOW PROBLEMS

Problems of resistance to flow can be quickly solved with the aid of the slide-rule calculator obtainable from Tube Turns Division of Chemetron Corporation, PO Box 987, Louisville, KY 40201.

#### PIPERACKS

##### 6.1.2

A 'pipeway' is the space allocated for routing several parallel adjacent lines. A 'piperack' is a structure in the pipeway for carrying pipes and is usually fabricated from steel, or concrete and steel, consisting of connected  $\square$ -shaped frames termed 'bents' on top of which the pipes rest. The vertical members of the bents are termed 'stanchions'. Figure 6.3 shows two piperacks using this form of construction, one of which is 'double-decked'. Piperacks for only two or three pipes are made from 'T'-shaped members, termed 'tee-head supports'.

Piperacks are expensive, but are necessary for arranging the main process and service lines around the plant site. They are made use of in secondary ways, principally to provide a protected location for ancillary equipment.

Pumps, utility stations, manifolds, fire-fighting and first-aid stations can be located under the piperack. Lighting and other fixtures can be fitted to stanchions. Air-cooled heat exchangers can be supported above the piperack.

The smallest size of pipe run on a piperack without additional support is usually 2 inch. It may be more economic to change proposed small lines to 2-inch pipe, or to suspend them from 4-inch or larger lines, instead of providing additional support.

Table S-1 and charts S-2 give stress and support data for spans of horizontal pipe.

### KEY FOR FIGURE 6.3

- (1) WHEN USING A DOUBLE DECK, IT IS CONVENTIONAL TO PLACE UTILITY AND SERVICE PIPING ON THE UPPER LEVEL OF THE PIPERACK
- (2) DO NOT RUN PIPING OVER STANCHIONS AS THIS WILL PREVENT ADDING ANOTHER DECK
- (3) PLACE LARGE LIQUID-FILLED PIPES NEAR STANCHIONS TO REDUCE STRESS ON HORIZONTAL MEMBERS OF BENTS. HEAVY LIQUID-FILLED PIPES (12-IN AND LARGER) ARE MORE ECONOMICALLY RUN AT GRADE—SEE NOTE (12)
- (4) PROVIDE DISTRIBUTED SPACE FOR FUTURE PIPES—APPROXIMATELY AN ADDITIONAL 25 PERCENT (THAT IS, 20 PERCENT OF FINAL WIDTH SEE TABLES A-1)
- (5) HOT PIPES ARE USUALLY INSULATED AND MOUNTED ON SHOES
- (6) WARM PIPES MAY HAVE INSULATION LOCALLY REMOVED AT SUPPORTS
- (7) THE HEIGHT OF A RELIEF HEADER IS FIXED BY ITS POINT OF ORIGIN AND THE SLOPE REQUIRED TO DRAIN THE LINE TO A TANK, ETC.
- (8) ELECTRICAL AND INSTRUMENT TRAYS (FOR CONDUIT) AND CABLES ARE BEST PLACED ON OUTRIGGERS OR BRACKETS AS SHOWN, TO PRESENT THE LEAST PROBLEM WITH PIPES LEAVING THE PIPEWAY. ALTERNATELY, TRAYS MAY BE ATTACHED TO THE STANCHIONS
- (9) WHEN CHANGE IN DIRECTION OF A HORIZONTAL LINE IS MADE, IT IS BEST ALSO TO MAKE A CHANGE OF ELEVATION (EITHER UP OR DOWN). THIS AVOIDS BLOCKING SPACE FOR FUTURE LINES. 90-DEGREE CHANGES IN DIRECTION OF THE WHOLE PIPEWAY OFFER THE OPPORTUNITY TO CHANGE THE ORDER OF LINES. A SINGLE DECK IS SHOWN AT AN INTER-MEDIATE ELEVATION
- (10) SOMETIMES INTERFACES ARE ESTABLISHED TO DEFINE BREAKPOINTS FOR CONTRACTED WORK (WHERE ONE CONTRACTOR'S PIPING HAS TO JOIN WITH ANOTHERS). AN INTERFACE IS AN IMAGINARY PLANE WHICH MAY BE ESTABLISHED FAR ENOUGH FROM A WALL, SIDING, PROCESS UNIT, OR STORAGE UNIT TO ENABLE CONNECTIONS TO BE MADE
- (11) PIPES SHOULD BE RACKED ON A SINGLE DECK IF SPACE PERMITS
- (12) PIPING SHOULD BE SUPPORTED ON SLEEPERS AT GRADE IF ROADS, WALKWAYS, ETC., WILL NOT BE REQUIRED OVER THE PIPEWAY AT A LATER DATE. PIPING 'AT GRADE' SHOULD BE 12 INCHES OR MORE ABOVE GRADE
- (13) CURRENT PRACTICE IS TO SPACE BENTS 20-25 FEET APART. THIS SPACING IS A COMPROMISE BETWEEN THE ACCEPTABLE DEFLECTIONS OF THE SMALLER PIPES AND THE MOST ECONOMIC BEAM SECTION DESIRED FOR THE PIPERACK. PIPERACKS ARE USUALLY NOT OVER 25 FEET IN WIDTH. IF MORE ROOM IS NEEDED, THE PIPERACK IS DOUBLE- OR TRIPLE-DECKED
- (14) MINIMUM CLEARANCE UNDERNEATH THE PIPERACK IS DETERMINED BY AVAILABLE MOBILE LIFTING EQUIPMENT REQUIRING ACCESS UNDER THE PIPERACK. VERTICAL CLEARANCES SHOULD BE AS SET OUT IN TABLE 6.1 BUT CANNOT NECESSARILY BE ADHERED TO AS ELEVATIONS OF PIPES AT INTERFACES ARE SOMETIMES FIXED BY PLANT SUBCONTRACTORS. IF THIS SITUATION ARISES, THE PIPING GROUP SHOULD ESTABLISH MAXIMUM AND MINIMUM ELEVATIONS WHICH THE PIPING SUBCONTRACTORS MUST WORK TO—THIS HELPS TO AVOID PROBLEMS AT A LATER DATE. CHECK THE MINIMUM HEIGHT REQUIRED FOR ACCESS WHERE THE PIPERACK RUNS PAST A UNIT OR PLANT ENTRANCE
- (15) WHEN SETTING ELEVATIONS FOR THE PIPERACK, TRY TO AVOID POCKETS IN THE PIPING. LINES SHOULD BE ABLE TO DRAIN INTO EQUIPMENT OR LINES THAT CAN BE DRAINED
- (16) GROUP HOT LINES REQUIRING EXPANSION LOOPS AT ONE SIDE OF THE PIPERACK FOR EASE OF SUPPORT—SEE FIGURE 6.1
- (17) LOCATE UTILITY STATIONS, CONTROL (VALVE) STATIONS, AND FIREHOSE POINTS ADJACENT TO STANCHIONS FOR SUPPORTING
- (18) LEAVE SPACE FOR DOWNCOMERS TO PUMPS, ETC., BETWEEN PIPERACK AND ADJACENT BUILDING OR STRUCTURE

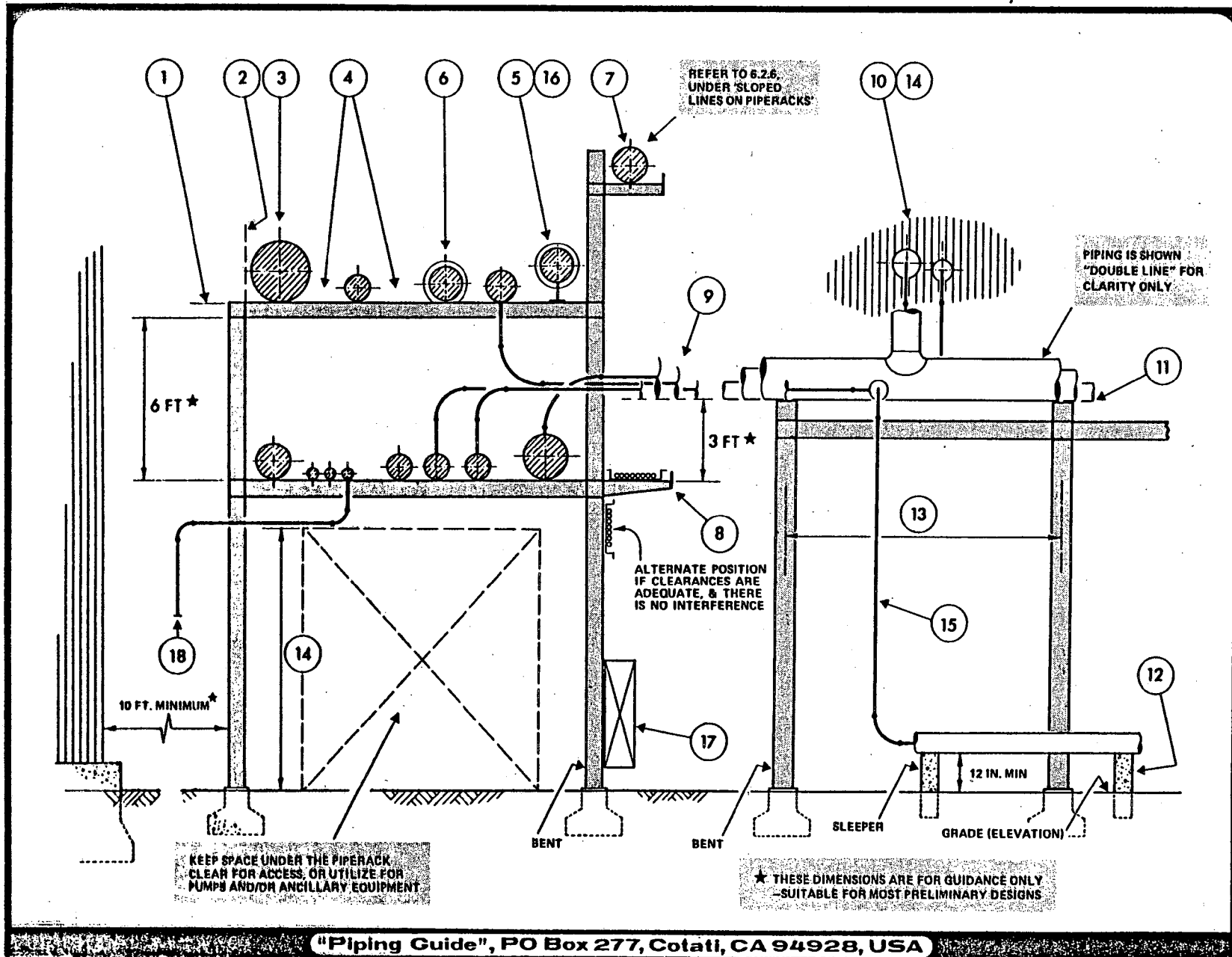


FIGURE 6.3

Valves are used for these purposes:

- (1) Process control during operation
- (2) Controlling services and utilities—steam, water, air, gas and oil
- (3) Isolating equipment or instruments, for maintenance
- (4) Discharging gas, vapor or liquid
- (5) Draining piping and equipment on shutdown
- (6) Emergency shutdown in the event of plant mishap or fire

#### WHICH SIZE VALVE TO USE ?

Nearly all valves will be line size — one exception is control valves, which are usually one or two sizes smaller than line size; never larger.

At control stations and pumps it has been almost traditional to use line-size isolating valves. However, some companies are now using isolating valves at control stations the same size as the control valve, and at pumps are using 'pump size' isolating valves at suction and discharge. The choice is usually an economic one made by a project engineer.

The sizes of bypass valves for control stations are given in 6.1.4, under 'Control (valve) stations'.

#### WHERE TO PLACE VALVES

See 6.3.1 for valving pumps, under 'Pump emplacement & connections'.

- Preferably, place valves in lines from headers (on piperacks) in horizontal rather than vertical runs, so that lines can drain when the valves are closed. (In cold climates, water held in lines may freeze and rupture the piping: such lines should be traced — see 6.8.2)
- To avoid spooling unnecessary lengths of pipe, mount valves directly onto flanged equipment, if the flange is correctly pressure-rated. See 6.5.1 under 'Nozzle loading'
- A relief valve that discharges into a header should be placed higher than the header in order to drain into it
- Locate heavy valves near suitable support points. Flanges should be not closer than 12 inches to the nearest support, so that installation is not hampered
- For appearance, if practicable, keep centerlines of valves at the same height above floor, and in-line on plan view

#### OPERATING ACCESS TO VALVES

- Consider frequency of operation when locating manually-operated valves
- Locate frequently-operated valves so they are accessible to an operator from grade or platform. Above this height and up to 20 ft, use chain operators or extension stem. Over 20 ft, consider a platform or remote operation

ORDER OF PREFERENCE FOR VALVE LOCATION	STEM CENTERLINE ELEVATION FOR HORIZONTAL VALVES		HANDWHEEL ELEVATION FOR VERTICAL VALVES (upright, closed)	MINIMUM ELEVATION OF HANDWHEEL RIM FOR TILTED VALVES (handwheel overhead)	
	OPERATING	MAINTENANCE		ANGLE OF STEM FROM VERTICAL	MINIMUM ELEVATION
1st	3'-6" to 4'-6"	3'-6" to 4'-6"	3'-0" to 4'-3"		
2nd	2'-0" to 3'-6"	1'-0" to 3'-6"	2'-0" to 3'-0"		
3rd (HEAD HAZARD) ½ handwheel diameter	4'-6" to 6'-6" and 6'-0" to 7'-6"	4'-6" to 7'-6"		30°	5'-0"
				45°	5'-6"
				60°	6'-0"
ACCEPTABLE FOR 1-INCH AND SMALLER VALVES	0'-6" to 2'-0"				

\* REFER TO CHART P-3 IN PART II  
 † TO MINIMIZE HAZARD TO PERSONNEL IF VALVES ARE TO BE LOCATED AT HEIGHTS WITHIN 2nd AND 3rd CHOICES, AVOID POINTING STEMS INTO WALKWAYS AND WORKING AREAS. TRY TO PLACE VALVES CLOSE TO WALLS OR LARGE ITEMS WHICH ARE CLEARLY SEEN.

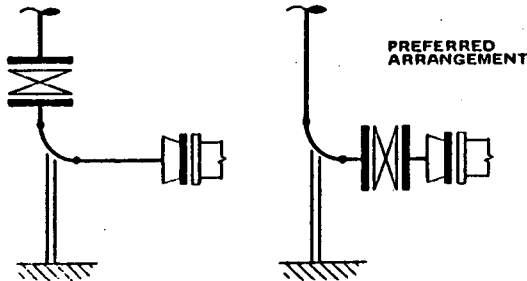
- Infrequently-used valves can be reached by a ladder—but consider alternatives
- Do not locate valves on piperacks, unless unavoidable
- Group valves which would be out of reach so that all can be operated by providing a platform, if automatic operators are not used
- If a chain is used on a horizontally-mounted valve, take the bottom of the loop to within 3 ft of floor level for safety, and provide a hook nearby to hold the chain out of the way—see 3.1.2, under 'Chain'
- Do not use chain operators on screwed valves, or on any valve 1½-inches and smaller
- With lines handling dangerous materials it is better to place valves at a suitably low level above grade, floor, platform, etc., so that the operator does not have to reach above head height

#### ACCESS TO VALVES IN HAZARDOUS AREAS

- Locate main isolating valves where they can be reached in an emergency such as an outbreak of fire or a plant mishap. Make sure that personnel will be able to reach valves easily by walkway or automobile
- Locate manually-operated valves at the plant perimeter, or outside the hazardous area
- Ensure that automatic operators and their control lines will be protected from the effects of fire
- Make use of brick or concrete walls as possible fire shields for valve stations
- Inside a plant, place isolating valves in accessible positions to shut feed lines for equipment and processes having a fire risk
- Consider the use of automatic valves in fire-fighting systems to release water, foam and other fire-fighting agents, responding to heat-fusible links, smoke detectors, etc., triggered by fire or undue rise in temperature—advice may be obtained from the insurer and the local fire department

## MAKE MAINTENANCE SIMPLE

- Provide access for mobile lifting equipment to handle heavy valves
- Consider providing lifting davits for heavy valves difficult to move by other means, if access is restricted
- If possible, arrange valves so that supports will not be on removable spools:



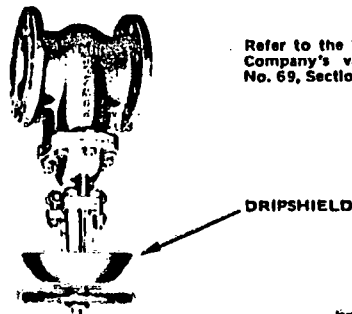
- A plug valve requiring lubrication must be easily accessible, even though it may not be frequently operated

## MAKE MAINTENANCE SAFE

- Use line-blind valves, spectacle plates or the 'double block and bleed' where positive shutoff is required either for maintenance or process needs – see 2.7

## ORIENTATION OF VALVE STEMS

- Do not point valve stems into walkways, truckways, ladder space, etc.
- Unless necessary, do not arrange gate and globe valves with their stems pointing downward (at *any* angle below the horizontal), as:—
  - (1) Sediment may collect in the gland packing and score the stem.
  - (2) A projecting stem may be a hazard to personnel.
- If an inverted position is necessary, consider employing a dripshield:



Refer to the William Powell Company's valve catalog, No. 69, Section 19, page 353

(COURTESY POWELL VALVE COMPANY)

## CLOSING DOWN LINES

Consider valve-closing time in shutting down or throttling large lines. Rapid closure of the valve requires rapid dissipation of the liquid's kinetic energy, with a risk of rupturing the line. Long-distance pipelines present an example of this problem.

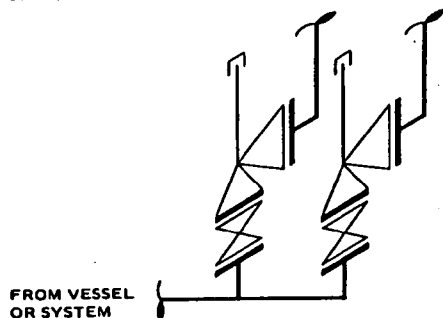
A liquid line fitted with a fast-closing valve should be provided with a standpipe upstream and close to the valve to absorb the kinetic energy of the liquid. A standpipe is a closed vertical branch on a line: air or other gas is trapped in this branch to form a pneumatic cushion.

## IF THERE IS NO P&ID .....

- Provide valves at headers, pumps, equipment, etc., to ensure that the system will be pressure-tight for hydrostatic testing, and to allow equipment to be removed for maintenance without shutting down the system
- Provide isolating valves in all small lines branching from headers—for example, see figure 6.12
- Provide isolating valves at all instrument pressure points for removal of instruments under operating conditions
- Provide valved drains on all tanks, vessels, etc., and other equipment which may contain or collect liquids
- Protect sensitive equipment by using a fast-closing check valve to stop backflow before it can gather momentum
- Consider butt-welding or ring-joint flanged valves for lines containing hazardous or 'searching' fluids. Hydrogen is especially liable to leak
- Consider seal welding screwed valves if used in hydrocarbon service—see chart 2.3 (inset sketch)
- Provide sufficient valves to control flows
- Consider providing a concrete pit (usually about 4 ft x 4 ft) for a valve which is to be located below grade
- Consider use of temporary closures for positive shutoff—see 2.7
- Provide a bypass if necessary for equipment which may be taken out of service
- Provide a bypass valve around control stations if continuous flow is required. See 6.1.4 and figure 6.6. The bypass should be at least as large as the control valve, and is usually globe type, unless 6-inch or larger, when a gate valve is normally used (see 3.1.4, under 'Gate valve')
- Provide an upstream isolating valve with a small valved bypass to equipment which may be subject to fracture if heat is too rapidly applied on opening the isolating valve. Typical use is in steam systems to lessen the risk of fracture of such things as castings, vitreous-lined vessels, etc.
- Consider providing large gate valves with a valved bypass to equalize pressure on either side of the disc to reduce effort needed to open the valve

## PIPING SAFETY & RELIEF VALVES

- Refer to 3.1.9 for valve orientation
- Extend safety-valve discharge risers that discharge to atmosphere at least 10 ft above the roof line or platform for safety. Support the vent pipe so as not to strain the valve or the piping to the valve. Pointing the discharge line upward (see figure 6.4) imposes less stress when the valve discharges than does the horizontal arrangement
- The downstream side of a safety valve should be unobstructed and involve the minimum of piping. The downstream side of a relief or safety-relief valve is piped to a relief header or knockout drum—see 6.11.3, under 'Venting gases', and 6.12, under 'Relieving pressure—liquids'
- Pipe exhausting to atmosphere is cut square, not at a slant as formerly done, as no real advantage is gained for the cost involved
- Normally, do not instal a valve upstream of a pressure-relief valve protecting a vessel or system from excessive pressure. However, if an isolating valve is used to facilitate maintenance of a pressure-relief valve, the isolating valve is 'locked open'—sometimes termed 'car sealed open' (CSO)
- In critical applications, two pressure-relief valves provided with isolating valves can be used



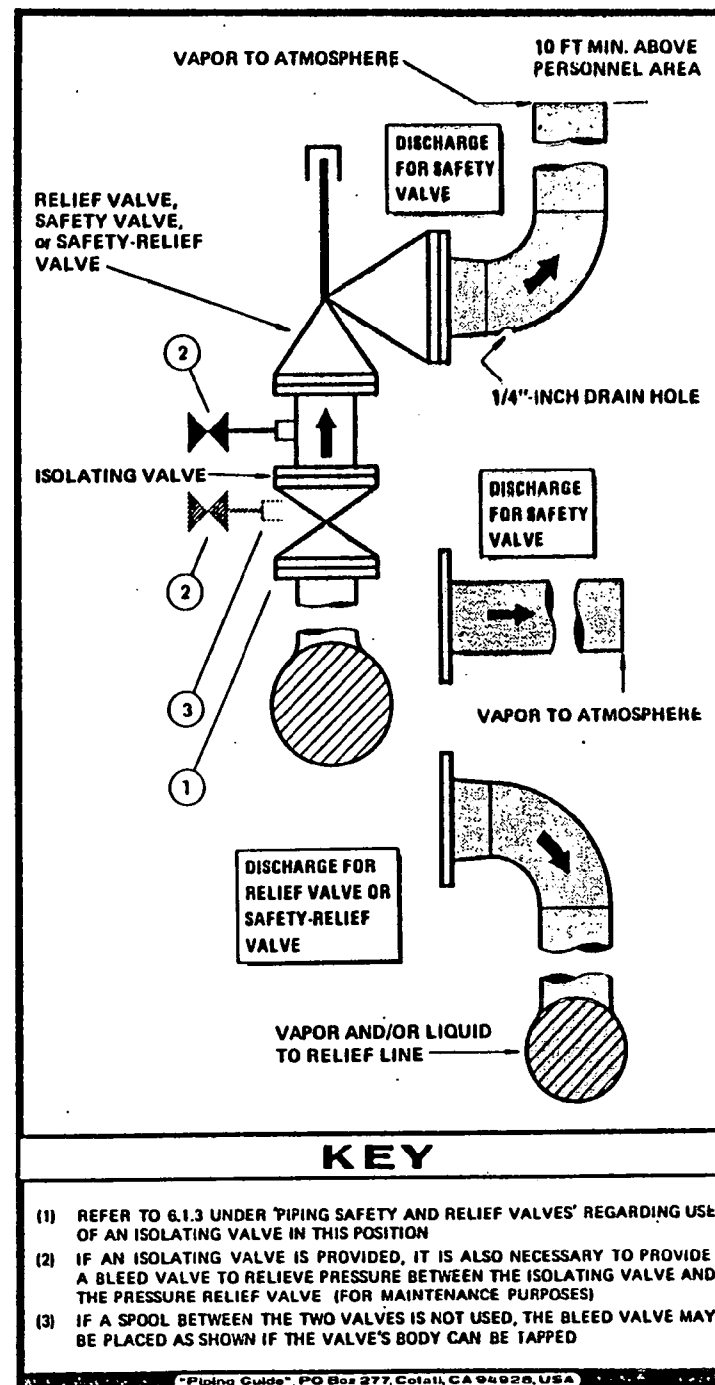
The installation of pressure-relieving devices and the use of isolating valves in lines to and from such devices is governed by the Code for Pressure Piping, ANSI B31 and the ASME Boiler and Pressure Vessel Code.

## INSTALLING BUTTERFLY VALVES

- Ensure that the disc has room to rotate when the valve is installed, as the disc enters the piping in the open position
- Place butterfly valves with integral gaskets between welding-neck or socket-welding flanges—see 3.1.6, under 'Butterfly valve'. The usual method of welding a slip-on flange (see figure 2.7) will not give an adequate seal, unless the pipe is finished smooth with the face of the flange

## PRESSURE-RELIEF-VALVE PIPING

FIGURE 6.4



## CONTROL (VALVE) STATIONS

6.1.4

A control station is an arrangement of piping in which a control valve is used to reduce and regulate the pressure or rate of flow of steam, gas, or liquid.

Control stations should be designed so that the control valve can be isolated and removed for servicing. To facilitate this, the piping of the stations should be as flexible as circumstances permit. Figure 6.5 shows ways of permitting control valve removal in welded or screwed systems. Figure 6.6 shows the basic arrangement for control station piping.

The two isolating valves permit servicing of the control valve. The emergency bypass valve is used for manual regulation if the control valve is out of action.

The bypass valve is usually a globe valve of the same size and pressure rating as the control valve. For manual regulation in lines 6-inch and larger, a gate valve is often the more economic choice for the bypass line—refer to 3.1.4, under 'Gate valve'.

Figures 6.7–11 show other ways of arranging control stations—many more designs than these are possible. These illustrations are all schematic and can be adapted to both welded and screwed systems.

## DESIGN POINTS

- For best control, place the control station close to the equipment it serves, and locate it at grade or operating platform level
- Provide a pressure-gage connection downstream of the station's valves. Depending on the operation of the plant, this connection may either be fitted with a permanent pressure indicating gage, or be used to attach a gage temporarily (for checking purposes)
- Preferably, do not 'sandwich' valves. Place at least one of the isolating valves in a vertical line so that a spool can be taken out allowing the control valve to be removed
- If the equipment and piping downstream of the station is of lower pressure rating than piping upstream, it may be necessary to protect the downstream system with a pressure-relief valve
- Provide a valved drain near to and upstream of the control valve. To save space, the drain is placed on the reducer. The drain valve allows pressure between the isolating valve(s) and control valve to be released. One drain is used if the control valve fails open, and two drains (one each side of the control valve) if the control valve fails closed
- Locate stations in rack piping at grade, next to a bent or column for easy supporting

## DRAFTING THE STATION

In plan view, instead of drawing the valves, etc., the station is shown as a rectangle labeled 'SEE DETAIL "X"' or 'DWG "Y"—DETAIL "X"', if the elevational detail appears on another sheet. See chart 5.7.

## UTILITY STATIONS

6.1.5

A utility station usually comprises three service lines carrying steam, compressed air and water. The steam line is normally ¾-inch minimum, and the other two services are usually carried in 1-inch lines. These services are for cleaning local equipment and hosing floors. (Firewater is taken from points fed from an independent water supply.)

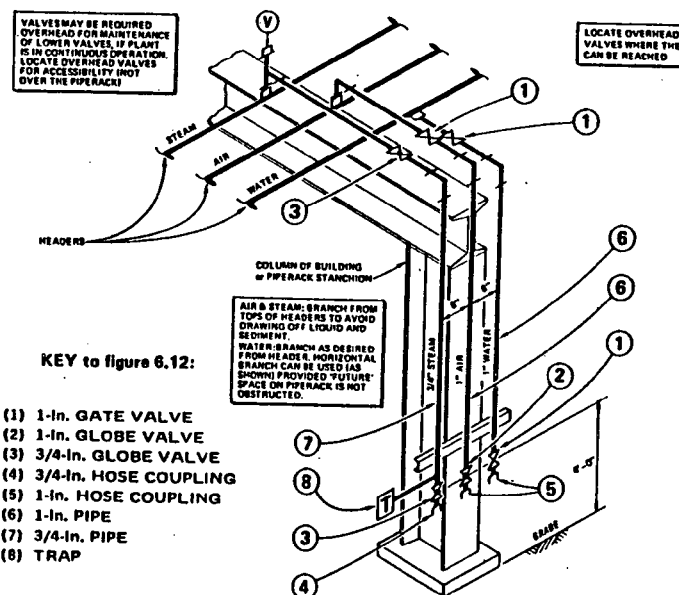
The steam line is fitted with a globe valve and the air and water lines with gate valves. All are terminated with hose connections about 3½ ft above floor or grade. A utility station should be located at some convenient steel column for supporting, and all areas it is to serve should be reachable with a 50-ft hose.

Most companies have a standard design for a utility station. Figure 6.12 shows a design for a standard station which can be copied onto one of the design drawings for reference, or otherwise supplied with the drawings to the erecting contractor who usually runs the necessary lines. A notation used on plan views to indicate the station and services required is:

SERVICES:	WATER, AIR, STEAM	WATER, AIR	WATER, STEAM	AIR, STEAM
STATION SYMBOL:	WAS	WA	WS	AS

UTILITY STATION

FIGURE 6.12



If subject to freezing conditions, utility station steam lines are usually trapped (otherwise, the trap can be omitted). Water is sometimes run underground in cold climates using an additional underground cock or plug valve with an extended key for operating, and a self-draining valve at the base of the riser. Another method to prevent freezing, is to run the water and steam lines in a common insulation.

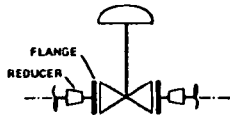
6.1.3  
6.1.5

FIGURES  
6.4 & 6.12

# SCHEMATIC CONTROL STATION ARRANGEMENTS

## PIPING FITTINGS ALLOWING CONTROL VALVE REMOVAL

### FLANGED CONTROL VALVES



### SCREWED CONTROL VALVES

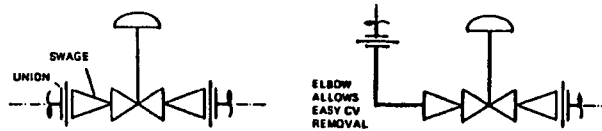
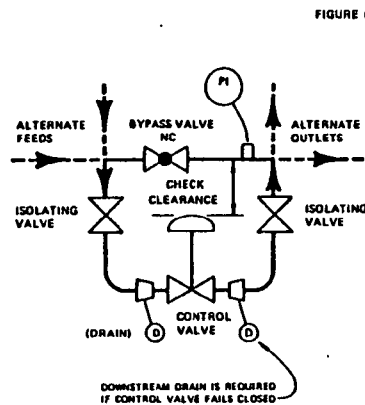
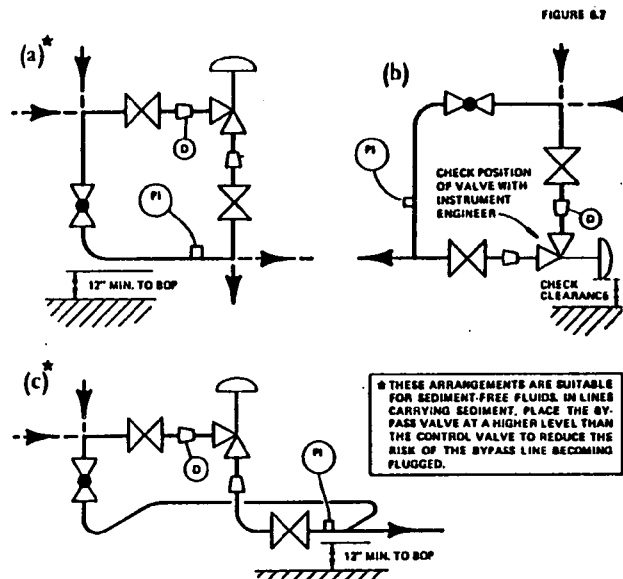


FIGURE 6.6

## BASIC ARRANGEMENT



## ARRANGEMENTS FOR ANGLE CV's



## STATIONS FOR LIQUIDS HARMFUL TO PERSONNEL

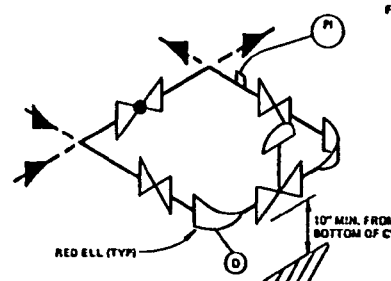
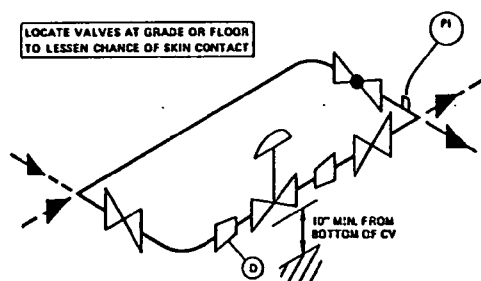
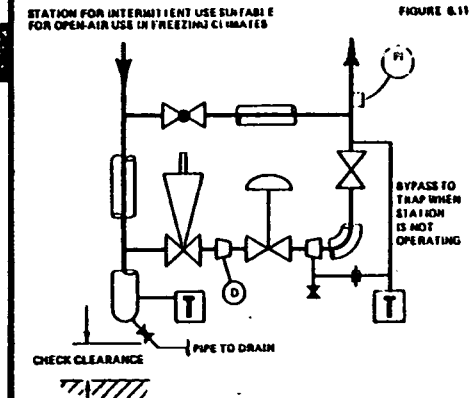
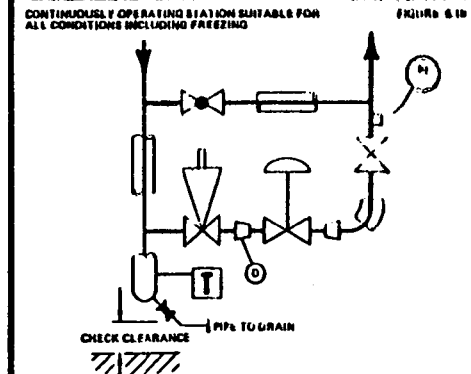
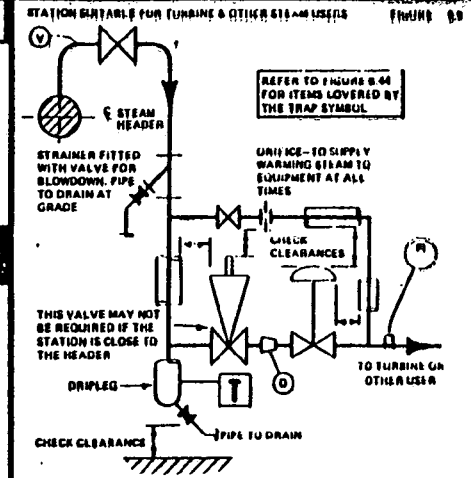


FIGURE 6.9

## FIGURES 6.5-6.11

## STEAM STATIONS





## ARRANGING SUPPORTS FOR PIPING

6.2

Pipe is held either from above by hangers or by supports of various types on which it rests. Hangers are also referred to as supports. Refer to 2.12 for typical hardware.

In the open, single pipes are usually routed so that they may be supported by fixtures to buildings or structures. A group of parallel pipes in the open is normally supported on a piperack—see 6.1.2.

Within a building, piping is routed primarily with regard to its process duty and secondarily with regard to existing structural steelwork, or to structural steel which may be conveniently added. Separate pipe-holding structures inside buildings are rare.

### FUNCTIONS OF THE SYSTEM OF SUPPORT

6.2.1

The mechanical requirements of the piping support system are:

- (1) To carry the weight of the piping filled with water (or other liquid involved) and insulation if used, with an ample safety margin — use a factor of 3 (= ratio of load just causing failure of support or hanger to actual load) or the safety factor specified for the project. External loading factors to be considered are the wind loads, the probable weight of ice buildup in cold climates, and seismic shock in some areas
- (2) To ensure that the material from which the pipe is made is not stressed beyond a safe limit. Maximum tensile stress occurs in the pipe cross sections at the supports. Table S-1 gives spans for steel and aluminum pipe at the respective stress limits 4000 and 2000 PSI. Charts S-2 give the maximum overhangs if a 3-ft riser is included in the span. The system of supports should minimize the introduction of twisting forces in the piping due to offset loads on the supports—the method of cantilevered sections set out in 6.2.4 substantially eliminates torsional forces
- (3) To allow for draining. Holdup of liquid can occur due to pipes sagging between supports. Complete draining is ensured by making adjacent supports adequately tilt the pipe—see 6.2.6
- (4) To permit thermal expansion and contraction of the piping—see 6.1.1, under 'Stresses on piping'
- (5) To withstand and dampen vibrational forces applied to the piping by compressors, pumps, etc.

### PIPING SUPPORT GROUP RESPONSIBILITIES

6.2.2

A large company will usually have a specialist piping support group responsible for designing and arranging supports. This group will note all required supports on the piping drawings (terminal job) and will add drawings of any special details.

The piping support group works in cooperation with a stress analysis group—or the two may be combined as one group—which investigates areas of stress due to thermal movement, vibration, etc., and makes recommendations to the piping group. The stress group should be supplied with preliminary layouts for this purpose by the piping group, as early as possible.

Supports for lines smaller than 2-inch and non-critical lines are often left to the 'field' to arrange, by noting 'FIELD SUPPORT' on the piping drawings.

### LOADS ON SUPPORTS

Refer to table P-1, which lists the weights per foot of pipe and contained water (see 6.11.2). Weights of fittings, flanges, bolts, valves and insulation are given in table W-1, reproduced by permission of the Bergen-Paterson Pipesupport Corporation.

### ARRANGING POINTS OF SUPPORT

6.2.3

Pipe supports should be arranged bearing in mind all five points in 6.2.1. Inside buildings, it is usually necessary to arrange supports relative to existing structural steelwork, and this restricts choice of support points.

The method of support set out in 6.2.4 is ideal: In practice, some compromise may be necessary. The use of dummy legs and the addition of pieces of structural steel may be needed to obtain optimal support arrangements.

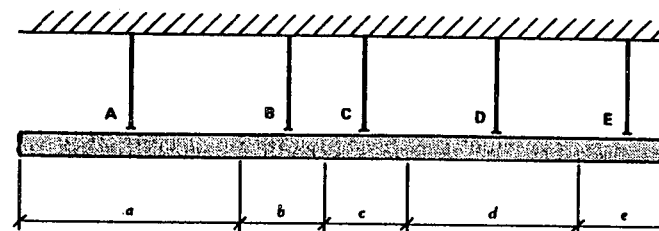
### CALCULATING PREFERRED POINTS OF SUPPORT

6.2.4

Ideally, each point of support would be at the center of gravity of an associated length of piping. Carrying this scheme thru the entire piping system would substantially relieve the system from twisting forces, and supports would be only stressed vertically. A method of balancing sections of pipe at single support points is illustrated for a straight run of pipe in figure 6.13.

#### BALANCING SECTIONS OF PIPE

FIGURE 6.13



Consider hanger B associated with a length of pipe  $b$ . This length of pipe is supported by B, located at its center of gravity, which is at the midway point for a straight length of uniform pipe. Hangers A, C, D and E are likewise placed at the respective centers of gravity of lengths of pipe  $a$ ,  $c$ ,  $d$  and  $e$ . If any length of pipe is removed, the balance of the rest of the line would be unaffected. Each of the hangers must be designed to adequately support the load of the associated piping—see 6.2.1, point (1).

The presence of heavy flanges, valves, etc., in the piping will set the center of gravity away from the midpoint of the associated length. Calculation of support points and loadings is more quickly done using simple algebra. Answers may be found by making trial-and-error calculations, but this is much more tedious.

6.2  
6.2.4

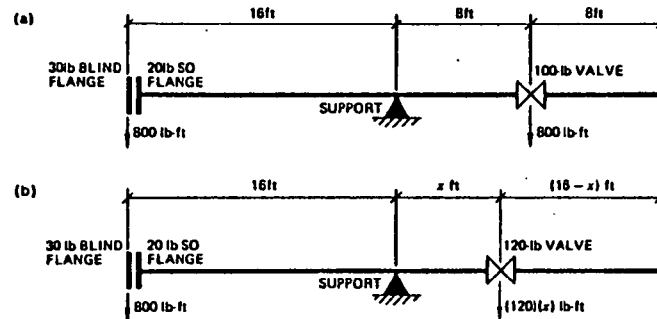
FIGURES  
6.5-6.11 & 6.13

Correct location of piping supports can be determined by the use of 'moments of force'. Multiplying a force by the distance of its line of action from a point gives the 'moment' of the force about that point. A moment of force can be expressed in lb-ft (pounds weight times feet distance). The forces involved in support calculations either are the reactions at supports and nozzles, or are the downward-acting forces due to the weight of pipe, fittings, valves, etc.

In figure 6.14(a), the moment about the support of the two flanges is  $(30 + 20)(16) = 800$  lb-ft, counter-clockwise. The moment of the 100-lb valve about the support is  $(100)(8) = 800$  lb-ft, clockwise. As the lengths of pipe each side of the support are about the same, they may be omitted from the moment equation. The problem is simplified to balancing the valve and flanges.

USE OF MOMENTS

FIGURE 6.14



Suppose it was required to balance this length of piping with a 120 lb valve on the right—where should the 120 lb valve be placed?

Referring to figure 6.14(b), if  $x$  represents the unknown distance of the 120 lb valve from the support, the piping section would be in balance if:

$$(50)(16) = (120)(x).$$

That is, if  $x = (50)(16)/(120) = (800)/(120) = 6$  ft 8 in.

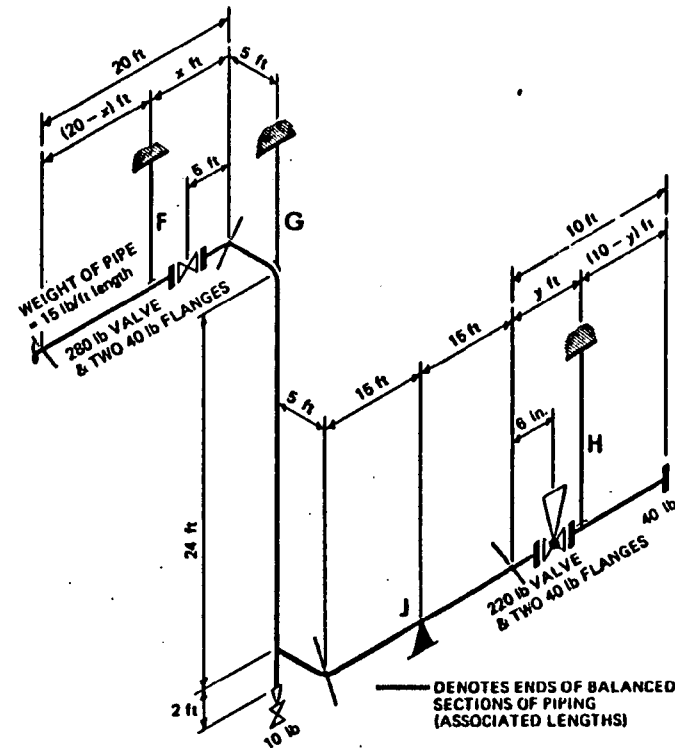
A more involved example follows:—

Figure 6.15 shows a length of 4-inch piping held by the hangers F, G, and H, and support J. The lengths of associated piping are shown by dashed separation lines. The weights of pipe and fittings are shown on the drawing. The 4-inch pipe is assumed to weigh 15 lb per foot of length. Welded elbows and tees are assumed to weigh the same as line pipe.

First consider the section associated with hanger F. The weight of pipe to the left of F is  $(15)(20 - x)$  lb, and as its center of gravity is at  $(20 - x)/(2)$  ft, its moment on the hanger is  $(15)(20 - x)^2/(2)$  lb-ft. The heavy valve and flanges are assumed to have their mass center 5 ft from the end, and their moment is  $(x - 5)(360)$  lb-ft. Ignoring the pipe 'replaced' by the valve, the weight of pipe to the right of F is  $(15)(x)$  lb and its moment about F is  $(15)(x)(x)/(2)$  lb-ft. As the associated length is in balance:

CALCULATING PIPE SUPPORTS

FIGURE 6.15



$$(15)(20 - x)^2/(2) = (360)(x - 5) + (15)(x^2)/(2)$$

$$x = (80)/(11), \text{ or about } 7 \text{ ft } 3 \text{ in.}$$

The  $x^2$  terms canceled—this must be so, as there can physically be only one value for  $x$ . The load on hanger F is  $(20)(15) + (360)$  or 660 lb.

The support J should be at the center of the associated length of pipe, as already shown in figure 6.15, and the load on the support is  $(30)(15)$ , or 450 lb.

The hanger G is easily seen to be suitably placed, as there is 5 ft of 4-inch pipe overhanging each side. Only the load on the hanger need be calculated, which is  $(5 + 5 + 24 + 2)(15) + (10)$ , or 550 lb.

The location of hanger H has to be found by a calculation like that for hanger F, except that the heavy terminal flange has also to be taken into account. The moment equation in lb-ft is:

$$(300)(y - 0.5) + (15)(y^2)/(2) = (15)(10 - y)^2/(2) + (40)(10 - y)$$

which gives  $y$  as nearly 2 ft 8 in.

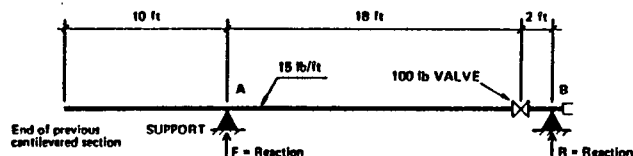
The load on hanger H is about  $(220) + (3)(40) + (15)(10)$ , or 490 lb.

## PROBLEM OF THE END

The supported length at one end of a run of piping may be cantilevered in the same way as the other lengths, and this has the advantage that if the piping terminates at a nozzle the load on the nozzle is minimal. However, it may be necessary to use or arrange a support at or near the end of a piping run. If the end of the run is vertical, the end support should be designed to carry the vertical run. The problem is usually more complex when the end of the run is horizontal.

The locations of fittings and support points will usually be already defined, and the problem is to calculate the reaction on the terminal support, and to see that the support is designed to withstand the load on it. In calculating the load on the terminal support, it should be made certain that the load is downward—with some arrangements, the piping would tend to raise itself off the terminal support (negative load) and if this type of arrangement is not changed, the terminal support will have to anchor the piping.

The sketch shows a horizontal end arrangement. Taking moments in lb-ft about the support A:



$$(15)(10)(\frac{1}{2})(10) = (15)(18+2)(\frac{1}{2})(18+2) + (100)(18) - (R)(18+2)$$

which gives

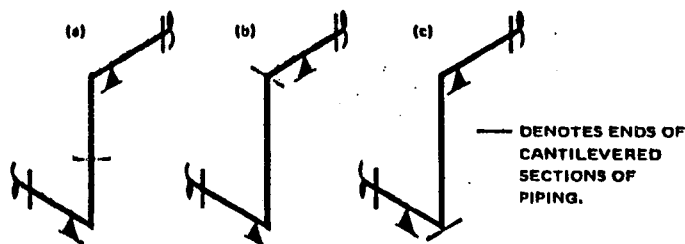
$$R = 202\frac{1}{2} \text{ lb.}$$

The reaction, F, on the support A can be calculated by taking moments about the support B or another axis, or more simply by equating vertical forces:

$$F + 202\frac{1}{2} = (15)(10+18+2) + 100 = 550, \text{ which gives } F = 347\frac{1}{2} \text{ lb.}$$

## PROBLEM OF THE RISER

Supports for lines changing in direction can be calculated by the cantilever method. Sketch (a) below shows that the weight of the vertical part of the piping can be divided between two cantilevered sections in any proportion suited to the available support points. Sketches (b) and (c) show the vertical piping associated wholly with the left- or right-hand cantilevered sections. The piping may be supported by means of a dummy leg, if direct support is not practicable.



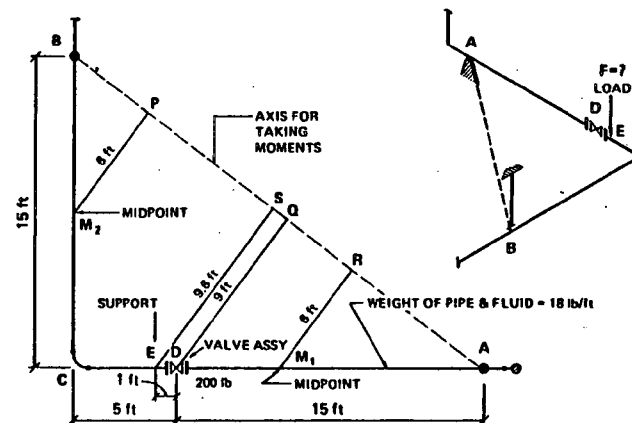
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6.2.4

## GRAPHIC METHOD FOR FINDING LOADS ON SUPPORTS

The following graphical method permits quick calculation of bearing loads for 'corner' piping arrangements.

**PROBLEM** To find the load to be taken by a support to be placed at point 'E' in the piping arrangement shown:



## SOLUTION

- (1) Draw the plan view to any convenient scale (as above)
- (2) Add the axis line AB (this must pass thru points of support)
- (3) Divide the run of piping into parts. Piping between the support points A and B is considered in three parts: (1) The valve, (2) The length of pipe BC, (3) The length of pipe AC—the short piece of line omitted for the valve is ignored, and the effect of the elbow neglected.
- (4) Drop perpendiculars from midpoints  $M_1$  and  $M_2$ , the valve and support point E to the axis line.
- (5) Take moments about the axis line, measuring the lengths of perpendiculars  $M_2P$ ,  $ES$ ,  $DQ$  and  $M_1R$  directly from the plan view (these lengths are noted on the sketch):

PIPE LENGTH AC	PIPE LENGTH CB	VALVE ASSY.	LOAD ON SUPPORT
$(20)(18)(6)$	$+ (15)(18)(6)$	$+ (200)(9)$	$= (F)(9.6)$

which gives the load on the support at E as:

$$F = 581 \text{ lb}$$

## EXTENSION OF THE METHOD

The same method can be used if the angle at the corner is different from 90 degrees, or if vertical lines are included in the piping.

## NOTES

- (1) The axis line must pass thru points of support. If the axis line is not horizontal, the lengths of the perpendiculars are still measured directly from the plan view.
- (2) This method does not take into account additional moments due to bending and torsion of pipe. However, it is legitimate to calculate loads on supports as if the pipe is rigid.

This problem often occurs when running pipes from one piperack to another, with a change in elevation, as in figure 6.15. Too much overhang will stress the material of the pipe beyond a safe limit near one of the supports adjacent to the bend, and the designer needs to know the allowable overhang.

The stresses set up in the material of the pipe set practical limits on the overhangs allowed at corners. The problem is like that for spans of straight pipe allowable between supports. Overhangs permitted by stated limits for stress are given in charts S-2.

#### PIPE SUPPORTS ALLOWING THERMAL MOVEMENT

6.2.5

Piping subject to large temperature changes should be routed so as to flex under the changes in length—see figure 6.1. However, hangers and supports must permit these changes in length. Figures 2.72 A & B show a selection of hangers and supports able to accommodate movement. For single pipes hung from rod or bar hangers, the hanger should be sufficiently long to limit total movement to 10 degrees of arc.

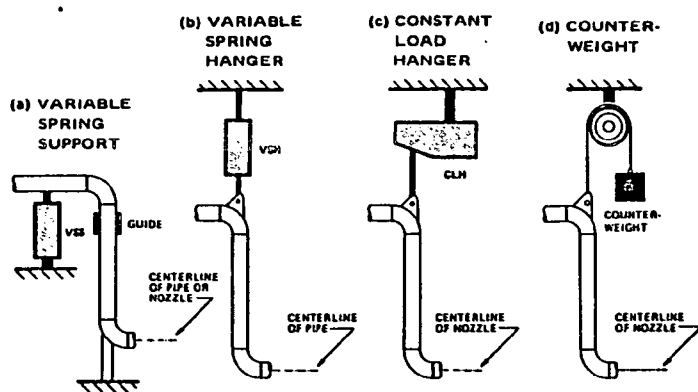
#### SPRING SUPPORTS

There are two basic types of spring support: (1) Variable load. (2) Constant load—refer to 2.12.2. Apart from cost, the choice between the two types depends on how critical the circumstances are. For example, if a vertical line supported on a rigid support at floor level is subject to thermal movement, a variable-spring hanger or support at the top of the line is suitable—see figure 6.16 (a) and (b).

If a hot line comes down to a nozzle connected to a vessel or machine, and it is necessary to keep the nozzle substantially free from vertical loading, a constant-load hanger can be used—see figure 6.16(c). Cheaper alternate methods of supporting the load are by a cable-held weight working over a pulley, as illustrated in figure 6.16(d), or by a cantilevered weight.

VARIABLE- & CONSTANT-LOAD HANGERS & SUPPORTS

FIGURE 6.16



#### SLOPED LINES AVOID POCKETING AND AID DRAINING

6.2.6

As pipe is not completely rigid, sagging between points of support must occur. In many instances, sagging is acceptable, but in others it must be restricted.

The nature of the conveyed material, the process, and flow requirements determine how much sagging can be accepted. Sagging is reduced by bringing adjacent points of support closer. Pocketing of liquid due to sagging can be eliminated by sloping the line so that the difference in height between adjacent supports is at least equal to triple the deflection (sag) at the mid-point. Lines which require sloping include blowdown headers, pressure-relief lines, and some process, condensate and air lines. (Air lines are discussed in 6.3.2, and draining of compressed-air lines in 8.11.4.)

Complete draining may be required for lines used in batch processing to avoid contamination, or where a product held in a line may degenerate or polymerize, or where solids may settle and become a problem.

In freezing conditions, lines conveying condensate from traps to drains are sloped; condensate headers may be sloped (as an alternative to steam tracing), depending on the rate of flow.

In the past, steam lines were sloped to assist in clearing condensate, but the improved draining is now not considered to be worth the difficulty and expense involved.

#### SLOPED LINES ON PIPERACKS

Sloped lines can be carried on brackets attached to the piperack stanchions (see figure 6.3). To obtain the required change in elevation at each bent, the brackets may be attached at the required elevations; alternately, a series of brackets can be arranged at the same elevation and the slope obtained by using shoes of different sizes—this method leads to fewer construction problems.

Shoes of graded sizes are also the best method for sloping smaller lines on the piperack. It is not usual or desirable to hang lines from the piperack unless necessary vertical clearances can be maintained.

#### SLOPED LINES IN BUILDINGS

Inside a building, both large and small sloped lines can rest on steel brackets, or be held with hangers. Rods with turnbuckles are used for hangers on lines required to be sloped. Otherwise, drilled flat bar can be used. (Adjustable brackets are available from the Unistrut and Kindorf ranges of support hardware.)

#### SUPPORTING PIPE MADE FROM PLASTICS OR GLASS

6.2.7

Pipe made either from flexible or rigid plastics cannot sustain the same span loads as metal pipe, and requires a greater number of support points. One way of providing support is to lay the pipe upon lengths of steel channel sections or half sections of pipe, or by suspending it from other steel pipes. The choice of steel section would depend on the span loads and the size and type of plastic pipe.

For glass process and drain lines, hangers for steel pipe are used, provided that they hold the pipe without causing local strains and are padded so as not to crack the pipe. Rubber and asbestos paddings are suitable. Uninsulated horizontal lines from 1 to 6 inch in size containing gas or liquid of specific gravity less than 1.3 should be supported at 8 to 10 ft intervals. Couplings and fittings should be about 1 ft from a point of support.

## DESIGN POINTERS

6.2.8

Terms such as 'dummy leg', 'anchor', 'shoe', etc., used in detailing supporting hardware are explained in 2.12.2. Refer to chart 5.7 for symbols.

## GENERAL

- Design hangers for 2½-inch and larger pipe to permit adjustment after installation
- If piping is to be connected to equipment, a valve, etc., or piping assembly that will require removal for maintenance, support the piping so that temporary supports are not needed
- Base load calculations for variable-spring and constant-load supports on the operating conditions of the piping (do not include the weight of hydrostatic test fluid)
- If necessary, suspend pipes smaller than 2-inch nominal size from 4-inch and larger pipes

## DUMMY LEGS

Table 6.3 suggests sizes for dummy legs. The allowable stress on the wall of the elbow or line pipe to which the dummy leg is attached sets a maximum length for the leg. The advice of the stress group should be sought.

APPROXIMATE SIZES FOR DUMMY LEGS

TABLE 6.3

NPS of Piping (inches)	2	3	4	6	8	10	12	14
NPS of Pipe forming Leg (in.)	1½	2	3	4	6	8	8	10
Size of W-Flange (in.)					6	8	8	10

## ANCHORS

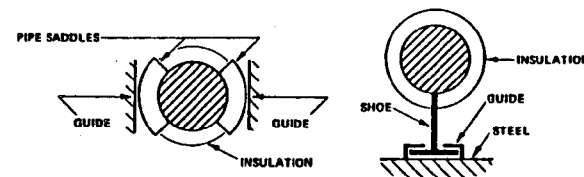
Anchors are required as stated in the following two points. However, advice from the stress and/or piping support groups should be obtained:

- Provide anchors as necessary to prevent thermal or mechanical movement overloading nozzles on vessels or machinery, branch connections, cast-iron valves, etc.
- Provide anchors to control direction of expansion; for example, at battery limits and on piping leaving units, so that movement is not transmitted to piping on a piperack

## SHOES, GUIDES, & SADDLES

- Do not use shoes on uninsulated pipes, unless required for sloping purposes. For reduced friction where lines are long and subject to movement, slide plates are an alternative—see 2.12.2.
- Use of wye-type shoes enables pipes to be placed on the shoe before welding and makes construction easier—see figure 2.72A
- Welding the pipe directly to shoes is not always acceptable; for example with rubber-lined pipe. Bolted or strapped shoes are more suitable

- Check the code pertinent to the project, as it may prohibit 'partial' welds for supports—that is, welds that do not encircle the pipe
- Provide slots in shoes to accept the straps or wires used to hold insulation to pipe
- Provide guides for long straight pipes subject to thermal movement, either by guiding the shoe or by guiding pipe support saddles attached to the pipe, as shown:



- For better stress distribution in the pipe wall, pipe support saddles are usually used on large lines. They can also be used for lines that may twist over when moving

## SUPPORTING VALVES

- Provide support as close as possible to heavy valves, or try to get valves moved close to a suitable point where support can be provided
- Large valves and equipment such as meters located at grade will usually require a concrete foundation for support

## WELDING PIPE-SUPPORT & PLATFORM BRACKETS TO VESSELS, Etc.

- Instruct the vendor to add brackets required on pressure vessels prior to stress-relieving and testing—otherwise, retesting and recertification may be obligatory
- It is permissible to specify brackets to be welded to non-pressure vessels provided that the strength of the vessel is not degraded

## SUPPORTING PIPE AT NOZZLES

Ensure that nozzles on machinery, compressors, pumps, turbines, etc., are substantially free from loads transmitted by the piping, which may be due to the weight of the piping, or to movement in the piping resulting from contraction, expansion, twisting, vibration or surging. Equipment suppliers will sometimes state maximum loadings permissible at nozzles. *Excessive loads applied to nozzles on machinery can force it from alignment and may cause damage.*

Piping to pumps, turbines, etc., should be supported adequately, but should allow the equipment to be removed. Supports for this piping are best made integral with the concrete foundations, especially if thermal movement occurs and should be on the same level as the base of the equipment, so that on heating or cooling, vertical differential expansion and contraction between supports and equipment will be minimized.

6.2.4  
6.2.8

FIGURE  
6.16

TABLE  
6.3

**PUMP EMPLACEMENT & CONNECTIONS**
**6.3.1**
**TYPICAL PIPING FOR CENTRIFUGAL PUMPS**

Most pumps used in industry are of the centrifugal type. Figures 6.17 and 6.18 show typical piping and fittings required at a centrifugal pump together with the valves necessary to isolate the pump from the system.

The check valve is required to prevent possible flow reversal in the discharge line. A permanent in-line strainer is normally used for screwed suction piping and a temporary strainer for butt-welded/flanged piping. The temporary strainer is installed between flanges—see figure 2.69. A spool is usually required to facilitate removal.

Although centrifugal pumps are provided with suction and discharge ports of cross-sectional area large enough to cope with the full rated capacity of the pump, it is often necessary with thick fluids or with long suction lines to use an inlet pipe of larger size than the inlet port, to avoid cavitation. Cavitation is the pulling by the pump of vapor spaces in the pumped liquid, causing reduction of pumping efficiency, noisy running, and possible impeller and bearing damage. Refer to 6.1.3, under 'Which size valve to use?'

Most pumps have end suction and top discharge. Limitations on space may require another configuration, such as top suction with top discharge, side suction with side discharge, etc. Determination of nozzle orientation takes place when equipment layout and piping studies are made.

**AUXILIARY, TRIM, or HARNESS PIPING**

Pumps, compressors and turbines may require water for cooling bearings, for mechanical seals, or for quenching vapors to prevent their escape to atmosphere. Piping for cooling water or seal fluid is usually referred to as auxiliary, trim, or harness piping, and the requirement for this piping is normally shown on the P&ID. This piping is usually shown in isometric view on one of the piping drawings.

In order to cool the gland or seal of a centrifugal pump and ensure proper sealing, it is usually supplied with liquid from the discharge of the pump, by a built-in arrangement, or piped from a connection on the pump's casing. The gland may be provided with a cooling chamber, requiring piped water. If a pump handles hot or volatile liquid, seal liquid may be piped from an external source.

**DRAINING**

Each pump is usually provided with a drain hub 4 to 6 inches in diameter, positioned about 9 inches in front of the pump foundation on the centerline of the pump. The drain hub is piped to the correct sewer or effluent line—see 6.13. If two small pumps have a common foundation, they can share the same drain hub.

Most centrifugal pumps have baseplates that collect any leakage from the pump. The baseplate will have a threaded connection which is piped to the drain hub. Waste seal water is also piped to the drain hub—see figure 6.19.

- In outside installations in freezing climates, provide a valved drain from the pump's casing
- Provide a short spool for a 3/4-inch drain between the on/off valve and the check valve, to drain the discharge line. If the valve is large enough, the drain can be made by drilling and tapping a boss on the check valve, as shown in figure 6.17, note (3), in which instance no spool is required.

**INSTALLATION**

- Do not route piping over the pump, as this interferes with maintenance. It is better to bring the piping forward of the pump as shown in figure 6.17
- Leave vertical clearance over pumps to permit removal for servicing—sufficient headroom must be left for a mobile crane for all but the smaller pumps, unless other handling is planned
- If pumps positioned close to supply tanks are on separate foundations, avoid rigid piping arrangements, as the tanks will 'settle' in the course of time
- Locate the pump as closely as practicable to the source of liquid to be pumped from storage tanks, sumps, etc., with due consideration for flexibility of the piping
- Position valves for ease of operation placing them so they are unlikely to be damaged by traffic and will not be a hazard to personnel—see table 6.2 and chart P-2
- The foundation may be of any material that has rigidity sufficient to support the pump baseplate and withstand vibration. A concrete foundation built on solid ground or a concrete slab floor is usual. The pump is positioned, the height fixed (using packing), and the grout is then poured. Grout thickness is not usually less than one inch—see figure 6.17
- A pit in which a pump is installed should have a drain, or have a sump that can be drained or pumped out
- Make the concrete foundation at least as large as the baseplate, and ensure that concrete extends at least 3 inches from each bolt

**VALVES**

- Valves are 'line size' unless shown otherwise on the P&ID. See 6.1.3 under 'Which size valve to use?'
- Use tilting disc or swing check valves for preference
- Do not use globe valves for isolating pumps. Suction and discharge line isolating valves are usually gate valves, but may be other valves offering low resistance to flow

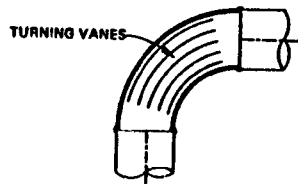
## SUCTION LINE

To avoid cavitation, the pump must be at the correct elevation, related to the level or head of the liquid being pumped. If the location of the pump has not previously been established on an equipment arrangement drawing, refer to the engineer involved.

Concentric reducers are used in lines 2-inch and smaller. Eccentric reducers are used in lines 2½-inch and larger, and are arranged to avoid: (1) Creating a vapor space. (2) Creating a pocket which would need to be drained. These conditions set the configuration of the reducer—that is, whether it is to be installed 'top flat' or 'bottom flat'.

If a centrifugal pump has the suction nozzle at the end (in line with the drive shaft), an elbow may be connected directly to the nozzle at any orientation.

If a pump has the suction nozzle at the side with split flow to the impellor provide a straight run of pipe equal to 3 to 5 pipe diameters of the suction line to connect to the nozzle. Alternately, an elbow may be connected to the suction nozzle, but it must be arranged in a plane at 90 degrees to the driving shaft, to promote equal flow to both sides of the impellor. If an elbow must be in the same plane as the driving shaft of the pump, consider the use of turning (or splitter) vanes to induce more even flow. Uneven flow causes damage to the impellor and bearings.



- Route suction lines as directly as possible so as not to starve the pump and incur the risk of cavitation
- If the pump draws liquid from a sump at a lower elevation, provide a combined foot valve and strainer. A centrifugal pump working in this situation requires priming initially—provide for this by a valved branch near the inlet port, or by other means
- Provide a strainer in the suction line—see figures 6.17 thru 6.21. Do not place a temporary startup screen immediately downstream of a valve, as debris may back up and prevent the valve from being closed

## DISCHARGE LINE

The outlet pipe for centrifugal and other non-positive displacement pumps is in most cases chosen to be of larger bore than the discharge port, in order to reduce velocity and consequent pressure drop in the line. A concentric reducer or reducing elbow is used in the discharge line to increase the diameter. There is no restriction on the placement of elbows in discharge lines as there is in suction lines.

- Provide a pressure connection in the discharge line, close to the pump outlet — see figures 6.17 thru 6.21. It may be necessary to provide a short spool for this purpose if there is no pressure point tapping on the pump discharge nozzle
- For locations of drain connections in the discharge line, see figures 6.17 thru 6.21

## PUMPS WITH SCREWED CONNECTIONS

A pump with screwed connections requires unions in the suction and discharge lines to permit removal of the pump.

## PIPING FOR POSITIVE-DISPLACEMENT PUMPS

Reciprocating and rotary pumps of this type must be protected against overloading due to restriction in the discharge line. If a positive-displacement pump is not equipped with a relief valve by the manufacturer, provide a relief valve between the pump discharge nozzle and the first valve in the discharge line. The discharge from the relief valve is usually connected to the suction line between the isolating valve and the pump.

As positive displacement pumping does not greatly change the flow velocity, reducers and increasers are not usually required in suction and discharge lines. See figures 6.20 and 6.21. A positive-displacement pump having a pulsating discharge may set the piping into vibration, and to reduce this an air chamber (pneumatic reservoir) such as a standpipe can be provided downstream of the discharge valve.

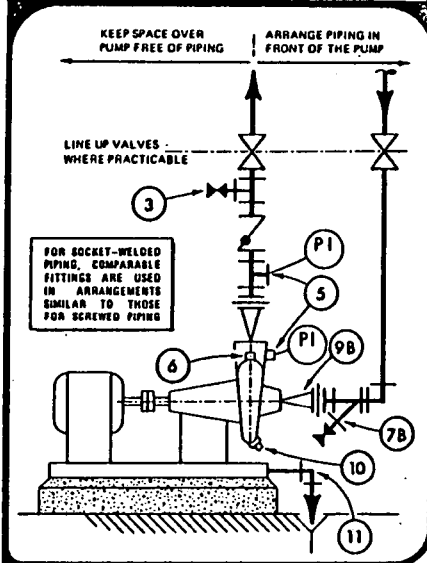
## KEEPING MATERIAL FROM SOLIDIFYING IN THE PUMP

It may be necessary to trace a pump (see 6.8.2) in order to keep the conveyed material in a fluid state, especially after shutdown. This problem arises either with process material having a high melting point, or in freezing conditions. Alternately, jacketed pumps can be employed (such as Foster jacketed pumps available from Parks-Cramer).

FIGURES 6.17 THRU 6.21 ARE ON THE FOLLOWING THREE PAGES, & THE KEY FOR THESE FIGURES IS ON THE THIRD OF THESE PAGES

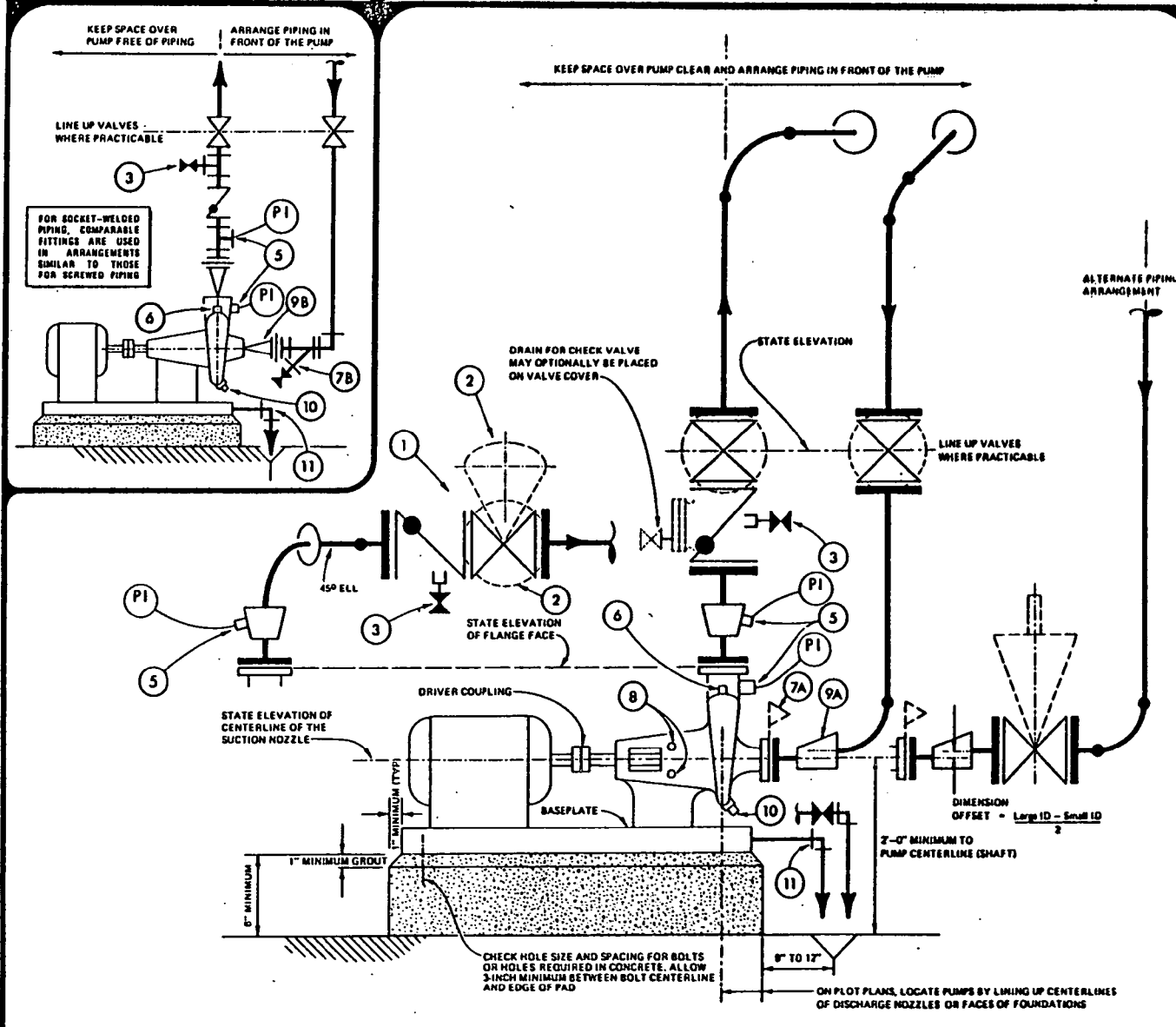
# CENTRIFUGAL PUMP PIPING IN ELEVATION

SCREWED PIPING FIGURE 6.18



FLANGED BUTT-WELDED PIPING

FIGURE 6.17





# PIPING TO CENTRIFUGAL PUMPS—ALTERNATIVES

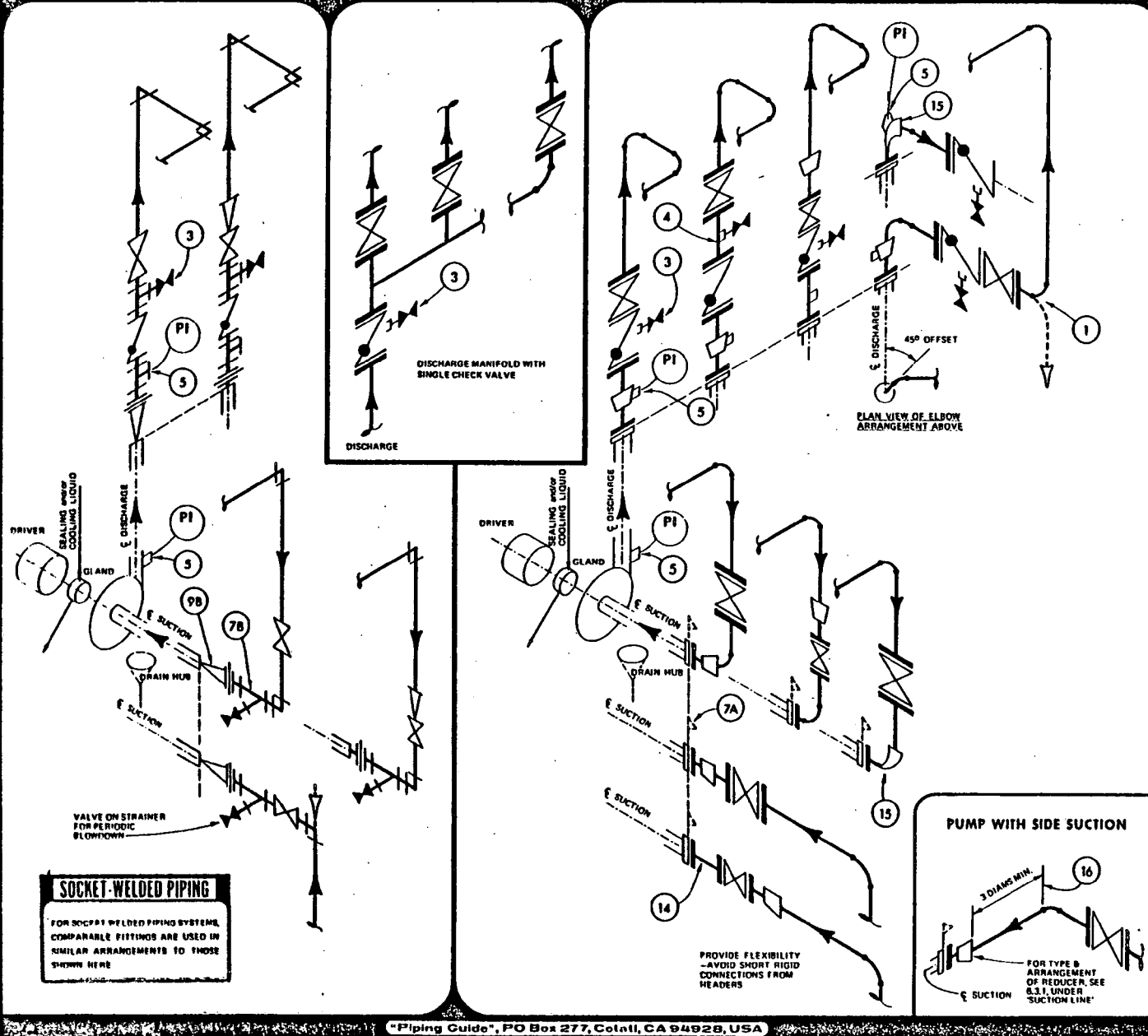
○ REFER ALSO TO 6.1.3, "WHICH SIZE VALVE TO USE"

FIGURE 6.19

## SCREWED PIPING

## DISCHARGE MANIFOLD

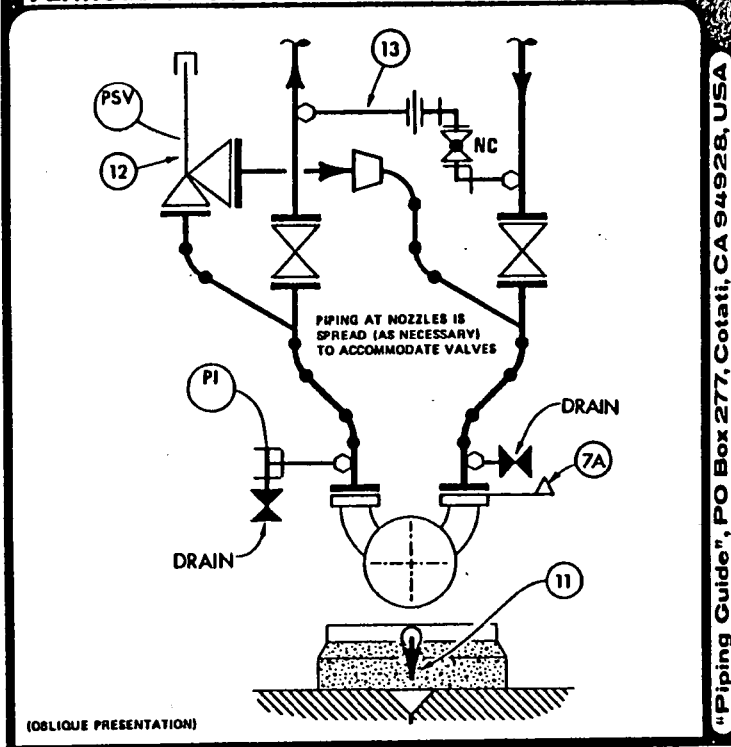
## FLANGED BUTT-WELDED PIPING



FIGURES 6.17-6.19

# PIPING FOR POSITIVE-DISPLACEMENT PUMPS

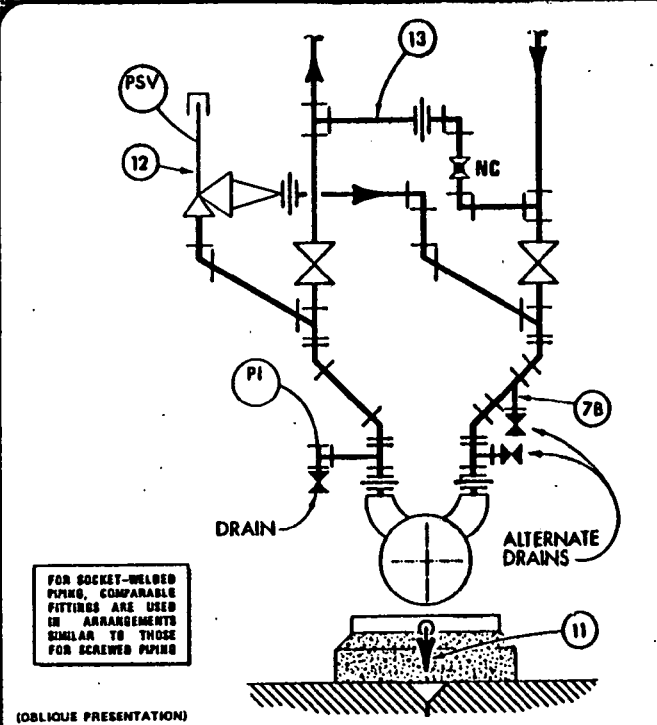
FLANGED BUTT-WELDED PIPING FIGURE 6.20



"Piping Guide", PO Box 277, Cotati, CA 94928, USA

SCREWED PIPING

FIGURE 6.21



## KEY FOR FIGURES 6.17-6.21

- (1) ALTERNATE HORIZONTAL DISCHARGES, WITH LINE OFFSET AND WITH VALVES LAID OVER AND OFFSET AS NECESSARY—THIS MAY BE NECESSARY IF THE VERTICAL POSITION PLACES HANDWHEEL OUT OF REACH OR IF DISCHARGE NEEDS TO TURN DOWN
- (2) ALTERNATE POSITIONS FOR HANDWHEEL
- (3) PROVIDE 1/2 TO 3/4-INCH DRAIN ON CHECK VALVE ABOVE DISC (A DRAINPOINT OR BOSS IS USUALLY PROVIDED ON 2-INCH AND LARGER VALVES) AND RUN LINE TO DRAIN. OTHERWISE, PLACE DRAIN ON SPOOL BETWEEN CHECK AND ISOLATING VALVES. ON SCREWED AND SOCKET-WELDED PIPING, PROVIDE A TEE FOR THE DRAIN CONNECTION
- (4) SPOOL FOR DRAIN POINT, IF DRAIN CANNOT GO ON CHECK VALVE
- (5) ALTERNATE PRESSURE GAGE POINTS ON DISCHARGE PIPING IF POINT IS NOT PROVIDED ON PUMP BY VENDOR
- (6) CASING VENT. CAN BE USED FOR SEAL LIQUID TAKEOFF
- (7A) TEMPORARY STARTUP STRAINER
- (7B) PERMANENT LINE STRAINER FOR SCREWED OR SOCKET-WELDED PIPING
- (8) CONNECTIONS FOR COOLING OR SEAL LIQUID. USUALLY WATER OR OIL
- (9A) REDUCER
- (9B) SNAGE (SWAGED NIPPLE) [CONCENTRIC TYPES MAY BE USED ON PUMPS WITH INLET PORTS 2-INCH AND SMALLER]
- (10) CASING DRAIN PLUG. RUN VALVED LINE IF LIQUID IS LIKELY TO FREEZE
- (11) PIPE BASEPLATE OF PUMP TO DRAIN HUB. PROVIDE HUB AT EACH PUMP PIPE HUB TO APPROPRIATE DRAIN OR SEWER. IF TWO PUMPS ARE ON A COMMON BASE, THEY CAN SHARE THE SAME HUB
- (12) BYPASS PROTECTS POSITIVE-DISPLACEMENT PUMP AND DRIVER IF AN ATTEMPT IS MADE TO OPERATE PUMP WITH A DISCHARGE VALVE CLOSED
- (13) BYPASSES FOR PUMPS OPERATING IN PARALLEL ALLOW FLOW IN SUCTION AND DISCHARGE LINES TO A HEADER IF A PUMP IS SHUT DOWN
- (14) SPOOL FOR TEMPORARY STRAINER
- (15) REDUCING ELBOW MAY REPLACE REGULAR ELBOW AND REDUCER
- (16) IF A PUMP HAS SIDE SUCTION WITH SPLIT FLOW TO IMPELLOR, PROVIDE 3 OR MORE DIAMETERS OF STRAIGHT PIPE AS SHOWN, OR CONNECT AN ELBOW IN A PLANE AT 90 DEGREES TO THE IMPELLOR SHAFT

Refer to 3.2.2 for a description of compressors and associated equipment. A compressor supplies compressed air or a gas to process or other equipment. A compressor is usually purchased as a 'package unit', which includes coolers, and the designer is left with the problem of installing it and piping auxiliaries to it. These various auxiliaries are shown in figure 6.23.

Compressors may be installed in the open, or within a plant or separate compressor house. An arrangement of compressor, ancillary equipment and distribution lines is shown in figure 6.22 (derived from an illustration by Atlas Copco).

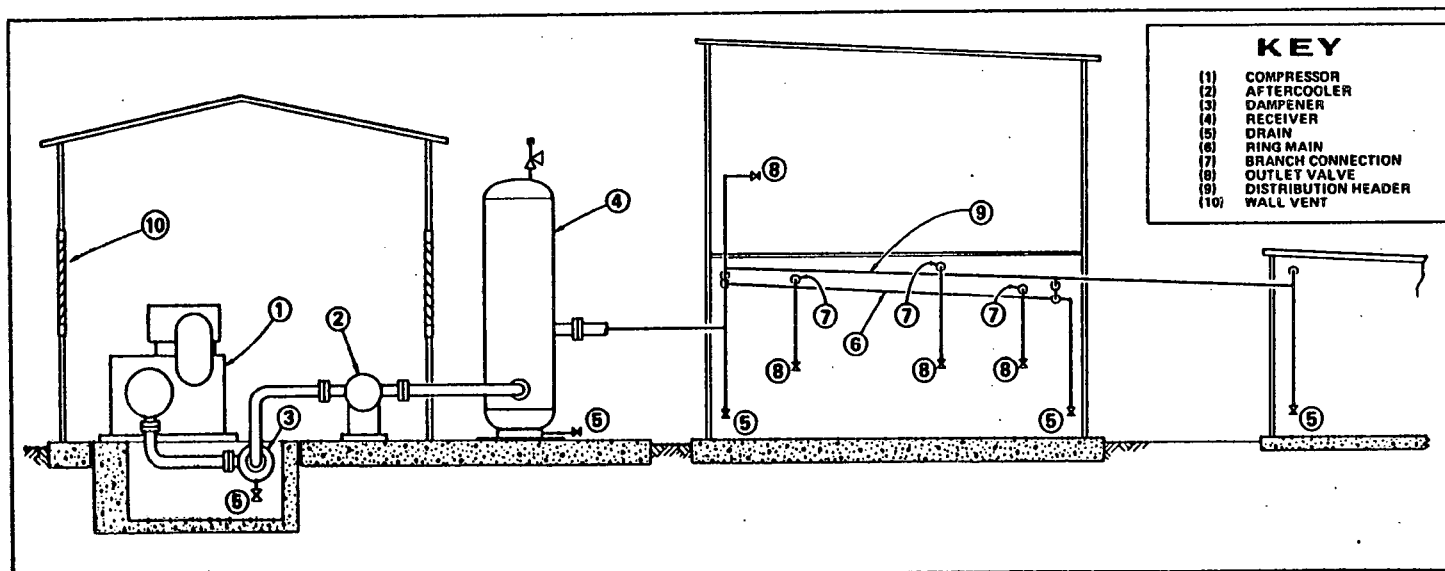
#### COMPRESSOR HOUSE

- If the compressor is handling a gas heavier than air, eliminate pits or trenches in the compressor house to avoid a suffocation or explosion risk
- Provide air entry louvers if a compressor takes air from within a compressor house or other building
- Provide maintenance facilities, including a lifting rail or access for mobile lifting equipment. Allow adequate floor space for use during maintenance. Additional access may be required for installation
- Prevent transmission of vibration by providing a foundation for the compressor, separate from the compressor-house foundation
- Consider the use of noise-absorbing materials and construction for a compressor house

The vendor's drawings should be examined to determine what auxiliary piping, valves and equipment covered in the following design points are to be supplied with the compressor by the vendor:

- Install the compressor on a concrete pad or elevated structure. Piling is often a necessary part of the foundation
- Large reciprocating compressors are often installed on an elevated structure to allow access to valves and provide space for piping. Provide a platform for operation and maintenance of such an installation
- Keep piping clear of cylinders of reciprocating compressors and provide withdrawal space at cylinder heads
- Use long-radius elbows or bends, not short-radius elbows or miters
- If the compressor and the pressurized gas are cooled with water, route cooling water first to the aftercooler, then to the intercooler (for a two-stage machine), and lastly to the cylinder jackets (or casing jacket, if present, in other types of compressor)
- Arrange an air compressor, associated equipment and piping so that water is able to drain continuously from the system
- Pipe a separate trapped drain for each pressure stage. Ensure that the pressure into which any trap discharges will be lower than that of the system being drained—less the pressure drop over the trap and its associated piping. Do not pipe different pressure stages thru separate check valves to a common trap
- If a toxic or otherwise hazardous gas is to be compressed, vent possible shaft seal leakage to the suction line to avoid a dangerous atmosphere forming around the compressor
- Do not overlook substantial space required for lube oil and seal oil control consoles for compressors
- Discuss piping arrangement with the stress group

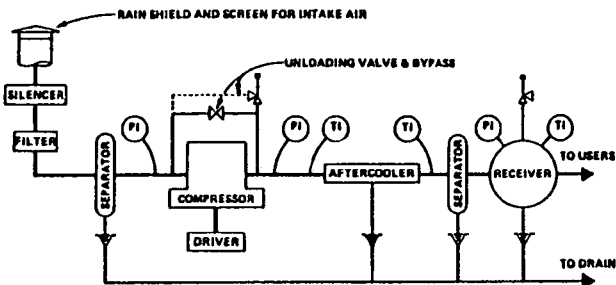
FIGURE 6.22

FIGURES  
6.20-6.22

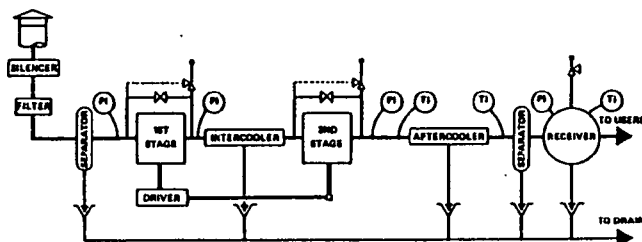
## SCHEMATIC ARRANGEMENTS OF COMPRESSED-AIR EQUIPMENT

FIGURE 6.23

### (a) SINGLE-STAGE COMPRESSOR



### (b) TWO-STAGE COMPRESSOR



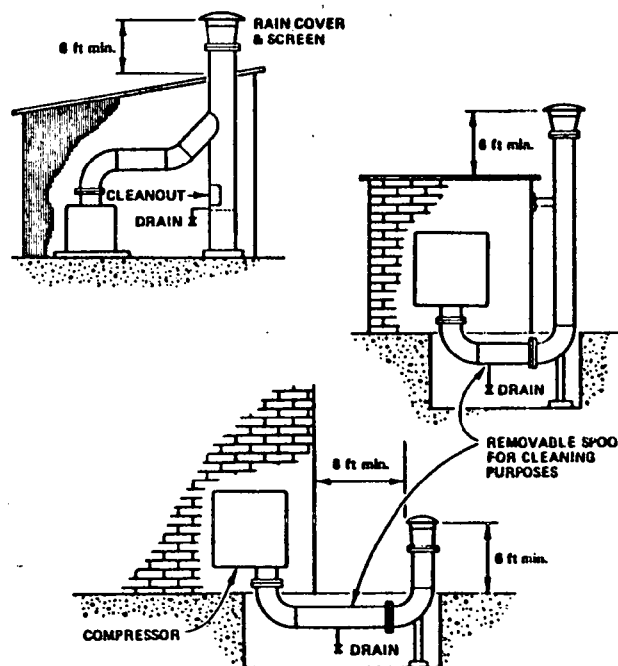
## SUCTION PIPING FOR AIR COMPRESSORS

- To reduce damage to a compressor by abrasion or corrosion, the air supply needs to be free from solids and water (water in the air intake does not affect operation of liquid-ring air compressors). Air intakes are best located where the atmosphere is uncontaminated by exhaust gases, industrial operations, or by traffic
- For efficiency the air supply should be taken from the coolest source such as the shaded side of a building, keeping to building clearances shown in figure 6.24
- If the air supply is from outside the building, locate the suction point above the roofline, and away from walls to avoid excessive noise
- Keep suction piping as short as possible. If a line is unavoidably long and condensate likely to form, provide a separator at the compressor intake
- Provide a rain cover and screen as shown in figure 6.24
- Small (and sometimes medium-sized) air compressors usually take air from inside a building. Large air compressors take air from outside a compressor house (figure 6.24): this minimizes effects on the building of pulsations radiated from the air inlet. In both instances, a filter is needed to remove dust, which is always present to some extent
- Filters must have capacity to retain large quantities of impurities with low pressure drop, and must be rugged enough to withstand pulsations from reciprocating compressors

- Provide a pressure gage connection between filter and compressor to allow the pressure drop across the filter to be measured in order to check when cleaning or replacement is needed
- Use a temporary screen at the compressor inlet at startup—see 2.10.4
- Avoid low points in suction lines where moisture and dirt can collect. If low points cannot be avoided, provide a clean-out—see figure 6.24
- If the suction line is taken from a header, take it from the top of the header to reduce the chance of drawing off moisture or sediment
- A line-size isolating valve is required for the suction line if the suction line draws from a header shared with other compressors
- Consider pickling or painting the inside of the suction piping to inhibit rust formation and lessen the risk of drawing rust into the compressor

## SUCTION LINES TO AIR COMPRESSORS

FIGURE 6.24



## DISCHARGE PIPING (GENERAL)

Discharge piping should be arranged to allow for thermal movement and draining. Anchors and braces should be provided to suppress vibration. The outflow from the aftercooler will usually be wet (from the excess moisture in suction air) and this water must be continually removed.

- An isolating valve in the discharge line is line-size
- Provide discharge piping with connections for temperature and pressure gages
- Provide an unloading valve and bypass circuit connected upstream of the discharge isolating valve, and downstream of the suction isolating valve, so as to ensure circulation thru the compressor during unloading, and to permit equalizing pressure in the compressor—see 3.2.2, under 'Unloading'
- Normally locate a receiver close to the compressor. (Auxiliary receivers may be located near points of heavy use.)
- For draining compressed-air discharge lines, refer to 6.11.4

The use of dampeners and volume bottles in the discharge is discussed in 3.2.2, under 'Equipment for compressors'.

#### LOADS & VIBRATION

The design of supports for piping to large compressors (especially for reciprocating machines) requires special knowledge. Usually, collaboration is necessary with the piping support group, the stress group, and the compressor manufacturer's representative. A major problem is that the compressor may be forced from alignment with its driver if the piping and supports are not properly arranged.

If a diesel or gasoline engine is used as driver, a flexible joint on the engine's exhaust pipe will reduce transmission of vibration, and protect the exhaust nozzle. Flexible connections are sometimes needed on discharge and suction piping. Pulsation in discharge and—to a lesser extent—suction lines, tends to vibrate piping. This effect is reduced by using bellows, large bends and laterals, instead of elbows and tees.

#### INSTRUMENTATION & INSTRUMENT CONNECTIONS

Figure 6.23 shows the more useful locations for pressure and temperature gages, but does not show instrumentation for starting, stopping and unloading the compressors. Simple compressor control arrangements using pressure switches have long been used, but result in frequent starting and stopping of the compressor, causing unnecessary wear to equipment.

Automatic control using an unloading valve is superior: table 3.6 gives the working principles—see 3.2.2, under 'Unloading'. Further information can be found in the 'Compressor installation manual' (Atlas-Copco). Unloading valves are allocated instrument numbers.

The air-pressure signals for unloading, starting, loading and stopping a compressor should be free from pulsations. It is best to take these signals from a connection on the receiver or a little downstream of it.

Details of construction of instrument connections are given in 6.7. Instrument branches should be braced to withstand transmission of line vibration.

#### ISOLATING VALVES FOR COMPRESSOR

Compressors operating in parallel should be provided with isolating valves arranged so that any compressor in the group may be shut down or removed. An isolating valve at the discharge should be placed downstream of the pressure-relief valve and any bypass valve connection. The isolating valve at the suction should be upstream of the bypass valve connection. Isolating valves are not required for a single compressor installation.

#### PRESSURE-RELIEF VALVES

Pressure-relief valves should be installed on interstage piping and on a discharge line from a compressor to the first downstream isolating valve. A pressure-relief valve may be vented to the suction line—see figure 6.23. Each pressure-relief valve should be able to discharge the full capacity of the compressor.

#### CHECK VALVE

Unless supplied with (or integral with) a compressor, a check valve must be provided to prevent backflow of stored compressed air or other gas.

#### DISTRIBUTION OF COMPRESSED AIR

Headers larger than 2-inch are often butt welded. Distribution lines are screwed and usually incorporate malleable-iron fittings, as explained in 2.5.1. Equipment used in distribution piping is described in 3.2.2.

A more efficient layout for compressed air lines is the ring main with auxiliary receivers placed as near as possible to points of heavy intermittent demand. The loop provides two-way air flow to any user.

#### COMPRESSED AIR USAGE

The compressed air provided for use in plants is designated 'instrument air', 'plant air' or 'process air'. Instrument air is cleaned and dried compressed air, used to prevent corrosion in some instruments. Plant air is compressed air but is usually neither cleaned nor dried, although most of the moisture and oil, etc., can be collected by a separator close to the compressor, especially if adequate cooling can take place. Plant air is used for cleaning, power tools, blowing out vessels, etc: if used for air-powered tools exclusively, some suspended oil is advantageous for lubrication, although filter/lube units are usually installed in the air line to the tool.

Process air is compressed air, cleaned and dried, which may be used in the process stream for oxidizing or agitation. The trend is to supply cleaned and dried air for both general process and instrument purposes. This avoids running separate lines for process and instrument air.

Process and instrument air for some applications requires to have an oil content less than 10 parts per million. As almost all oily contaminants are present as extremely small droplets (less than 1 micron in diameter) mechanical filtration may be ineffective; adsorption equipment can efficiently remove the oil.

## PIPING TO STEAM TURBINES

6.4

A turbine is a machine for deriving mechanical power (rotating shaft) from the expansion of a gas or vapor (usually air or steam, in industrial plants).

Steam turbines are used where there is a readily-available source of steam, and are also used to drive standby process pumps in critical service in the event of an electrical power failure, and emergency standby equipment such as firewater pumps and electric generators.

Figure 6.9 shows a schematic arrangement of piping for automatic operation. There are similarities between steam-turbine and pump and compressor piping. Their common requirements are:-

- (1) To limit loads on nozzles from weight of piping or from thermal movement
- (2) To provide access and overhead clearance
- (3) To prevent harmful material from entering the machine

### INLET (STEAM FEED)

6.4.1

In order to guard against damage to a steam turbine, protective piping arrangements such as those mentioned in table 6.4 are needed in the steam feed.

PROTECTIVE PIPING FOR FEEDING  
STEAM TO TURBINE

TABLE 6.4

HAZARD TO TURBINE	PROTECTIVE PIPING
FOREIGN MATTER & WATER IN THE STEAM FEED	DRIPLEG & STRAINER, or SEPARATOR, IN THE FEED LINE (See figure 6.9)
EXCESSIVE PRESSURE IN STEAM FEED CAUSING OVER-FAST RUNNING OR CASING RUPTURE	PRESSURE RELIEF VALVE &/OR CONTROL VALVE IN THE FEED LINE
THERMAL SHOCK, DUE TO TOO RAPID HEATING ON STARTUP	ORIFICE BYPASS TO FEED SMALL AMOUNT OF STEAM TO TURBINE AT ALL TIMES

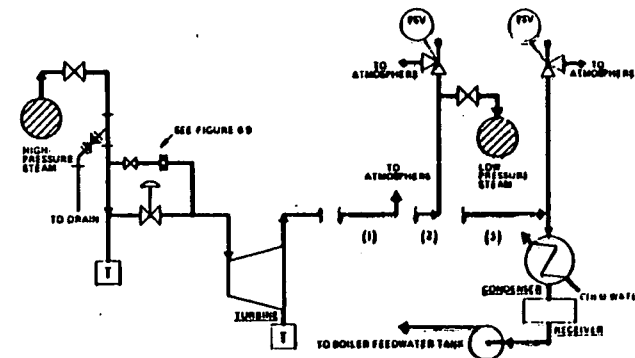
### EXHAUST (STEAM DISCHARGE)

6.4.2

Figure 6.25 shows three methods for dealing with the turbine's exhaust. Steam from an intermittently operated turbine may be run to waste and all that is required is a simple run of pipe to the nearest outside wall or up thru the roof. Exhausts should be well clear of the building and arranged so as not to be hazardous to personnel. The turbine discharge will include drops of water and oil from the turbine, which are best collected and run to drain. A device suitable for this purpose is a Swartwout 'exhaust head' shown in figure 6.26. Alternately, steam discharged from a continuously running turbine may be utilized elsewhere, in a lower-pressure system.

## TURBINE EXHAUST ARRANGEMENTS

FIGURE 6.25



### KEY:

- (1) Exhaust is discharged directly to atmosphere. Suitable for small turbine in intermittent use.
- (2) Exhaust is taken to a low-pressure header for use elsewhere. Suitable for continuously-operating turbine, to avoid wasting steam.
- (3) Exhaust is condensed to increase pressure drop across the turbine.

## BYPASS STEAM & OTHER PIPING FOR TURBINES

6.4.3

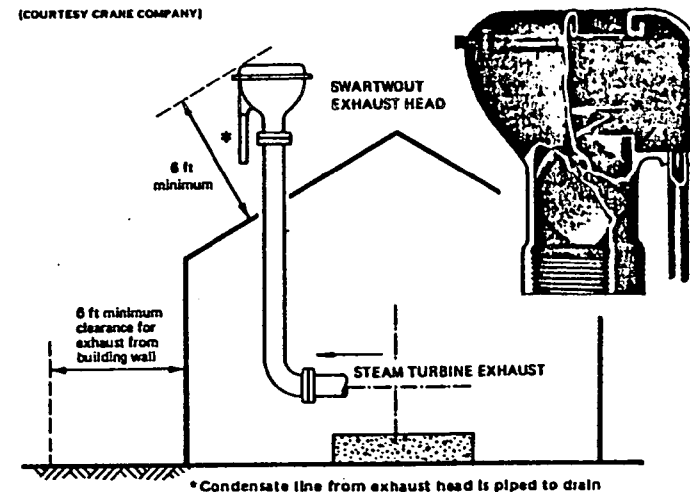
An orifice plate is used as a 'bleed' bypass to ensure that steam constantly passes thru the turbine. An orifice plate is used rather than a straight pipe, as a changeable constriction is needed. Alternately, the small amount of steam needed to keep the turbine warm can be admitted by a cracked-open valve in a bypass—a wasteful and uncertain practice.

A trap is fitted to the casing of the turbine to remove condensate. Piping is provided to supply seal liquid to the turbine's bearings—refer to 6.3.1, under 'Auxiliary, trim, or harness piping'.

### SWARTWOUT HEAD

(COURTESY CRANE COMPANY)

FIGURE 6.26



## VESSEL CONNECTIONS

6.5.1

Vessel connections are often made with couplings (for smaller lines), flanged or welding nozzles, and pads fitted with studs, designed to mate with flanged piping. Nozzle outlets are also made by extrusion, to give a shape like that of the branch of a welding tee—this gives a good flow pattern, but is an expensive method usually reserved for such items as manifolds and dished heads. Weldolets, sockolets and thredolets are suitable for vessel connections and are available flat-based for dished heads, tanks, and large vessels.

Almost any type of connection may be made to open vessels or vessels vented to atmosphere, but for pressure vessels, the applicable design code will dictate requirements for connections (and possible reinforcement—see 2.11).

## PRESSURE VESSELS

With exceptions and limitations stated in section 8 of the ASME Boiler and Pressure Vessel Code, vessels subject to internal or external operating pressures not exceeding 15 PSI need not be considered to be pressure vessels. A vessel operating under full or partial vacuum and not subject to an external pressure greater than 15 PSI would not require Code certification.

## VESSEL DRAWING &amp; REQUIRED NOZZLES

Preliminary piping layouts are made to determine a suitable nozzles arrangement. A sketch of the vessel showing all pertinent information is sent to the vessel fabricator, who then makes a detail drawing. The preliminary studies for pressure vessel piping layouts should indicate where pipe supports and platforms (if required) are to be located. In the event that the vessel has to be stress-relieved, the fabricator can provide clips or brackets—see 6.2.8, under 'Welding pipe-support and platform brackets to vessels, etc.'

Figure 5.14 shows the type of drawing or sketch sent to a vessel fabricator.

## NOZZLES NEEDED ON VESSELS

- Nozzles needed on non-pressure vessels include: inlet, outlet, vent (gas or air), manhole, drain, overflow, agitator, temperature element, level instrument, and a 'steamout' connection, sometimes arranged tangentially, for cleaning the vessel
- Nozzles needed on pressure vessels include: inlet, outlet, manhole, drain, pressure relief, agitator, level gage, pressure gage, temperature element, vent, and for 'steamout', as above
- Check whether nozzles are required for an electric heater, coils for heating or cooling, or vessel jacket. A jacket requires a drain and vent
- Check special nozzle needs, such as for flush-bottom tank valves (see 3.1.9)

## PIPE FLEXIBLY TO NOZZLES

- Provide additional flexibility in lines to a vessel from pumps and other equipment mounted on a separate foundation (if liable to settle)
- Be cautious in making rigid straight connections between nozzles. Such connections may be acceptable if both items of equipment are on the same foundation, and are not subject to more than normal atmospheric temperature changes (see figure 6.1)

## NOZZLE LOADING

- Ensure that a nozzle can take the load imposed on it by connected piping—see 6.2.8, under 'Supporting pipe at nozzles'. Manufacturers often can provide nozzle-loading data for their standard equipment
- Check all connections to ensure that stresses due to thermal movement, and shock pressures ('kicks') from opening pressure relief valves, etc., are safely handled

FRACTIONATION COLUMN PIPING  
(OR TOWER PIPING)

6.5.2

As columns and their associated equipment take different forms, according to process needs, the following text gives a simplified explanation of column operation, and outlines basic design considerations.

## THE COLUMN'S JOB

A fractionation column is a type of still. A simple still starts with mixed liquids, such as alcohol and water produced by fermenting a grain, etc., and by boiling produces a distillate in which the concentration of alcohol is many times higher than in the feed. In the petroleum industry in particular, mixtures not of two but a great many components are dealt with. Crude oil is a typical feed for a fractionation column, and from it the column can form simultaneously several distillates such as wax distillate, gas oil, heating oil, naphtha and fuel gases. These fractions are termed 'cuts'.

## COLUMN OPERATION

The feed is heated (in a 'furnace' or exchanger) before it enters the column. As the feed enters the column, quantities of vapor are given off by 'flashing', due to the release of pressure on the feed.

As the vapors rise up the column, they come into intimate contact with downflowing liquid—see figure 6.29. During this contact, some of the heavier components of the vapor are condensed, and some of the lighter components of the downflowing liquid are vaporized. This process is termed 'refluxing'.

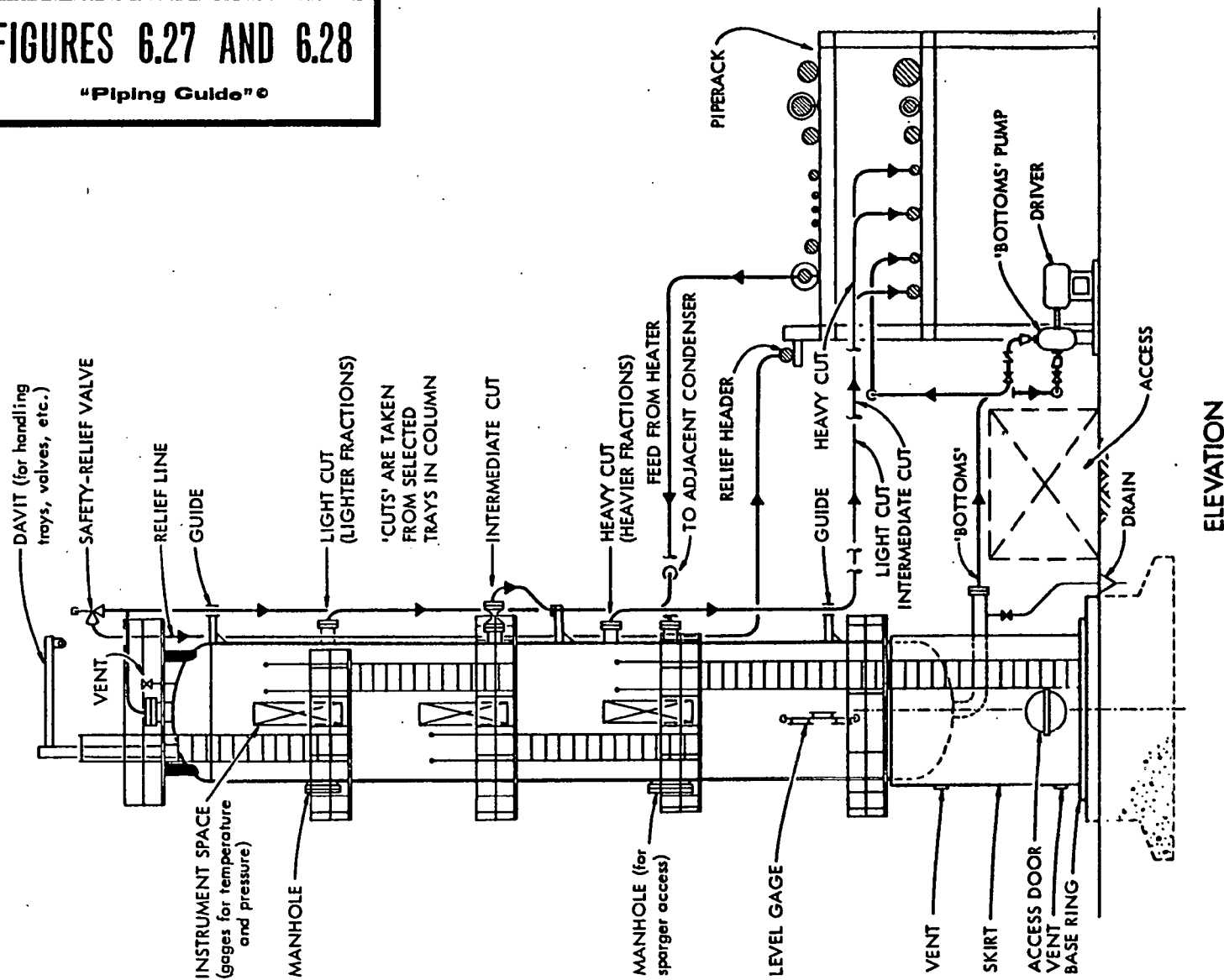
If the composition of the feed remains the same and the column is kept in steady operation, a temperature distribution establishes in the column. The temperature at any tray is the boiling point of the liquid on the tray. 'Cuts' are not taken from every tray. The P&ID shows cuts that are to be made, including alternatives—nozzles on selected trays are piped, and nozzles for alternate operation are provided with line blinds or valves.

6.4  
5.2FIGURES  
6.25 & 6.26TABLE  
6.4

# COLUMN PIPING

## FIGURES 6.27 AND 6.28

"Piping Guide"®



ELEVATION

FIGURE 6.27



Trays are of various designs. Their purpose is to collect a certain amount of liquid but allow vapors to pass up thru them so that vapor and liquid come into contact. (Refer to figure 6.29, which shows simple bubblecap trays—many tray designs are available.)

TRAYS &amp; BUBBLECAPS

FIGURE 6.29

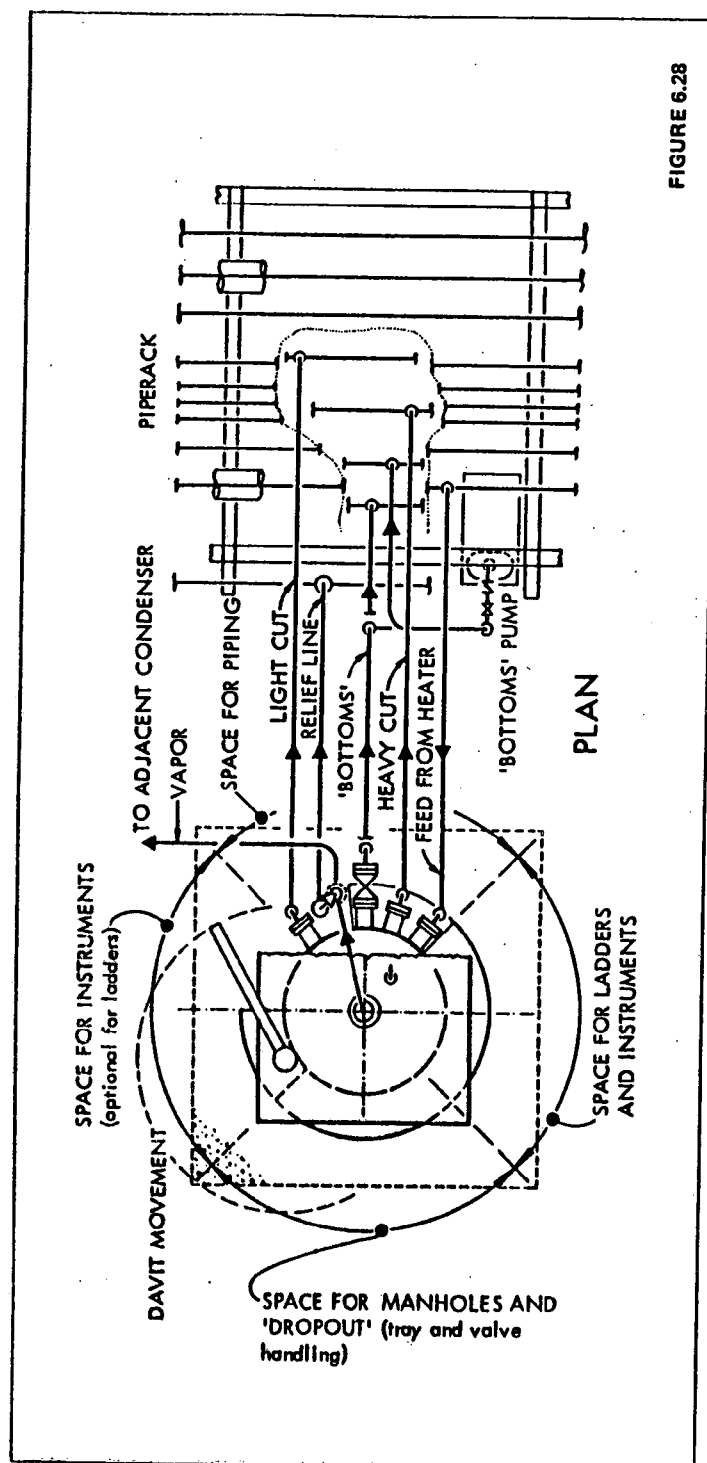
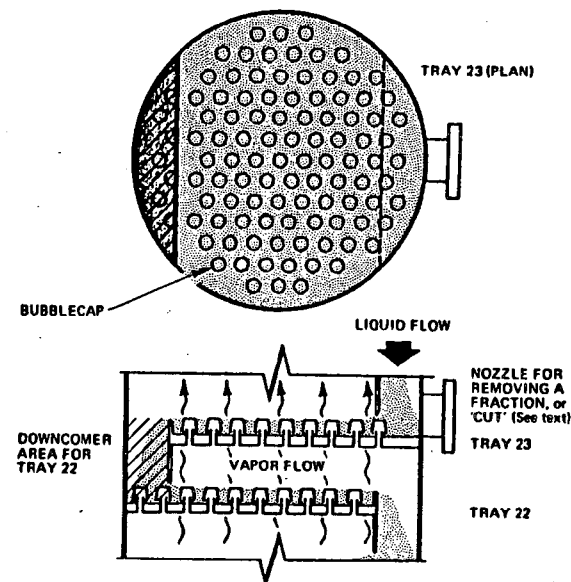


FIGURE 6.28

To produce the required 'cuts', a column operates under steady temperature, feed, and product removal conditions. Starting from cold, products are collected after steady conditions are reached, and the column is then operated continuously.

All materials enter and leave the column thru pipes; therefore columns are located close to piperacks. Figures 6.27 and 6.28 show an arrangement. Products from the column are piped to collecting tanks (termed 'drums', 'accumulators', etc.) and held for further processing, or storage.

If the vapor from the top of the column is condensible, it is piped to a condenser to form a volatile liquid. The condenser may be mounted at grade, or sometimes on the side of the column.

Product from the top of the column may be gaseous at atmospheric pressure after cooling; if the product liquefies under moderate pressure, it may be stored pressurized in containers.

In addition to the condenser for the top product, a steam-heated heat exchanger, termed a 'reboiler', may be used to heat material drawn from a selected level in a column; the heated material is returned to the column. Reboilers are required for tall columns, and for columns operated at high temperatures, which are subject to appreciable loss of heat. Mounting the reboiler on the side of the column minimizes piping.

FIGURES  
6.27 & 6.29

Material from the bottom of a column is termed 'bottoms', and must be pumped away (see figure 6.27)—this material consists of 'heavier' (higher molecular weight) liquids which either did not vaporize, or had condensed, plus any highly viscous material and solids in the feed.

### COLUMN ORIENTATION & REQUIREMENTS

Simultaneously with orientating nozzles and arranging piping to the column, the piping designer decides the positions of manholes, platforms, ladders, davit, and instruments.

COLUMN ORIENTATION

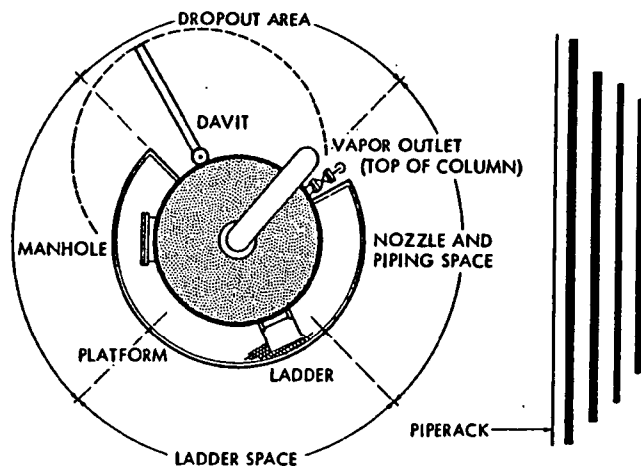


FIGURE 6.30

Manholes are necessary to allow installation and removal of tray parts.

Platforms and ladders are required for personnel access to valves on nozzles, to manholes, and to column instruments.

A davit is needed to raise and lower column parts, and a dropout area has to be reserved.

### MANHOLES & NOZZLES

For a particular project or column, manholes are preferably of the same type. They should be located away from piping, and within range of the davit.

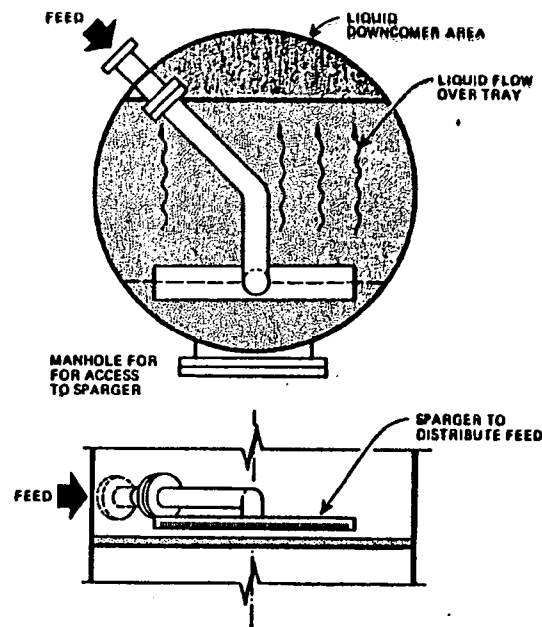
If required, manholes can be placed off the column centerlines (plan view).

The manhole serving the sparger unit (figure 6.31) should permit easy removal of the unit, which may be angled to place the feed connection in a desired position.

The portions of the column wall available for nozzles are determined by the orientation and type of tray—see figure 6.29. Elevations of nozzles are taken from the column data sheet (normally in the form of a vessel drawing).

SPARGER UNIT

FIGURE 6.31



If the cuts are to be taken either from even-numbered trays, or from odd-numbered trays, all nozzles can be located on one side of the column, facing the piperack. If cuts are to come from both even- and odd-numbered trays, it will almost certainly be impossible to arrange all nozzles toward the piperack. (See 'Arranging column piping', this section.)

### PLATFORMS & LADDERS

Platforms are required under manholes, valves at nozzles, level gages, controllers if any, and pressure relief valves. Columns may be grouped and sometimes interconnecting platforms between columns are used. Individual platforms for a column are usually shaped as circular segments, as shown in figure 6.30. A platform is required at the top of the column, for operating a davit, a vent on shutdown, and for access to the safety-relief valve. This top platform is often rectangular.

Usual practice is to provide a separate ladder to go from grade past the lowest platform. Ladders are arranged so that the operator steps sideways onto the platforms.

Ladder length is usually restricted to 30 ft between landings. Some States allow 40 ft (check local codes). If operating platforms are further apart than the maximum permissible ladder height, a small intermediate platform is provided.

Ladders and cages should conform to the company standard and satisfy the requirements of the US Department of Labor (OSHA), part 1910 (D).

## DAVIT

Referring to figure 6.30, the davit should be located at the top of the column so that it can lower and raise tray parts, piping, valves, etc., between the platforms and the dropout area at grade.

## ARRANGING COLUMN PIPING

To achieve simplicity and good arrangement, some trial-and-error working is necessary. Columns are major pieces of equipment, and their piping needs take precedence over other piping.

As lines from nozzles on the column are run down the length of the column, it is logical to start arranging downcomers from the top and proceed down the column. A lower nozzle may need priority, but usually piping can be arranged more efficiently if the space requirements of piping coming from above are already established.

Sometimes tray spacing is increased slightly to permit installation of manholes. It may be possible to rotate trays within limits, to overcome a difficulty in arranging column piping. Such changes in tray spacing and arrangement must be sanctioned by the process engineer and vessel designer.

- Allocate space for vertical lines from lower nozzles, avoiding running these lines thru platforms if possible
- Lines from the tops of columns tend to be larger than others. Allocate space for them first, keeping the lines about 12 inches from the platforms and the wall of the column—this makes supporting easier, and permits access to valves, instruments, etc.
- Allocate space for access (manholes, ladders) clear of piping—especially clear of vertical lines
- Provide a clear space for lowering equipment from the top of a column (for maintenance, etc.)
- Provide access for mobile lifting equipment to condenser and reboiler
- Provide clearance to grade (approximately 8ft) under the suction line, from the column to the bottoms pump
- Arrange vent(s) in the skirt of the column
- Ensure that no low point occurs in the line conveying 'bottoms' to the suction port of the bottoms pump, in order to avoid blocking of this line due to cooling, etc.

## INFORMATION NEEDED TO ARRANGE THE COLUMN PIPING

- Plot plan showing space available for column location, and details of equipment which is to connect to the column
- P&ID for nozzle connections, NPSH of bottoms pump, instrumentation, line blinds, relief valves, etc.
- Column data sheets and sketch of column showing elevations of nozzles

- Line designation sheets, to obtain operating temperatures of lines for calculating thermal movement
- Details of trays and other internal parts of the column
- Restrictions on the heights of ladders
- Operational requirements for the plant

## BOTTOMS PUMP & ELEVATION OF COLUMN

The elevation of a column is set primarily by the NPSH required by the bottoms pump, the access required under the suction line to the bottoms pump, and by requirements for a thermosyphon reboiler, if used.

## VALVES

Valves and blinds which serve the tower should be positioned directly on nozzles, for economy. It is desirable to arrange other valves so that lines are self-draining.

Platforms should be located to give access to large valves. Small valves may be located at the ends of platforms. Control valves should be accessible from operating platforms or from grade.

The pressure-relief valve for the relief line should be placed at the highest point in the line, and should be accessible from the top platform.

Valves should not be located within the skirt of the column.

## INSTRUMENTS & CONNECTIONS

Temperature connections should be located to communicate with liquids in the trays, and pressure connections with the vapor spaces below the trays. Access to isolated gages can be provided by ladder.

Gages, and gage and level glasses, must be visible when operating valves, and be accessible for maintenance.

Gages and other instruments should be located clear of manholes and accessways to ladders and platforms. If necessary, temperature and pressure gages may be located for reading from ladders. Locating instruments at one end of a circular platform may allow a narrower platform.

## THERMAL INSULATION

Thermal insulation of the exterior of a column may be required in order to reduce heat loss to the atmosphere. Insulation may be inadequate to maintain the required temperature distribution; in these circumstances, a reboiler is used. Thermal insulation is discussed in 6.8.1.

## FOUNDATION FOR COLUMN

The base ring of a column's skirt is attached to a reinforced-concrete construction. The lower part of this construction, termed the 'foundation', is below grade, and is square in plan view; the upper part, termed the 'base', to which the base ring is attached, is usually octagonal and projects above grade approximately 6 inches.

Heat exchangers are discussed in 3.3.5.

### DATA NEEDED TO PLAN EXCHANGER PIPING

6.6.1

Preliminary exchanger information should be given early to the piping group, so that piping studies can be made with special reference to orientation of nozzles. Before arranging heat-exchanger piping, the following information is needed:

**PROCESS FLOW DIAGRAM** This will show the fluids that are to be handled by the exchangers, and will state their flow rates, temperatures and pressures.

**EXCHANGER DATA SHEETS** One of these sheets is compiled for each exchanger design by the project group. The piping group provides nozzle orientation sketches (resulting from the piping studies). The data sheet informs the manufacturer or vendor of the exchanger concerning performance and code stamp requirements, materials, and possible dimensional limitations.

### TEMA CODING FOR EXCHANGER TYPE

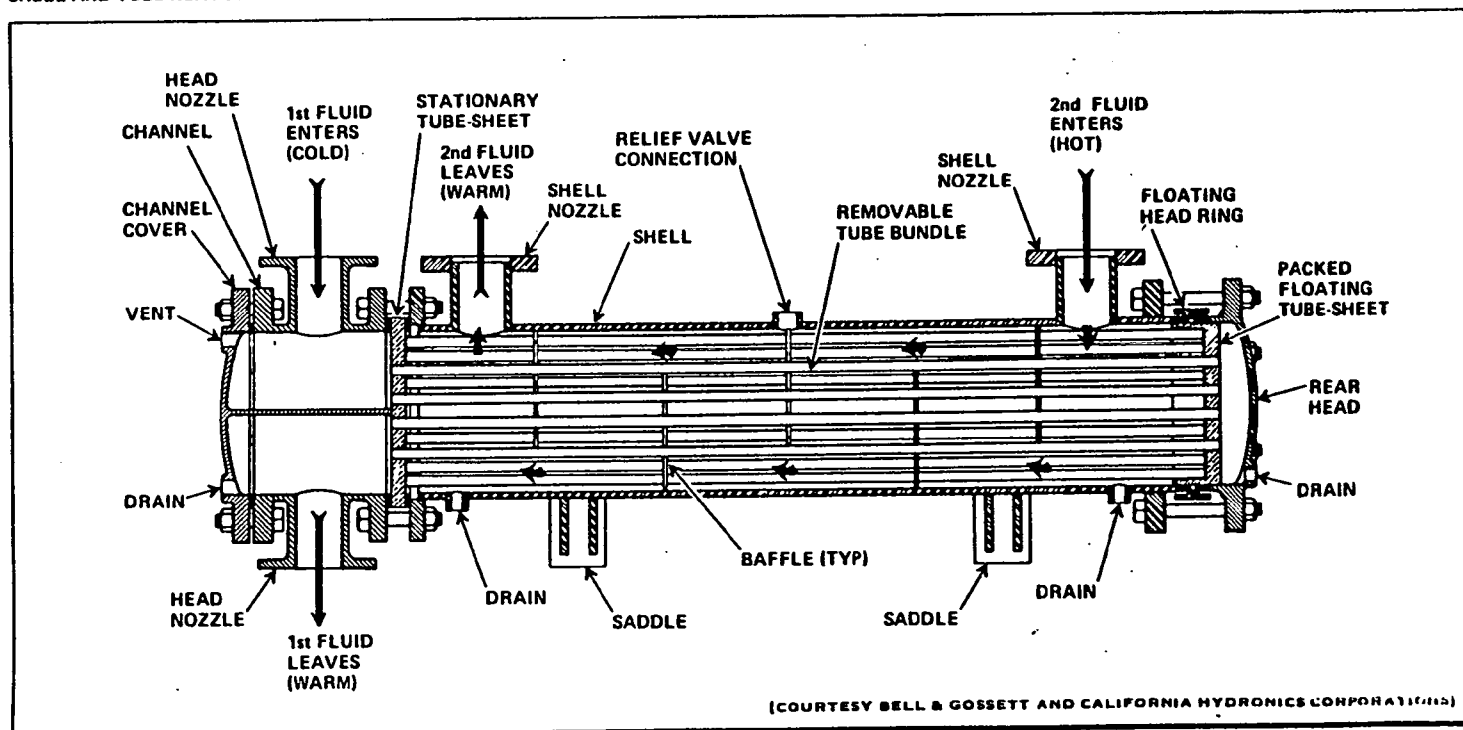
The Tubular Exchangers Manufacturers Association (TEMA) has devised a method for designating exchanger types, using a letter coding. The exchanger shown in figure 6.32 would have the basic designation AEW. See chart H-1.

### Engineering Notes:

- Provide the shell with a pressure-relieving device to protect against excessive shell-side pressure in the event of internal failure
- Put fouling and/or corrosive fluids inside the tubes as these are (except U-type) easily cleaned, and cheaper to replace than the shell
- Put the hotter fluid in the tubes to reduce heat loss to the surroundings
- However, if steam is used to heat a fluid in an exchanger, passing the steam thru the shell has advantages: for example, condensate is far easier to handle shellside. Insulation of the shell is normally required to protect personnel, and to reduce the rates of condensate formation and heat loss
- Pass refrigerant or cooling liquid thru the tubes, if the exchanger is not insulated, for economic operation
- If heat transfer is between two liquids, a countercurrent flow pattern will usually give greater overall heat transfer than a parallel flow pattern, other factors being the same
- Orientate single-tube spiral, helical and U-tube exchangers (with steam fed thru the tube) to permit outflow of condensate

SHELL-AND-TUBE HEAT EXCHANGER WITH REMOVABLE TUBE BUNDLE

FIGURE 6.32



#### Nozzle Positions:

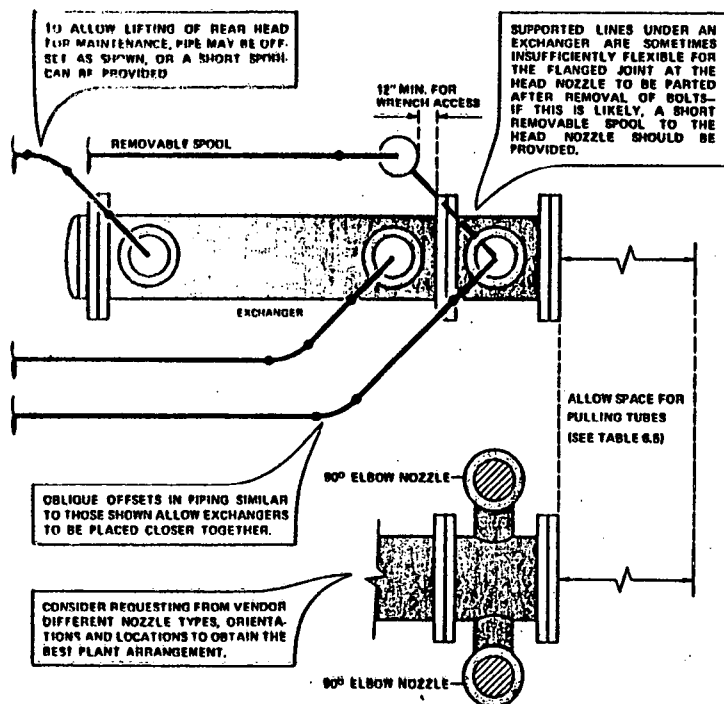
- Arrange nozzles to suit the best piping and plant layout. Nozzles may be positioned tangentially or on elbows, as well as on vertical or horizontal centerlines (as usually offered at first by vendors). Although a tangential or elbowed nozzle is more expensive, it may permit economies in piping multiple heat exchangers
- Make condensing vapor the descending stream
- Make vaporizing fluid the ascending stream

#### Locating Exchangers:

- Position exchangers so that piping is as direct and simple as possible. To achieve this, consider alternatives, such as reversing flows, arranging exchangers side-by-side or stacking them, to minimize piping
- Elevate an exchanger to allow piping to the exchanger's nozzles to be arranged above grade or floor level, unless piping is to be brought up thru a floor or from a trench
- Exchangers are sometimes of necessity mounted on structures, process columns and other equipment. Special arrangements for maintenance and tube handling will be required

#### PIPING TO NOZZLES OF HEAT EXCHANGERS

FIGURE 6.33

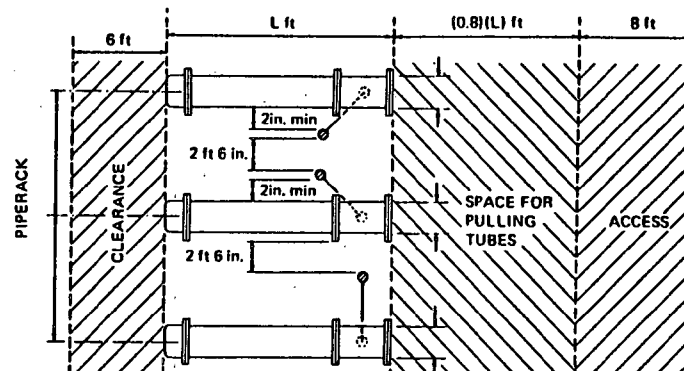


#### MINIMUM SPACING & CLEARANCES FOR MULTIPLE HEAT EXCHANGERS

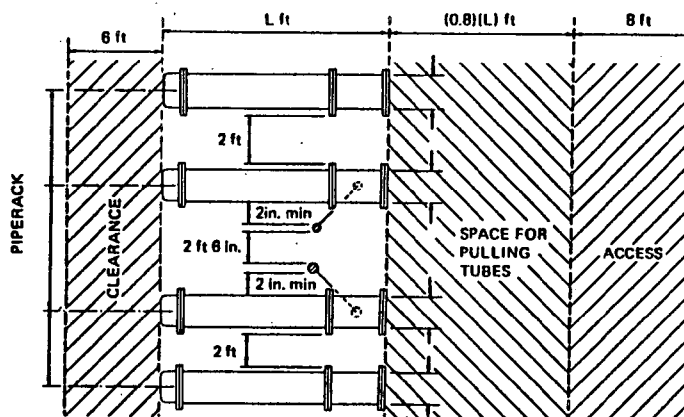
TABLE 6.5

6 .6  
.6.2

(a) Exchangers arranged with 2 ft 6 in. operating space between piping



(b) Exchangers arranged with 2 ft 0 in. maintenance space between paired units and 2 ft 6 in. operating space between piping



NOTES	(1) Show outlines of exchanger supports or foundations before arranging piping
	(2) Add to clearances shown, thicknesses of insulation for exchanger shells and connected piping
	(3) Provide additional clearance to the 2'-6" operating space if valve handwheels and valve stems, etc., protrude, depending on piping arrangement

#### Operating and Maintenance Requirements:

- Access to operating valves and instruments (on one side only suffices)
- Operating space for any davit, monorail or crane, etc., both for movement and to set loads down
- Access to exchanger — space is needed for tube-bundle removal, for cleaning, and around the exchanger's bolted ends (channelcover and rear head) and the bolted channel-to-shell closure
- Access for tube bundle removal is often given on manufacturers' drawings, and is usually about 1½ times the bundle length. 15 to 20 ft clearance should be allocated from the outer side of the last exchanger in a row for mobile lifting equipment access and tube handling

FIGURES  
6.32 & 6.33

TABLE  
6.5

# INSTRUMENT CONNECTIONS

ALTERNATE BRANCH CONNECTIONS SUITABLE FOR INSTRUMENTS ARE DESCRIBED IN 2.3.2 (FOR BUTT-WELDED SYSTEMS), 2.4.2 (FOR SOCKET-WELDED SYSTEMS) AND IN 2.6.2 (FOR SCREWED SYSTEMS)

## CHART 6.2

LINE SIZE (INCHES)		1/2	3/4	THRU 1 1/2	2	2 1/2	3	4	6	AND LARGER
TEMPERATURE CONNECTIONS	SCREWED THERMOWELLS IN STRAIGHT RUNS	<p>PIPE, 4" MIN. x 6" LONG</p> <p>THREADOLET, 1"</p> <p>SWAGE, TEE-BLE</p> <p>LINE EXPANSION REQUIRED FOR THERMOWELL PENETRATION</p>			<p>THREADOLET, 1"</p> <p>PIPE, 4" MIN. x 6" LONG</p> <p>REDUCER, SW</p>			<p>ALTERNATE CONNECTIONS</p> <p>THREADOLET, 1" THREADED</p> <p>THREADOLET, 1"</p>		
	SCREWED THERMOWELLS IN ELBOWS	<p>SWAGE, TEE</p> <p>TEE, SCRD 1" MIN</p> <p>IF D IS 1" OR LARGER, A REDUCING BUSHING MAY BE NEEDED TO FIT THERMOWELL</p> <p>*Swages are not needed if D is 1" or larger</p>			<p>REDUCER, 3" x D" SW</p> <p>ELBOW, 3" SW</p> <p>ELBOWLET, 1" THREADED</p>			<p>ELBOW, D" SW</p> <p>ELBOWLET, 1" THREADED</p>		
	FLANGED THERMOWELLS IN STRAIGHT RUNS	<p>IF GREATER STRENGTH IS REQUIRED, THE NIPPLE IS SHORTENED SO THAT THE WELD IS PARTLY ON THE SHOULDER OF THE NIPPLET</p>			<p>FLANGE, 1 1/2" SW</p> <p>REDUCER, SW</p> <p>NIPPLET, 1 1/2" PSE</p> <p>REDUCER, SW</p> <p>PIPE, 4" MIN x 6" LONG</p>			<p>FLANGE, 1 1/2" SW</p> <p>NIPPLET, 1 1/2" PSE</p>		
	FLANGED THERMOWELLS IN ELBOWS				<p>SWAGE, D" x 3" PSE-BLE</p> <p>ELBOW, 2" SW</p> <p>FLANGE, 1 1/2" SW</p> <p>NIPPLE, 1 1/2" x 3" PSE</p> <p>ELBOWLET, 1 1/2" SW</p>			<p>ELBOW, D" SW</p> <p>FLANGE 1 1/2" SW</p> <p>NIPPLE, 1 1/2" x 3" PSE</p> <p>ELBOWLET, 1 1/2" SW</p>		
	SCREWED CONNECTIONS FOR PRESSURE INSTRUMENTS	<p>SCRD NIPPLE, 1/2" x 3" TBE</p> <p>TEE, 1/2" SCRD</p>			<p>SWAGE, D" x 3/4" TBE (OR NIPPLE, 3/4" TBE)</p> <p>TEE, D" SCRD</p>			<p>VALVE, 3/4"</p> <p>NIPPLET, 3/4"</p> <p>Optional for 6-inch and larger lines</p>		
SOCKET-WELDED CONNECTIONS FOR PRESSURE INSTRUMENTS	<p>VALVE, 1/2"</p> <p>SCRD NIPPLE, 1/2" x 3" PSE-TBE</p> <p>TEE, 1/2" SW</p>			<p>VALVE, 3/4"</p> <p>SWAGE, D" x 3/4" PSE-TBE (OR NIPPLE, 3/4" PSE-TBE)</p> <p>TEE, D" SW</p>						
DIAPHRAGM-ISOLATED INSTRUMENT CONNECTIONS (for welded lines)	<p>CONNECTIONS SMALLER THAN 3/4-INCH ARE NOT USED BY SOME COMPANIES</p> <p>DIAPHRAGM ASSEMBLY</p> <p>NIPPLE, 3/4" x 3"</p> <p>VALVE, 3/4"</p> <p>NIPPLET, 3/4"</p>			<p>DIAPHRAGM ASSEMBLY</p> <p>NIPPLE, 3/4"</p> <p>VALVE, 3/4"</p> <p>NIPPLET, 3/4"</p>			<p>DIAPHRAGM ASSEMBLY</p> <p>NIPPLE, 1" x 3"</p> <p>VALVE, 1"</p> <p>NIPPLET, 1"</p>			
"Piping Guide", P.O. Box 277, Colton, CA 94928, USA										

## INSTRUMENT CONNECTIONS

6.7

### PRIMARY CONNECTIONS TO LINES & EQUIPMENT

6.7.1

Connections will usually be specified by company standards or by the specifications for the project. If no specification exists, full- and half-couplings, swaged nipples, threaded nipples, nipolets and elbolets, etc., may be used. Chart 6.2 illustrates instrument connections used for lines of various sizes. The fittings shown in chart 6.2 are described in chapter 2. Orifice flange connections are discussed in 6.7.5.

### CHOOSING THE CONNECTION

6.7.2

The choice of instrument connection will depend on the conveyed fluid and sometimes on the required penetration of the element into the vessel or pipe. Instrument connections should be designed so that servicing or replacement of instruments can be carried out without interrupting the process. Valves are needed to isolate gages for maintenance during plant operation and during hydrostatic testing of the piping system. These valves are shown in chart 6.2 and are referred to as 'root' or 'primary' valves.

### TEMPERATURE & PRESSURE CONNECTIONS

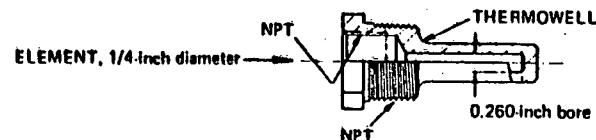
6.7.3

Chart 6.2 illustrates various methods for making temperature and pressure connections. At the bottom of chart 6.2 a method of connecting a diaphragm flange assembly (diaphragm isolator) is shown. Corrosive, abrasive or viscous fluid in the process line presses on one side of the flexible diaphragm, and the neutral fluid (glycol, etc.) on the other side transmits the pressure.

If the conveyed fluid is hazardous or under high pressure a branch fitted with a bleed valve is inserted between the gage and its isolating valve, to relieve pressure and/or drain the liquid before servicing the gage. The bleed valve can also be used to sample, or for adding a comparison gage.

- Position connections for instruments so that the instruments can be seen when operating associated valves, etc.
- Pressure connections for vessels containing liquids are usually best located above liquid level
- A temperature-measuring element is inserted into a metal housing termed a 'thermowell'. Place thermowells so that they are in contact with the fluid—an elbow is a good location, due to the increased turbulence

### THERMOWELL CONSTRUCTION (EXAMPLE)



## LEVEL GAGE CONNECTIONS (TYPICAL)

6.7.4

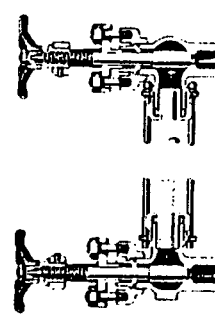
- Locate a liquid level controller (float type, for example) clear of any turbulence from nozzles
- More than one level gage, level switch, etc., may be required on a vessel: consider installing a 'strongback' to a horizontal vessel on which instrument connections have to be made—see figure 6.34(c)

### LEVEL-GAGE CONNECTIONS

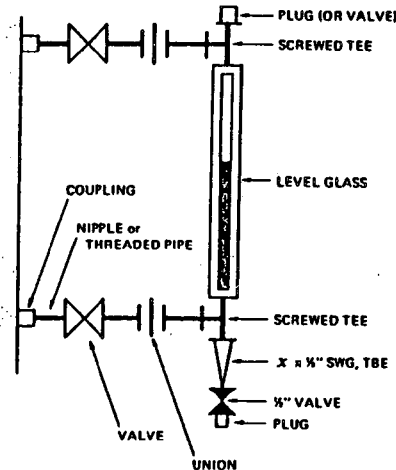
FIGURE 6.34

#### (a) LEVEL GAGE ASSEMBLY

(COURTESY THE WILLOW COMPANY)



#### (b) CONNECTIONS FOR A GAGE GLASS



#### (c) CONNECTIONS ON STRONGBACK

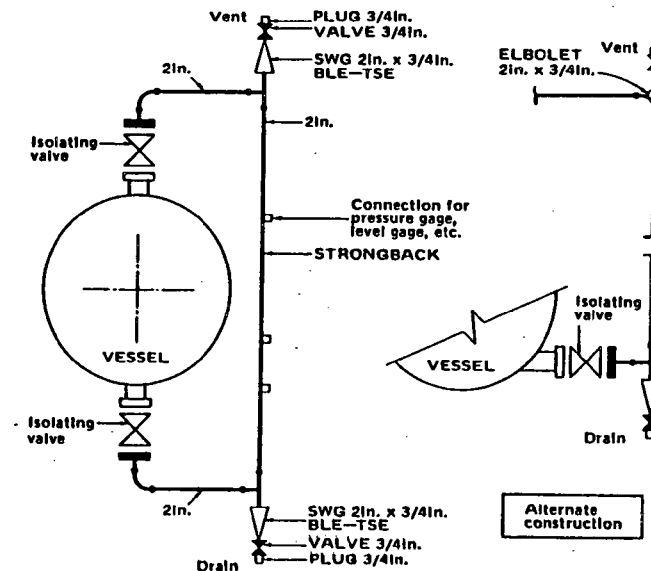


CHART  
6.2

FIGURE  
6.34

### ROTAMETER CONNECTIONS

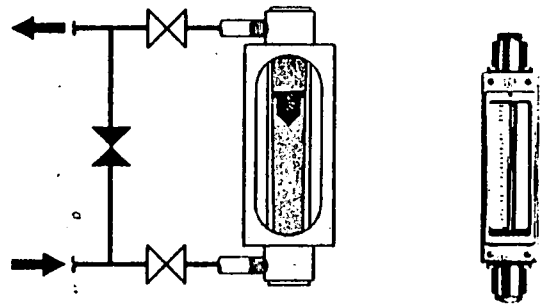
A rotameter consists of a transparent tube with tapered and calibrated bore, arranged vertically, wide end up, supported in a casing or framework with end connections. The instrument should be connected so that flow enters at the lower end and leaves at the top. A ball or spinner rides on the rising gas or liquid inside the tapered tube — the greater the flow rate, the higher the ball or spinner rides. Isolating valves and a bypass should be provided, as in figure 6.35

ROTAMETER

FIGURE 6.35

(a) PIPING TO ROTAMETER

(b) INDUSTRIAL ROTAMETER



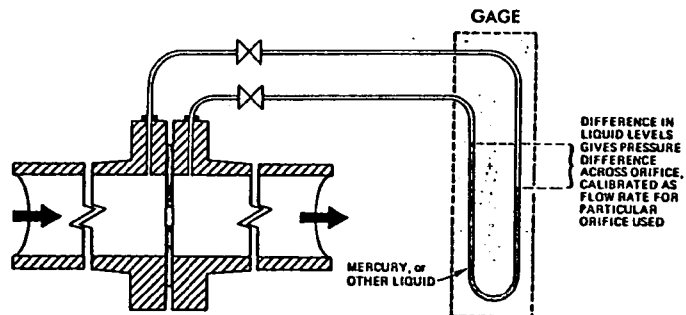
(COURTESY BK INSTRUMENTS DIV. OF  
SCHUTTE & ADERTING COMPANY)

### ORIFICE PLATE ASSEMBLY

An 'orifice plate' is a flat disc with a precisely-made hole at its center. It offers a well-defined obstruction to flow when inserted in a line—see figure 6.36. The resistance of the orifice sets up a pressure difference in the fluid either side of the plate, which can be used to measure the rate of flow.

ORIFICE PLATE ASSEMBLY & GAGE (MANOMETER)

FIGURE 6.36



The orifice plate is held between special flanges having 'orifice taps'—these are tapped holes made in the flange rims, to which tubing and a pressure gage can be connected, as in figure 6.36. A pressure gage may be termed a 'manometer'.

Manometers for use with orifice plate assemblies are calibrated in terms of differential pressure by the manufacturer. The meter run (that is, the piping in which the orifice plate is to be installed) must correspond with the piping used to calibrate the orifice plate—the readings will be in error if there is very much variation in these two piping arrangements.

Sometimes the orifice assembly includes adjacent piping, ready for welding in place. Otherwise, lengths of straight pipe, free from welds, branches or obstruction, should be provided upstream and downstream of the orifice assembly.

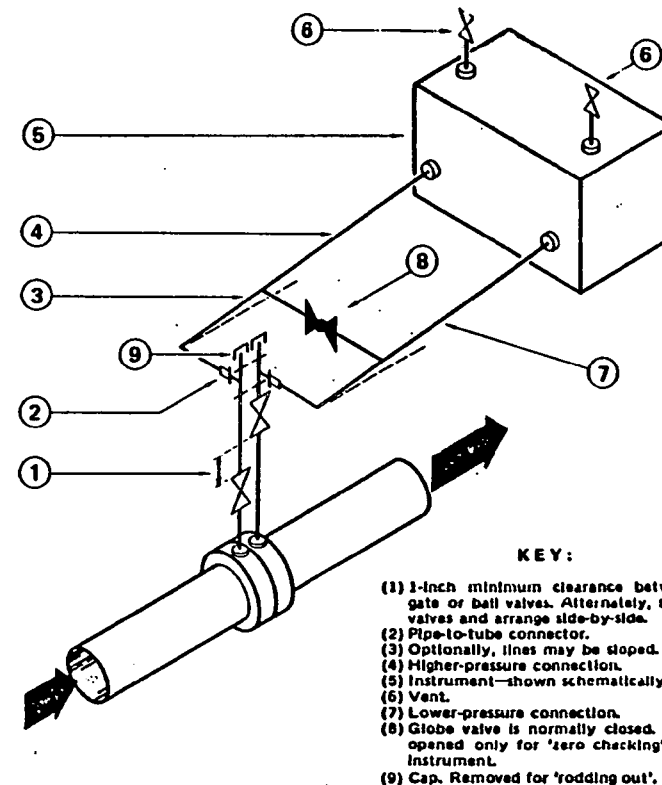
Table 6.6 shows lengths of straight pipe required upstream and downstream of orifice flanges (for different piping arrangements) to sufficiently reduce turbulence in liquids for reliable measurement.

### PIPING TO FLANGE TAPS

Figure 6.37 shows a suitable tapping and valving arrangement at orifice flange taps. In horizontal runs, the taps are located at the tops of the flanges in gas, steam and vapor lines. An approximately horizontal position avoids vapor locks in liquid lines. Taps should not be pointed downward, as sediment may collect in pipes and tubes.

CONNECTIONS TO ORIFICE FLANGES  
& INSTRUMENT

FIGURE 6.37





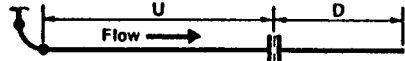
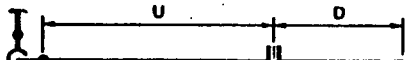
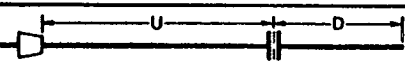
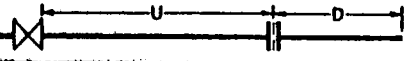
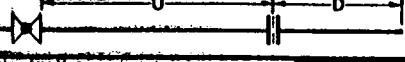
STRAIGHT PIPE RUN TO THE ORIFICE

The arrangement of orifice plate assemblies should be made in consultation with the instrument engineer. Usually, it is preferred to locate orifice plate assemblies in horizontal lines.

Flow conditions consistent with those used to calibrate the instrument are ensured by providing adequately long straight sections of pipe upstream and downstream of the orifice. Table 6.6 gives lengths that have been found satisfactory for liquids.

STRAIGHT PIPE UPSTREAM & DOWNSTREAM OF ORIFICE ASSEMBLY

TABLE 6.6

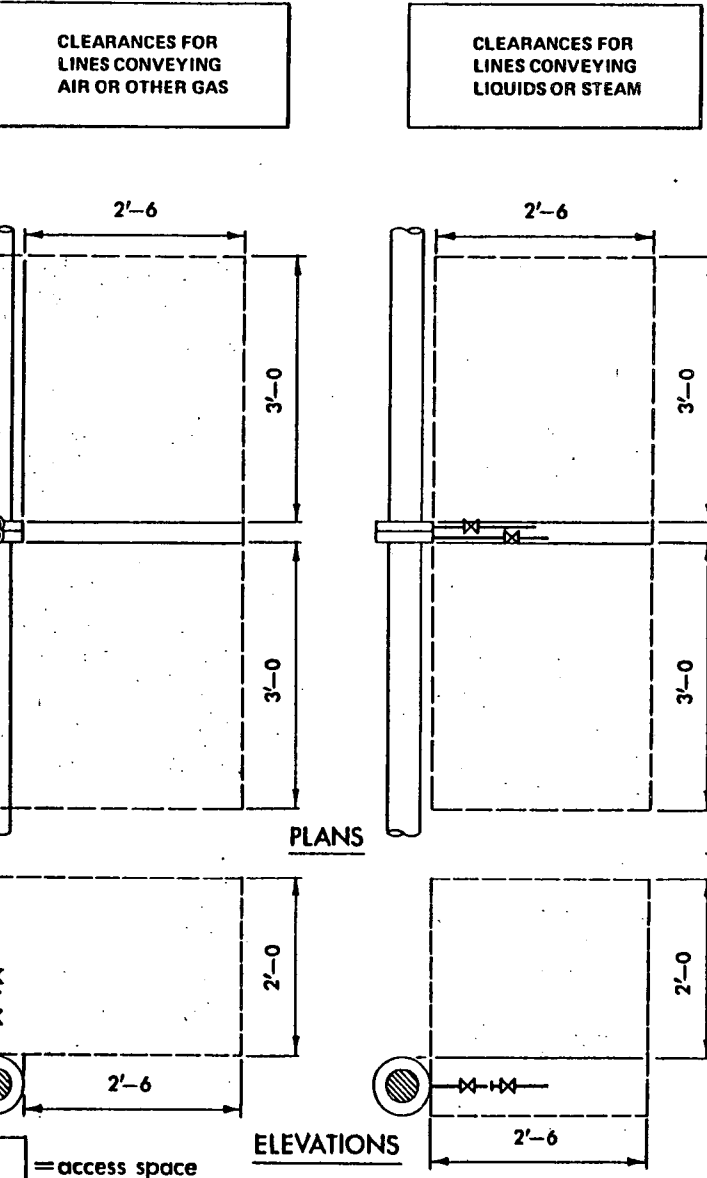
KEY NUMBER OF PIPING ARRANGEMENT	U-UPSTREAM D-DOWNSTREAM	RATIO OF INTERNAL DIAMETERS OF ORIFICE PLATE AND PIPE					
		1 : 8	1 : 4	3 : 8	1 : 2	5 : 8	3 : 4 *
		MINIMUM RUNS OF STRAIGHT PIPE REQUIRED UPSTREAM AND DOWNSTREAM OF ORIFICE, IN PIPE DIAMETERS (NPS)					
1	U	6	6	6	6%	10	17
	D	2%	3	3%	3%	4	4%
2	U	13	13	13	15	20	31
	D	2%	3	3%	3%	4	4%
3	U	6	6	6	7%	10%	13%
	D	2%	3	3%	3%	4	4%
4	U	5	5	5%	6%	8%	11
	D	2%	3	3%	3%	4	4%
5	U	18%	18%	21%	25	32	44
	D	2%	3	3%	3%	4	4%
* USE THIS COLUMN FOR PRELIMINARY PLANNING							
KEY: PIPING ARRANGEMENTS FOR ABOVE RUN LENGTHS							
1	Ell or Tee						
2	Two 90° Ells						
3	Reducer or Increaser						
4	Gate Valve						
5	Globe Valve						

CLEARANCES

Clear space should be left around an orifice assembly. Figure 6.38 shows minimum clearances required for mounting instruments, seal pots, etc., and for maintenance.

CLEARANCES TO ORIFICE ASSEMBLIES

FIGURE 6.38



## KEEPING PROCESS MATERIAL AT THE RIGHT TEMPERATURE

6.8

To ensure continuity of plant operations it is necessary to maintain some process, service and utility lines within a desired temperature range in order to keep materials in a fluid state, to prevent degradation, and to prevent damage caused by liquids freezing in cold conditions. Piping can be kept warm by insulation, or by applying heat to the insulated piping—this is 'jacketing' or 'tracing', as discussed in 6.8.2 and 6.8.3.

### THERMAL INSULATION

6.8.1

#### REFERENCE

'Keeping piping hot—Part I'. Chapman F.S. & Holland F.A. 1965. Chemical Engineering reprint. Chemical Engineering, Dec 20

#### INSULATION

'Insulation' is covering material having poor thermal conductivity applied externally to pipe and vessels, and is used: (1) To retain heat in a pipe or vessel so as to maintain process temperature or prevent freezing. (2) To minimize transfer of heat from the surroundings into the line or vessel. (3) To safeguard personnel from hot lines. The choice of insulation is normally included with the piping specification. The method of showing insulation on piping drawings is included in chart 5.7.

Installed insulation normally consists of three parts: (1) The thermal insulating material. (2) The protective covering for it. (3) The metal banding to fasten the covering. Most insulating materials are supplied in formed pieces to fit elbows, etc. Formed coverings are also available. Additionally, it is customary to paint the installed insulation, and to weatherproof it before painting, if for external use. See [43, pages 6.14 to 6.16] and [27, chapter 9].

The principal thermal insulating materials and their accepted approximate maximum line temperatures, where temperature cycling (repetitive heating and cooling periods) occurs are: asbestos (1200 F), calcium silicate (1200 F), cellular glass [foamglas] (800 F), cellular silica (1600 F), diatomaceous silica plus asbestos (1600 F), mineral fiber (250–1200 F, depending on type), mineral wool (1200 F), magnesia (600 F), and polyurethane foam (250 F). Certain foamed plastics have a very low conductivity, and are suitable for insulating lines as cold as –400 F. Rock cork [bonded mineral fiber] is satisfactory down to –250 F, and mineral wool down to –150 F.

#### HOW THICK SHOULD INSULATION BE ?

Most insulation in a plant will not exceed 2 inches in thickness. A rough guide to insulation thicknesses of the more common materials required on pipe to 8-inch size is:

#### GUIDE TO INSULATION THICKNESS

TABLE 6.7

APPLICATION	TYPICAL INSULATING MATERIAL	USUAL THICKNESS OF INSULATION
Hot Lines (to 500 F)	Asbestos, Silicate, Magnesia	1 to 2 inches
Cold Lines (to –150 F)	Mineral Wool	1 to 3 inches
Personnel Protection	Asbestos, Silicate, Magnesia	1 inch

For personnel protection insulation should be provided up to a height of about 8 ft above operating floor level. Alternately, wire mesh guards can be provided. The following more-detailed table gives insulation thickness for heat conservation, based on 85% magnesia to 600 F, and calcium silicate above 600 F.

#### INSULATION REQUIRED FOR PIPE AT VARIOUS TEMPERATURES

TABLE 6.8

NOMINAL PIPE SIZE (INCHES)	1/8	1/4	3/8	1/2	3/4	1	1 1/4	1 1/2	2	2 1/2	3	4	6	8	10	12	14	16	18	20	24
TEMPERATURE (Degrees F)	THICKNESS OF INSULATION (IN.) FOR STATED TEMPERATURE RANGE																				
below 400	1	1	1	1	1	1	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4
400–649	1	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4
650–899	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4
900–1049	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4
1050–1200	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4	1 1/4

### JACKETING & TRACING

6.8.2

#### REFERENCES

'Keeping piping hot—part II'. Chapman F.S. & Holland F.A. 1966. Chemical Engineering, Jan 17

'Winterizing chemical plants'. House F.F. 1967. Chemical Engineering, Sep 11

'Pipe tracing & insulation'. House F.F. 1968. Chemical Engineering, Jun 17

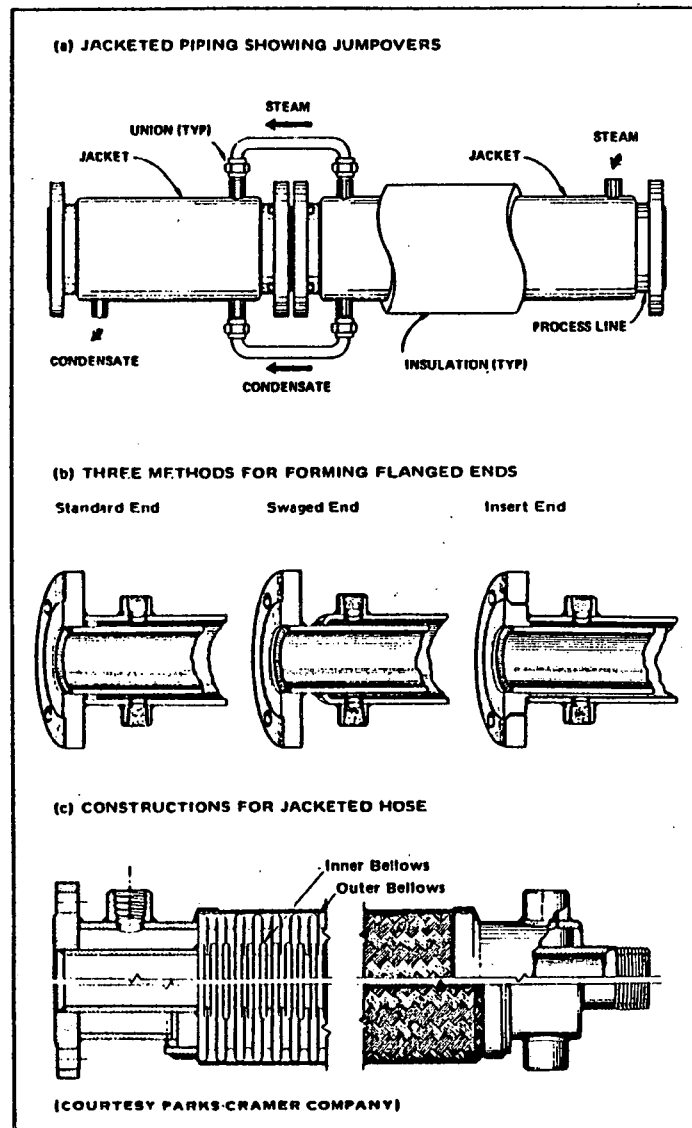
The common methods by which temperatures are maintained, other than by simple insulation, are jacketing and tracing (with insulation).

#### JACKETING

Usually, 'jacketing' refers to double-walled construction of pipe, valves, vessels, hose, etc., designed so that a hot or cold fluid can circulate in the cavity between the walls. Heating media include water, oils, steam, or proprietary high-boiling-point fluids which can be circulated at low pressure, such as Dowtherm or Therminol. Cooling media include water, water mixtures and various alcohols.

Jacketed pipe can be made by the piping fabricator, but an engineered system bought from a specialist manufacturer would be a more reliable choice. The jumper lines connecting adjacent jackets, thru which the heating or cooling medium flows are factory-made by the specialist manufacturer with less joints than those made on-site, where as many as nine screwed joints may be necessary to make one jumper. Details of the range of fittings, valves and equipment available and methods of construction for steel jacketed piping systems can be found in the Parks-Cramer Company's catalog J77.

Another type of jacketing is 'Platecoil' (Tranter Manufacturing Inc.) which is a name given to heat transfer units fabricated from embossed metal sheets, joined together to form internal channeling thru which the heating (or cooling) fluid is passed. The term 'jacketing' is also applied to electric heating pads or mantles which are formed to fit equipment. It also sometimes refers to the spiral winding of electric tracing and fluid tracing lines around pipes, vessels, etc.



### TRACING

External 'tracing' consists in running tubing filled with a hot fluid (usually steam), or electric heating cables, in contact with the outer surface of the pipe to be kept warm. The tubing or cables may be run parallel to the pipe or wound spirally around it. The pipe and tracer(s) are encased in thermal insulation.

An alternative, now little used due to sealing and cleaning problems, is internal tracing by means of tubing fitted inside the line to be heated. An internal tracer is termed a 'gutterline'.

'Unitrace' (Aluminum Company of America) is an integral product and tracer pipe extruded in aluminum, which gives excellent heat transfer. The system uses flanges and jumpover fittings similar to those used for jacketed systems to connect adjacent traced sections of the lines.

Electric tracing allows close control of temperature, and can provide a wider range of temperatures than steam heating.

### GETTING HEAT TO THE PROCESS LINE (USING STEAM)

If the process line temperature has to approach that of the available steam, jacketing gives the best results. Barton and Williams have stated [4] that the cheaper method of welding steam tracers directly to the process lines has proven adequate. In this unusual method, the welding is 'tack' or continuous depending on how much heat is required to be transferred thru the weld.

A greater rate of heat transfer may be achieved by using two (seldom more) parallel tracers. Sometimes a single tracer is spirally wound about the pipe, but spiral winding should be restricted to vertical lines where condensate can drain by gravity. If the temperature of the conveyed fluid has to be closely maintained, winding the tracer is too inaccurate—but it is a suitable method for getting increased heating in non-critical applications.

To improve heat transfer between the tracer and pipe, they may either be pressed into contact by banding or wiring them together at frequent (1 to 4 ft) intervals, or a heat-conducting cement such as 'Thermon' can be applied. Unless used to anchor the tracer, banding is normally applied sufficiently loosely to permit the tracer to expand.

Hot spots occur at the bands. If this is undesirable for a product line, a thin piece of asbestos may be inserted between tracer and line.

### CHOOSING THE SYSTEM

There are advantages and disadvantages with the various systems. Piping which is to be externally traced can be planned with little concern for the tracing.

Fluid-jacketed systems are flanged, and last-minute changes could result in delays. Jacketing offers superior heat transfer and should be seriously considered for product lines, especially for those conveying viscous liquids and material which may solidify, whereas service lines usually just need to be kept from freezing and tracing is quite adequate for them. If process material has to be kept cold in the line, refrigerant-jacketed systems are the only practicable choice.

For process lines, all systems should be evaluated on the criteria of heat distribution, initial cost and long-term operating and maintenance costs before a decision can be made.

### WHERE TRACING & JACKETING ARE SHOWN

Using the symbols given in chart 5.7, tracing is shown on the plan and elevation drawings of the plant piping and it will similarly be indicated on the isometric drawings. It will also be indicated on any model used. Tracing is one of the last aspects of plant design, and steam subheaders can either be shown directly on the piping drawings or on sepias or film prints.

## STEAM TRACING

6.8.3

This is a widely-used way of keeping lines warm—surplus steam is usually available for this purpose. Figure 6.40 shows typical tracing arrangements. A steam-tracing system consists of tracer lines separately fed from a steam supply header (or subheader), each tracer terminating with a separate trap. Horizontal pipes are commonly traced along the bottom by a single tracer. Multiply-traced pipe, with more than two tracers, is unusual.

## STEAM PRESSURE FOR TRACING

Steam pressures in the range 10 to 200 PSIG are used. Sometimes steam will be available at a suitable pressure for the tracing system, but if the available steam is at too high a pressure, it may be reduced by means of a control (valve) station—see 6.1.4. Low steam pressures may be adequate if tracers are fitted with traps discharging to atmospheric pressure. If a pressurized condensate system is used, steam at 100 to 125 PSIG is preferred.

## SIZING HEADERS

The best way to size a steam subheader or condensate header serving several tracers is to calculate the total internal cross-sectional area of all the tracers, and to select the header size offering about the same flow area. Table 6.9 allows quick selection if the tracers are all of the same size:

NUMBER OF TRACERS PER HEADER

TABLE 6.9

HEADER SIZE (IN.)	SIZE OF TRACER (IN.)				
	1/4	3/8	1/2	3/4	1
	NUMBER OF TRACERS				
1/2	9	4	2	1	—
1	18	7	4	2	1
1 1/2	36	16	9	4	2
2	64	28	18	7	4

## MAXIMUM LENGTHS & RISES

The rate at which condensate forms and fills the line determines the length of the tracer in contact with the pipe. Too many variables are involved to give useful maximum tracer lengths. Most companies have their own design figure (or figures based on experience) for this: usually, length of tracer in contact with pipe does not exceed 250 ft.

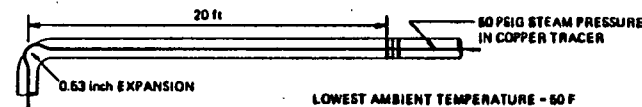
1 PSI steam will lift condensate about 2.3 ft, and therefore vertical rises will present no problem unless low-pressure steam is being used. Companies prefer to limit the vertical rise in a tracer at any one place to 6 ft (for 25-49 PSIG steam) or 10 ft (for 50-100 PSIG steam). As a rough guide, the total height, in feet, of all the rises in one tracer may be limited to one quarter of the initial steam pressure, in PSIG. For example, if the initial steam pressure is 100 PSIG, the total height of all risers in the tracer should be limited to 25 ft. The rise for a sloped tracer is the difference in elevations between the ends of the sloping part of the tracer.

## EXPANSION OF THE TRACER, & ANCHORING

Expansion can be accommodated by looping the tracer at elbows and/or providing horizontal expansion loops in the tracer. Vertical downward expansion loops obstruct draining and will cause trouble in freezing climates, unless the design includes a drain at the bottom of the loop, or a union to break the loop. It is necessary to anchor tracers to control the amount of expansion that can be tolerated in any one direction. Straight tracers 100 ft or longer are usually anchored at their midpoints.

Expansion at elbows must be limited where no loop is used and excessive movement of the tracer could lift the insulation. In such cases the tracer is anchored not more than 10 to 25 ft away from an elbow which limits start-up expansion to 1/2 to 3/4 inch in most cases. The distance of the anchor from the elbow is best calculated from the ambient and steam temperatures.

**EXAMPLE:** System traced with copper tubing: coefficient of linear expansion of copper = 0.000009 per deg F. Steam pressure to be used = 50 PSIG (equivalent steam temperature 298F). Lowest ambient temperature = 50 F. If the anchor is located 20 ft from the elbow, the maximum expansion in inches is  $(298-50)(0.000009)(20)(12) = 0.53$  in. This expansion will usually be tolerable even for a small line with the tracer construction for elbows shown in figure 6.40.



## PIPE, TUBE & FITTINGS FOR TRACING

SCH 80 carbon steel pipe, or copper or stainless steel tubing is used for tracers. Selection is based on steam pressure and required tracer size. In practice, tracers are either 1/2 or 3/8-inch size, as smaller sizes involve too much pressure drop, and larger material does not bend well enough for customary field installation.

1/2-inch OD copper tube is the most economic material for tracing straight piping. 3/8-inch OD copper tubing is more useful where small bends are required around valve bodies, etc. Copper tubing can be used for pressures up to 150 PSIG (or to 370 F). Table T-1 gives data for copper tube.

Supply lines from the header are usually socket welded or screwed and seal-welded depending on the pressures involved and the company's practice. A pipe-to-tube connector is used to make the connection between the steel pipe and tracer tube — see figure 2.41.

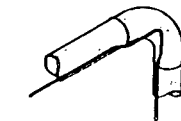
## TRACING VALVES & EQUIPMENT

Different methods are used. Some companies require valves to be wrapped with tracer tubing. Others merely run the tubing in a vertical loop alongside and against the valve body. In either method, room should be left for removing flange bolts, and unions should be placed in the tracer so that the valve or equipment can be removed.

**FIGURE 6.40**

6.8.3

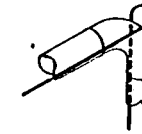
## TRACER AT ELBOWS



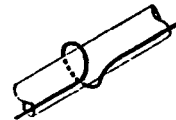
BRING TRACER TO SIDE TO  
ALLOW FOR EXPANSION AND TO  
IMPROVE HEATING OF ELBOW



## TRACE BACK OF ELBOW IN FREEZING CLIMATES



### UNION TO BREAK LOOP AND DRAIN LINE IN FREEZING CONDITIONS



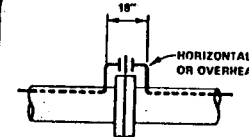
VERTICAL RISE  
• d • NUMBER OF COILS



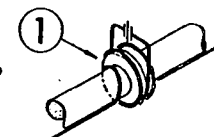
**STEEL TRACER  
CAN BE WELDED  
TO FLAT BAR**

- (1) THE TOTAL VERTICAL RISE IS EQUAL TO THE SUM OF ALL RISERS—SEE "MAXIMUM LENGTHS & RISES", 6.3
- (2) PIPE-TO-TUBE CONNECTORS ARE USED FOR JOINING SCREWED PIPING TO COPPER OR STAINLESS-STEEL TUBING. 3000 PSI FS UNIONS ARE USED FOR CS TRACERS. UNIONS AT TRACER TERMINATIONS ARE COVERED BY THE TRAP SYMBOL—SEE FIGURES 6.43 AND 6.44
- (3) FOR FREEZING CLIMATES, USE TRACING ARRANGEMENTS THAT CAN DRAIN, OR PROVIDE FOR AIR PURGING

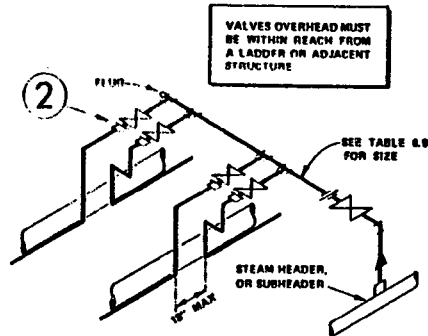
## TRACER AT FLANGES



**HORIZONTAL,  
OR OVERHEAD**



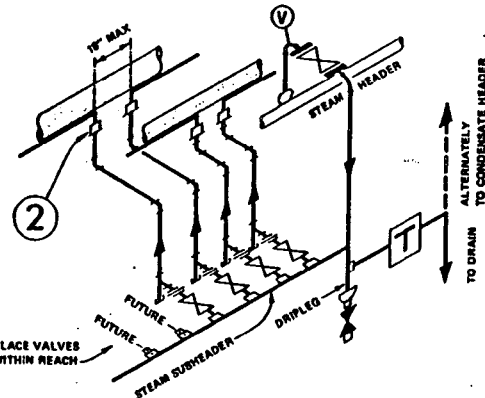
## TRACER AT VALVES



**VALVES OVERHEAD MUST  
BE WITHIN REACH FROM  
A LADDER OR ADJACENT  
STRUCTURE**

SEE TABLE 0.9  
FOR SIZE

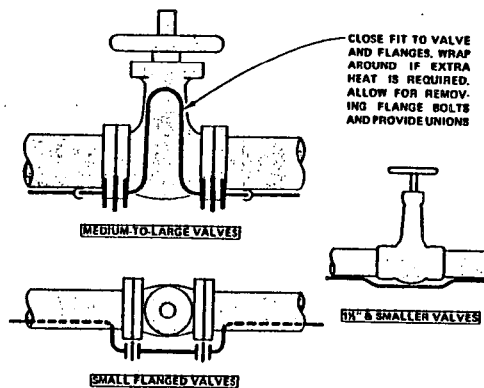
**STEAM HEADER,  
OR SUBHEADER.**



## PLACE VALVES

FIGURE 1

TO DRAIN  
ALTERNATELY  
TO CONDENSATE HEADS



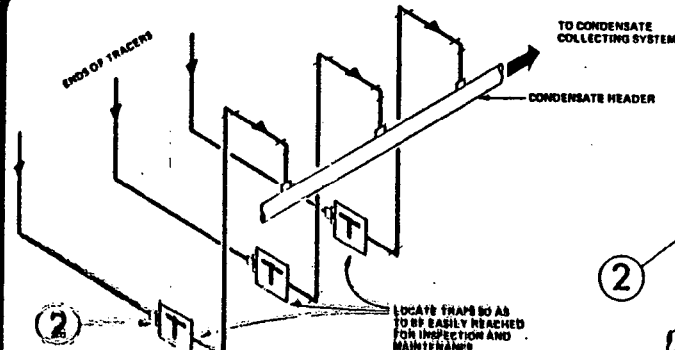
**CLOSE FIT TO VALVE AND FLANGES. WRAP AROUND IF EXTRA HEAT IS REQUIRED. ALLOW FOR REMOVING FLANGE BOLTS AND PROVIDE UNIONS**

**MEDIUM-TO-LARGE VALVES**

### 1 1/2" & SMALLER VALVES

### SMALL FLANGED VALVES

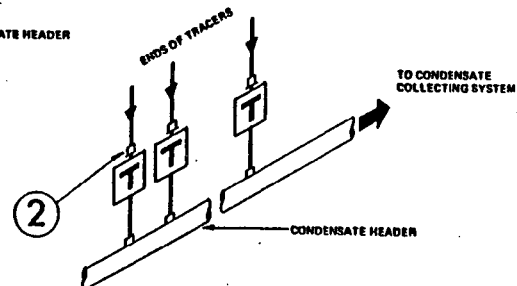
## TRACING VESSELS



**TO CONDENSATE  
COLLECTING SYSTEM**

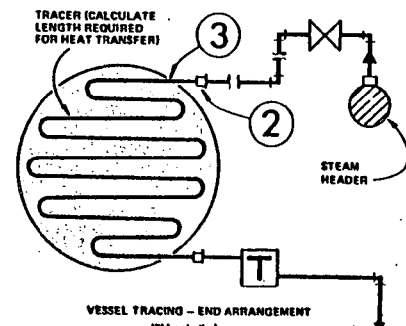
- CONDENSATE HEADER

LOCATE TRAPS SO AS  
TO BE EASILY REACHED  
FOR INSPECTION AND  
MAINTENANCE



**TO CONDENSATE  
COLLECTING SYSTEM**

**CONDENSATE HEADER**



**TRACER (CALCULATE  
LENGTH REQUIRED  
FOR HEAT TRANSFER)**

## STEAM HEADER

**VESSEL TRACING - END ARRANGEMENT**

**"Piping Guide", PO Box 277, Cotati, CA 94928, USA**

**FIGURE 6.40**

TABLE  
6.9

## DESIGN POINTS FOR STEAM TRACING & INSULATION

- Run tracers parallel to and against the underside of the pipe to be heated
- Ensure that the temperature limit for process material is not exceeded by the temperature of the steam supplying the tracer. Hot spots occur at bands—see 6.8.2, under 'Getting heat to the process line'
- Run a steam subheader from the most convenient source if there is no suitable existing steam supply that can be used either directly or by reducing the pressure of the available steam
- Take tracer lines separately from the top of the subheader, and provide an isolating valve in the horizontal run
- Feed steam first to the highest point of the system of lines to be traced, so that gravity will assist the flow of condensate to trap(s) and condensate header
- Do not split (branch) a tracer and then rejoin—the shorter limb would take most of the steam
- Preferably, absorb expansion of the tracer at elbows. If loops are used in the line, arrange them to drain on shutdown
- Keep loops around flanges horizontal or overhead, and provide unions so that tracers can be disconnected at flanges
- If possible, group supply points and traps, locating traps at grade or platform level
- Do not place a trap at every low point of a tracer (as is the practice with steam lines) but provide a trap at the end of the tracer
- Do not run more than one tracer to a trap
- Increased heating may be obtained:
  - (1)\* By using more than one tracer
  - (2) By winding the tracer in a spiral around the line
  - (3) By applying heat-transfer cement to the tracer and line
  - (4) By welding the tracer to the line—refer to 6.8.2, under 'Getting heat to the process line'
- Reserve spiral winding of tracers for vertical lines where condensate can drain by gravity flow
- In freezing conditions, provide drains at low points—and at other points where condensate could collect during shutdown
- Provide slots in insulation to accommodate expansion of the tracer where it joins and leaves the line to be traced
- Indicate thickness of insulation to envelop line and tracer, and show whether insulation is also required at flanges
- Indicate limits for insulation for personnel protection—see 6.8.1, under 'How thick should insulation be?', and chart 5.7
- Provide crosses instead of elbows and flanged joints at intervals in heated lines conveying materials which may solidify, to permit cleaning if the heating fails

## STEAM & LOW-PRESSURE HEATING MEDIA

6.9

### EXPLANATIONS OF STEAM TERMS

6.9.1

#### HOW STEAM IS FORMED

Steam is a convenient and easily handled medium for heating, for driving machinery, for cleaning, and for creating vacuum.

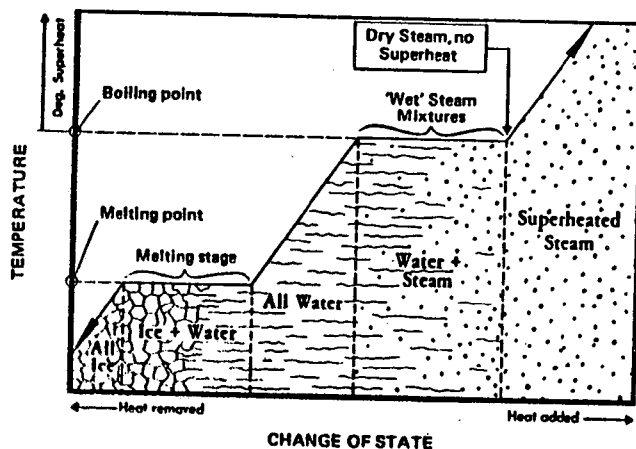
After water has reached the boiling point, further addition of heat will convert water into the vapor state: that is, steam. During boiling there is no further rise in temperature of the water, but the vaporization of the water uses up heat. This added heat energy, which is not shown by a rise in temperature, is termed 'latent heat of vaporization', and varies with pressure.

In boiling one pound of water at atmospheric pressure (14.7 PSIA) 970.3 BTU is absorbed. If the steam condenses back into water (still at the boiling temperature and 14.7 PSIA) it will release exactly the amount of heat it absorbed on vaporizing.

The term 'saturated steam' refers to both *dry steam* and *wet steam*, described below. Steam tables give pressure and temperature data applicable to dry and to wet steam. Small amounts of air, carbon dioxide, etc., are present in steam from industrial boilers.

#### STEAM/WATER/ICE DIAGRAM

CHART 6.3



#### DRY STEAM

Dry steam is a gas, consisting of water vapor only. Placed in contact with water at the same temperature, dry steam will not condense, nor will more steam form—liquid and vapor are in equilibrium.

#### WET STEAM

Wet steam consists of water vapor and suspended water particles at the same temperature as the vapor. Heating ability ('quality') varies with the percentage of dry steam in the mixture (the water particles contain no latent heat of vaporization). Like dry steam, wet steam is in equilibrium with water at the same temperature.

#### SUPERHEATED STEAM

If heat is added to a quantity of dry steam, the temperature of the steam will rise, and the number of degrees rise in temperature is the 'degrees of superheat'. Thus, superheat is 'sensible' heat — that is, it can be measured by a thermometer.

#### EFFECT OF PRESSURE CHANGE

Under normal atmospheric pressure (14.7 PSIA) pure water boils at 212 F. Reduction of the pressure over the water will lower the boiling point. Increase in pressure raises the boiling point. Steam tables give boiling points corresponding to particular pressures.

#### FLASH STEAM

Suppose a quantity of water is being boiled at 300 PSIA (corresponding to 417 F). If the source of heat is removed, boiling ceases. If the pressure over the water is then reduced, say from 300 to 250 PSIA, the water starts boiling on its own, without any outside heat applied, until the temperature drops to 401 F (this temperature corresponds to 250 PSIA). Such spontaneous boiling due to reduction in pressure is termed 'flashing', and the steam produced, 'flash steam'.

The data provided in steam tables enable calculation of the quantity and temperature of steam produced in 'flashing'.

#### CONDENSATE — WHAT IT IS & HOW IT FORMS

Steam in a line will give up heat to the piping and surroundings, and will gradually become 'wetter', its temperature remaining the same. The change of state of part of the vapor to liquid gives heat to the piping without lowering the temperature in the line. The water that forms is termed 'condensate'. If the line initially contains superheated steam, heat lost to the piping and surroundings will first cause the steam to lose sensible heat until the steam temperature drops to that of dry steam at the line pressure.

#### AIR IN STEAM

With both dry and wet steam, a certain pressure will correspond to a certain temperature. The temperature of the steam at various pressures can be found in steam tables. If air is mixed with steam, this relationship between pressure and temperature no longer holds. The more air that is admixed, the more the temperature is reduced below that of steam at the same pressure. There is no practicable way to separate air from steam (without condensation) once it is mixed.

#### LOW-PRESSURE HEATING MEDIA

6.9.2

Special liquid media such as Dowtherms (Dow Chemical Co.) and Therminols (Monsanto Co.) can be boiled like water, but the same vapor temperatures as steam are obtained at lower pressures. Heating systems using these liquids are more complicated than steam systems, and experience with them is necessary in order to design an efficient installation. However, the basic principles of steam-heating systems apply.

6.8.3  
6.9.2

CHART  
6.3

## STEAM PIPING

6.10

### REMOVING AIR FROM STEAM LINES

6.10.1

Air in steam lines lowers the temperature for a given pressure, and calculated rates of heating may not be met. See 6.9.1 under 'Air in steam'.

The most economic means for removing air from steam lines is automatically thru temperature-sensitive traps or traps fitted with temperature-sensitive air-venting devices placed at points remote from the steam supply. When full line temperature is attained the vent valves will close completely. See 6.10.7 under 'Temperature-sensitive (or thermostatic) traps'.

### WHY PLACE VENTS AT REMOTE POINTS ?

On start-up, cold lines will be filled with air. Steam issuing from the source will mix with some of this air, but will also act as a piston pushing air to the remote end of each line.

### WHY REMOVE CONDENSATE ?

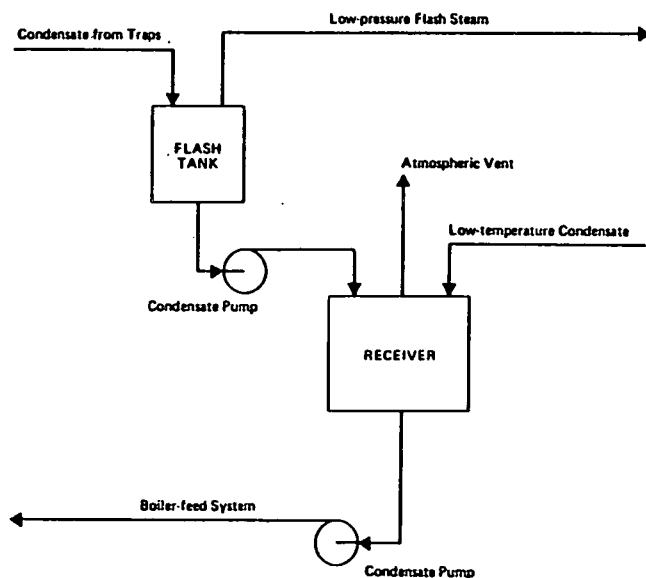
6.10.2

In heating systems using steam with little or no superheat, steam condenses to form water, termed 'condensate', which is essentially distilled water. Too valuable to waste, condensate is returned for use as boiler feedwater unless it is contaminated with oil (usually from a steam engine) or unless it is uneconomic to do so, when it can either be used locally as a source of hot water, or run to a drain. If condensate is not removed:—

- Steam with entrained water droplets will form a dense water film on heat transfer surfaces and interfere with heating
- Condensate can be swept along by the rapidly-moving steam (at 120 ft/sec or more) and the high-velocity impact of slugs of water with fittings, etc. (waterhammer) may cause erosion or damage

### UTILIZING CONDENSATE

FIGURE 6.41



In early steam systems, there was considerable waste of steam and condensate after passing thru heating coils, etc., as steam was merely vented to the open air. Later, the wastefulness of this resulted in closed steam lines from which only the condensed steam was removed and then re-led to the boiler. The removal of condensate to atmospheric pressure was effected with traps—special automatic discharge valves—see 6.10.7.

This was a much more efficient system, but it still wasted flash steam. On passing thru the traps, the depressurized condensate boiled, generating lower pressure steam. In modern systems, this flash steam is used and the residual condensate returned to the boiler.

### STEAM SEPARATOR OR DRYER

6.10.3

This is an in-line device which provides better drying of steam being immediately fed to equipment. A separator is shown in figure 2.67. It separates droplets entrained in the steam which have been picked up from condensate in the pipe and from the pipe walls, by means of one or more baffles (which cause a large pressure drop). The collected liquid is piped to a trap.

### SLOPING & DRAINING STEAM & CONDENSATE LINES

6.10.4

Sloping of steam and condensate lines is discussed in 6.2.6, under 'Sloped lines avoid pocketing and aid draining'.

Condensate is collected from a steam line either by a steam separator (sometimes termed a 'dryer')—see 6.10.3 above—or more cheaply by a dripleg (drip pocket or well — see below) from where it passes to a trap for periodic discharge to a condensate return line or header which will be at a lower pressure than the steam line. The header is either taken to a boiler feedwater tank feeding make-up water to the boiler or to a hotwell for pumping to the boiler feedwater tank.

### DRIPLEGS COLLECT CONDENSATE

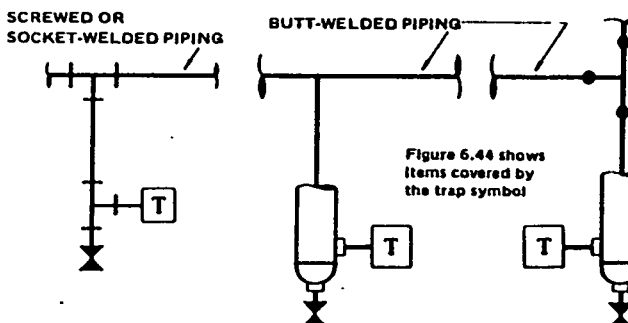
6.10.5

It is futile to provide a small dripleg or drain pocket on large lines, as the condensate will not be collected efficiently.

Driplegs are made from pipe and fittings. Figure 6.42 shows three methods of construction, and table 6.10 suggests dripleg and valve sizes.

### DRIPLEG CONSTRUCTIONS

FIGURE 6.42





	DIMENSIONS & SIZES (NOMINAL) IN INCHES											
LINE SIZE	*	3	4	6	8	10	12	14	16	18	20	24
DIMENSION 'A'		3	4	6	6	8	8	10	12	12	12	12
DIMENSION 'B'		12	12	14	14	16	16	18	20	21	22	24
SIZE OF V <sub>1</sub>		½	½	½	½	½	½	1	1	1	1	1
SIZE OF V <sub>2</sub>		½	½	½	½	½	1	1	1	1	1	1

TO 2"

\*For lines 2-inch and smaller, use ½-inch pipe, valves and fittings, reducing line size at the trap as necessary

Figure 2.70 shows dripleg construction

STEAM LINE PRESSURE FORCES CONDENSATE INTO RECOVERY SYSTEM 6.10.6

In almost every steam-heating system where condensate is recovered the trapped condensate has to be lifted to a condensate header and run to a boiler feedwater tank, either directly or via a receiver. Each PSI of steam pressure behind a trap can lift the condensate about two feet vertically. The pressure available for lifting the condensate is the pressure difference between the steam and condensate lines less any pressure drop over pipe, valves, fittings, trap, etc.

STEAM TRAPS 6.10.7

The purpose of fitting traps to steam lines is to obtain fast heating of systems and equipment by freeing the steam lines of condensate and air. A steam trap is a valve device able to discharge condensate from a steam line without also discharging steam. A secondary duty is to discharge air—at start-up, lines are full of air which has to be flushed out by the steam, and in continuous operation a small amount of air and non-condensable gases introduced in the boiler feedwater have also to be vented.

Some traps have built-in strainers to give protection from dirt and scale which may cause the trap to jam in an open position. Traps are also available with checking features to safeguard against backflow of condensate. Refer to the manufacturers' catalogs for details.

Choosing a trap from the many designs should be based on the trap's ability to operate with minimal maintenance, and on its cost. To reduce inventory and aid maintenance, the minimum number of types of trap should be used in a plant. The assistance of manufacturers' representatives should be sought before trap types and sizes are selected.

Steam traps are designed to react to changes in temperature, pressure or density:

TEMPERATURE-SENSITIVE (or 'THERMOSTATIC') TRAPS are of two types: The first type operates by the movement of a liquid-filled bellows, and the second uses a bimetal element. Both types are open when cold and readily discharge air and condensate at start-up. Steam is in direct contact with the closing valve and there is a time delay with both types in operating. A large dripleg allowing time for condensate to cool improves operation. As these traps are actuated by temperature differential, they are economic at steam pressures greater than 6 PSIG. The temperature rating of the bellows and the possibility of damage by waterhammer should be considered—refer to 6.10.8.

IMPULSE TRAPS are also referred to as 'thermodynamic' and 'controlled disc'. These traps are most suited to applications where the pressure downstream of the trap is less than about half the upstream pressure. Waterhammer does not affect operation. They are suitable for steam pressures over 8 PSIG.

DENSITY-SENSITIVE TRAPS are made in 'float' and 'bucket' designs. The float trap is able to discharge condensate continuously, but this trap will not discharge air unless fitted with a temperature-sensitive vent (the temperature limitation of the vent should be checked). Float traps sometimes may fail from severe waterhammer. The inverted bucket trap (see 3.1.9) is probably the most-used type. The trap is open when cold, but will not discharge large quantities of air at startup unless the bucket is fitted with a temperature-sensitive vent. The action in discharging condensate is rapid. Steam will be discharged if the trap loses its priming water due to an upstream valve being opened; refer to note (9) in the key to figure 6.43. Inverted bucket traps will operate at pressures down to 1/4 PSIG.

FLASHING 6.10.8

Refer to 6.9.1. When hot condensate under pressure is released to a lower pressure return line, the condensate immediately boils. This is referred to as 'flashing', and the steam produced as 'flash steam'.

The hotter the steam line and the colder the condensate discharge line, the more flashing will take place; it can be severe if the condensate comes from high pressure steam. Only part of the condensate forms steam. However, if the header is inadequately sized to cope with the quantity of flash steam produced and backpressure builds up, waterhammer can result.

Often, where a trap is run to a drain, a lot of steam seems to be passing thru the trap, but this is usually only from condensate flashing.

DRAINING SUPERHEATED STEAM LINES 6.10.9

Steam lines with more than a few degrees of superheat will not usually form condensate in operation. During the warming-up period after starting a cold circuit, the large bulk of metal in the piping will nearly always use up the degrees of superheat to produce a quantity of condensate.

6.10.10.9

FIGURES 6.41 & 6.42

TABLE 6.10



Start-ups are infrequent and with more than a few degrees of superheat it is unnecessary to trap a system which is continuously operated. These superheated steam lines can operate with driplegs only, and are usually fitted with a blowdown line having two valves so that condensate can be manually released from the dripleg after startup.

A superheated steam supply to an intermittently operated piece of equipment will require trapping directly before the controlling valve for the equipment, as the temperature will drop at times allowing condensate to form.

#### PREVENT TRAPS FROM FREEZING

6.10.10

Insulation and steam or electric tracing of the trap and its piping may also be required in freezing environments. Temperature-sensitive and impulse traps are not subject to freezing trouble if mounted correctly, so that the trap can drain. Bucket traps are always mounted with the bucket vertical and a type with top inlet and bottom outlet should be chosen, unless the trap can be drained by fitting an automatic drain.

#### GUIDELINES TO STEAM TRAP PIPING

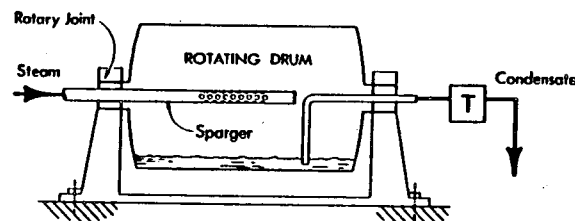
6.10.11

- Figures 6.43 thru 6.45 are a guide to piping traps from driplegs, lines, vessels, etc.
- Try to group traps to achieve an orderly arrangement
- Unless instructed otherwise, pipe, valves and fittings will be the same size as the trap connections, but not smaller than 3/4 in.
- Traps are normally fitted at a level lower than the equipment or dripleg that they serve
- Trap each item of equipment using steam separately, even if the steam pressure is common
- Provide driplegs (and traps on all steam lines with little or no superheat) at low points before or at the bottom of risers, at pockets and other places where condensate collects on starting up a cold system. Table 6.10 gives dripleg sizes
- Locate driplegs at the midpoints of exchanger shells, short headers, etc. If dual driplegs are provided it is better to locate them near each end
- For installations in freezing conditions, where condensate is wasted, preferably choose traps that will not pocket water and which can be installed vertically, to allow draining by gravity. Otherwise, select a trap that can be fitted with an automatic draining device by the manufacturer
- Avoid long horizontal discharge lines in freezing conditions, as ice can form in the line from the trap. Keep discharge lines short and pitch them downward, unless they are returning condensate to a header
- For efficient operation of equipment such as heat exchangers using large amounts of steam, consider installing a separator in the steam feed

- 'Syphon' removal of condensate: In certain instances it is not possible to provide a gravity drain path – for example, where condensate is formed inside a rotating drum. The pressure of the steam is used to force ('syphon') the condensate up a tube and into a trap. Figure 6.45 shows such an arrangement

TRAPPING ARRANGEMENT FOR ROTATING DRUM

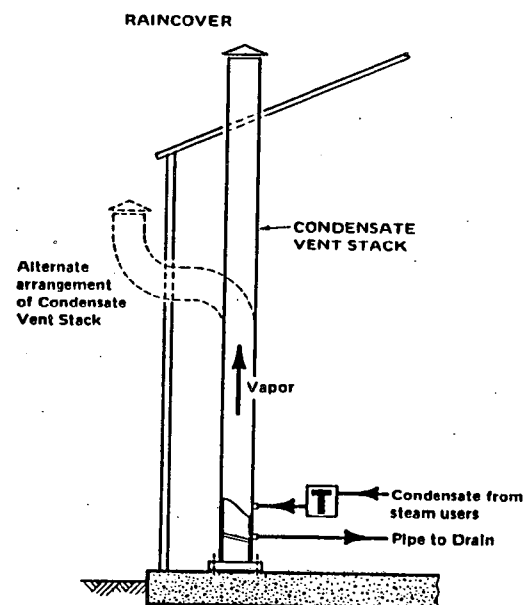
FIGURE 6.45



- If condensate is continuously discharging to an open drain in an inside installation a personnel hazard or objectionable atmosphere may be created. To correct this, discharge piping can be connected to an exhaust stack venting to atmosphere and a connection to the main drain provided, as in figure 6.46

CONDENSATE VENT STACK

FIGURE 6.46



FIGURES  
6.43–6.46

## WHY VENTS ARE NEEDED

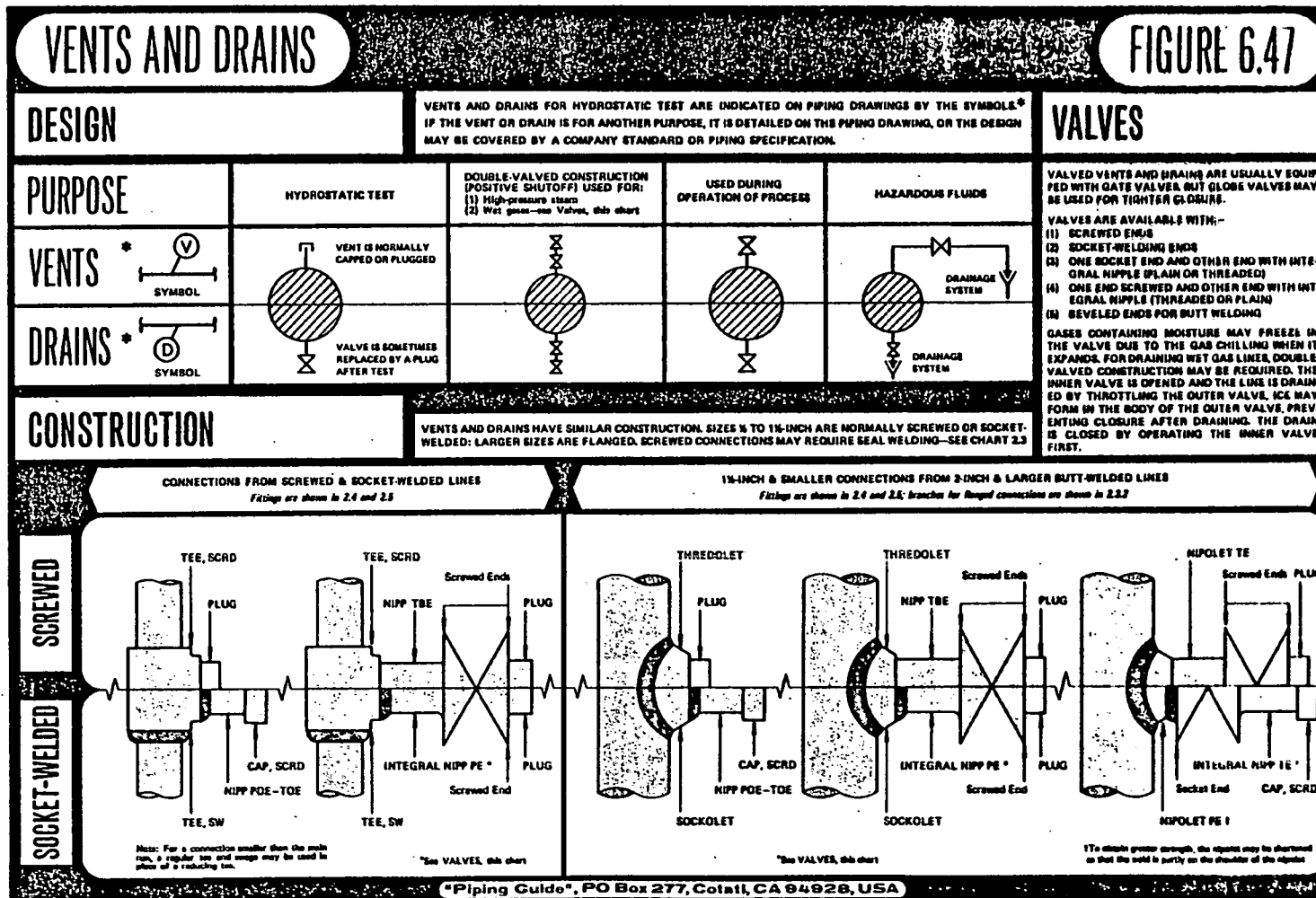
6.11.1

Vents are needed to let gas (usually air) in and out of systems. When a line or vessel cools, the pressure drops and creates a partial vacuum which can cause syphoning or prevent draining. When pressure rises in storage tanks due to an increase in temperature, it is necessary to release excess pressure. Air must also be released from tanks to allow filling, and admitted to permit draining or pumping out liquids.

Unless air is removed from fuel lines to burners, flame fading can result. In steam lines, air reduces heating efficiency.

After piping has been erected, it is often necessary to subject the system to a hydrostatic test to see if there is any leakage. In compliance with the applicable code, this consists of filling the lines with water or other liquid, closing the line, applying test pressure, and observing how well pressure is maintained for a specified time, while searching for leaks.

As the test pressure is greater than the operating pressure of the system, it is necessary to protect equipment and instruments by closing all relevant valves. Vessels and equipment usually are supplied with a certificate of code compliance. After testing, the valved drains are opened and the vent plugs temporarily removed to allow air into the piping for complete draining.



Positions of the required vent and drain points are established on the piping drawings. (P&ID's will show only process vents, such as vacuum breakers, and process drains.) Refer to figure 6.47 for construction details.

### VENTING GASES

6.11.3

Quick-opening vents of ample size are needed for gases. Safety and safety-relief valves are the usual venting means. See 3.1.9 for pressure-relieving devices, and 6.1.3, under 'Piping safety and relief valves'.

Gases which offer no serious hazard after some dilution with air may be vented to atmosphere by means ensuring that no direct inhalation can occur. If a (combustible) gas is toxic or has a bad odor, it may be piped to an incinerator or flarestack, and destroyed by burning.

### DRAINING COMPRESSED-AIR LINES

6.11.4

Air has a moisture content which is partially carried thru the compressing and cooling stages. It is this moisture that tends to separate, together with any oil, which may have been picked up by the air in passing thru the compressor.

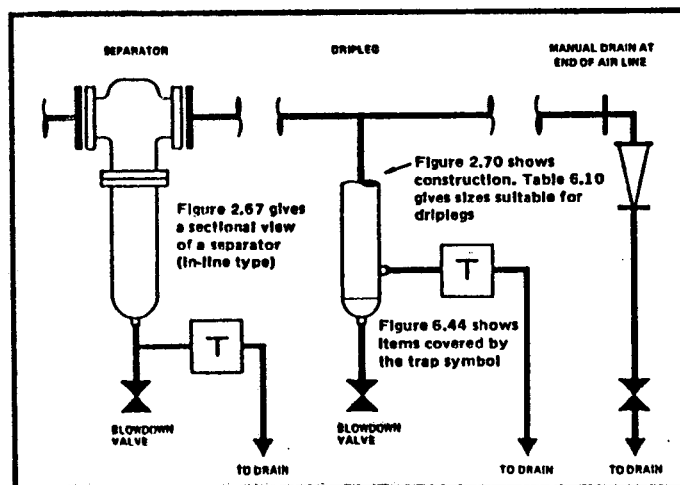
If air for distribution has not been dried, distribution lines should be sloped toward points of use and drains: lines carrying dried air need not be sloped. Sloping is discussed in 6.2.6.

If the compressed-air supply is not dried, provide:—

- (1) Traps at all drains from equipment forming or collecting liquid—such as intercooler, aftercooler, separator, receiver.
- (2) Driplegs with traps on distribution headers (at low points before rises) and traps or manual drains at the ends of distribution headers.

### LIQUID REMOVAL FROM AIR LINES

FIGURE 6.48



### RELIEVING PRESSURE—LIQUIDS

6.12

The buildup of pressure in a liquid is halted by discharging a small amount of liquid. Relieving devices having large ports are not required. Relief valves—see 3.1.9—are used, and need to be piped at the discharge side, but the piping should be kept short. See 6.1.3 under 'Piping safety & relief valves'.

Rarely will the relieved liquid be sufficiently non-hazardous to be piped directly to a sewer. Often the liquid is simply to be reclaimed. Relieved liquid is frequently piped to a 'knockout drum', or to a sump or other receiver for recovery. The P&ID should show what is to be done with the relieved liquid.

### RELIEF HEADERS

6.12.1

Headers should be sized to handle adequately the large amounts of vapor and liquid that may be discharged during major mishap. Relief headers taken to knockout drums, receivers or incinerators, are normally sloped. Refer to 6.2.6 and figure 6.3, showing the preferred location of a relief header on a piperack.

### WASTES & EFFLUENTS

6.13

Manufacturing processes may generate materials that cannot be recycled, and for which there is no commercial use. These materials are termed 'waste products', or 'wastes'. An 'effluent' is any material flowing from a plant site to the environment. Effluents need not be polluting: for example, properly-treated waste water may be discharged without harming the environment or sewage-treatment plants.

Restrictions on the quantities and nature of effluents discharged into rivers, sewers or the atmosphere, necessitate treatment of wastes prior to discharge. Waste treatment is increasingly a factor in plant design, whether wastes are processed at the plant, or are transported for treatment elsewhere. For in-plant treatment, waste-treatment facilities are described on separate P&ID's (see 5.2.4) and should be designed in consultation with the responsible local authority.

Liquid wastes have to be collected within a plant, usually by a special drainage system. Corrosive and hazardous properties of liquid wastes will affect the choice and design of pipe, fittings, open channels, sumps, holding tanks, settling tanks, etc. Because many watery wastes are acidic and corrosive to carbon steel, collection and drainage piping is often lined or made of alloy or plastic. Sulfates frequently appear in wastes, and special concretes may be necessary for sewers, channels, sumps, etc., because sulfates deteriorate regular concretes.

Flammable wastes may be recovered and/or burned in smokeless incinerators or flarestacks. Vapors from flammable liquids present serious explosion hazards in collection and drainage systems, especially if the liquid is insoluble and floats.

Wastes may be held permanently at the manufacturing site. Solid wastes may be piled in dumps, or buried. Watery wastes containing solids may be pumped into artificial 'ponds' or 'lagoons', where the solids settle.

## REFERENCES

- 'National Fire Codes'. National Fire Protection Association, Vol I, Flammable liquids. Vol. 2, Gases. Vol. 3, Combustible solids, dusts & explosives
- 'Flashpoint index of tradename liquids'. NFPA. 1964. No. 325A
- 'Fire protection for chemicals'. Bahme C.W. 1961. NFPA
- 'Fire protection in refineries'. American Petroleum Institute. 1959. RP 2001. 4th edn
- 'Protection against ignitions arising out of static, lightning & stray currents'. API. 1967. RP 2003. 2nd edn
- 'Welding or hot-tapping on equipment containing flammables'. API. 1963. PSD 2201 (Free)
- 'Guide for the safe [hot] storage & loading of heavy oil & asphalt'. API. 1966. PSD 2205 (Free)

TANK SPACINGS (NFPA)

TABLE 6.11

CONDITIONS	MINIMUM INTER-TANK CLEARANCE
FLAMMABLE or COMBUSTIBLE LIQUID STORAGE TANKS	Whichever is greatest:— 3ft (Sum of diameters of adjacent tanks)/6 (Diameter of smaller tank)/2
CRUDE PETROLEUM 126,000 gal max tank size Non-congested locale	3 ft
CRUDE PETROLEUM 126,000 gal min larger tank Producing area	Diameter of smaller tank
UNSTABLE FLAMMABLE and UNSTABLE COMBUSTIBLE LIQUID STORAGE TANKS	(Sum of diameters of adjacent tanks)/2
LIQUEFIED PETROLEUM GAS CONTAINER from Flammable or Combustible Liquid Storage Tank	20 ft
LIQUEFIED PETROLEUM GAS CONTAINER outside diked area containing Flammable or Combustible Liquid Storage Tank(s)	10 ft from centerline of dike wall  NOTE: If LPG container is smaller than 126 gal (US) and each liquid storage tank is smaller than 550 gal, exemption applies
TANKS surrounded by other Tanks	Authority Limit*

*For minimum clearances from property lines and public ways, consult Chapter II, Vol 1 of the National Fire Codes\**

\*For LPG tanks, the US Department of Labor gives clearances in tables H-23, H-33, etc. part 1910-110 of 'Occupational safety and health standards', 1971. These standards also give clearances for ammonia tanks, in part 1910-111.

## SOME GUIDELINES

- Apply the recommendations relating to the project of the NFPA, API or other advisory body
- Check insurer's requirements
- Isolate flammable liquid facilities so that they do not endanger important buildings or equipment. In main buildings, isolate from other areas by firewalls or fire-resistive partitions, with fire doors or openings and with means of drainage
- Confine flammable liquid in closed containers, equipment, and piping systems. Safe design of these should have three primary objectives: (1) To prevent uncontrolled escape of vapor from the liquid. (2) To provide rapid shut-off if liquid accidentally escapes. (3) To confine the spread of escaping liquid to the smallest practicable area
- If tanks containing flammable material are sited in the open, it is good practice to space them according to the minimum separations set out in the NFPA Code (No. 395. 'Farm storage of flammable liquids') and to provide dikes (liquid-retaining walls) around groups of tanks. Additional methods for dealing with tank fires are: (1) To transfer the tank's contents to another tank. (2) To stir the contents to prevent a layer of heated fuel forming
- Locate valves for emergency use in plant mishap or fire—see 6.1.3
- Valves for emergency use should be of fast-acting type
- Provide pressure-relief valves to tanks containing flammable liquid (or liquefied gas) if exposed to strong sunlight and/or high ambient temperature, so that vapor under pressure can escape
- Consider providing water sprays for cooling tanks containing flammable liquid which are exposed to sunlight
- Provide ample ventilation in buildings for all processing operations so that vapor concentration is always below the lower flammability limit. Process ventilation should be interlocked so that the process cannot operate without it
- Install explosion panels in buildings to relieve explosion pressure and reduce structural damage
- Install crash panels for personnel in hazardous areas
- Ensure that the basic protection, automatic sprinklers, is to be installed
- Some hazards require special fixed extinguishing systems—foam, carbon dioxide, dry chemical or water spray—in addition to sprinklers. Seek advice from the fire department responsible for the area, and from the insurers

## BUILDINGS IN RELATION TO PIPING

6.15

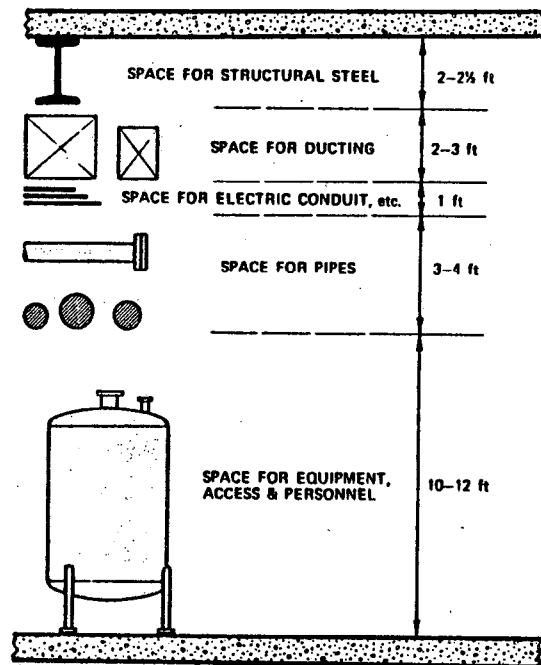
### SPACE BETWEEN FLOORS

6.15.1

To avoid interferences and to simplify design, adequate height is necessary between floors in buildings and plants for piping, electrical trays, and air ducts if required. Figure 6.49 suggests vertical spacings:

#### VERTICAL SPACING BETWEEN FLOOR & CEILING

FIGURE 6.49



### INSTALLATION OF LARGE SPOOLS & EQUIPMENT

6.15.2

Large openings in walls, floors or the roof of a building may be needed for installing equipment. Wall and roof openings are covered when not in use, but sometimes floor openings are permanent and guarded with railings, etc.

### BUILDING LAYOUT

6.15.3

#### RELATION TO PROCESS

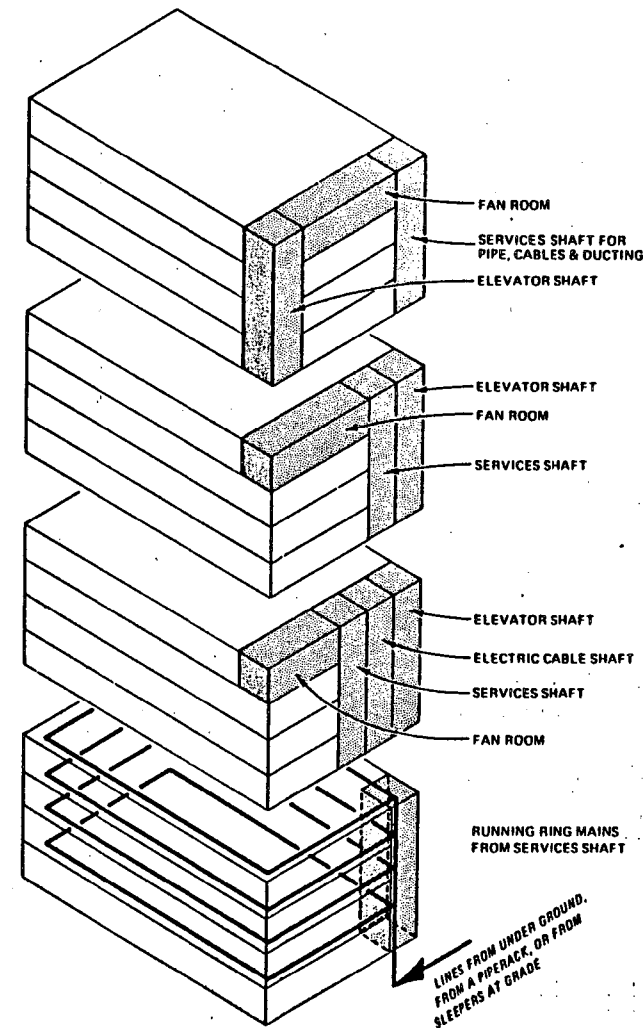
Different processes require different types of buildings. Some processes are best housed in single-story buildings with the process beginning at one end and finishing at the other end. Other processes are better assisted by gravity, starting at the top of a building or structure and finishing at or near grade.

## BUILDING SHAFTS FOR SERVICES

Provision of a services shaft or 'chase' in multi-storied buildings greatly simplifies arrangement of vertical piping, ducting and electric cables communicating between floors. Conceptual arrangements of services and elevator shafts, with fan room for air-conditioning and/or process needs, are shown in figure 6.50. Services shafts can be located in any position suitable to the process, and need not extend the whole height of the building.

### SUGGESTED BUILDING LAYOUTS

FIGURE 6.50



6.14  
6.15.3

FIGURES  
6.49 & 6.50

TABLE  
6.11

# STANDARDS & CODES:

## PIPING SYSTEMS, SYMBOLS, PIPE, PIPESUPPORTS, FLANGES, GASKETS, FITTINGS, PUMPS, VALVES, STEAM TRAPS, VESSELS, EXCHANGERS, & SCREWTHREADS

### REFERENCES

- 'Codes & Standards for today's Industry'. ASME Staff Report. 1966. Mechanical Engineering, Jun. Vol 88. (6)
- 'Piping Codes & Standards'. Wright L. E. 1968. Chemical Engineering, Jun 17. 247-50
- 'Piping codes & the chemical plant'. Canham W. G. 1966. Chemical Engineering, Oct 10. 119-204

### WHAT ARE STANDARDS & CODES ?

7.1

Both standards and codes are documents which establish methods for manufacture and testing. The documents are prepared and kept current by committees whose members represent industry, government, universities, institutes, professional societies, trade associations, labor unions, etc.

Proven engineering practices form the basis of standards and codes, so that they embody minimum requirements for selection of material, dimensions, design, erection, testing, and inspection, to ensure the safety of piping systems. Periodic revisions are made to reflect developments in the industry.

The terms 'standard' and 'code' have become almost interchangeable, but documents are termed codes when they cover a broad area, have governmental acceptance, and can form a basis for legal obligations. 'Recommendations' document advisable practice. 'Shall' in the wording of standards and codes denotes a requirement or obligation, and 'should' implies recommendation.

### FOUR REASONS FOR THEIR USE

7.2

- (1) Items of hardware made according to a standard are interchangeable, and of known dimensions and characteristics
- (2) Compliance with a relevant code or standard guarantees performance, reliability, quality, and provides a basis for contract negotiations, for obtaining insurance, etc.
- (3) A lawsuit which may follow a plant mishap, possibly due to failure of some part of a system, is less likely to lead to a punitive judgement if the system has been engineered and built to a code or standard
- (4) Codes often supply the substance for Federal, State, and Municipal safety regulations. However, the US Federal Government may, as needed, devise its own regulations, which are sometimes in the form of a code

### WHO ISSUES STANDARDS ?

7.3

The American Standards Association was founded in 1918 to authorize national standards originating from five major engineering societies. Previously a chaotic situation had arisen as many societies and trade associations had been issuing individual standards which sometimes overlapped. In 1967, the name of the ASA was changed to the USA Standards Institute, and in 1969 a second change was made, to American National Standards Institute. Standards previously issued under the prefixes 'ASA' and 'USASI' are now prefixed 'ANSI'.



Not all USA standards and codes are issued directly by the Institute. The American Society of Mechanical Engineers, the Instrument Society of America, and several other organizations issue standards and codes that apply to piping. Table 7.1 lists the principal sources.

Other countries also issue standards. The British Standards Institution (BSI) in the UK, the Deutscher Normenausschuss (DIN) in West Germany, and the Swedish national organization (SIS) issue many standards. Addresses of the UK, West-German, and Swedish national bodies are given at the foot of table 2.1. Copies of foreign standards can be obtained directly, or from the American National Standards Institute, Inc, 1430 Broadway, New York, NY 10018.

## IDENTIFYING THE SOURCES OF STANDARDS 7.4

The tables in 7.5.6 give the initial letters of the standards-issuing organizations preceding the number of the standard, thus: 'ASTM N28'. Table 7.1 includes the initials used in tables 7.3 thru 7.15, and gives the full titles of the organizations. (Table 7.1 is not a comprehensive listing.)

PRINCIPAL ORGANIZATIONS  
ISSUING STANDARDS

TABLE 7.1

INITIALS	FULL TITLE OF ORGANIZATION
AIA	American Insurance Association *
ANSI	American National Standards Institute †
API	American Petroleum Institute
ASME	American Society of Mechanical Engineers
ASTM	American Society for Testing and Materials
AWS	American Welding Society
AWWA	American Waterworks Association
FCI	Fluid Controls Institute
GSA	General Service Administration
ISA	Instrument Society of America
MSS	Manufacturers' Standardization Society of the Valve and Fittings Industry
NFPA	National Fire Protection Association
PFI	Pipe Fabrication Institute
USDC	United States Department of Commerce

\*Standards formerly issued by Underwriters' Laboratories Inc.  
†Formerly, United States of America Standards Institute, and American Standards Association.

## PRINCIPAL DESIGN-ORIENTATED CODES 7.5

### ANSI CODE B31 7.5.1

The most important code for land-based pressure-piping systems is ANSI B31. Parts of this code which apply to various types of plant piping are listed in table 7.2.

ANSI CODE B31 FOR PRESSURE PIPING

TABLE 7.2

PETROLEUM REFINERY PIPING	B31.3-1966	Piping for refineries and petrochemical plants conveying petrochemicals, chemicals, water and steam.
POWER PIPING	B31.1.0-1967*	Piping for industrial applications. State law may require adherence.
CHEMICAL PLANT PIPING	B31.6-?	Still in preparation. Usually chemical plant piping complies with the 'Power piping' code.
FUEL GAS PIPING	B31.2-1968	Piping for conveying and handling combustible hydrocarbon gases.
REFRIGERATION PIPING	B31.5-1966	Principal application is the piping of package units.
NUCLEAR POWER PIPING	B31.7-1969	More stringent design and inspection requirements than other B31 codes. To be applied to pressure piping where escape of fluid from the system would incur a radiation hazard.

\* B31.1-1955 is out of print. The 'Power piping' code will eventually be designated B31.1-1967

### AMERICAN PETROLEUM INSTITUTE'S CODE 2510-1965 7.5.2

This second edition covers design and construction of liquefied petroleum gas installations at marine and pipeline terminals, natural gas processing plants, refineries and tank farms.

The two following codes are not directly related to piping, but frequently are involved in the piping designer's work:

### API-ASME UNFIRED PRESSURE VESSEL CODE 7.5.3

This code applies to piping that is attached to a pressure vessel in petrochemical service. If the vessel is fabricated largely from fittings, construction will come entirely under the code.

### ASME BOILER & PRESSURE VESSEL CODE 7.5.4

The background of this code is described in the 'History of the boiler code' (ASME: 1955). The ASME Boiler and Pressure Vessel Code is mandatory in many States, with regard to design, material specification, fabrication, and erection. Compliance is required in the USA and Canada in order to qualify for insurance. The 1971 version of the Code consists of the following eleven sections:-

#### ASME BOILER & PRESSURE VESSEL CODE

	section
Power boilers	1
Material specifications	2
Nuclear power plant components	3
Heating boilers	4
Nondestructive examination	5
Recommended rules for care and operation of heating boilers	6
Recommended rules for care of power boilers	7
Pressure vessels	8
Welding qualifications	9
Fiberglass-reinforced plastic pressure vessels	10
Rules for Inservice Inspection of nuclear reactor coolant systems	11

7.1  
5.4

TABLES  
7.1 & 7.2

## CODES FOR MARINE PIPING

7.5.6

Requirements for merchant and naval vessels are contained in the following standards:

- (1) American Bureau of Shipping: 'Rules for building and classing vessels'
- (2) Lloyds' Register of Shipping: 'Rules'
- (3) US Coast Guard: 'Marine engineering regulations and material specifications'
- (4) US Navy, Bureau of Ships: 'General specifications for building naval vessels', 'General machinery specifications'

## SELECTED STANDARDS

7.5.6

The following tables are not comprehensive: a selection has been made from standards relating to piping design and technology. Sources of these standards may be found from table 7.1. Addresses of the issuing organizations may be found from the current edition of 'Encyclopedia of associations: Vol 1, National organizations of the United States' (Gale Research Company).

## STANDARDS FOR SYMBOLS & DRAFTING

TABLE 7.3

Piping	Graphic symbols for pipe fittings, valves and piping	ANSI Z32.2.3
	Graphic symbols for plumbing	ANSI Y32.4
	Graphic symbols for fluid power diagrams	ANSI Y32.10
	Fluid power diagrams	ANSI Y14.17
Process Engineering	Graphic symbols for process flow diagrams in petroleum and chemical industries	ANSI Y32.11 ASME K40
	Operation and process flow charts	ASME No. 101
	Letter symbols for chemical engineering	ANSI Y10.12
	Letter symbols for hydraulics	ANSI Y10.2
	Letter symbols for petroleum reservoir engineering and electric logging	ANSI Y10.15
Instrumentation	Instrumentation symbols and identification	ISA S5.1
Welding	Graphic symbols for welding	ANSI Y32.3
	Standard welding symbols and rules for their use	AWS A2.0
Heating and Ventilating	Graphic symbols for heating, ventilating, and air conditioning	ANSI Z32.2.4
Electrical	Electrical and electronics diagrams	ANSI Y14.15
Drafting	Size and format	ANSI Y14.1
	Line conventions, sectioning and lettering	ANSI Y14.2
	Projections	ANSI Y14.3
	Pictorial drawing	ANSI Y14.4
	Dimensioning and tolerancing for engineering drawings	ANSI Y14.5
	Screw threads	ANSI Y14.6
	Nomenclature, definitions and letter symbols for screw threads	ANSI B1.7

## PRINCIPAL STANDARDS FOR PIPE

TABLE 7.4

Steel or iron	Specification for welded and seamless steel pipe	ANSI B125.1 ASTM A53 ASME SA53
	Specification for seamless carbon-steel pipe for high-temperature service	ANSI B36.3 ASTM A106
	Specification for electric-fusion(arc)-welded steel-plate pipe (sizes 16 inch and over)	ANSI B36.4 ASTM A134
	Specification for electric-resistance-welded steel pipe	ANSI B125.3 ASTM A135 ASME SA135
	Wrought-steel and wrought-iron pipe	ANSI B36.10 ASME M31 ISO R64
	Stainless-steel pipe	ANSI B36.19
	Specification for seamless and welded austenitic stainless-steel pipe	ANSI B125.18 ASTM A312
	Specification for seamless ferritic alloy steel pipe for high-temperature service	ANSI B125.24 ASTM A336
	Threaded cast-iron pipe for drainage, vent, and waste services	ANSI A40.5 ASME M27
	Specification for line pipe	API 5L
	Specification for line pipe, high test	API 5LX
Non-ferrous metals	Specification for aluminum alloy seamless pipe and seamless extruded tube	ANSI H38.7 ASTM B241
	Specification for general requirements for wrought seamless copper and copper-alloy tube	ANSI H23.4 ASTM B261
	Lead pipe	GSA WW-P-325
	Specification for nickel seamless pipe and tube *	ANSI H34.1 ASTM B161
Plastics	Specification for polyethylene (PE) plastic pipe, SCH 40	ANSI B72.8 ASTM D2104
	Polyethylene pipe	USDC CS-197
	Specification for poly(vinyl chloride) (PVC) plastic pipe, SCH's 40, 80, & 120	ANSI B72.7 ASTM D1785
	Polyvinyl chloride pipe, dimensions and tolerances for	USDC CS-207
	Specification for acrylonitrile-butadiene-styrene (ABS) plastic pipe (SDR-PR & Class T)	ANSI B72.3 ASTM D2282
	Specification for acrylonitrile-butadiene-styrene (ABS) plastic pipe, SCH's 40 & 80	ANSI B72.5 ASTM D1527
	Specification for cellulose acetate butyrate (CAB) plastic pipe, SCH 40	ANSI B72.4 ASTM D1503

\*Made to stainless-steel schedules, ANSI B36.19

## STANDARDS FOR HANGERS & SUPPORTS

TABLE 7.5

Application	Pipe hangers and supports—selection and application	MSS SP-69
Production	Pipe hangers and supports—material and design	MSS SP-68

## STANDARDS FOR PIPING (DESIGN &amp; FABRICATION)

TABLE 7.6

Drafting	Method for dimensioning piping assemblies	PFI ES2
	Minimum length and spacing for welded nozzles	PFI ES7
Fabrication	Butt-welding ends for pipe, valves, flanges, and fittings	ANSI B16.25
	End preparation, and machined backing rings for butt welds	PFI ES1
	End preparation for manual inert-gas tungsten-arc root-pass welding	PFI ES21
	Fabricating tolerances	PFI ES3
	Stress relieving welded attachments	PFI ES10
	Heat treatment of ferrous pipe welds	PFI ES19
Testing	Shop hydrostatic testing of fabricated piping	PFI ES4
	Classification of shop testing, inspection, and cleaning	PFI ES13
	Ultrasonic inspection of seamless piping	PFI ES18

## STANDARDS FOR FLANGES

TABLE 7.7

Steel	Steel pipe flanges and flanged fittings	ANSI B16.5 ASME M15
	Large diameter carbon steel flanges	API 605
	MSS steel pipe line flanges	MSS SP-44
	High-pressure chemical industry flanges and threaded stubs for use with lens gaskets	MSS SP-65
	Unfired pressure vessel flange dimensions	ANSI B16.30 ASME J27
Cast iron	Cast-iron pipe flanges and flanged fittings, 25, 125, 250, and 800 PSI	ANSI B16.1 ASME J17
	MSS 150 PSI corrosion-resistant cast flanges and flanged fittings	MSS SP-51
Finishing	Finishes for contact faces for connecting end flanges of ferrous valves and fittings	MSS SP-6

## STANDARDS FOR GASKETS

TABLE 7.8

Metallic	Ring-joint gaskets and grooves for steel pipe flanges	ANSI B16.20 ASME L30
	Metallic gaskets for refinery piping (double-jacketed, corrugated, and spiral-wound)	API 601
Non-metallic	Raised-face flange gaskets, limiting dimensions of which meet requirements of ANSI B16.5	MSS SP-47
	Non-metallic gaskets for pipe flanges	ANSI B16.21 ASME L15

## STANDARDS FOR FITTINGS

TABLE 7.9

Steel	Factory-made wrought steel butt-welding fittings	ANSI B16.9 ISO R285
	Wrought steel butt-welding short-radius elbows and returns	ANSI B16.28 ASME M53
	Butt-welding ends for pipe, valves, flanges, and fittings	ANSI B16.25 ASME J13
	Steel butt-welding fittings (26-inch and larger)	MSS SP-48
	High-strength wrought welding fittings	MSS SP-63
	Forged-steel fittings, socket-welding and threaded	ANSI B16.11 ASME M16
Stainless steel	Wrought stainless-steel butt-welding fittings	MSS SP-43
Iron	Cast-iron screwed fittings, 125 and 250 PSI	ANSI B16.4
	Cast-iron threaded drainage fittings	ANSI B16.12 ASME J21
	Malleable-iron screwed fittings, 150 and 300 PSI	ANSI B16.3 ASME L5
Ferrous	Ferrous pipe plugs, bushings and locknuts with pipe threads	ANSI B16.14 ASME J32
Copper alloy	Wrought copper and wrought copper alloy solder-joint drainage fittings	ANSI B16.29 ASME N57
	Cast bronze fittings for flared copper tubes	ANSI B16.26 ASME J8
Plastics	Plastic insert fittings for flexible polyethylene pipe	ANSI B16.27 ASME L37

## STANDARDS FOR PUMPING MACHINERY

TABLE 7.10

Centrifugal pumps	Centrifugal pumps	ASME PTC8.2
	Centrifugal pumps for general refinery services	API 610
Positive-displacement pumps	Displacement pumps	ASME PTC7.1
	Reciprocating steam-driven positive-displacement pumps	ASME PTC7
	Displacement compressors, vacuum pumps and blowers	ASME PTC9
Compressors and exhausters	Installation of blower and exhaust systems for dust, stock and vapor removal or conveying	ANSI Z33.1 NFPA 91 AIA 91
	Compressors and exhausters	ASME PTC10
	Ejectors and boosters	ASME PTC24
Nuclear power	Nuclear power plant components (Section 3, ASME Boiler Code)	ASME F3

7 .5.5  
.5.6TABLES  
7.3-7.10

## STANDARDS FOR VALVES

TABLE 7.11

Steel	Steel gate valves (flanged or butt-welding ends) for refinery use. 5th edn.	API 600
	Specification for pipeline valves (steel gate, plug, ball, and check valves)	API 6D
	Compact design carbon-steel gate valves for refinery use	API 602
	Pressure-temperature ratings for steel butt-welding-end valves	MSS SP-66
Iron	Cast-iron pipeline valves	MSS SP-62
	Flanged nodular iron gate and plug valves for refinery use. 2nd edn.	API 604
	MSS 150 PSI corrosion-resistant cast flanged valves	MSS SP-42
	150 PSI light-wall, corrosion-resistant gate valves for refinery use (1/4-inch to 12-inch inclusive). 1st edn.	API 603
Ferrous	Face-to-face and end-to-end dimensions of ferrous valves	ANSI B16.10
	Finishes for contact faces of connecting end flanges of ferrous valves and fittings	MSS SP-6
Bronze	MSS 125 PSI bronze gate valves	MSS SP-37
Butterfly	Butterfly valves	MSS SP-67
Relief	Safety and relief valves with atmospheric or superimposed back-pressure before discharging	ASME PTC25.2
Control	Uniform face-to-face dimensions for flanged control valve bodies	ISA RP4.1
	Recommended procedure in rating flow and pressure characteristics of solenoid valves for liquid service	FCI 68-2
	Recommended procedure in rating flow and pressure characteristics of solenoid valves for gas service	FCI 68-1
	Recommended voluntary standards for face-to-face dimensions of control valves in sizes 10-inch thru 16-inch in ratings of 125 PSI thru 250 PSI for cast iron, and 150, 300, and 600 PSI for cast steel	FCI 65-2
	Recommended voluntary standard formulas for sizing control valves	FCI 62-1
	Definitions for regulator capacities	FCI 68-1
	Standard classification and terminology for power-actuated valves	FCI 55.1

## STANDARDS FOR STEAM TRAPS

TABLE 7.12

Rating	Pressure rating standard for steam traps	FCI 69-1
	Voluntary standards for determining industrial steam trap capacity rating	FCI 65-3
Testing	Life-cycling tests applicable to balanced pressure thermostatic trap elements	FCI 68-3

## STANDARDS FOR UNFIRED VESSELS &amp; TANKS

TABLE 7.13

Pressure vessels	Pressure vessels (Section 8, ASME Boiler Code)	ASME FBAA8
Low-pressure tanks	Recommended rules for design and construction of large welded low-pressure storage tanks	API 620
	Welded steel tanks for oil storage	API 650
	Venting atmospheric and low-pressure storage tanks	API 2000
Nuclear vessels	Safety standard for design, fabrication and maintenance of steel containment structures for stationary nuclear power reactors	ANSI NS.2 ASME N42
	Nuclear power plant components (Section 3, ASME Boiler Code)	ASME F3

## STANDARDS FOR HEAT EXCHANGERS

TABLE 7.14

Exchangers	Heat exchangers for general refinery services	API 660
	Tube dimensions for heat exchangers	API 640
Heaters	Feedwater heaters	ASME PTC12.1

## SCREW THREADS FOR PIPING, NUTS &amp; BOLTS

TABLE 7.16

General	Unified screw threads	ANSI B1.1 ASME M28
	Unified screw threads—metric translation	ANSI B1.1a
	Metric screw threads	ASME N46
	Nomenclature, definitions, and letter symbols for screw threads	ANSI B1.7 ASME L11
Pipe	Pipe threads (except dryseal)	ANSI B2.1 ASME L18
	Dryseal pipe threads	ANSI B2.2 ASME M36
Hose	Firehose coupling screw thread	ANSI B26 ASME J34
	Hose coupling screw threads	ANSI B2.4 ASME K14
Valves, fittings, and flanges	Specification for wellhead equipment	API 6-A
Nuts and bolts	Square and hex nuts	ANSI B18.2.2 ASME M43 ISO R272
	Square and hex bolts and screws	ANSI B18.2.1 ASME M44 ISO R272

# ABBREVIATIONS

## FOR PIPING DRAWINGS & INDUSTRIAL CHEMICALS

8.1

### ABBREVIATIONS USED ON PIPING DRAWINGS, DOCUMENTS, Etc.

8.1

<b>A</b>		<b>E</b>		<b>ID</b>	
A	(1) Air (2) Absolute	E	East	ID	(1) Inside diameter (2) Internal diameter
ABS	Absolute	ECN	Engineering change number	IMP	Imperial. [British unit]
AGA	American Gas Association	EFW	Electric-fusion-welded	IPS	Iron pipe size
AISI	American Iron and Steel Institute	ELL	Elbow	IS	Inside screw. [Of valve stem]
ANSI	American National Standards Institute	ERW	Electric-resistance-welded	ISO	Isometric drawing
API	American Petroleum Institute			IS&Y	Inside screw and yoke
ASTM	American Society for Testing and Materials	<b>F</b>		<b>K</b>	
AWS	American Welding Society	F	Fahrenheit	K	Kilo, times one thousand, x1000
AWWA	American Waterworks Association	F&D	Faced and drilled	KG	Kilogram
<b>B</b>		FAHR	Fahrenheit	<b>L</b>	
BBL	Barrel	FBW	Furnace-butt-welded	L	Liquid
BC	Bolt circle	FCN	Field change number	LB,Lb	Pound weight
BLE	Beveled large end	FD&SF	Faced, drilled and spot-faced	LT	Light-wall [of Pipe]
BLK	Black	FE	Flanged end	LR	Long radius. [Of Elbow]
BLVD	Beveled	FF	(1) Flat face(d) (2) Full face [of gasket] (3) Flange face [dimensioning]	<b>M</b>	
BOP	Bottom [of outside] of pipe. Used for pipe support location	FLG	Flange	M	(1) Meter (2) Mega, times one million, 1 000 000. [On old drawings, x1 000]
BS	British Standard	FLGD	Flanged	<b>MACH</b>	
BTU	British thermal unit	FOB	(1) Flat on bottom. [Indicates orientation of eccentric reducer] (2) Freight on board. [Indicates location of supply of vendor's freight at the stated price] (3) Free on board. [Indicates location of supply of vendor's freight]	MACH	Machined
BW	(1) Butt weld (2) Butt welded	FOT	Flat on top. [Indicates orientation of eccentric reducer]	MATL	Material
<b>C</b>		FRP	[Glass-] fiber reinforced pipe	MAWP	Maximum allowable working pressure
C	(1) Centigrade, or Celsius (2) Condensate	FS	Forged steel	MAX	Maximum
CENT	Centigrade	FW	Field weld	MCC	Motor control center
CFM	Cubic feet per minute	<b>G</b>		M/C	Machine
CHU	Centigrade heat unit	G	(1) Gas (2) Grade (3) Gram	MFR	Manufacturer
CI	Cast iron	GAL	Gallon	MI	Malleable iron
CM	Centimeter	GALV	Galvanized	MIN	(1) Minimum (2) Minute. [Of time]
Cr	Chromium	GPH	Gallons per hour	MM	Millimeter
CS	(1) Carbon steel (2) Cold spring	GPM	Gallon per minute	Mo	Molybdenum
CSC	Car-sealed closed. Denotes a valve to be locked in the closed position under all circumstances other than repair to adjacent piping	<b>H</b>		MSS	Manufacturers' Standardization Society of the Valve and Fittings Industry
CSO	Car-sealed open. See CSC	H	(1) Horizontal (2) Hour	<b>N</b>	
CTR	Center	HEX	Hexagon(al)	N	North
CU	Cubic	Hg	Mercury	NC	Normally closed
<b>D</b>		HPT	Hose-pipe thread	NEMA	National Electrical Manufacturers' Assn.
DEG	Degree	HR	Hour	Ni	Nickel
DIA	Diameter	<b>I</b>		NIC	Not in contract
DIN	Deutsche Industrie Norm [German standard]	IE	Invert elevation	NO	Normally open
DO	Drawing office	<b>J</b>		NPSC	2.5.5
DRG	Drawing. [Not preferred]	<b>K</b>		NPSF	2.5.5
DWG	Drawing	<b>L</b>		NPSH	(1) Net positive suction head. [3.2.1] (2) 2.5.5
		<b>M</b>		NPSI	2.5.5
		<b>N</b>		NPSL	2.5.5
		<b>O</b>		NPSM	2.5.5

NPT National pipe thread  
 NPTF 2.5.5  
 NRS Non-rising stem. [Of valve]  
 O  
 O Oil  
 OD Outside diameter  
 OS Outside screw. [Valve stem]  
 OS&Y Outside screw and yoke. [Valve stem]

P  
 P&ID Piping and instrumentation diagram  
 PBE Plain both ends. [Swage, etc.]  
 PE Plain end. [Pipe, etc.]  
 PFI Pipe Fabrication Institute  
 POE Plain one end. [Nipple, etc.]  
 PS (1) Pipe support. [Anchor, guide or shoe, or items combined to form the support]  
 (2) Pre-spring  
 PSI Pound [weight] per square inch. [Pressure]  
 PSIA Pound per square inch absolute  
 PSIG Pound per square inch gage

R  
 RED Reducing  
 RF Raised face  
 RJ Ring joint  
 RPM Revolutions per minute  
 RS Rising stem. [Of valve]

S  
 S (1) South  
 (2) Steam

SAE Society of Automotive Engineers  
 SCH Schedule. [Of pipe]  
 SCRD Screwed  
 SF Spot-faced  
 SKT Socket  
 SMLS Seamless  
 Si Silicon  
 SO Slip-on  
 SP (1) Sample point  
 (2) Standard practice. [MSS term]

SR Short radius. [Of elbow]  
 SST Stainless steel  
 ST Steam trap  
 STM Steam  
 STD Standard  
 STR Straight  
 SW Socket welding  
 SWG Swage  
 SWG Swaged nipple  
 NIPP  
 SWP Steam working pressure

T  
 T (1) Temperature  
 (2) Trap  
 T&C Threaded and coupled. [Pipe]  
 TEMA Tubular Exchanger Manufacturers' Assn.  
 TGT Tangent  
 TOE Threaded one end. [Nipple or Swage]  
 TOS Top of support  
 TPI Threads per inch  
 TSE Threaded small end  
 TYP Typical. [Used to avoid redrawing similar arrangements]

U  
 UNC 2.6.3  
 UNF 2.6.3  
 UNS 2.6.3

V  
 V (1) Vertical  
 (2) Vanadium

W  
 W (1) West  
 (2) Water  
 WGT Weight  
 WLD Weld(ed)  
 WN Welding neck  
 WOG Water, oil and gas  
 WP (1) Workpoint or reference point  
 (2) Markings with this prefix designate certain steels and are used on pipe, fittings and plate. Example: 'WPI' marked on forged fittings denotes A181 grade 2. Refer to ASME SA-234, tables 1 and 2.

WT Weight  
 X  
 XH Extra-heavy. [See Index]  
 XS Extra-strong  
 XXS Double-extra-strong

#### OTHER

⌒ Centerline  
 ∅ Diameter

## ABBREVIATIONS FOR COMMERCIAL CHEMICALS

8.2

ABBREVIATION	CHEMICAL NAME	AREA OF USE	D		
A	Acetone dicarboxylic acid Air-entraining agent 83% ammonium nitrate in water	Drugs Concrete	DAP	Diammonium phosphate	Agriculture
			DCO	Dehydrated castor oil	Paint
			DMC	Dimethylammonium dimethyl carbamate	Refining
			DMF	Dimethyl formamide	
B	Benzyl para-amino phenol Butylated hydroxyanisole Benzene hexachloride Butylated hydroxytoluene 77-78% sulfuric acid ('blown oil of vitreol') Benzaldehyde Benzoic acid	Fuel Food General Food General General General	DMU	Dimethyl urea	
			DNA	Dinonyladipate	Plastics
			DNM	Dinonyl maleate	Plastics
			DNP	Dinonyl phthalate	Plastics
			DNT	Dinitrotoluene	Explosives
			DOP	Diocetyl phthalate	Plastics
			DOV	96% sulfuric acid ('distilled oil of vitreol')	General
			DSP	Disodium phosphate	General
			DTBP	Ditertiary-butyl peroxide	Plastics
			DVB	Divinyl benzene	Plastics
C	Carbon monoxide 95-96% sulfuric acid ('concentrated oil of vitreol') Carbon dioxide	General General	DPG	Diphenyl guanidine	Rubber
			DOPA	3,4-dihydroxyphenylaniline	Rubber
			E		
			EA	Ethylidene aniline	Rubber
CO			EDTA	Ethylene diamine tetra-acetic acid	Food

ABBREVIATION MEANING AREA OF USE

## F

FA Furfuryl alcohol General  
FGAN Ammonium nitrate Agriculture  
FPA Fluorophosphoric acid  
FREON One of a large number of chloro- or fluoro- substituted hydrocarbons Refrigeration, General

## H

HCN Hydrocyanic acid, hydrogen cyanide Plating  
HET Hexa-ethyl tetraphosphate Agriculture  
HMDT Hexamethylene triperoxide  
HMT Hexamethylene tetramine  
HNM Mannitol hexanitrate Explosives  
HTP 100% hydrogen peroxide Rocketry, General  
(‘high test peroxide’),  
Branched aliphatic alcohols of high b.pt.  
Water

## H2O

## I

IMS Commercial ethyl alcohol (Brit.) General  
IPA Isophthalic acid  
IPC Isopropyl n-phenyl carbonate  
IPS Isopropyl alcohol (Shell Oil Co.) General

## L

LOX Liquid oxygen Rocketry  
LPC Lauryl pyridinium chloride Soaps  
LPG Liquefied petroleum gases, mainly butane and propane Fuel

## M

MBMC Monotertiary butyl-methyl-cresol General  
MEK Methyl-ethyl-ketone Paint, General  
MEP 2-methyl, 5-ethyl pyridine  
MIRC Methyl isobutyl carbinol  
MIBK Methyl-isobutyl-ketone  
MNA Methyl-nonyl acetaldehyde  
MNPT m-nitro p-toluidine  
MNT Mononitro toluene Explosives  
MSG Monosodium glutamate Food

## N

NBA n-bromacetamide  
NBS n-bromosuccinamide  
NCA n-chloracetamide  
NCS n-chlorosuccinamide  
NH powder Explosive powder  
N2 Nitrogen

## O

OMPA Octamethyl pyrophosphoramidate  
ONB o-nitrobiphenyl  
OPE Octylphenoxyethanol  
O2 Oxygen  
O3 Ozone

## P

PAS p-aminosalicylic acid Drugs  
PB Polybutene Plastics  
PBNA Phenyl beta-naphthylamine Rubber  
PDB p-dichlorobenzene Agriculture  
PE Penta-erythritol  
PETN Penta-erythritol tetranitrate Explosives  
PTFE Polytetrafluorethylene Plastics  
PVA or PVAL Polyvinyl alcohol  
PVAc Polyvinyl acetate  
PVB Polyvinyl butyrol  
PVC Polyvinyl chloride  
PVM Polyvinyl methyl-ether

## R

RNV Sulfuric acid (‘refined oil of vitreol’) General

## S

S Sulfur General  
SAP Sodium acid pyrophosphate  
SDA Specially denatured alcohol General  
SO2 Sulfur dioxide General

## T

TCA Sodium tetrachloracetate Agriculture  
TCE 1,1,1-trichloroethane Dry cleaning  
TCP Tricresyl phosphate Fuel, Plastics  
TEG Triethylene glycol Refining  
TEL Tetraethyl lead Fuel  
TEP Tetraethyl pyrophosphate Agriculture  
TFA Tetrahydrofurfuryl alcohol  
TNA Trinitroaniline  
TNB Trinitrobenzene Explosives  
TNG Trinitroglycerine Explosives  
TNM Trinitromethane Explosives  
TNT Trinitrotoluene  
TNX Trinitroxylene Explosives  
TOF Trioctyl phosphate Explosives  
TPG Triphenyl guanidine Plastics  
TSP Trisodium o-phosphate Rubber  
Tetrasodium phosphate

## V

VA Vinyl acetate

## Z

ZMA Zinc methylarsenate Timber

8.1  
8.2

# INDEX & GLOSSARY

## A

**ABBREVIATIONS.** 8  
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**AFTERCooler.** 3.2.2  
**AGITATOR.** table 3.7  
**AIR IN STEAM.** 6.9.1, 6.10.1  
**AIR LINE.** Liquid removal. 6.11.4  
**ALLOYS.** For pipe. 2.1.4  
**AMBIENT.** Pertaining to the surroundings. Usually refers to temperature  
**AMERICAN STANDARDS ASSOCIATION.** 7.3  
**ANCHOR.** 2.12.2, 6.2.8. A pipe fixture used to hold piping rigidly at a chosen point. Position where piping is restrained is termed the 'anchor point'  
**ANGLE VALVE.** 3.1.5  
**ANSI.** 7.3  
**ARCHIVE.** Place where drawings, specifications, etc., may be permanently stored  
**ASA.** 7.3  
**ATTRITION.** See 'Change of particle size' 3.3.4  
**AUTOCLAVE.** Vessel in which material or reactants are held under controlled conditions (time, temperature, pressure, atmosphere, etc.)  
**AUXILIARY PIPING.** 6.3.1

## B

**BACK WELD.** In piping, a continuous weld made at the back of a butt weld—possible only if there is access to the interior  
**BACKCHECK.** 6.4.2  
**BACKING RING—Chill ring.** chart 2.1, figure 2.1  
**BALL FLOAT VALVE.** 3.1.9  
**BALL VALVE.** Check valve. 3.1.7  
**BALL VALVE.** Rotary. 3.1.6  
**BAROMETRIC LEG.** If a process which takes place below atmospheric pressure requires water or other liquid to be continuously drained from it, this may be achieved by connecting the drain to a vertical pipe termed a 'barometric leg', the lower end of which is inserted in a seal pot. When the leg and seal are primed with liquid draining from a low-pressure process can occur continuously. If the pressure of the process approaches zero (absolute) the leg must be at least 34 ft in height.  
**BARSTOCK PLUG.** 2.5.4, figure 2.55  
**BARSTOCK VALVE.** 3.1.11. Valve machined from solid metal  
**BATTERY LIMIT.** Arbitrary line shown on drawings to define on-plot and off-plot areas. Also used to define limits of contractual responsibility within an on-plot area.  
**BENCHMARK.** 6.3.1, figure 5.12  
**BENDS, BUTT WELDING.** 2.3.1  
**BENT.** 6.1.2  
**BEVEL.** The ends of pipe and butt-welding fittings are beveled (see chart 2.1) to aid making welded joints  
**BIBB.** 3.1.11  
**BILL OF MATERIEL.** 5.6.1  
**BLEED RING.** 2.7.1, figure 2.60, chart 5.7  
**BLEED VALVE.** 3.1.11, figure 2.60  
**BLENDER.** 3.3.2, table 3.7  
**BLIND FLANGE.** 2.7.1, 2.7.2, figure 2.61. Flange with no central opening used for closure of flanged terminations. Rated similarly to other types of flange—see tables F  
**BLOCK VALVE.** 3.1.11  
**BLOWDOWN VALVE.** 3.1.11

**BLOWDOWN SYSTEM.** A (discharge) piping arrangement for removing material from a process, vessel, boiler, etc.  
**BLOWER.** 3.2.2  
**BLOWOFF SYSTEM.** Piping hookup used for blowing scale and foreign matter from tanks, boilers, etc.  
**BLOWOFF VALVE.** 3.1.9  
**BOILER FEEDWATER.** 6.10.2  
**BOLT HOLES in flanges.** 2.6.2, tables F  
**BONNET.** 3.1.2  
**BOTTOMS.** See 'COLUMN OPERATION' 6.5.2  
**BREECHLOCK.** See 'Bonnet' 3.1.2  
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**BREATHING VALVE.** 3.1.11  
**BRITISH STANDARDS INSTITUTE.** 7.3  
**BRUNING.** 4.4.11  
**BUILDING LAYOUT.** 6.15.3  
**BUILDINGS.** In relation to piping. 6.15, figures 6.49 & 6.50  
**BULLHEAD TEE.** 2.3.2  
**BUND.** See 'DIKE'  
**BURIED PIPE.** Dimensioning. table 5.2  
**BURSTING DISC—Rupture disc.** 3.1.9  
**BUSHING.** Hexagon. Screwed. 2.5.1, figure 2.42  
**BUTT-WELDED PIPE JOINTS.** 2.3  
**BUTTERFLY VALVE.** 3.1.6  
**BYPASS.** Valved length of piping that allows full or partial flow, arranged around a valve, valve assembly, equipment, etc. See figures 6.6 thru 6.11 for examples  
**BYPASS VALVE.** 3.1.11

## C

**CAP**  
 Butt-welding. 2.3.3, figure 2.20  
 Screwed. 2.5.4, figure 2.54  
 Socket-welding. 2.4.4, figure 2.36  
**CARBON STEELS** are iron-based alloys having properties chiefly determined by their carbon content  
**CATCHBASIN.** Receptacle designed to separate matter from a waste stream  
**CATCHMENT.** Reservoir or basin  
**CATHODIC PROTECTION.** Buried pipe can be protected from corrosion by wiring buried sacrificial anodes (usually cylinders of zinc) to the pipe. Galvanic corrosion then tends to occur in the zinc instead of the steel. Protection may also be provided by means of electric voltages and ground currents  
**CAVITATION.** 6.3.1  
**CENTRIFUGE.** 3.3.3, table 3.8  
**CERTIFIED DRAWING/PRINT.** Final vendor's print of equipment showing dimensions which will be maintained during manufacture  
**CHATTERING.** 3.1.4  
**CHECK VALVE.** 3.1.7  
**CHECKER.** 4.1.2, 5.4.1  
**CHIEF DRAFTSMAN.** 4.1.2  
**CHILL RING—Backing ring.** chart 2.1, figure 2.1  
**CIVIL PIPING.** 1.1  
**CLEANOUT.** Arrangement for cleaning out a line or vessel  
**CLEARANCE.** 6.1.1, table 6.1  
 Orifice plate assembly. figure 6.38  
**CLOSING DOWN LINES.** 6.1.3  
**CLOSURES.** Permanent. figure 2.20  
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**CLOSURES.** Temporary. 2.7, table 2.6  
**COAST & GEODETIC SURVEY.** 5.3.1  
**COATINGS.** For pipe. 2.1.4  
**COCK.** Simple plug valve in the smaller sizes  
**CODES**  
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 API-ASME code for unfired pressure vessels. 7.5.3  
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**COLD SPRING.** 6.1.1, figure 6.2  
**COLOR CODING**  
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**COLUMN**  
 Fractionation. Distillation. 6.5.2, table 3.8  
**COLUMN PIPING.** 6.5.2  
**COMMERCIAL PIPING.** 1.1  
**COMPANION FLANGE.** A flange—or a flanging arrangement—custom-fabricated to mate with non-standard flanges on some special items of equipment  
**COMPOSITION DISC.** 3.1.5. Non-metallic disc used in certain globe valves  
**COMPRESSOR.** 3.2.2  
 Piping. 6.3.2  
**COMPRESSED AIR LINES.** Draining. 6.11.4  
**CONDENSATE.** 6.9.1, 6.10.2  
**CONNECTION.** To equipment. See **NOZZLE, CONNECTOR**  
 Pipe-to-tube. 2.5.1, figure 2.41  
 Quick connector. 2.8.1  
**CONSOLE.** An arrangement of gages and controls mounted in a desk or cabinet, from which a process may be monitored and controlled  
**CONSTANT LOAD HANGER.** 2.12.2  
**CONTINUATION SHEET.** See 'Process & service lines on piping drawings' 5.2.8. Any sheet on which information is continued  
**CONTROL STATION.** 6.1.4, figures 6.6 thru 6.11  
 Symbol. chart 6.7  
**CONTROL VALVE.** 3.1.10, figure 3.4  
**CONVEYED FLUID.** This term is used in the Guide for liquid or gas carried by piping  
**COOLER.** Heat exchanger used to cool process fluid  
**COOLING WATER.** Water used to cool process fluid or equipment  
**COORDINATE.** 5.3.1  
**COPYING PROCESSES.** 4.4.11  
**CORROSION.** Conveyed fluid may attack materials from which pipe and fittings are made. The degree of corrosion will depend on the pipe material, the conveyed fluid, its temperature and concentration, time of exposure, possible presence of water or air, and whether galvanic action is also present  
**CORROSION ALLOWANCE.** Additional thickness of metal in excess of that calculated for strength  
**COUPLING**  
 Screwed. FULL-. 2.5.1, 2.5.3, figures 2.37 & 2.49  
 Screwed. HALF-. 2.5.3, figure 2.49  
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 Socket-welding. FULL-. 2.4.1, figure 2.21  
 Socket-welding. HALF-. 2.4.3, figure 2.31  
 Socket-welding. REDUCER. 2.4.1, figure 2.22  
**CRASH PANEL.** Breakable panel thru which personnel may escape from a hazard in a building  
**CROSS**  
 Butt-welding. 2.3.2, figure 2.17  
 Screwed. 2.5.2, figure 2.48  
 Socket-welding. 2.4.2, figure 2.30

**CRYOGENIC.** Describes very low temperatures and equipment used at these temperatures. Term usually applies to -200 F and colder  
**CYCLONE.** 3.3.3, table 3.8

## D

**DAMPENER.**  
 For compressor. 3.2.2  
 Hydraulic. 2.12.2  
**DASHPOT.** Piston-type device used for damping mechanical movement  
**DATUM.** See 'Vertical reference' 5.3.1  
**DAVIT.** 6.5.2, figure 6.27  
**DAY TANK.** Term used for storage tank, holding limited supply of fuel, etc.  
**DEAD WEIGHTING.** Method of measuring pressure of fluid in a line. Device having a platform on which weights can be placed, temporarily fitted to vertical valved branch—weights take line pressure. Used for calibration  
**DEADMAN.** Anchor permanently set into ground for erection purposes—used for securing cables  
**DEAERATOR.** 3.3.3, table 3.8  
**DEFLECTION OF PIPE.** 6.2.6, table 5-1  
**DEFOAMER.** 3.3.3, table 3.8  
**DEMINERALIZED WATER.** Water with all forms of hardness (dissolved minerals) removed  
**DESICCANT.** A drying agent, such as concentrated sulfuric acid or silica gel  
**DESICCATOR.** Machine for removing water or other liquid from a process material by applying vacuum, heat, or by chemical means  
**DESUPERHEATER.** Device for reducing superheat in steam, usually by adding water to the steam  
**DETAIL.** See 'Elevations (sections) & details' 5.2.8  
**DEWPOINT.** The temperature at which a vapor forms liquid ('dew') on cooling  
**DIAPHRAGM VALVE.** 3.1.11  
**DIAZO.** 4.4.11  
**DIKE.** Shaped wall or embankment surrounding one or more storage tanks to form a basin able to hold entire contents of tank(s) in event of leakage or rupture  
**DIMENSIONING.** 5.3, figure 6.13, table 5.2  
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**DIVERTING VALVE.** 3.1.8  
**DOUBLE-BLOCK-AND-BLEED.** 2.7.1, figure 2.60.  
 See 'Make maintenance safe' 6.1.3



**DOUBLE EXTRA STRONG.** 2.1.3. Manufacturers' standard for wall thickness of pipe and fittings

**DOWNCOMER.** A line which conveys fluid downward

**DOWTHERM.** 6.9.2. See 'Jacketing' 6.8.2

**DRAFTING**  
Control stations. 6.1.4. chart 5.7  
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**DRAFTSMAN.** 4.1.2

**DRAIN**  
Location. 6.1.1, figure 6.47  
On P&ID. 5.2.4  
On pump. 6.3.1  
Symbol. chart 5.7, chart 5.28

**DRAIN HUB.** Funnel fitted in floor and connected to a drain line

**DRAIN VALVE.** 3.1.11

**DRAINAGE.** (1) System of drains, (2) Act or process of draining

**DRAINING**  
Air line. 6.11.4  
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**DRAWING NUMBER.** 4.2.4

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**DRIP VALVE.** 3.1.11. A drain valve used on driplegs  
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**DRYSEAL.** 2.5.6

**DUMMY LEG.** 2.12.2, figure 2.72A, table 6.3

**OYELINE.** 4.4.11

## E

**EDUCTOR.** 3.3.2, table 3.7

**EFFLUENT.** 6.13

**ELBOLET**  
Butt welding. 2.3.2, figure 2.14  
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**ELBOW-ELL**  
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## ELEVATIONS

Dimensions. 5.3.2, table 5.2  
Views. 5.2.8. See 'Elevations (sections) & details' 5.2.8

**ELL.** See ELBOW

**EJECTOR.** A type of pump in which a partial vacuum is created by passing steam or other fluid under pressure thru a neck or venturi with a branch at the narrowest part. A suction is created in the branch

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**EXPANDER FLANGE.** 2.3.1, figure 2.9

**EXPANSION.** Thermal movement. 6.1.1  
Of steel. chart 6.1  
Loop. figure 6.1

**EXPANSION JOINT.** 2.9.1, figures 2.63 thru 2.66

**'EXTRA HEAVY.'** Traditional term used for 250 PSI cast-iron fittings and 300 PSI malleable-iron fittings. These pressure ratings are for 'working steam pressure' (WSP)

**EXTRA-STRONG.** Manufacturers' standard for wall thickness of pipe and fittings. 2.1.3

**EXTRUDED NOZZLE.** Hot-formed outlet made in pipe or vessel by pulling shaped dies thru a hole made in the wall

## F

**FAN.** table 3.3

**FIELD.** (1) Construction site ('job site'), where piping is erected. (2) Field engineering office

**FIELD WELD.** Weld made at the time of erection of piping at the site  
Symbol for. chart 5.3, figure 5.15

**FILING DRAWINGS.** 4.3, 4.4.10

**FILLET WELD.** chart 5.9

**FINISHED GRADE.** 5.3.1

**FIREFIGHTING.**  
Station. 6.1.2

**FIREWATER.** Independent supply of water for firefighting

**FIRST-AID STATION.** Location. 6.1.2

**FITTING MAKEUP**  
Dimensioning for. 5.3.5  
Fitting makeup. 5.3.3

**FITTINGS.** 2.2.4  
Butt-welding. 2.3, chart 2.1  
Ordering. 5.6.3  
Screwed. 2.5, chart 2.3  
Socket-welding. 2.4, chart 2.2

**FLAG.** To identify an item on a drawing by means of a flag, panel or other mark

**FLAME ARRESTOR.** A device to prevent a flame-front from moving upstream in a line or vessel. For small lines, may consist of a wire screen. For larger lines, arrangements of multiple parallel plates or tubes are used. Principally used on vent lines to tanks. Symbol. chart 5.7

**FLAMMABLE LIQUID.** Safety guidelines. 6.14

**FLANGE.** 2.2.3, 2.3.1, figures 2.6 thru 2.10  
Bolt and studbolt for. 2.6.3, figure 2.57, tables F  
Bolt hole. 2.6.2, tables F  
Expander. 2.3.1, figure 2.9  
Facing. 2.6.1, figure 2.56  
Gasket. 2.6.4, figure 2.56, table 2.5  
Lap joint. 2.3.1, figure 2.10  
Reducing. 2.3.1, figure 2.8  
Screwed. 2.5.1, figure 2.45  
Slip-on. 2.3.1, figure 2.7  
Socket-welding. 2.4.1, figure 2.27  
Welding-neck. 2.3.1, figure 2.6

**FLAP VALVE.** 3.1.11

**FLARESTACK.** A stack located away from the processing area, to which relief headers may be run for burning waste hydrocarbons or other flammable vapors. 6.11.3

**FLASH STEAM.** 6.9.1

## FLASHING

Steam. 6.10.8

Building construction. A piece of metal or other material used to cover or protect certain joints, such as where a chimney joins a roof

**FLASHPOINT.** Of flammable liquid. Temperature at which the amount of vapor given off is sufficient to form a flammable mixture with air over the surface, so that a momentary flash will occur when a source of ignition is applied. Hazardous liquids have low flashpoints

**FLAT FACE.** Flange. 2.6.1

**FLEXIBILITY.** figure 6.1

**FLEXIBLE PIPING.** 2.9.2  
Expansion joint. 2.9.1

**FLOTATION TANK.** table 3.8

**FLOOR STAND.** See 'Stem' 3.1.2

**FLOW DIAGRAM.** 5.2.3

**FLOW LINE**  
On flow diagram. 5.2.3  
On P&ID. 5.2.4

**FLUID.** Any material capable of flowing. In the Guide, term is used to denote either a liquid or a gas. Powders may also be considered fluids

**FLUSH-BOTTOM TANK VALVE.** 3.1.9

**FOOT VALVE.** 3.1.7

**FOREIGN MATTER.** Any unwanted material that enters a system from outside

**FOREIGN PRINT.** Print of a drawing originating in another group, department or company

**FRACTIONATION COLUMN.** 3.3.3, table 3.8  
Piping. 6.5.2

**FROST LINE.** The lowest depth in the ground which chills to 32 F (0 C)

**FULL-COUPLING.** See COUPLING

## G

**GAGE.** A device for measuring or registering level, pressure, temperature, etc.

**GAGE GLASS.** Glass used to show liquid level, usually in the form of a vertical glass tube with end connections

**GALVANIZING.** The coating of metal with zinc by electroplating or hot-dipping

**GASKET.** 2.6.4, table 2.5  
Dimensioning. See 'Dimensioning to joints' 5.3.3

**GATE VALVE.** 3.1.4

**GIRT.** A horizontal member of a building to which the panels forming the sides of the building are fitted.

**GLAND.** A sleeve within a stuffing box fitted over a shaft or valve stem and tightened against compressible packing so as to prevent leakage while allowing the shaft or stem to move

**GLASS PIPE.** 2.1.4  
Supporting. 6.2.7

**GLOBE VALVE.** 3.1.5

**GRADE.** See 'Vertical reference' 5.3.1

**GRADE BEAM.** Beam which is used to support a floor at ground level

**GROUND JOINT.** A connection in which two machined metallic surfaces are joined face-to-face

**GROUP LEADER.** 4.1.2

**GROUT.** A thin concrete poured on a set concrete foundation, between the foundation and the baseplate of the equipment which will rest on it. The baseplate is firmly bolted down on the level surface of the grout after it has hardened

**GUIDE.** 2.12.2, 6.2.8, figure 2.72A

**GUTLINE.** See 'Tracing' 6.8.2

## H

**HALF-COUPLING**  
Screwed. 2.5.3, figure 2.49  
Socket-welding. 2.4.3, figure 2.31

**HANDRAIL.** See RAILING

**HANGER.** 2.12.2  
Constant-load hanger. 2.12.2  
Spring hanger. 2.12.2

**HARNESS PIPING.** 6.3.1

**HEAD.** Pressure. 3.2.1

**HEADER.** A pipe serving as a principal supply or return line

**HEADER VALVE.** 3.1.11

**HEAT EXCHANGER.** 3.3.5, figure 6.32, chart H-1  
Data sheet. 6.6.1  
Piping to. 6.6

**HEXAGON BUSHING.** 2.5.1, figure 2.42

**HIGH POINT FINISHED GRADE.** See 'Vertical reference' 5.3.1

**HOLDING TANK.** Tank in which liquid (or gas) is held pending further processing or treatment

**HOMOGENIZER.** 3.3.4

**HOSE CONNECTOR.** 2.8.1

**HOSE VALVE.** 3.1.11

**HOT TAP.** This is a technique for branching into a line under pressure without having to close the line down

**HOTWELL.** A sump, tank, or other receptacle for holding discharges of hot liquids. 6.10.4

**HYDRAULIC ACCUMULATOR.** Stores liquid under pressure. Typically a device consisting of a cylinder and piston which is actuated by a weight, spring, or compressed gas. On the opposite side of the piston, the driven fluid, such as water or oil, is stored

**HYDRAULIC DAMPENER.** 2.12.2  
Symbol. chart 5.28

**HYDRAULIC RESISTANCE** of pipe and fittings. 6.1.1, table F-10

**HYDROSTATIC TESTING.** 6.11.2

**HYGIENIC CONSTRUCTION.** Pipe, valves, pumps and other equipment used to handle foodstuffs and drugs should be hygienically constructed which means that all surfaces contacting the material must be corrosion-proof, smooth, and non-toxic. Plastics and rubbers should not incorporate (as fillers) substances that may contaminate. Materials free from such contaminants may be referred to as 'white' rubber, etc.

## I

**INCONEL.** A high-nickel alloy containing chromium and iron. Resistant to oxidation and corrosion

**INCHASER-Swage** or reducer

**INSTRUMENT AIR.** See 'Compressed-air usage' 6.3.2

**INSTRUMENT CONNECTION.** 6.7, chart 6.2

**INSTRUMENT LOOP.** 5.5.3

**INSTRUMENT SOCIETY OF AMERICA.** 5.5.1, table 7.3

**INSTRUMENTATION.** 5.5  
Coding. table 5.3  
Function. 5.5.2  
Mounting. 5.5.4  
On flow diagram. 5.2.3  
On P&ID. 5.2.4  
Signal lead. 5.5.6, chart 5.1

**INSULATION.** Thermal  
On P&ID. 5.2.4  
Personnel protection. 6.8.1  
Thickness. 6.8.1, tables 6.7 & 6.8

**INTERCOOLER.** 3.2.2

**INTERCONNECTING P&ID.** 5.2.4

**INTERFACE.** Boundary common to two systems, figure 6.3 points (10) & (14)

**INVERT ELEVATION ('IE')** is the elevation of the bottom of the internal surface of a buried pipe. table 5.2

**INVENTORY.** A listing of pipe and other items of hardware maintained in stock

**IRON PIPE.** 2.1.4

**IRON PIPE SIZE.** 2.1.3, table P-1

**ISO=Isometric.** 5.2.6, 5.2.9, figures 5.15 & 5.16  
Checking. 5.4.4  
Numbering. 5.2.9

**ISOLATING VALVE.** 3.1.11

**ISSUING DRAWINGS.** 5.4.3

## J

**JACK SCREW.** Screw provided in orifice flanges and sometimes flanges for line blinds. Two screws are provided (one per flange) placed 180 degrees apart. figure 2.59

JACKETING. 6.8.2  
JOB FUNCTIONS. 4.1.2  
JOB NUMBER. Company account number to which work is charged. Appears on all paperwork for the project  
JUMPOVER. table A-2. 6.8.2

## K

KEY PLAN. 5.2.7  
KNIFE-EDGE VALVE. 3.1.11  
KNOCK-OUT DRUM or POT. A stream of gas containing drops of liquid is passed thru a knock-out drum in order to slow down the flow and allow the liquid to separate and collect  
KINETIC ENERGY. Energy pertaining to the velocity of material

## L

LADDER. chart P-2  
LAND on beveled end. chart 2.1  
LANTERN RING. See 'Bonnet' 3.1.2  
LAP-JOINT FLANGE. 2.3.1. figure 2.10  
LATERAL  
Butt-welding. 2.3.2. figure 2.18  
Screwed. 2.5.2. figure 2.47  
Socket-welding. 2.4.2. figure 2.29  
LATROLET  
Butt-welding. 2.3.2. figure 2.15  
Screwed. 2.5.3. figure 2.52  
Socket-welding. 2.4.3. figure 2.34  
LEROY. 4.4.6  
LETTERING. 4.4.6  
LEVEL GAGE. 6.7.4  
LINE BLIND. 2.7.1. figure 2.59  
Symbol. chart 5.6  
LINE BLIND VALVE. 2.7.1. 3.1.4  
LINE DESIGNATION SHEET. 4.2.3. 6.2.5  
LINE NUMBER  
P&ID. 5.2.4  
Piping drawing. See 'Process & service lines on piping drawings' 5.2.8  
Iso. 5.2.9  
Spool. 5.2.9  
LINEN. Drafting sheet. 4.4.1  
LININGS for pipe. 2.1.4  
LIST OF EQUIPMENT. 4.2.2  
LIST OF MATERIAL. 5.6.1  
LOAD CELL. Weighing mechanism installed in the supports of tanks, etc.  
LOW-PRESSURE HEATING MEDIA. 6.9.2  
LUG. Projecting piece on a vessel, frame, etc., by which it may be held or lifted

## M

MAIN. A principal section of pipe supplying service or process fluid  
Ring main. The fluid is continuously circulated around a closed loop of piping and may be drawn off at any point. Useful for slurries and other fluids that may settle or separate  
MAKEUP WATER. Water is lost in many processes and operations. Water inventory is restored by adding makeup water.  
MALLEABLE IRON. A ductile cast iron produced by controlled annealing of white cast iron.  
MANHOLE. table 6.1  
In column. 6.5.2  
MANIFOLD. A chamber or pipe (header) having several branches  
MANOMETER. See 'Orifice plate assembly' 6.7.5  
MANUFACTURERS' WEIGHT. 2.1.3  
MATCHLINE. See 'Process & service lines on piping drawings' 5.2.8. figure 5.8  
MATERIAL BALANCE. A detailed tabulation of process material flowing into, thru and out of the process, showing the distribution of all significant components, including impurities

MATERIAL TAKEOFF. Estimated quantities for materials, taken from drawings  
MILL. Symbol. chart 5.2A  
MITER. 2.3.1. figure 2.5  
MIXER. 3.3.2. table 3.7  
MIXING. 3.3.2  
MIXING VALVE. 3.1.11  
MODEL of plant. 4.4.12  
MONEL. Alloys consisting mainly of nickel and copper, which have good resistance to corrosion, abrasion and heat  
MONUMENT. 6.3.1. figure 5.12  
MULTI-PORT VALVE. 3.1.8  
MYLAR FILM. 4.4.1

## N

NEEDLE VALVE. 3.1.5  
NIPOLET. Integral nipple/weldolet  
Plain. 2.4.3. figure 2.35  
Screwed. 2.5.3. figure 2.53  
NIPPLE  
Screwed. 2.5.1. figure 2.39  
Shaped. 2.3.2. figure 2.19  
NON-RETURN VALVE. 3.1.7. 3.1.11  
NON-RISING STEM. See 'Stem' 3.1.2. Type of valve stem which rotates but does not rise when valve is operated  
NORTH. Plant & true. See 'Horizontal reference' 5.3.1 & 'Allocating space on the sheet' 5.2.8. figure 5.11  
NOZZLE. A protruding port of a vessel, tank, pump, etc., to which piping is connected  
Column. 6.5.2  
Heat exchanger. 6.6.2  
Pump. See 'Typical piping for centrifugal pumps' 6.3.1  
Supporting pipe at. 6.2.8  
Vessel. 6.5.1  
NUB. Spacer (protrusion) on a backing ring or insert  
NUMBER OF LINE. See 'Flow lines on P&ID's' 5.2.4

## O

OBLIQUE DRAWING. 5.2.6  
ON-PLOT. Refers to the area of a particular plant unit, or complex. There can be more than one on-plot area in the same manufacturing site. See BATTERY LIMIT  
OFF-PLOT. Refers to area outside the on-plot area, or to area between on-plot areas. See BATTERY LIMIT  
ON-SITE-In the field. Operations carried out at the construction site are termed on-site operations  
OPERATOR for valve. 3.1.2  
OPERATING HEIGHTS FOR VALVES. 6.1.3. table 6.2. table P-2  
ORIFICE PLATE ASSEMBLY. 6.7.5. figure 6.36  
Clearance around. figure 6.38  
ORIFICE PIPE RUN. table 6.6  
ORIFICE TAP. See 'Piping to flange taps' 6.7.5  
ORTHOGONAL DRAWING. 5.2.6  
OUTSIDE SCREW. See 'Stem' 3.1.2  
OUTSIDE SCREW & YOKE-OS&Y. See 'Stem' 3.1.2

## P

P&ID=Piping and Instrumentation diagram. 5.2.4  
PACKING. Compressible material held in the stuffing box of a seal  
PACKLESS VALVE. See 'Seals' 3.1.2  
PANTOGRAPH. 4.4.8  
PAPER. 4.4.1  
Copying papers. 4.4.1  
PAPER STOCK VALVE. 3.1.11  
PARTS LIST. 5.6.1  
PENCIL. For drafting. 4.4.2  
PENSTOCK. A channel leading water to a turbine or waterwheel

pH. A measure of the acid or alkaline strength of solutions. Neutral solutions have a pH of 7. The pH falls below 7 with increasing acidity, and rises above 7 with increasing alkalinity  
PHOTOGRAPHIC AIDS. 4.4.13  
PICTORIAL VIEWS. 6.2.8  
PIECEMARK=mark number. See 'Numbering Isos. spool sheets, & spools' 5.2.9  
PINCH VALVE. 3.1.5  
PIPE  
Data. table P-1  
Definition. 2.1.1  
Diameters of. 2.1.3. table P-1  
Fittings. 2.2.4. tables D  
Hanger. 2.12  
How to specify. 5.6.3  
Joints for. 2.2  
Lengths of. 2.1.2  
Linings. 2.1.4  
Lugs welded onto. 2.12.3  
Materials. 2.1.4  
Steels. table 2.1  
Ordering. 5.6.3  
Piperack. 6.1.2. figure 6.3  
Pressure limits. 2.1.5  
Schedule number. 2.1.3  
Sizes. 2.1.2. table P-1  
Sleeve. 6.2.8  
Spacing. table A-1  
Spans. table S-1. charts S-2  
Support. 6.2.2.12  
Temperature limits. 2.1.5  
Threads. 2.5.6  
Wall thickness. 2.1.3  
Welding to. 2.12.3  
PIPE DOPE. Sealing compound used for making screwed pipe connection  
PIPE SUPPORT. 6.2.2.12  
Calculations. 6.2.4  
Design functions. 6.2.1  
Expansion. 6.2.5  
Loading. 6.2.2. table S-1. charts S-2  
Spring hanger and support. 6.2.5  
PIPE-TO-TUBE CONNECTOR. figure 2.41  
PIPERACK. 6.1.2. figure 6.3  
PIPEWAY. 6.1.2  
PIPING  
Butt-welded. 2.3. chart 2.1  
Screwed. 2.5. chart 2.3  
Socket-welded. 2.4. chart 2.2  
PIPING & INSTRUMENTATION DIAGRAM. 5.2.4  
PIPING DRAWINGS. 5.2.7. 5.2.8  
Background. 5.2.8  
Centerline. 5.3.2. chart 5.1  
Checking. 5.4.2  
Dimensioning. 5.3  
Identifying sections. See 'Elevations (sections) & details' 5.2.8. chart 5.8  
Instrument connections. chart 6.2. 5.2.8  
Issuing. 5.4.3  
Line number. See 'Flow lines on P&ID' 5.2.4. 5.2.8  
Points to check. 5.4.4  
Presentation. figure 5.5  
Title block. 5.2.8. figure 5.9  
PIPING FABRICATION DRAWING. 5.2.9  
PIPING GROUP. 4.1  
PIPING LAYOUT. Design notes. 6.1  
PIPING SPECIFICATION. 4.2.1  
PIPING USES. 1.1  
PLAN. View for drawing. 5.2.6. 5.2.8  
PLANIMETER. 4.4.8  
PLANT. Building of. 1.2. chart 1.1  
PLANT AIR. See 'Compressed-air usage' 6.3.2  
PLANT CONSTRUCTION. chart 1.1  
PLANT NORTH. See 'Horizontal reference' 5.3.1. figure 5.11  
PLASTIC PIPE. 2.1.4  
Supporting. 6.2.7  
PLENUM. Distribution component of a mechanical system of ventilation. Fresh air is forced into a box or chamber ('plenum') for distribution in a building  
PLOT PLAN. 5.2.7  
PLUG. Barstock. figure 2.55

PLUG GATE VALVE. 3.1.4  
PLUG VALVE. 3.1.4  
PLUMBING. 1.1  
POCKETING. In lines. 6.2.8  
POLYMERIZATION. Generally, chemical reaction in which molecules combine to give larger molecules. Term mostly applied to reactions giving giant molecules from small molecules, as in the production of plastics.  
'POP' SAFETY VALVE. 3.1.9  
POTABLE WATER=Drinking water  
PORT of valve. Refers to the seat aperture of a valve, but sometimes to the valve's ends  
PRESSURE, ABSOLUTE. Pressure expressed relative to absolute vacuum. British unit, pound per square inch absolute, abbreviated PSIA. Normal atmospheric pressure is taken as 14.7 PSIA  
PRESSURE, GAGE. Gage pressure is expressed as pressure in excess of normal atmospheric pressure. British unit, pound per square inch gage, abbreviated PSIG, normally taken as 14.7 PSI  
PRESSURE REGULATOR. 3.1.10  
PRESSURE SEAL. Valve. See 'Bonnet' 3.1.2  
PRESSURE VESSEL. 6.5.1  
PRIMARY VALVE. 3.1.11  
PRIME-Priming water, etc.  
PROCESS EQUIPMENT. Equipment by which (or in which) is effected a physical or chemical change in process material. 3.3  
PROCESS PIPING. 1.1  
PROCESS WATER. Water that is added to the process stream  
PROJECT GROUP. chart 4.1  
PROPERTY LINE. Boundary of the site  
PROPORTIONING PUMP. 3.3.2. table 3.7  
PROPORTIONING VALVE. 3.3.2. table 3.7  
PUMP. 3.2.1  
Piping. 6.3.1  
Selection. chart 3.3  
PUMP PIPING. 6.3.1  
PURGING. The flushing out of unwanted material from a system. Example, flowing piping with nitrogen to remove atmospheric oxygen  
PURLIN. A longitudinal member fixed externally to the roof frame of a building to which the roofing panels are fitted  
PYROMETER. A device used for measuring higher temperatures

## Q

QUICK-ACTING OPERATORS. For valves. 3.1.2  
QUICK CONNECTOR. 2.8.1  
QUICK COUPLING. 2.8.2

## R

RAILING  
Dimensioning. table 6.1. chart P-2  
Symbol. chart 5.8  
RAISED FACE (of flange). 2.6.1  
RANDOM LENGTH OF PIPE. 2.1.2  
RAPIDOGRAPH. Pen. 4.4.6  
RATINGS OF FITTINGS. table 2.2  
REACTION VESSEL. 3.3.1  
REACTOR. Apparatus in which reaction of process chemicals is carried out  
REBOILER. See 'Column operation' 6.6.2  
RECEIVER. 3.2.2  
REDUCER  
Butt-welding. 2.3.1. figure 2.3  
Screwed. 2.5.1. figure 2.38  
Socket-welding. 2.4.1. figure 2.22  
REDUCING ELBOW. 2.3.1. figure 2.2  
REDUCER INSERT. 2.4.1. figure 2.23  
REDUCING FLANGE. 2.3.1. figure 2.8  
REDUCING TEE. How to order. 2.3.2. table D-6  
REGULATING VALVE. 3.1.11  
REFERENCE DRAWING. Any drawing made by the design group for a company 'standard' drawing) to which reference is made. The complete list of reference drawing numbers is best written on the main arrangement drawing

REFERENCE POINT, 5.3.1, figure 5.11  
REFLUXING. See 'Column operation' 6.5.2  
REINFORCEMENT, 2.11

Symbols, chart 5.3

REINFORCING RING. Shaped metal ring for strengthening stub-ins, vessel nozzles, etc.

RELIEF HEADER, 6.12.1, figure 6.3 point (7)

RELIEF VALVE, 3.1.9, 6.1.3

RELIEVING PRESSURE. Of liquids, 6.12

REMOVABLE SPOOL, 2.7.1, figure 2.61

RESISTANCE TO FLOW. Of piping, 6.1.1

RETURN, 2.3.1, figure 2.2

REVAMP. Re-working or modifying an existing installation, 4.4.13

REVISION. Of drawings. See 'Issuing drawings' 5.4.3

RING JOINT, 2.6.1, figure 2.56

Spacing & Numbers, table R-1

RING MAIN, figures 6.22 & 6.50. See MAIN

RISER. A line which conveys fluid upward

ROLLED ELL/ROLLED TEE. See 'Plan view piping drawings' 5.2.8

ROOT GAP, 5.3.5, chart 2.1

ROOT PENETRATION. Depth to which a groove (butt) weld extends into the 'root joint' (either side of root gap)

ROOT VALVE, 3.1.11,

ROTAMETER, 6.7.5, figure 6.35

ROTARY BALL VALVE, 3.1.6

ROUNDHEAD PLUG, figure 2.55

RUNUNDER, table A-3

RUPTURE DISC, 3.1.9

## S

SADDLE. (1) Shaped metal piece used for reinforcement, 2.11, figure 2.71, chart 5.3

(2) Shaped metal piece attached to insulated pipe as a bearing surface for supporting, 2.12.2, 6.2.8, figure 2.72A&B

### SAFETY

Guidelines for flammable liquids, 6.14

Valve placement, 6.1.3, table 5.7, chart P-2

SAFETY-RELIEF VALVE, 3.1.9, 6.1.3

SAFETY VALVE, 3.1.9, 6.1.3

SAGGING OF PIPE, 6.2.6

SAMPLE POINT. It is often necessary to take a sample of material from a product line. Usually a small branch line with sampling valve is all that is required. However, if a high-pressure line has to be sampled it is best to run the sample line to a small drum or vessel which has a vent to atmosphere. To sample a high-pressure, high-temperature line, it is necessary to provide a suitable cooler, usually a vessel with cold water circulating around a coil which is to be connected to the sample pump

SAMPLING VALVE, 3.1.9, 3.1.11

SANITARY CONSTRUCTION. See HYGIENIC CONSTRUCTION

SATURATED STEAM, 6.9.1,

SCHEDULE NUMBER, 2.1.3

SCHEMATIC DIAGRAM, 5.2.2

SCREEN, 2.10.4

SCREWED PIPING, 2.5. Most-used term for assembly of components and pipe, employing threaded ends for attachment

SCRUBBER, 3.3.3, table 3.8

SEAL WELD. Term used for circumferential fillet weld, chart 2.3

SEALING WATER. Water used for sealing

SEAMLESS. Pipe formed by rolling and piercing a solid billet is termed 'seamless'

SEARCHING. Term usually refers to penetrating ability of a thin liquid

SECTION. See 'Elevations (sections) & details' 5.2.8, chart 5.8

SECTION LEADER, chart 4.2

SECURITY, 5.2.1

SEPIA, 4.4.1

SEPARATOR, 2.10.2, 6.10.3

SEPARATION, 3.3.3

SERVICE PIPING, 1.1

On P&ID, 5.2.4

SET PRESSURE. Pressure at which a pressure controller or valve is set to operate

SETTLEMENT STRAIN, 6.1.1, figure 6.1

SETTLING TANK. Tank in which process stream or effluent can be held to allow solids to separate, 3.3.3, table 3.8

SEWAGE. Wastes from plant operations, commercial buildings, etc., sometimes including ground or surface water

SEWERAGE. The collection and/or disposal of sewage

SHOE. Device welded to or clamped to a pipe which provides a bearing for support, 2.12.2, 6.2.8

SHUTOFF VALVE, 3.1.11

SIGHT GLASS. Window in a line or vessel

SITE. Area of plant construction

SITE PLAN, 5.2.7

SKELP. Metal in strip form that is fed into rolls to form pipe

SLIP-ON FLANGE, 2.3.1, figure 2.7

SLEEVE (for pipe). Usually a large-diameter pipe around which concrete is poured. Reinforces such openings as those in walls, floors, etc.

SLOPING LINES, 6.2.6, 6.10.4

SLURRY VALVE, 3.1.11

SNUBBER, 2.12.2

SOCKET-WELDED PIPING, 2.4

SOCKET-WELDING FLANGE, 2.4.1, figure 2.27

SOCKET. 2.4.3, figure 2.32

SOUR WATER. Water that has an acid content. Term may refer to an acidic effluent

SPARGER. A steam pipe with holes in it to disperse steam into water, etc. figure 6.45

SPATTER. The metal particles thrown off during arc or gas welding

### SPECIFICATION

Change of. See 'Process & service lines on piping drawings' 5.2.8, figure 5.15

Piping, 4.2.1

SPECTACLE PLATE, 2.7.1, figure 2.59, chart 5.6

SPIRAL SOCK VALVE, 3.1.11

### SPOOL

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STAINLESS STEELS are iron-based alloys incorporating 11.5 to 24% chromium, 6 to 15% nickel, up to 0.2% carbon, and small amounts (in certain alloys) of other elements

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STRAIN. Reaction, such as elongation or compression, to stress. See STRESS

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STRESS. Force applied to material. Common stresses on pipe are due to pressure of contained fluid, and loading (self- or applied) causing bending of pipe. Ratio of stress/strain is termed the 'modulus'

STRESS RELIEVE. Removal of internal strains in a metal part by heating and controlled cooling

STRESSES ON PIPING, 6.1.1

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STRONGBACK. Pipe spool connected externally to vessel, on which instruments are mounted, figure 6.34(c)

STRUT. Any of various structural-steel members (such as make up trusses) primarily intended to resist longitudinal compression

STUB. Short length of pipe sometimes with shaped end

STUB-IN, 2.3.2, figure 2.11

STUDBOLT, 2.6.3, tables F

STUFFING BOX. Recess in body or casing of a valve, pump, expansion joint, etc., containing packing material under pressure so as to form a seal about a sliding or rotating part

SUBHEADER. A header which is a branch from a larger header

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SWAGE-Swaged nipple

SWAGED NIPPLE

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THERMAL MOVEMENT. Changes in length (expansion or contraction) occurring in piping with variation of temperature

THERMAL STRESS, 6.1.1

THERMINOL, 6.9.2. See 'Jacketing' 6.8.2

THERMON. See 'Getting heat to the process line' 6.8.2

THERMOWELL. A pocket, either screwed into a line fitting (such as a coupling or thredolet) or welded into a pipe, to accommodate a thermocouple or thermometer bulb, 6.7.3

THREAD. For pipe and fittings, 2.5.5

THREDOLET, 2.5.3, figure 2.50

THROAT TAP. A tapped pressure connection made in the neck of a welding-neck flange as an alternative to using an orifice flange

THROTTLING. Close regulation of flow thru a valve in the just-open position

THROTTLING VALVE, 3.1.11

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On P&ID, 5.2.4

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TRIM. Critical internal surfaces of a valve body are sometimes made of special material such as stainless steel. These parts may include the disc and seat, stem, or other internal surfaces

TRIM PIPING, 6.3.1

TRUSS. Structural frame based on the geometric rigidity of the triangle, composed of compression and tension members termed struts and ties

TUBE, 2.1.1

TURBINE PIPING, 6.4

TURNKEY PLANT. A plant constructed and made ready for client's immediate operation

TUBE, 2.1.1

TURBINE PIPING, 6.4

TURNKEY PLANT. A plant constructed and made ready for client's immediate operation

TUBE, 2.1.1

TURBINE PIPING, 6

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- On P&ID. 5.2.4
- On tank. Symbol, chart 5.7
- Symbol, chart 5.7

### VESSEL CONNECTION. 6.5.1

### VESSEL DRAWING. 5.2.7, figure 5.14

### VESSEL PIPING. 6.5.1

### VICTAULIC COUPLING. A 'quick connect' method of joining pipe, fittings, valves, and equipment; manufactured by the Victaulic Company of America. 2.8.2, figure 2.62

## W

**WATERHAMMER.** A concussion due to: (1) Pressure waves traveling in piping and meeting with obstructions. A valve closing too rapidly will create a pressure wave. (2) Condensate hurled against obstructions by high-velocity steam. See 6.10.2, 6.10.6

**WELD GAP.** 5.3.5, charts 2.1 & 2.2

**WELDING-NECK FLANGE.** See 'Flanges' 2.3.1, figure 2.6

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**WELDING TO PIPE.** 2.12.3

**WELDLET.** 2.3.2, figure 2.13

**WET STEAM.** 6.9.1, chart 6.3

**WINTERIZING.** The provision of insulation, tracing, jacketing or other means to prevent freezing of equipment and process or other fluids exposed to low temperatures

Insulation. 6.8.1, tables 6.7 & 6.8

Jacketing. 6.8.2, figure 6.39, chart 5.7

Tracing. 6.8.2, figure 6.40, chart 5.7

**WIRE DRAWING.** Term describing the erosion of valve seats, usually due to the cutting action of foreign particles in high-velocity fluids occurring when flow is throttled

**WORK POINT.** An arbitrary reference from which dimensions are taken

## Y

**YARD PIPING.** Piping within the site and external to buildings.

**YOKE.** See 'Stem' 3.1.2

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## PART II

# THE 'PIPING' GUIDE'

## A COMPACT REFERENCE FOR THE DESIGN AND DRAFTING OF INDUSTRIAL PIPING SYSTEMS

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# ARRANGING LINES SPACING IN PIPEWAYS

## LINES WITHOUT FLANGES—DIMENSION 'L'

		NOMINAL PIPE SIZE (INCHES)																
		2	3	4	6	8	10	12	14	16	18	20	24					
NOMINAL PIPE SIZE (INCHES)	2	5	5	6	7	8	9	10	11	12	13	14	16					
	3	5	6	6	8	9	10	11	11	12	13	14	16					
	4	6	6	7	8	9	10	11	12	13	14	15	17					
	6	7	8	8	9	10	11	12	13	14	15	16	18					
	8	8	9	9	10	11	12	13	14	15	16	17	19					
	10	9	10	10	11	12	13	14	15	16	17	18	20					
	12	10	11	11	12	13	14	15	16	17	18	19	21					
	14	11	11	12	13	14	15	16	16	17	18	19	21					
	16	12	12	13	14	15	16	17	17	18	19	20	22					
	18	13	13	14	15	16	17	18	18	19	20	21	23					
NOMINAL PIPE SIZE (INCHES)	20	14	14	15	16	17	18	19	19	20	21	22	24					
	24	16	16	17	18	19	20	21	21	22	23	24	26					

"Piping Guide", PO Box 277, Cotati, CA 94926, USA

## LINES WITH FLANGES—DIMENSION 'L'

### 150 & 150 PSI, FLANGED

		NOMINAL PIPE SIZE (INCHES)																
		2	3	4	6	8	10	12	14	16	18	20	24					
NOMINAL PIPE SIZE (INCHES)	2	6	6	7	8	9	10	11	12	13	14	15	17					
	3	6	7	8	9	10	10	12	13	14	15	16	17					
	4	7	8	8	9	10	11	12	13	14	15	16	18					
	6	8	9	9	10	11	12	13	14	15	16	17	19					
	8	9	10	10	12	13	14	15	16	17	18	19	21					
	10	11	11	12	13	14	15	16	17	18	19	20	22					
	12	12	13	13	14	15	16	17	18	19	20	21	23					
	14	13	14	14	15	16	17	18	19	20	21	22	24					
	16	14	15	15	17	18	19	20	20	21	22	23	25					
	18	15	16	16	17	18	19	20	21	22	23	24	26					
NOMINAL PIPE SIZE (INCHES)	20	16	17	17	19	20	21	22	22	23	24	25	27					
	24	19	19	20	21	22	23	24	24	25	26	27	29					

### 300 & 300 PSI, FLANGED

		NOMINAL PIPE SIZE (INCHES)																
		2	3	4	6	8	10	12	14	16	18	20	24					
NOMINAL PIPE SIZE (INCHES)	2	6	6	7	8	9	10	11	12	13	14	15	17					
	3	6	7	8	9	10	10	12	13	14	15	16	18					
	4	7	8	8	9	10	11	12	13	14	15	16	19					
	6	8	9	9	10	11	12	13	14	15	16	17	20					
	8	9	10	10	12	13	14	15	16	17	18	19	21					
	10	11	11	12	13	14	15	16	17	18	19	20	22					
	12	12	13	13	14	15	16	17	18	19	20	21	23					
	14	13	14	14	15	16	17	18	19	20	21	22	24					
	16	14	15	15	17	18	19	20	20	21	22	23	25					
	18	15	16	16	17	18	19	20	21	22	23	24	26					
NOMINAL PIPE SIZE (INCHES)	20	16	17	17	19	20	21	22	22	23	24	25	27					
	24	19	19	20	21	22	23	24	24	25	26	27	29					

TABLES GIVE THE MINIMUM SPACING. INCREASE THESE DIMENSIONS:  
(1) FOR INSULATION  
(2) IF THERMAL MOVEMENT WOULD REDUCE CLEARANCE

## PIPE CENTER-TO-SURFACE DIMENSION 'S'

### CLEARANCE

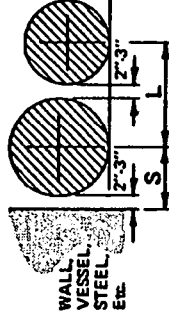
### 2 TO 3 IN. 1 TO 2 IN.

PIPE WITHOUT FLANGES	FLANGE RATING PSI	
	150	300

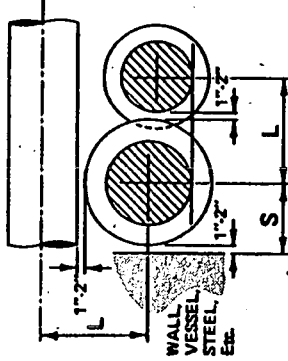
NOMINAL PIPE SIZE (INCHES)	2	4	4	5	5
	3	4	4	5	6
	4	5	6	6	7
	6	6	7	8	8
	8	7	8	9	10
	10	8	9	10	11
	12	9	11	12	12
	14	9	12	13	13
	16	10	13	14	15
	18	11	14	15	16
NOMINAL PIPE SIZE (INCHES)	20	12	15	17	17
	24	14	17	19	20

## TABLES A-1

### PIPE WITHOUT FLANGES



### PIPE WITH FLANGES



### INSULATION

FIGURES IN THE TABLES ARE SPACINGS FOR BARE PIPES. FOR INSULATED LINES, ADD THE THICKNESS OF INSULATION AND COVERING TO THESE FIGURES.

## 150 & 300 PSI, FLANGED

		NOMINAL PIPE SIZE (INCHES)															
300	150	2	3	4	6	8	10	12	14	16	18	20	24				
		2	3	4	6	8	9	10	11	12	13	14	15	16	17	19	21
		6	7	8	9	10	11	12	13	14	15	16	17	19	21		
		7	7	8	9	10	11	12	13	14	15	16	17	19	21		
		8	8	9	10	11	12	13	14	15	16	17	19	21	23		
		9	10	11	12	13	14	15	16	17	17	19	21	23			
		10	11	12	13	14	15	16	17	17	19	21	23				
		12	13	14	15	16	17	18	19	20	21	22	23	24	26		
		14	15	15	16	17	18	19	20	21	22	23	25				
		16	15	16	16	18	19	20	21	21	22	23	24	26			
		18	17	18	19	20	21	22	22	23	24	25	27				
		20	18	18	19	20	21	22	23	24	25	26	27	29			
		24	21	21	22	23	24	25	26	26	27	28	29	31			

## 300 & 600 PSI, FLANGED

		NOMINAL PIPE SIZE (INCHES)															
600	300	2	3	4	6	8	10	12	14	16	18	20	24				
		2	3	4	6	8	9	10	11	12	13	14	15	17	18	21	22
		6	7	8	9	10	11	12	13	14	15	16	17	18	21		
		7	7	8	9	11	12	13	15	16	17	18	21				
		8	9	9	10	11	12	14	15	16	18	19	22				
		10	10	11	12	13	14	15	16	18	19	20	23				
		8	11	12	13	14	15	16	17	19	20	21	24				
		10	13	14	15	16	17	18	18	20	21	22	25				
		12	14	15	16	17	18	19	19	21	22	23	26				
		14	15	16	17	18	19	20	20	21	22	24	26				
		16	16	17	17	18	19	20	21	22	23	24	25	27			
		18	17	18	18	19	20	21	22	23	24	25	26	28			
		20	19	19	20	21	22	23	24	24	25	26	27	29			
		24	21	22	22	23	24	25	26	27	28	29	30	32			

## 150 & 600 PSI, FLANGED

		NOMINAL PIPE SIZE (INCHES)															
600	150	2	3	4	6	8	10	12	14	16	18	20	24				
		2	3	4	6	8	9	10	11	12	13	14	15	16	17	19	21
		6	6	7	8	9	10	11	12	13	14	15	16	19			
		7	7	8	9	10	11	12	13	14	15	16	17	19			
		8	9	9	10	11	12	13	14	15	16	17	20				
		10	10	11	12	13	14	15	16	17	18	19	20	21	23		
		12	14	15	16	17	18	19	20	21	22	23	24				
		14	15	16	17	18	19	20	20	21	22	23	25				
		16	16	17	17	18	19	20	21	22	23	24	25	27			
		18	17	18	19	20	21	22	23	24	25	26	28				
		20	19	19	20	21	22	23	24	25	26	27	29				
		24	21	22	23	24	25	26	27	28	29	30	32				

## 600 & 600 PSI, FLANGED

		NOMINAL PIPE SIZE (INCHES)															
600	600	2	3	4	6	8	10	12	14	16	18	20	24				
		2	3	4	6	8	9	10	11	12	13	14	15	17	19	21	22
		6	7	7	8	9	9	10	10	11	12	13	14	17			
		8	10	11	12	13	14	15	16	17	18	19	20	20			
		10	11	11	12	13	14	15	16	17	18	19	20	21	22	23	
		12	14	14	15	16	17	18	19	20	21	22	23	24	25		
		14	15	15	16	17	18	19	20	21	22	23	24	25	26	27	
		16	16	17	17	18	19	20	21	22	23	24	25	26	27	28	29
		18	17	18	18	19	20	21	22	23	24	25	26	27	28	29	30
		20	19	19	20	21	22	23	24	24	25	26	27	29			
		24	21	22	22	23	24	25	26	27	28	29	30	32			

## PIPEWAY WIDTH

When the order of lines, line sizes, pressure ratings (for lines with flanges) and insulation thicknesses have been decided, determine pipeway width from tables A-1 thru A-3, adding 25% for the final design to include 20% of the distributed space for future piping.

To obtain a preliminary estimate of the pipeway width required for a selection of lines without flanges, in the size range 2- thru 8-inch NPS, either of the following factors may be used (the first is preferable):—

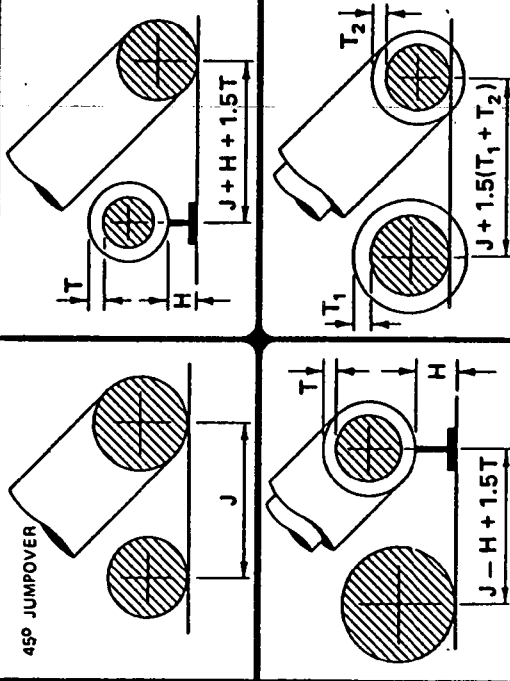
- (1) If all pipe sizes are known, add nominal sizes in inches together and multiply by 0.34 to estimate the width in feet.
- (2) If only the number of lines is known, multiply this number by 1.43 to estimate the width in feet.

Either factor gives a pipeway width which includes insulation for 25% of lines, allows 20% of the width for the addition and re-sizing of lines, and allocates a further 20% of the width for future piping.

# 45° JUMPOVERS

## TABLE A-2

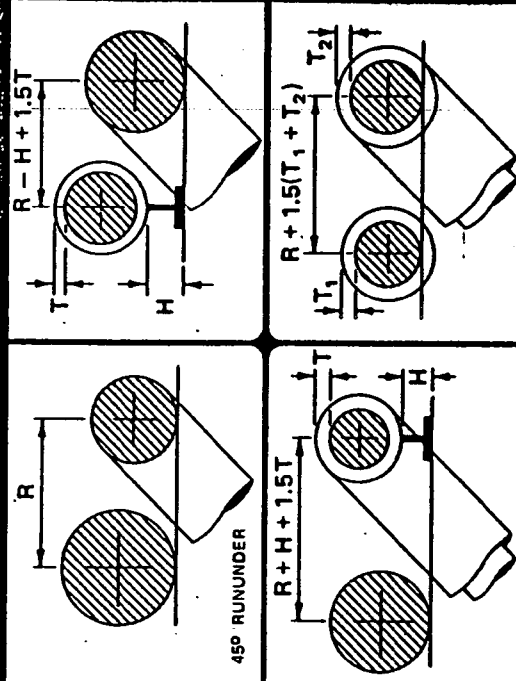
		BASIC SPACING 'J'											
		JUMPOVER (NPS in INCHES)											
ADJACENT LINE (NPS in INCHES)		2	3	4	6	8	10	12	14	16	18	20	24
		7	7	7	8	8	8	9	9	9	10	10	11
3	3	8	8	8	9	9	10	10	10	11	11	12	12
4	4	9	9	10	10	11	11	11	12	12	12	13	14
6	6	12	12	13	13	14	14	14	15	15	15	16	16
8	8	14	14	15	15	16	16	17	17	17	18	19	19
10	10	17	17	18	18	19	19	19	20	20	20	21	21
12	12	19	19	20	20	21	21	22	22	22	23	24	24
14	14	21	21	22	22	23	23	24	24	24	25	26	26
16	16	23	23	24	24	25	25	26	26	26	27	28	28
18	18	26	26	27	27	28	28	28	29	29	30	31	32
20	20	28	28	29	29	30	30	31	31	31	32	33	34
24	24	33	33	34	34	35	35	36	36	36	37	38	39



# 45° RUNUNDERS

## TABLE A-3

		BASIC SPACING 'R'											
		RUNUNDER (NPS in INCHES)											
ADJACENT LINE (NPS in INCHES)		2	3	4	6	8	10	12	14	16	18	20	24
		7	8	9	12	14	17	19	21	23	26	28	33
3	3	7	8	9	12	14	17	19	21	23	26	28	33
4	4	7	8	10	12	15	17	20	21	24	26	28	33
6	6	8	9	10	13	15	18	20	22	24	26	29	34
8	8	8	9	11	13	15	18	20	22	24	27	29	34
10	10	8	10	11	14	16	19	21	22	25	27	30	34
12	12	9	10	11	14	16	19	21	23	25	28	30	35
14	14	9	10	12	14	17	19	22	23	26	28	30	35
16	16	9	11	12	15	17	20	22	24	26	28	31	36
18	18	10	11	12	15	17	20	22	24	26	29	31	36
20	20	10	12	13	15	18	20	23	24	27	29	32	36
24	24	11	12	14	16	19	21	24	25	28	30	32	37



### NOTES FOR TABLES A-2 & A-3





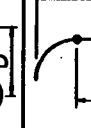
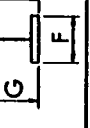

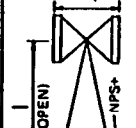

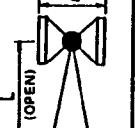

- (1) SPACINGS SHOWN IN THE DIAGRAMS ALLOW 2 TO 2.7 INCHES CLEARANCE
- (2) IN TABLES A-2 & A-3, 'H' IS THE EFFECTIVE SHOE HEIGHT, AND 'T' IS THE THICKNESS OF INSULATION (WITH COVERING)
- (3) FOR SIMPLICITY, THE FACTOR 1.5 HAS BEEN SUBSTITUTED IN ALL EXPRESSIONS FOR THE FACTOR  $2^{1/2}$  (=1.414...)



600 PSI BUTT-WELDED PIPING DIMENSIONS

TABLE D-1

DIMENSIONS IN THIS TABLE INCLUDE 1/4-INCH RAISED FACE ON FLANGES

NOMINAL PIPE SIZE (IN.)		2	3	4	6	8	10	12	14	16	18	20	24
STRAIGHT TEE		2 1/2	3 3/8	4 1/2	5 5/8	7	8 1/2	10	11	12	13 1/2	15	17
WELDOLET STANDARD WEIGHT DIMENSIONS ARE ROUNDED UP TO 1/16 INCH AND INCLUDE ROOT GAP		1 5/8	1 7/8	2 1/8	2 3/8	2 5/8	3 1/4	3 5/8	3 7/8	4 1/8	4 3/4	4 11/16	5 5/8
	FULL												
REDUCERS CONCENTRIC & ECCENTRIC		1 5/8	1 7/8	2 1/8	2 3/8	2 5/8	3 1/4	3 5/8	3 7/8	4 1/8	4 3/4	4 11/16	5 5/8
	RED.												
90° LR ELLS		3	4 1/2	6	9	12	15	18	21	24	27	30	36
90° SR ELL		2	3	4	6	8	10	12	14	16	18	20	24
45° ELL (LR)		1 3/8	2	2 1/2	3 3/4	5	6 1/2	7 1/2	8 3/4	10	11 1/4	12 1/2	15
OFFSET (TWO 45° ELLS)		1 5/8	2 1/8	3 3/8	5 5/8	7 1/8	8 13/16	10 1/8	12 3/8	14 1/8	15 5/8	17 11/16	21 1/8
	A												
90° OFFSET BEND (45° ELL + 90° LR ELL)		4 1/4	6 3/8	8 1/2	12 3/4	17	21 1/4	25 3/8	29 7/8	34 3/8	38 7/8	42 11/16	51 1/8
	B												
90° LR ELL + WELDING-NECK		6 1/8	8	10 1/4	13 3/8	17 1/2	21 1/2	24 3/4	27 3/4	31 1/2	34 1/2	37 3/4	44 1/4
	C												
RAISED-FACE FLANGE		6 1/2	8 1/4	10 3/4	14	16 1/2	20	22	23 3/4	27	29 1/4	32	37
	D												
PLUG REGULAR PATTERN: 2"-10" VENTURI TYPE: 8"-24"		3 1/8	3 1/2	4 1/4	4 7/8	5 1/2	6 1/4	6 3/8	7 1/4	7 3/4	8 1/4		
	E												
GATE DIMENSIONS ALSO APPLY TO GATE VALVES WITH BUTT-WELDING ENDS		11 1/2	14	17	22	26	31	33	35	39	43	47	55
	F												
BALL DIMENSIONS FOR FULL-PORT VALVES (OVER 6", CRANE VALVES)		9	12	16	22	24	28	30	36	38	42		
	G												
GLOBE DIMENSIONS ALSO APPLY TO GLOBE VALVES WITH BUTT-WELDING ENDS		20 5/8	25 3/4	33	46 1/2	53	65 1/8	73	80 13/16	92 1/8	98 1/2	106 3/8	126
	H												
CHECK TILTING: 2"-12" SWING: 2"-12" LIFT: 2"-12"		11 1/2	14	17	22	26	31	33	35	39	43	47	55
	I												
NOMINAL PIPE SIZE (IN.)		2	3	4	6	8	10	12	14	16	18	20	24

## NOTE

"H", "I", "K", AND "L" DIMENSIONS ARE THE LARGEST DIMENSIONS FOR MANUALLY-OPERATED CAST-STEEL VALVES FROM THE FOLLOWING MAKERS: CHAPMAN, CRANE, GRINNELL, HANCOCK, JENKINS, LUNKENHEIMER, PACIFIC, POWELL, STOCKHAM, VOGT, AND WALLWORTH/ALLOYCO

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# 300

## 300 PSI BUTT-WELDED PIPING DIMENSIONS

## TABLE D-2

NOMINAL PIPE SIZE (IN.)		2	3	4	6	8	10	12	14	16	18	20	24
STRAIGHT TEE		2½	3½	4½	5½	7	8½	10	11	12	13½	15	17
WELDOLET	REDUCING TEES DIMENSIONS OF ARE IN TABLE D-6												
	FULL NPS	1½	1¾	2½	2½	2½	3½	3½	3½	3¾	4½	4¾	5½
REDUCERS	CONCENTRIC	1½	1¾	2½	2½	2½	3½	3½	3½	3¾	4½	4¾	5½
	ECCENTRIC	1½	1¾	2½	2½	2½	3½	3½	3½	3¾	4½	4¾	5½
90° LR ELLS		3	4½	6	9	12	15	18	21	24	27	30	36
90° SR ELL		2	3	4	6	8	10	12	14	16	18	20	24
45° ELL (LR)		1½	2	2½	3½	5	6½	7½	8½	10	11½	12½	15
OFFSET (TWO 45° ELLS)	A	1½	2½	3½	5½	7½	8½	10½	12½	14½	15½	17½	21½
	B	4½	6½	8½	12½	17½	21½	25½	29½	34½	38½	42½	51½
90° OFFSET BEND (45° ELL + 90° LR ELL)	C	3½	4½	6	9	12	15	18½	21½	24½	27½	30½	36½
	D	4½	6½	8½	12½	17½	21½	25½	29½	34½	38½	42½	51½
90° LR ELL + WELDING-NECK	E	5½	7½	9½	12½	15	17½	20½	23	25½	28	30½	36
	F	6½	8½	10	12½	15	17½	20½	23	25½	28	30½	36
RAISED-FACE FLANGE	G	2½	3½	3½	3½	4½	4½	5½	5½	5½	6½	6½	6½
	H	8½	11½	12	15½	16½	18	19½	20½	23	25½	28	36
PLUG		8	10	12	16	20	24	24	28	32	36	39	45
GATE	I	20½	24½	28½	38½	48½	58½	66½	75½	81	91½	101½	122½
	J	8½	11½	12	15½	16½	18	19½	20½	23	25½	28	36
BALL	K	8½	11½	12	15½	16½	18	19½	20½	23	25½	28	36
	L	10	12	14	22	24	26	30	30	33	36	44½	45
GLOBE	M	19½	24	26½	31½	40½	48½	48½	48½	48½	48½	48½	48½
	N	10½	12½	14	17½	22	24½	28	28	28	28	28	28
CHECK		10½	12½	14	17½	21	24½	28	28	28	28	28	28
NOMINAL PIPE SIZE (IN.)		2	3	4	6	8	10	12	14	16	18	20	24

### NOTE

"H", "I", "K" AND "L" DIMENSIONS ARE THE LARGEST DIMENSIONS FOR MANUALLY-OPERATED CAST-STEEL VALVES FROM THE FOLLOWING MAKERS: CHAPMAN, CRANE, GRINNELL, HANCOCK, JENKINS, LUNKENHEIMER, PACIFIC, POWELL, STOCKHAM, VOGT, AND WALLWORTH/ALLOYCO

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



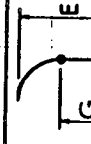
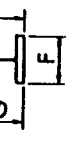
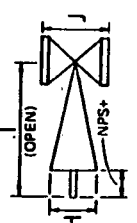

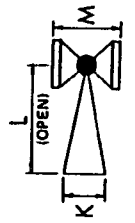

# 150

## 150 PSI BUTT-WELDED PIPING DIMENSIONS

TABLE D-3

DIMENSIONS IN THIS TABLE INCLUDE 1/16-INCH RAISED FACE ON FLANGES

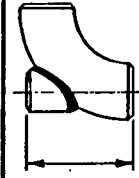
### NOMINAL PIPE SIZE (IN.)

	2	3	4	6	8	10	12	14	16	18	20	24
<b>STRAIGHT TEE</b> 	2½	3½	4½	5½	7	8½	10	11	12	13½	15	17
<b>WELDOLET</b> STANDARD WEIGHT DIMENSIONS ARE SHOWN UP TO 1/16 INCH, AND INCLUDE ROOT GAP	1½	1½	2½	2½	2½	3½	3½	3½	3½	4½	4½	5½
<b>REDUCERS</b> CONCENTRIC & ECCENTRIC	1½	1½	2½	2½	2½	3½	3½	3½	3½	4½	4½	5½
<b>90° LR ELLS</b> REGULAR & REDUCING	3	4½	6	9	12	15	18	21	24	27	30	36
<b>90° SR ELL</b> 	2	3	4	6	8	10	12	14	16	18	20	24
<b>45° ELL (LR)</b> 	1½	2	2½	3½	5	6½	7½	8½	10	11½	12½	15
<b>OFFSET</b> (TWO 45° ELLS) 	1½	2½	3½	5½	7½	10½	13½	16½	19½	22½	25½	30½
<b>90° OFFSET BEND</b> (45° ELL + 90° LR ELL) 	4½	6½	8½	12½	17½	21½	25½	29½	34½	38½	42½	51½
<b>90° LR ELL</b> + WELDING-NECK 	5½	7½	9	12½	16	19	22½	26	29	32½	35½	42
<b>RAISED-FACE FLANGE</b> 	6	7½	9	11	13½	16	19	21	23½	25	27½	32
<b>PLUG</b> SHORT PATTERN: 2"-12" VENTURI TYPE: 16"-24"	2½	2½	3	3½	4	4	4½	5	5	5½	5½	6
<b>GATE</b> 	7	8	9	10½	11½	13	14	14	14	14	14	14
<b>BALL</b> DIMENSIONS FOR FULL-PORT VALVES (OVER 12", CRANE VALVES) 	18½	22½	27½	36½	46½	52½	60½	70½	79½	89	97½	112½
<b>GLOBE</b> DIMENSIONS ALSO APPLY TO GLOBE VALVES WITH BUTT-WELDING ENDS 	7	8	9	10½	11½	13	14	15	16	17	18	20
<b>CHECK</b> TILTING: 2"-12" SWING: 2"-4", 8"-16" LIFT: 	8	9½	11½	14	19½	24½	27½	31	36			
<b>NOMINAL PIPE SIZE (IN.)</b>	2	3	4	6	8	10	12	14	16	18	20	24

### NOTE

"H", "I", "K", AND "L" DIMENSIONS ARE THE LARGEST DIMENSIONS FOR MANUALLY-OPERATED CAST-STEEL VALVES FROM THE FOLLOWING MAKERS: CHAPMAN, CRANE, GRINNELL, HANCOCK, JENKINS, LUNKENHEIMER, PACIFIC, POWELL, STOCKHAM, VOGT, AND WALLWORTH/ALLOYCO

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## ELBOLET DIMENSIONS

TABLE D-4

NOMINAL PIPE SIZE OF MAIN RUN (INCHES)														
NOMINAL PIPE SIZE OF BRANCH (INCHES)	1/2	3/4	1	1 1/4	1 1/2	2	3	4	6	8	10	12	14	16
	2	3	4	6	8	10	12	14	16	18	20	24		
1/2	3.57	5.98	7.29	10.04	12.70	15.42	18.07	20.17	22.79	25.45	28.11	33.39		
3/4	4.86	6.26	7.57	10.32	12.98	15.70	18.36	20.45	23.07	25.73	28.39	33.67		
1	5.17	6.57	7.89	10.64	13.29	16.01	18.67	20.76	23.39	26.04	28.70	33.98		
1 1/4	5.36	6.76	8.07	10.82	13.48	16.20	18.86	20.95	23.57	26.23	28.89	34.17		
1 1/2	5.61	7.01	8.32	11.07	13.86	16.45	19.11	21.20	23.82	26.48	29.14	34.42		
2	6.17	7.57	8.89	11.64	14.29	17.01	19.67	21.76	24.39	27.04	30.01	34.98		
3		8.24	9.56	12.31	14.96	17.68	20.34	22.43	25.06	27.71	30.37	35.65		
4			10.24	12.99	15.65	18.37	21.03	23.12	25.74	28.40	31.06	36.34		
6				14.70	17.36	20.08	22.73	24.83	27.45	30.11	32.77	38.05		
8						18.36	21.08	23.73	25.83	28.45	31.11	33.77	39.05	
10							22.89	25.55	27.64	30.27	32.92	35.58	40.86	
12								26.55	28.64	31.27	33.92	37.05	41.86	

DATA PROVIDED BY THE BONNEY FORGE DIVISION OF  
GULF & WESTERN INDUSTRIAL PRODUCTS COMPANY

NOMINAL PIPE SIZE  
OF BRANCH (INCHES)

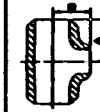
## SWAGES \*

SEAMLESS SWAGED NIPPLES—ALL WEIGHTS

TABLE D-5

NOMINAL PIPE SIZE (INCHES)	LARGER END		SMALLER END											
	2	2 1/2	3	4	6	7	8	10	12	14	16	18	20	24
END-TO-END LENGTHS (INCHES)	6 1/2		7		8 1/2		9		12		14		18	
	7		8		9 1/2		10		12 1/2		14 1/2		18 1/2	

\*Dimensions in this table are for Mills Iron Works Inc. swages, which are available with ends threaded, beveled, cut square, V-necked, and any combination of these terminations.



## REDUCING BUTT-WELDING TEES

TABLE D-6

NOMINAL PIPE SIZE OF RUN (IN.)														
DIMENSION 'A'	3	4	6	8	10	12	14	16	18	20	24			
	3.38	4.13	5.63	7.00	8.50	10.00	11.00	12.00	13.50	15.00	17.00			
DIMENSION 'B'	3.00	3.50	4.63											
	3.88	4.68	6.00	7.00										
	5.13	6.13	7.25	8.25										
		6.63	7.63	8.63	9.38	10.38								
			8.00	9.00	9.75	10.75	11.75	12.75						
				9.50	10.13	11.13	12.13	13.13	15.13					
					10.63	11.63	12.63	13.63	15.63					
						12.00	13.00	14.00	16.00					
							23.00	24.00	26.00					
								14.50	16.50					
20											17.00			

## BONNEY FORGE FITTINGS

TABLE D-7

TYPE OF BRANCH	TYPE OF CONNECTION	WEIGHT DESIGNATION	BRANCH SIZE NOMINAL PIPE SIZE (INCHES)	HEADER SIZE NOMINAL PIPE SIZE (INCHES)
WELDOLET, Reducing	Butt-welding	STD	1/8-30	3/8-36
		SCH 160, XKS	1/8-26	3/8-36
WELDOLET, Full-size	Butt-welding	STD	1/2-30	1/2-30
		SCH 160, XKS	1/2-26	1/2-30
SOCKOLET, Reducing	Socket-welding	STD	1/8-10	3/8-36
		SCH 160, XKS	1/8-2	3/8-36
SOCKOLET, Full-size	Socket-welding	STD	1/2-10	1/2-10
		SCH 160, XKS	1/2-2	1/2-10
THREDOLET, Reducing	Threaded	STD	1/8-10	3/8-36
		SCH 160, XKS	1/8-2	3/8-36
THREDOLET, Full-size	Threaded	STD	1/2-10	1/2-10
		SCH 160, XKS	1/2-2	1/2-10
ELBOLET	Butt-welding	STD	1/8-10	3/8-36
		SCH 160, XKS	1/8-2	3/8-36
SOCKOLET, 45 degree	Socket-welding	STD	1/8-10	3/8-36
		SCH 160, XKS	1/8-2	3/8-36
NIPDOLET	Threaded, or flange	STD	1/2-10	1/2-10
		SCH 160, XKS	1/2-2	1/2-10

# SOCKET-WELDED STEEL PIPING

TABLE D-8

PRESSURE RATING (PSI)		3000				6000			
NOMINAL PIPE SIZE (IN.)		1/2	3/4	1	1 1/2	1/2	3/4	1	1 1/2
45° ELL	A	0.88	1.00	1.13	1.38	1.00	1.13	1.31	1.69
	B	1.31	1.50	1.81	2.44	1.50	1.81	2.19	3.00
90° ELL	A	1.13	1.31	1.50	2.00	1.31	1.50	1.75	2.38
	B	1.31	1.50	1.81	2.44	1.50	1.81	2.19	3.00
TEE STRAIGHT TEE & REDUCING TEE		(Also, center-to-end dimensions for CROSS)							
LATERAL	A	1.13	1.31	1.50	2.00	1.31	1.50	1.75	2.38
	B	1.31	1.50	1.81	2.44	1.50	1.81	2.19	3.00
UNION	A	3.00	3.56	4.13	5.38	3.56	4.13	4.81	6.44
	B	1.50	1.75	2.00	2.69	1.75	2.00	2.38	3.56
	C	2.13	2.56	3.00	3.94	2.56	3.00	3.50	4.75
COUPLING	A	2.25	2.44	2.69	3.13	2.88	3.38	3.63	4.19
	B	1.81	2.19	2.56	3.44	2.19	2.56	3.06	4.13
SWAGE MILLS IRON WORKS 2"-24" SIZES; REFER NPS TO TABLE D-5	A	1.38	1.50	1.75	2.00	1.38	1.50	1.75	2.00
	B	1.25	1.50	1.81	2.50	1.50	1.75	2.25	3.00
REDUCER	A	2.75	3.00	3.50	4.50	2.75	3.00	3.50	4.50
	B	1.38	1.50	1.75	2.00	1.38	1.50	1.75	2.00
REDUCER INSERT	B	1.25	1.50	1.81	2.50	1.50	1.75	2.25	3.00
	1/2	--	1.50	1.31	1.44	--	1.88	2.13	2.00
	3/4	--	--	1.63	1.44	--	--	2.25	2.00
REDUCER INSERT	1	--	--	--	1.44	--	--	--	2.63

## 800 PSI VALVES

NOMINAL PIPE SIZE (IN.)		1/2	3/4	1	1 1/2	PIPE INSERTION LENGTH			
NOMINAL PIPE SIZE (IN.)		1/2	3/4	1	1 1/2	STANDARD GAP = 3/16 INCH			
GATE	L	3.50	3.88	4.25	5.50	NOMINAL PIPE SIZE (IN.)	1/2	3/4	1
	H	6.31	7.69	8.75	11.44		1/2	1	1 1/2
GLOBE	W	3.50	3.50	4.75	5.75	BONNEY-FORGE FITTINGS	3000	0.44	0.50
	L	3.25	3.50	5.00	7.00		6000	0.50	0.63
CHECK	H	6.19	6.38	7.81	10.00	SMITH VALVES	CONVENTIONAL PORT	0.63	0.56
	W	3.50	3.50	4.00	4.75		FULL PORT	0.75	0.81
CHECK	L	3.25	3.50	5.00	7.00	GLOBE, CHECK		0.44	0.56
	L	3.25	3.50	5.00	7.00	GLOBE, CHECK		0.44	0.56

## NOTES

DIMENSIONS IN THIS TABLE ARE ROUNDED UP TO THE NEAREST 1/16 INCH. UNLESS THE MAKER IS STATED, DIMENSIONS FOR FITTINGS ARE BASED ON THE LARGEST QUOTED BY: ANSI B16.11, BONNEY FORGE, GRINNELL, LADISH, AND VOGT. DIMENSIONS FOR SOCKET-WELDING UNIONS ARE BASED ON THE LARGEST QUOTED BY: CATAWISSA, CLAYTON MARK, GRINNELL, LADISH, AND VOGT. SOCKET DEPTH VARIES WITH SIZE, TYPE OF FITTING, AND MAKER.

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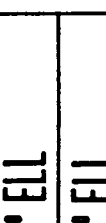





## FRACTIONAL EQUIVALENTS

0.06	0.13	0.19	0.25	0.31	0.38	0.44	0.50	0.56	0.63	0.69	0.75	0.81	0.88	0.94
1/16	1/8	3/16	1/4	5/16	3/8	7/16	1/2	9/16	5/8	11/16	3/4	13/16	7/8	15/16

# MALLEABLE-IRON FITTINGS

## TABLE D-9

(DIMENSIONS FOR BANDED FITTINGS)

PRESSURE RATING (PSI)		150 (STANDARD)							300							(EXTRA HEAVY)
NOMINAL PIPE SIZE (IN.)		1/2	3/4	1	1 1/2	2	3	1/2	3/4	1	1 1/2	2	3			
45° ELL		0.88	1.00	1.13	1.44	1.69	2.19	1.00	1.13	1.31	1.69	2.00	2.50			
90° ELL		1.13	1.31	1.50	1.94	2.25	3.13	1.25	1.44	1.63	2.13	2.50	3.38			
90° STREET ELL	A	1.13	1.31	1.50	1.94	2.25	3.13	1.25	1.44	1.63	2.13	2.50	3.38			
	B	1.63	1.88	2.19	2.69	3.31	4.56	2.00	2.19	2.56	3.13	3.69	5.13			
RETURN BEND	CLOSE	1.00	1.25	1.50	2.19	2.63				1.75	3.00	4.00				
	MEDIUM	1.25	1.50	1.88	2.50	3.00				2.50	3.50	6.00				
	OPEN	1.50	2.00	2.50	3.50	4.00	5.00			3.00	6.00	8.00				
STRAIGHT TEE		1.13	1.31	1.50	1.94	2.25	3.13	1.25	1.44	1.63	2.13	2.50	3.38			
LATERAL	A	2.38	2.81	3.31	4.38	5.19	7.31	2.75	3.25	4.25	5.81	5.75				
	C	1.75	2.06	2.44	3.31	3.94	5.63	2.00	2.38	3.25	4.56	4.50				
ALL-MALLEABLE-IRON, GROUND-JOINT UNIONS	A	1.81	2.00	2.19	2.63	3.06	3.88	2.13	2.31	2.56	3.06	3.44	4.31			
	B	1.63	1.88	2.06	3.00	2.44	4.94	1.81	2.25	2.56	3.38	4.06	5.69			
COUPLING		1.38	1.56	1.69	2.19	2.56	3.19	1.88	2.13	2.38	2.88	3.63	4.13			
NIPPLE	CLOSE NIPPLE	1.13	1.38	1.50	1.75	2.00	2.63	1.13	1.38	1.50	1.75	2.00	2.63			
CARBON-STEEL		AVAILABLE IN 2, 2 1/2, 3, 3 1/2, 4, 4 1/2, 5, 5 1/2, 6, 7, 8, 9, 10, 11, & 12-INCH LENGTHS (1/2- and 3/4-inch nipples are also available 1 1/2 inches long)														
SWAGE MILLS IRON WORKS CARBON-STEEL	REGULAR	2.75	3.00	3.50	4.50	6.50	8.00	2.75	3.00	3.50	4.50	6.50	8.00			
	VENTURI					7.00	8.25					7.00	8.25			
REDUCER		1.25	1.44	1.69	2.31	2.81	3.81	1.69	1.75	2.00	2.69	3.19	4.06			
THREAD ENGAGEMENT		0.50	0.56	0.69	0.69	0.75	1.00	0.50	0.56	0.69	0.69	0.75	1.00			

### NOTES

DIMENSIONS IN THIS TABLE ARE ROUNDED UP TO THE NEAREST 1/16th INCH. UNLESS THE MAKER IS STATED, DIMENSIONS FOR BANDED MALLEABLE-IRON FITTINGS ARE BASED ON THE LARGEST QUOTED BY: ANSI B16.3, CRANE, FLAGG, GRINNELL, AND STOCKHAM. DIMENSIONS FOR ALL-MALLEABLE-IRON GROUND-JOINT UNIONS ARE BASED ON THE LARGEST QUOTED BY: DART, FLAGG, AND STOCKHAM.

### FRACTIONAL EQUIVALENTS

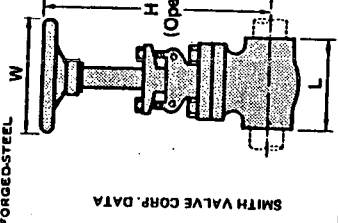
0.06	1/16	1/8	3/16	1/4	5/16	3/8	7/16	1/2	9/16	5/8	11/16	3/4	13/16	7/8	15/16

SCREWED STEEL PIPING

TABLE D-10

PRESSURE RATING (PSI)		2000				3000				6000			
NOMINAL PIPE SIZE (IN.)		1/2	3/4	1	1 1/2	1/2	3/4	1	1 1/2	1/2	3/4	1	1 1/2
45° ELL	A	0.88	1.00	1.13	1.38	1.00	1.13	1.31	1.69	1.13	1.31	1.38	1.75
	B	1.31	1.50	1.81	2.44	1.50	1.81	2.19	3.00	1.81	2.19	2.44	3.31
90° ELL	A	1.13	1.31	1.50	2.00	1.31	1.50	1.75	2.38	1.50	1.75	2.00	2.50
	B	1.31	1.50	1.81	2.44	1.50	1.81	2.19	3.00	1.81	2.19	2.44	3.31
TEE STRAIGHT TEE & REDUCING TEE	A	1.13	1.31	1.50	2.00	1.31	1.50	1.75	2.38	1.50	1.75	2.00	2.50
	B	1.31	1.50	1.81	2.44	1.50	1.81	2.19	3.00	1.81	2.19	2.44	3.31
LATERAL	A	3.56	4.13	4.81	6.44	3.56	4.13	4.81	6.44	4.13	4.81	5.38	6.00
	B	1.50	1.81	2.19	3.00	1.50	1.81	2.19	3.00	1.81	2.19	2.44	3.56
UNION	C	2.56	3.00	3.50	4.75	2.56	3.00	3.50	4.75	3.00	3.50	3.94	4.38
	A												
HALF-COUPLING	A												
	B	0.94	1.00	1.19	1.56	0.94	1.00	1.19	1.56	0.94	1.00	1.19	1.56
FULL-COUPLING	A	1.13	1.38	1.75	2.50	1.13	1.38	1.75	2.50	1.50	1.75	2.25	3.00
	B	1.88	2.00	2.38	3.13	1.88	2.00	2.38	3.13	1.88	2.00	2.38	3.13
NIPPLE	A	1.13	1.38	1.75	2.50	1.13	1.38	1.75	2.50	1.50	1.75	2.25	3.00
	B	1.13	1.38	1.50	1.75	1.13	1.38	1.50	1.75	1.13	1.38	1.50	1.75
CLOSE NIPPLE													
AVAILABILITIES OF SHORT AND LONG NIPPLES													
SWAGE	A												
	B	2.75	3.00	3.50	4.50	2.75	3.00	3.50	4.50	2.75	3.00	3.50	4.50
REDUCER	A	1.88	2.00	2.38	3.13	1.88	2.00	2.38	3.13	1.88	2.00	2.38	3.13
	B	1.13	1.38	1.75	2.50	1.13	1.38	1.75	2.50	1.50	1.75	2.25	3.00
HEXAGON BUSHING	A												
	B												
THREAD ENGAGEMENT	A												
	B												
TAPER TAPER	A												
	B												
FORGED-STEEL	A												
	B												
SMITH VALVE CORP. DATA	A												
	B												
W	A												
	B												
H	A												
	B												
L	A												
	B												
CHECK	A												
	B												

800 PSI VALVES



NOMINAL PIPE SIZE (IN.)		1/2	3/4	1	1 1/2
GATE	L	3.50	3.88	4.25	5.50
	H	6.31	7.69	8.75	11.44
GLOBE	W	3.50	3.50	4.75	5.75
	L	3.25	3.50	5.00	7.00
CHECK	H	6.19	6.38	7.81	10.00
	W	3.50	3.50	4.00	4.75
CHECK	L	3.25	3.50	5.00	7.00

NOTES

DIMENSIONS IN THIS TABLE ARE ROUNDED UP TO THE NEAREST 1/16th INCH. UNLESS THE MAKER IS STATED, DIMENSIONS FOR FITTINGS ARE BASED ON THE LARGEST QUOTED BY: ANSI B16.11, BONNEY FORGE GRINNELL, LADISH, AND VOGT. TABLED DIMENSIONS FOR SCREWED FORGED-STEEL UNIONS ARE BASED ON THE LARGEST QUOTED BY: CATAWISSA, CLAYTON MARK, GRINNELL, KEMPER & VOGT.

FITTINGS

# FLANGE DATA: 150-2500 PSI

FROM ANSI B16.5-1968 & MANUFACTURERS' DATA

TABLES F

REFER TO NOTES  
FOLLOWING TABLE F-9

BUTT-WELDING FLANGES \_\_\_\_\_ TABLES F-1-F-6  
LAP-JOINT STUB ENDS \_\_\_\_\_ TABLE F-7  
SMALL SOCKET-WELDING FLANGES \_\_\_\_\_ TABLE F-8  
SMALL SCREWED FLANGES \_\_\_\_\_ TABLE F-9

150 PSI FLANGE DATA

TABLE F-1

NOMINAL PIPE SIZE (INCHES)		2	3	4	6	8	10	12	14	16	18	20	24
FLANGE	OUTSIDE DIAMETER	6	7.5	9	11	13.5	16	19	21	23.5	25	27.5	32
	LENGTH THRU HUB Including 1/16" RF	2.5	2.75	3	3.5	4	4	4.5	5	5	5.5	5.69	6
	LONG WELDING-NECK	9	9	12	12	12	12	12	12	12	12	12	12
DIAMETER OF BORE - see Note (3)		Order to match pipe (otherwise ID matches STD pipe)											
BOLTING	BOLT HOLES PER FLANGE	4	4	8	8	8	12	12	12	16	16	20	20
	DIAMETER OF BOLT	0.63	0.63	0.63	0.75	0.75	0.88	0.88	1.00	1.00	1.13	1.13	1.25
	STUDBOLT THREAD LENGTH (Except lap-joint)	3	3.5	3.5	3.75	4	4.5	4.5	5	5.25	5.75	6	6.75
	RING JOINT	3.5	4	4	4.25	4.5	5	5	5.5	5.75	6.25	6.5	7.25

300 PSI FLANGE DATA

TABLE F-2

NOMINAL PIPE SIZE (INCHES)		2	3	4	6	8	10	12	14	16	18	20	24
FLANGE	OUTSIDE DIAMETER	6.5	8.25	10	12.5	15	17.5	20.5	23	25.5	28	30.5	36
	LENGTH THRU HUB Including 1/16" RF	2.75	3.13	3.38	3.88	4.38	4.63	5.13	5.63	5.75	6.25	6.38	6.63
	LONG WELDING-NECK	9	9	12	12	12	12	12	12	12	12	12	12
DIAMETER OF BORE - see Note (3)		Order to match pipe (otherwise ID matches STD pipe)											
BOLTING	BOLT HOLES PER FLANGE	8	8	8	12	12	16	16	20	20	24	24	24
	DIAMETER OF BOLT	0.63	0.75	0.75	0.75	0.88	1.00	1.13	1.13	1.25	1.25	1.25	1.50
	STUDBOLT THREAD LENGTH (Except lap-joint)	3.25	4	4.25	4.75	5.25	6	6.5	6.75	7.25	7.5	8	9
	RING JOINT	4	4.75	5	5.5	6	6.75	7.25	7.5	8	8.25	8.75	10

600 PSI FLANGE DATA

TABLE F-3

NOMINAL PIPE SIZE (INCHES)		2	3	4	6	8	10	12	14	16	18	20	24
FLANGE	OUTSIDE DIAMETER	6.5	8.25	10.75	14	16.5	20	22	23.75	27	29.25	32	37
	LENGTH THRU HUB Including 1/4" RF	3.13	3.5	4.25	4.88	5.5	6.25	6.38	6.75	7.25	7.5	7.75	8.25
	LONG WELDING-NECK	9	9	12	12	12	12	12	12	12	12	12	12
DIAMETER OF BORE - see Note (3)		Order to match pipe ID											
BOLTING	BOLT HOLES PER FLANGE	8	8	8	12	12	16	20	20	20	20	24	24
	DIAMETER OF BOLT	0.63	0.75	0.88	1.00	1.13	1.25	1.25	1.38	1.5	1.63	1.63	1.88
	STUDBOLT THREAD LENGTH (Except lap-joint)	4	4.75	5.5	6.5	7.5	8.25	8.5	9	9.75	10.5	11.25	12.75
	RING JOINT	4.25	5	5.75	6.75	7.75	8.5	8.75	9.25	10	10.75	11.5	13.25

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# FLANGE DATA: 150-2500 PSI

## TABLES F

900 PSI FLANGE DATA

NOMINAL PIPE SIZE (INCHES)		TABLE F-4														
FLANGE	OUTSIDE DIAMETER	2	3	4	6	8	10	12	14	16	18	20	24			
	LENGTH THRU HUB Including 1/4" RF	8.5	9.5	11.5	15	18.5	21.5	24	25.25	27.75	31	33.75	41			
		WELDING-NECK	4.25	4.25	4.75	5.75	6.63	7.5	8.13	8.63	8.75	9.25	10	11.75		
		LONG WELDING-NECK	9	12	12	12	12	12	12	12	12	12	12	12		
BOLTING	DIAMETER OF BORE — see Note (3)	Order to match pipe ID														
	BOLT HOLES PER FLANGE	8	8	8	12	12	12	16	20	20	20	20	20			
	DIAMETER OF BOLT	0.88	0.88	1.13	1.13	1.38	1.38	1.38	1.38	1.5	1.63	1.88	2			
	STUDBOLT THREAD LENGTH (Except lap-joint)	5.5	5.5	6.5	7.5	8.5	9	9.75	10.5	11	12.75	13.5	17			
		RAISED FACE	5.75	5.75	6.75	7.5	8.75	9.25	10	11	11.5	13.25	14	17.75		
		RING JOINT														

1500 PSI FLANGE DATA

NOMINAL PIPE SIZE (INCHES)		TABLE F-5														
FLANGE	OUTSIDE DIAMETER	2	3	4	6	8	10	12	14	16	18	20	24			
	LENGTH THRU HUB	8.5	10.5	12.25	15.5	19	23	26.5	29.5	32.5	36	38.75	46			
	Including 1/4" RF	4.25	4.88	5.13	7	8.63	10.25	11.38	12	12.5	13.13	14.25	16.25			
	WELDING-NECK	9	12	12	12	12	12	12	12	12	12	12	12	12		
BOLTING	LONG WELDING-NECK	9	12	12	12	12	12	12	12	12	12	12	12	12		
	DIAMETER OF BORE	Order to match pipe ID														
	— see Note (3)															
	BOLT HOLES PER FLANGE	8	8	8	12	12	12	12	16	16	16	16	16	16		
	DIAMETER OF BOLT	0.88	1.13	1.25	1.38	1.63	1.88	2	2.25	2.5	2.75	3	3.5			
	STUDBOLT THREAD LENGTH (Except lap-joint)	5.5	6.75	7.5	10	11.25	13.25	14.75	16	17.5	19.25	21	24	24		
	RAISED FACE	5.75	7	7.75	10.25	11.75	13.5	15.25	16.75	18.5	20.25	22.25	25.5			
	RING JOINT															

2500 PSI FLANGE DATA

NOMINAL PIPE SIZE (INCHES)		TABLE F-6														
FLANGE	OUTSIDE DIAMETER	2	3	4	6	8	10	12								
	LENGTH THRU HUB Including 1/4" RF	9.25	12	14	19	21.75	26.5	30								
	WELDING-NECK	5.25	6.88	7.75	11	12.75	16.75	18.5								
	LONG WELDING-NECK	9	12	12	12	12	12	12								
	DIAMETER OF BORE — see Note (3)	Order to match pipe ID														
BOLTING	BOLT HOLES PER FLANGE	8	8	8	8	12	12	12	12							
	DIAMETER OF BOLT	1	1.25	1.5	2	2	2.5	2.75								
	STUDBOLT THREAD LENGTH (Except lap-joint)	6.75	8.5	9.75	13.5	15	19	21								
	RAISED FACE	7	8.75	10.25	14	15.5	20	22								
	RING JOINT															

WHEN USING TABLES F  
FOR SLIP-ON AND  
SOCKET-WELDING  
FLANGES, REFER TO  
NOTES (4) and (5)

FRACTIONAL  
EQUIVALENTS

0.06	0.13	0.19	0.25	0.31	0.38	0.44	0.50	0.56	0.63	0.69	0.75	0.81	0.88	0.94		
1/16	1/8	3/16	1/4	5/16	3/8	7/16	1/2	9/16	5/8	11/16	3/4	13/16	7/8	15/16		

ASTM A182, F304, F304L, F316, F316L, F321, F321L, F347, F347L, F354, F354L, F360, F360L, F368, F368L, F384, F384L, F408, F408L, F446, F446L, F455, F455L, F504, F504L, F560, F560L, F575, F575L, F622, F622L, F660, F660L, F690, F690L, F703, F703L, F753, F753L, F803, F803L, F880, F880L, F903, F903L, F930, F930L, F938, F938L, F945, F945L, F955, F955L, F960, F960L, F970, F970L, F980, F980L, F990, F990L, F1000, F1000L, F1010, F1010L, F1020, F1020L, F1030, F1030L, F1040, F1040L, F1050, F1050L, F1060, F1060L, F1070, F1070L, F1080, F1080L, F1090, F1090L, F1100, F1100L, F1110, F1110L, F1120, F1120L, F1130, F1130L, F1140, F1140L, F1150, F1150L, F1160, F1160L, F1170, F1170L, F1180, F1180L, F1190, F1190L, F1200, F1200L, F1210, F1210L, F1220, F1220L, F1230, F1230L, F1240, F1240L, F1250, F1250L, F1260, F1260L, F1270, F1270L, F1280, F1280L, F1290, F1290L, F1300, F1300L, F1310, F1310L, F1320, F1320L, F1330, F1330L, F1340, F1340L, F1350, F1350L, F1360, F1360L, F1370, F1370L, F1380, F1380L, F1390, F1390L, F1400, F1400L, F1410, F1410L, F1420, F1420L, F1430, F1430L, F1440, F1440L, F1450, F1450L, F1460, F1460L, F1470, F1470L, F1480, F1480L, F1490, F1490L, F1500, F1500L, F1510, F1510L, F1520, F1520L, F1530, F1530L, F1540, F1540L, F1550, F1550L, F1560, F1560L, F1570, F1570L, F1580, F1580L, F1590, F1590L, F1600, F1600L, F1610, F1610L, F1620, F1620L, F1630, F1630L, F1640, F1640L, F1650, F1650L, F1660, F1660L, F1670, F1670L, F1680, F1680L, F1690, F1690L, F1700, F1700L, F1710, F1710L, F1720, F1720L, F1730, F1730L, F1740, F1740L, F1750, F1750L, F1760, F1760L, F1770, F1770L, F1780, F1780L, F1790, F1790L, F1800, F1800L, F1810, F1810L, F1820, F1820L, F1830, F1830L, F1840, F1840L, F1850, F1850L, F1860, F1860L, F1870, F1870L, F1880, F1880L, F1890, F1890L, F1900, F1900L, F1910, F1910L, F1920, F1920L, F1930, F1930L, F1940, F1940L, F1950, F1950L, F1960, F1960L, F1970, F1970L, F1980, F1980L, F1990, F1990L, F2000, F2000L, F2010, F2010L, F2020, F2020L, F2030, F2030L, F2040, F2040L, F2050, F2050L, F2060, F2060L, F2070, F2070L, F2080, F2080L, F2090, F2090L, F2100, F2100L, F2110, F2110L, F2120, F2120L, F2130, F2130L, F2140, F2140L, F2150, F2150L, F2160, F2160L, F2170, F2170L, F2180, F2180L, F2190, F2190L, F2200, F2200L, F2210, F2210L, F2220, F2220L, F2230, F2230L, F2240, F2240L, F2250, F2250L, F2260, F2260L, F2270, F2270L, F2280, F2280L, F2290, F2290L, F2300, F2300L, F2310, F2310L, F2320, F2320L, F2330, F2330L, F2340, F2340L, F2350, F2350L, F2360, F2360L, F2370, F2370L, F2380, F2380L, F2390, F2390L, F2400, F2400L, F2410, F2410L, F2420, F2420L, F2430, F2430L, F2440, F2440L, F2450, F2450L, F2460, F2460L, F2470, F2470L, F2480, F2480L, F2490, F2490L, F2500, F2500L, F2510, F2510L, F2520, F2520L, F2530, F2530L, F2540, F2540L, F2550, F2550L, F2560, F2560L, F2570, F2570L, F2580, F2580L, F2590, F2590L, F2600, F2600L, F2610, F2610L, F2620, F2620L, F2630, F2630L, F2640, F2640L, F2650, F2650L, F2660, F2660L, F2670, F2670L, F2680, F2680L, F2690, F2690L, F2700, F2700L, F2710, F2710L, F2720, F2720L, F2730, F2730L, F2740, F2740L, F2750, F2750L, F2760, F2760L, F2770, F2770L, F2780, F2780L, F2790, F2790L, F2800, F2800L, F2810, F2810L, F2820, F2820L, F2830, F2830L, F2840, F2840L, F2850, F2850L, F2860, F2860L, F2870, F2870L, F2880, F2880L, F2890, F2890L, F2900, F2900L, F2910, F2910L, F2920, F2920L, F2930, F2930L, F2940, F2940L, F2950, F2950L, F2960, F2960L, F2970, F2970L, F2980, F2980L, F2990, F2990L, F3000, F3000L, F3010, F3010L, F3020, F3020L, F3030, F3030L, F3040, F3040L, F3050, F3050L, F3060, F3060L, F3070, F3070L, F3080, F3080L, F3090, F3090L, F3100, F3100L, F3110, F3110L, F3120, F3120L, F3130, F3130L, F3140, F3140L, F3150, F3150L, F3160, F3160L, F3170, F3170L, F3180, F3180L, F3190, F3190L, F3200, F3200L, F3210, F3210L, F3220, F3220L, F3230, F3230L, F3240, F3240L, F3250, F3250L, F3260, F3260L, F3270, F3270L, F3280, F3280L, F3290, F3290L, F3300, F3300L, F3310, F3310L, F3320, F3320L, F3330, F3330L, F3340, F3340L, F3350, F3350L, F3360, F3360L, F3370, F3370L, F3380, F3380L, F3390, F3390L, F3400, F3400L, F3410, F3410L, F3420, F3420L, F3430, F3430L, F3440, F3440L, F3450, F3450L, F3460, F3460L, F3470, F3470L, F3480, F3480L, F3490, F3490L, F3500, F3500L, F3510, F3510L, F3520, F3520L, F3530, F3530L, F3540, F3540L, F3550, F3550L, F3560, F3560L, F3570, F3570L, F3580, F3580L, F3590, F3590L, F3600, F3600L, F3610, F3610L, F3620, F3620L, F3630, F3630L, F3640, F3640L, F3650, F3650L, F3660, F3660L, F3670, F3670L, F3680, F3680L, F3690, F3690L, F3700, F3700L, F3710, F3710L, F3720, F3720L, F3730, F3730L, F3740, F3740L, F3750, F3750L, F3760, F3760L, F3770, F3770L, F3780, F3780L, F3790, F3790L, F3800, F3800L, F3810, F3810L, F3820, F3820L, F3830, F3830L, F3840, F3840L, F3850, F3850L, F3860, F3860L, F3870, F3870L, F3880, F3880L, F3890, F3890L, F3900, F3900L, F3910, F3910L, F3920, F3920L, F3930, F3930L, F3940, F3940L, F3950, F3950L, F3960, F3960L, F3970, F3970L, F3980, F3980L, F3990, F3990L, F4000, F4000L, F4010, F4010L, F4020, F4020L, F4030, F4030L, F4040, F4040L, F4050, F4050L, F4060, F4060L, F4070, F4070L, F4080, F4080L, F4090, F4090L, F4100, F4100L, F4110, F4110L, F4120, F4120L, F4130, F4130L, F4140, F4140L, F4150, F4150L, F4160, F4160L, F4170, F4170L, F4180, F4180L, F4190, F4190L, F4200, F4200L, F4210, F4210L, F4220, F4220L, F4230, F4230L, F4240, F4240L, F4250, F4250L, F4260, F4260L, F4270, F4270L, F4280, F4280L, F4290, F4290L, F4300, F4300L, F4310, F4310L, F4320, F4320L, F4330, F4330L, F4340, F4340L, F4350, F4350L, F4360, F4360L, F4370, F4370L, F4380, F4380L, F4390, F4390L, F4400, F4400L, F4410, F4410L, F4420, F4420L, F4430, F4430L, F4440, F4440L, F4450, F4450L, F4460, F4460L, F4470, F4470L, F4480, F4480L, F4490, F4490L, F4500, F4500L, F4510, F4510L, F4520, F4520L, F4530, F4530L, F4540, F4540L, F4550, F4550L, F4560, F4560L, F4570, F4570L, F4580, F4580L, F4590, F4590L, F4600, F4600L, F4610, F4610L, F4620, F4620L, F4630, F4630L, F4640, F4640L, F4650, F4650L, F4660, F4660L, F4670, F4670L, F4680, F4680L, F4690, F4690L, F4700, F4700L, F4710, F4710L, F4720, F4720L, F4730, F4730L, F4740, F4740L, F4750, F4750L, F4760, F4760L, F4770, F4770L, F4780, F4780L, F4790, F4790L, F4800, F4800L, F4810, F4810L, F4820, F4820L, F4830, F4830L, F4840, F4840L, F4850, F4850L, F4860, F4860L, F4870, F4870L, F4880, F4880L, F4890, F4890L, F4900, F4900L, F4910, F4910L, F4920, F4920L, F4930, F4930L, F4940, F4940L, F4950, F4950L, F4960, F4960L, F4970, F4970L, F4980, F4980L, F4990, F4990L, F5000, F5000L, F5010, F5010L, F5020, F5020L, F5030, F5030L, F5040, F5040L, F5050, F5050L, F5060, F5060L, F5070, F5070L, F5080, F5080L, F5090, F5090L, F5100, F5100L, F5110, F5110L, F5120, F5120L, F5130, F5130L, F5140, F5140L, F5150, F5150L, F5160, F5160L, F5170, F5170L, F5180, F5180L, F5190, F5190L, F5200, F5200L, F5210, F5210L, F5220, F5220L, F5230, F5230L, F5240, F5240L, F5250, F5250L, F5260, F5260L, F5270, F5270L, F5280, F5280L, F5290, F5290L, F5300, F5300L, F5310, F5310L, F5320, F5320L, F5330, F5330L, F5340, F5340L, F5350, F5350L, F5360, F5360L, F5370, F5370L, F5380, F5380L, F5390, F5390L, F5400, F5400L, F5410, F5410L, F5420, F5420L, F5430, F5430L, F5440, F5440L, F5450, F5450L, F5460, F5460L, F5470, F5470L, F5480, F5480L, F5490, F5490L, F5500, F5500L, F5510, F5510L, F5520, F5520L, F5530, F5530L, F5540, F5540L, F5550, F5550L, F5560, F5560L, F5570, F5570L, F5580, F5580L, F5590, F5590L, F5600, F5600L, F5610, F5610L, F5620, F5620L, F5630, F5630L, F5640, F5640L, F5650, F5650L, F5660, F5660L, F

# FLANGE DATA: 150-2500 PSI

# TABLES F

**LAP-JOINT STUB ENDS: ANSI B16.9 & MSS SP 43**

**TABLE F-7**

NOMINAL PIPE SIZE (INCHES)		2	3	4	6	8	10	12	14	16	18	20	24
OVERALL LENGTH	STD. XS. XXS. 40S, 80S, 160S	ANSI B16.9 STUB ENDS, for use with lap-joint flange											
	6S and 10S	MSS SP-43 STUB ENDS, for use with slip-on flange											
		2.5	2.5	3	3.5	4	5	6					
OUTSIDE DIAMETER AT WELDING END, ANSI & MSS TYPES		2.38	3.5	4.5	6.63	8.63	10.75	12.75	14	16	18	20	24
THICKNESS OF LAP, ANSI & MSS types		NOMINAL PIPE WALL THICKNESS (+1/16 in., -0 in., for ANSI type) —Refer to tables P-1 for pipe wall thicknesses											
STUDBOLT LENGTHS FOR LAP JOINTS Refer to Note (7)	FLANGE COMBINATION	PSI RATING											
		INCREASE IN STUDBOLT LENGTH AS GIVEN IN TABLES F-1 thru F-6											
		150 or 300											
		Thickness of lap											
		Over 300											
		Thickness of lap minus 1/4 in.											
		Thickness of two laps											

**SMALL SOCKET-WELDING FLANGE DATA**

**TABLE F-8**

NOMINAL PIPE SIZE (INCHES)		1/8	1/4	3/8	1/2	5/8	3/4	1	1 1/4	1 1/2	2	2 1/2	3	3 1/2	4	5	6	8	10	12	14	16	18	20	24
FLANGE	OUTSIDE DIAMETER	2.5	3.0	4.25	5	5.75	6.5	7.5	8.5	9.5	11	12.5	14	16	18	20	22	24	26	28	30	32	34	36	38
	PIPE END TO FLANGE FACE (RF) Including 1/16-in. weld neck	0.31	0.25	0.25	0.31	0.36	0.43	0.53	0.63	0.75	0.87	1.0	1.125	1.25	1.44	1.64	1.84	2.04	2.25	2.44	2.64	2.84	3.04	3.25	3.44
	DIAMETER OF BORE	0.4	0.5	0.6	0.7	0.8	0.9	1.0	1.1	1.2	1.3	1.5	1.6	1.8	2.0	2.2	2.4	2.6	2.8	3.0	3.2	3.4	3.6	3.8	4.0
BOLTING	DIAMETER OF BOLT	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5
	STUDBOLT THREAD LENGTH	2.25	2.25	2.5	2.75	2.5	2.75	3	3.25	3.5	3	3.25	3.5	4	4	4	4	4	4	4	4	4	4	4	4
	RING JOINT	-	-	3	3.25	3	3.25	3.5	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4

**SMALL SCREWED FLANGE DATA**

**TABLE F-9**

NOMINAL PIPE SIZE (INCHES)		1/8	1/4	3/8	1/2	5/8	3/4	1	1 1/4	1 1/2	2	2 1/2	3	3 1/2	4	5	6	8	10	12	14	16	18	20	24
FLANGE	OUTSIDE DIAMETER	2.5	3.0	4.25	5	5.75	6.5	7.5	8.5	9.5	11	12.5	14	16	18	20	22	24	26	28	30	32	34	36	38
	PIPE END TO FLANGE FACE (RF) Based on nominal thread engagement	0.13	0.06	0	0.19	0.36	0.44	0.56	0.63	0.75	0.87	1.0	1.125	1.25	1.44	1.64	1.84	2.04	2.25	2.44	2.64	2.84	3.04	3.25	3.44
	BOLT HOLES PER FLANGE	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4
BOLTING	DIAMETER OF BOLT	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5
	STUDBOLT THREAD LENGTH	2.25	2.25	2.5	2.75	2.5	2.75	3	3.25	3.5	3	3.25	3.5	4	4	4	4	4	4	4	4	4	4	4	4
	RING JOINT	-	-	3	3.25	3	3.25	3.5	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4

\*Established by tests made under working conditions, with strength multiplied either to ANSI standard or to the API standard for line pipe service.

## NOTES

- 1 DIMENSIONS IN TABLES F-1 thru F-9 ARE IN INCHES.
- 2 DATA FOR FLANGE OUTSIDE DIAMETER, NUMBER OF BOLT HOLES PER FLANGE, AND BOLT DIAMETER GIVEN IN TABLES F-1 thru F-6 APPLY TO WELDING-NECK, SLIP-ON, SCREWED, LAP-JOINT AND BLIND FLANGES.
- 3 'DIAMETER OF BORE' DATA APPLY ONLY TO WELDING-NECK AND SOCKET-WELDING FLANGES. LONG WELDING-NECK FLANGES ARE BORED TO THE NOMINAL PIPE SIZE.
- 4 SLIP-ON FLANGES IN 2500 PSI RATING ARE NOT DEFINED BY ANSI B16.5-1968.
- 5 SOCKET-WELDING FLANGES ARE DEFINED BY ANSI B16.5-1968 IN THE FOLLOWING SIZES AND RATINGS ONLY: 1/2 in thru 3 in. (150, 300 and 600 PSI), 1/2 in. thru 2 1/2 in. (1500 PSI). DATA IN TABLES F-1 thru F-6 APPLY TO THESE AND OTHER SOCKET-WELDING FLANGES; REFER TO MANUFACTURERS FOR AVAILABILITY.
- 6 ANSI B16.5-1968 DOES NOT DEFINE LONG WELDING-NECK FLANGES. 'LENGTH THRU HUB' DIMENSIONS DIFFERENT FROM THOSE LISTED ARE ALSO AVAILABLE.
- 7 STUDBOLT THREAD LENGTHS GIVEN IN TABLE F-7 ARE CALCULATED ACCORDING TO THE METHOD SPECIFIED IN ANSI B16.5-1968.

# FLOW RESISTANCE OF FITTINGS & VALVES

NOMINAL PIPE SIZE (IN.)		1	1 1/2	2	3	4	6	8	10	12	14	16	18	20	24
FITTINGS & CONNECTIONS	90° LONG-RADIUS ELBOW	2.3	3.3	4.3	5.3	6.3	7.3	8.3	9.3	10.3	11.3	12.3	13.3	14.3	15.3
	90° SHORT-RADIUS ELBOW	2.3	3.3	4.3	5.3	6.3	7.3	8.3	9.3	10.3	11.3	12.3	13.3	14.3	15.3
OPEN VALVES	45° ELBOW (LONG RADIUS)	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	RETURN, LONG-RADIUS	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
FITTINGS & CONNECTIONS	RETURN, SHORT-RADIUS	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	90° MITERS	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
OPEN VALVES	2-PIECE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	3-PIECE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
FITTINGS & CONNECTIONS	4-PIECE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	5-PIECE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
OPEN VALVES	REDUCER and SWAGE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	VENTURI SWAGE - One listed NPS increase	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
FITTINGS & CONNECTIONS	STRAIGHT TEE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	UNION and COUPLING (Screened, pipe-to-pipe)	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
OPEN VALVES	REDUCING FLANGE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	BELLMOUTH OUTLET (Vessel-to-line)	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
FITTINGS & CONNECTIONS	INLET, Flush with Wall (Line-to-vessel)	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	OUTLET, Flush with Wall (Vessel-to-line)	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
OPEN VALVES	GATE VALVE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	GLOBE VALVE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
FITTINGS & CONNECTIONS	CHECK VALVE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	ROTARY BALL VALVE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
OPEN VALVES	BUTTERFLY VALVE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6
	PLUS VALVE	1.1	1.6	2.1	2.6	3.1	3.6	4.1	4.6	5.1	5.6	6.1	6.6	7.1	7.6

FLOW RESISTANCE IS STATED AS EQUIVALENT LENGTH OF PIPE IN FEET (REFER TO NOTES 1 & 2))

**NOTES**

(1) Hydraulic resistances are for turbulent flow and are given as lengths of SCH 40 pipe having the same resistance. For pipe with a thicker wall, use the resistance value for SCH 40 pipe having the closest internal diameter.

(2) Numbers in italics are resistances for screened valves and fittings. Upright numbers relate to flanged valves and butt-welding fittings.

(3) For reducing and increasing fittings, flow resistance is based on the nominal pipe size at the inflow end.

(4) The tabulated flow resistances are approximate and have been selected from several sources which do not always give comparable values. These sources include the Hydraulic Institute's "Friction Manual", the Crane Company's "Technical Paper 410", the "Reactors Handbook, Volume 4" (Interscience), the "Chemical Engineer's Handbook", (McGraw-Hill), "Cameron Hydraulic Data" (Ingersoll-Rand), and manufacturers' catalogs.

FRACTIONAL EQUIVALENTS	0.06	0.13	0.19	0.25	0.31	0.38	0.44	0.50	0.56	0.63	0.69	0.75	0.81	0.88	0.94
	1/16	1/8	3/16	1/4	5/16	3/8	7/16	1/2	9/16	5/8	11/16	3/4	13/16	7/8	15/16

# FLOW OF WATER THRU SCH 40 PIPE

## TABLE F-11

FLOW RATE		PRESSURE DROP (PSI) PER 100 FT SCH 40 PIPE															
GPM	Cu.ft./sec	1/8"	1/4"	3/8"	1/2"	3/4"	1"	1 1/4"	1 1/2"	2"	2 1/2"	3"	3 1/2"	4"	5"	6"	8"
.1	.00022	.56	.677														
.2	.00045	1.14	2.48	.62	.548												
.3	.00067	1.70	5.26	.93	1.16	.50	.255										
.4	.0089	2.26	9.00	1.24	1.98	.67	.436	.42	.136								
.5	.00111	2.82	13.58	1.55	3.00	.84	.656	.53	.205	.30	.030						
.6	.00134	3.38	19.12	1.85	4.22	1.01	.925	.63	.290	.36	.071						
.8	.00178	4.52	32.62	2.47	7.17	1.34	1.58	.84	.494	.48	.121						
1	.00223			3.09	10.91	1.68	2.39	1.06	.749	.60	.183						
2	.00446			6.18	39.60	3.36	8.68	2.11	2.72	1.20	.665						
3	.00668					5.04	18.46	3.17	5.77	1.80	1.41						
4	.00891					6.72	31.55	4.22	9.86	2.40	2.42						
5	.01114							5.28	14.92	3.01	3.64						
6	.01337							6.33	20.95	3.61	5.13						
8	.01782	1.26	.308							4.81	8.76						
10	.02228	1.58	.466							6.01	13.28						
15	.03342	2.36	.992	1.43	.285												
20	.04456	3.15	1.69	1.91	.486												
25	.05570	3.94	2.54	2.39	.736												
30	.06684	4.73	3.60	2.37	1.03	2.01	.424										
35	.07798	5.51	4.79	3.35	1.37	2.35	.566										
40	.08912	6.30	6.14	3.82	1.76	2.68	.724										
50	.1114	7.88	9.31	4.78	2.67	3.35	1.10	2.17	.371								
60	.1337	9.45	13.08	5.74	3.75	4.02	1.54	2.61	.520								
70	.1560			6.70	4.99	4.70	2.05	3.04	.693								
80	.1782			7.65	6.40	5.37	2.63	3.47	.890								
90	.2005			8.60	7.96	6.04	3.28	3.91	1.10								
100	.2228			9.56	9.69	6.71	3.98	4.34	1.34								
125	.2785					8.38	6.03	5.43	2.01								
150	.3342					10.1	8.46	6.52	2.86								
175	.3899					11.7	11.3	7.60	3.81								
200	.4456					13.4	14.4	8.69	4.89								
225	.5013							9.77	6.09								
250	.5570	2.78	.245					10.9	7.41								
275	.6127	3.06	.292					11.9	8.84								
300	.6684	3.33	.344					13.0	10.4								
350	.7798	3.89	.457					15.2	13.8								
400	.8912	4.44	.587														
450	1.003	5.00	.731														
500	1.114	5.55	.887														
550	1.225	6.11	1.07	3.53	.270												
600	1.337	6.66	1.25	3.85	.316												
650	1.449	7.22	1.45	4.17	.367	2.65	.118										
700	1.560	7.78	1.66	4.49	.420	2.85	.135										
750	1.671	8.33	1.89	4.81	.480	3.05	.154										
800	1.782	8.89	2.13	5.13	.540	3.26	.173										
850	1.894	9.44	2.38	5.45	.605	3.46	.194										
900	2.005	10.0	2.66	5.77	.677	3.66	.216										
950	2.117	10.6	2.93	6.09	.744	3.87	.238	2.58	.090								
1000	2.228	11.1	3.23	6.41	.817	4.07	.262	2.87	.109								
1100	2.451	12.2	3.85	7.06	.975	4.48	.313	3.15	.130								
1200	2.674	13.3	4.53	7.70	1.15	4.88	.368	3.44	.153								
1300	2.896	14.4	5.26	8.34	1.33	5.29	.420	3.73	.178								
1400	3.119	15.6	6.01	8.98	1.53	5.70	.479	4.01	.204								
1500	3.342	16.7	6.84	9.62	1.74	6.10	.536	4.30	.232								
1600	3.565	17.8	7.73	10.3	1.96	6.51	.598	4.59	.262								
1800	4.010	20.0	9.64	11.5	2.46	7.32	.732	5.16	.339								
2000	4.456	22.2	11.6	12.8	2.97	8.14	.953	5.73	.396								
2300	5.370	27.8	17.6	16.0	4.49	10.2	1.44	7.17	.601								
3000	6.584			19.2	6.30	12.2	2.02	8.60	.843								
3500	7.798			22.4	8.41	14.3	2.70	10.0	1.12								
4000	8.912			25.7	10.8	16.3	3.46	11.5	1.44								
4500	10.03			28.9	13.4	18.3	4.31	12.9	1.76								
5000	11.14					20.4	5.23	14.3	2.18								
6000	13.27					24.4	7.35	17.2	3.06								
7000	15.60					28.5	9.80	20.1	4.08								
8000	17.82							22.9	5.22								
9000	20.05							25.8	6.51								
10000	22.28							28.7	7.91								
12000	26.74																
14000	31.19																
16000	35.65																
18000	40.10																
20000	44.56																

"Piping Guide", PO Box 277, Cental, CA 94828, USA

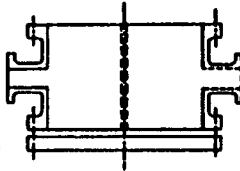

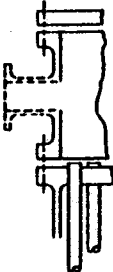
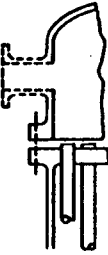
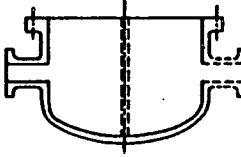

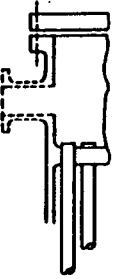
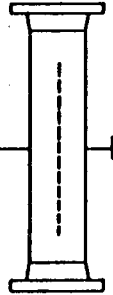
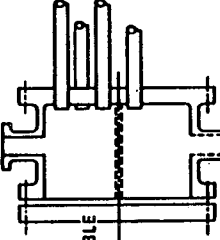

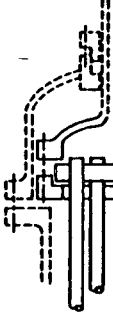
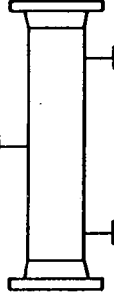
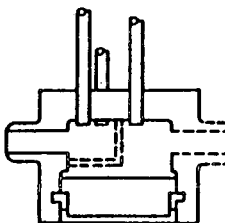
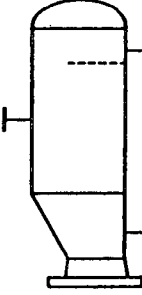
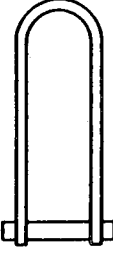
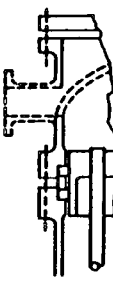
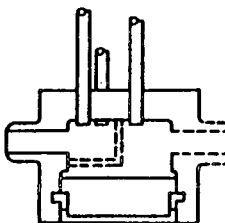
Reproduced by courtesy of the Lunkenhelmer Company. Data are based on the Saph and Schoer formula:  $p = LQ^{1.86}/43505$

# HEAT-EXCHANGER NOMENCLATURE

## CHART H-1

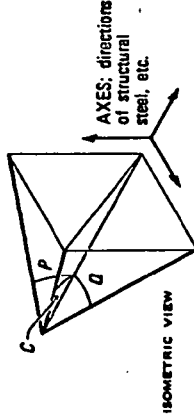
REPRODUCED BY PERMISSION OF THE TUBULAR EXCHANGER MANUFACTURERS ASSOCIATION

THREE LETTERS, SUCH AS AEW, BGP ARE DESIGNATED THE BASIC CONSTRUCTION OF THE EXCHANGER. REFER TO 5.6.1, "DATA NEEDED TO DESIGN EXCHANGER PIPING"

FRONT END STATIONARY HEAD TYPES		SHELL TYPES		REAR END HEAD TYPES	
A		E		L	
	CHANNEL COVER AND REMOVABLE COVER		ONE PASS SHELL	M	
B		F		N	
	BONNET (INTEGRAL COVER)	TWO PASS SHELL WITH LONGITUDINAL BAFFLE	G		P
C		H		S	
	REMOVABLE TUBE BUNDLE ONLY	DOUBLE SPLIT FLOW	J		T
D		K		U	
	CHANNEL INTEGRAL WITH TUBE-SHEET AND REMOVABLE COVER	KETTLE TYPE REBOILER	W		
					

# MEASUREMENTS

## COMPOUND ANGLES

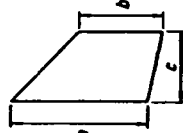


Compound angle,  $C$ , is given by:

$$(\tan C)^2 = (\tan P)^2 + (\tan Q)^2$$

## TRAPEZOID

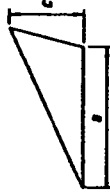
Trapezoid: A four-sided figure with two parallel sides, and the other two sides at any angle. Termed 'trapezium' in UK.



$$\text{AREA} = c(a + b)/2$$

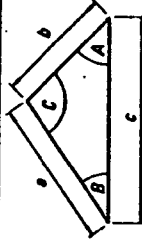
If  $a = b$ , this formula applies to any parallelogram or rectangle.

## TRIANGLE



$$\text{AREA} = ac/2$$

## TRIANGLES



THESE FORMULAS MAY BE USED FOR ALL (FLAT) TRIANGLES

If  $\theta$  is between  $90^\circ$  and  $180^\circ$ ,  
 $\sin \theta = \sin(180^\circ - \theta)$ ,  $\cos \theta = -\cos(180^\circ - \theta)$   
(These values may be found in tables)

KNOWN	REQUIRED	SOLUTION
Two angles	Third angle	$A = 180^\circ - (B + C)$
Three sides	Any angle	$\cos A = (b^2 + c^2 - a^2)/2bc$
	Area	$\text{Area} = [s(s-a)(s-b)(s-c)]^{1/2}$ , $s = (a+b+c)/2$
Two sides and included angle	Third side	$c = (a^2 + b^2 - 2ab \cos C)^{1/2}$
	Area	$(ab \sin C)/2$
Two sides and excluded angle (ambiguous)	Third side	$c = b \cos A \pm (a^2 - b^2 \sin^2 A)^{1/2}$
	Area	$(b/2) \sin A [b \cos A \pm (a^2 - b^2 \sin^2 A)^{1/2}]$
One side and adjacent angles	Adjacent side	$c = a \sin C / \sin(B + C)$
	Area	$a^2 \sin B \sin C / [2 \sin(B + C)]$

# CHART M-1

ALL ANGLES IN THESE FORMULAS ARE EXPRESSED IN DEGREES OF ARC

## AREAS & VOLUMES

### CIRCLE

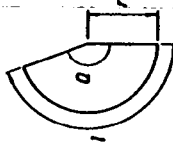
Refer to table M-3 for numerical values of circumferences and areas of full circles

#### FULL CIRCLE

$$\begin{aligned} \text{CIRCUMFERENCE} &= 2\pi r \\ &= 6.2831853r \\ \text{AREA} &= \pi r^2 \\ &= 3.1415927r^2 \end{aligned}$$

#### SECTOR (as shown)

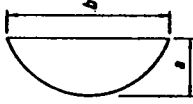
$$\begin{aligned} \text{LENGTH OF ARC} &= l = \pi r Q/180 \\ &= 0.0174533rQ \\ \text{AREA} &= \pi r^2 Q/360 \\ &= 0.0087266r^2 Q \end{aligned}$$



### SEGMENT OF CIRCLE

$$\begin{aligned} \text{DIAMETER} &= d = (a^2/4a) \\ \text{RADIUS} &= r = (a/2) + (b^2/8a) \\ \text{LENGTH OF ARC} &= l = (\pi r/180) \arccos[1 - (a/r)] \\ &= (\pi r/180) \arccos(b/2r) \\ \text{where } \pi/180 &= 0.03490659 \\ \text{AREA} &= (r^2 - rb + ab)/2 \end{aligned}$$

NOTE:  $\arccos(Q)$  = "angle in degrees whose cosine is Q", and  $\arcsin(Q)$  = "angle in degrees whose sine is Q".  
\*Valid for a positive and less than 2r.



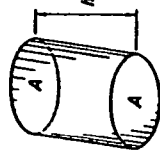
### ELLIPSE



$$\begin{aligned} \text{AREA} &= (\pi/4)(ab) \\ &= 0.7853982(ab) \\ \text{CIRCUMFERENCE} &= \pi[(a^2 + b^2)/2]^{1/2} \text{ approximately} \end{aligned}$$

### PRISM

BASE OF ANY SHAPE; UPRIGHT OR SLOPING

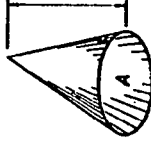


$$\begin{aligned} \text{AREA OF SECTION} &= A \\ \text{DISTANCE BETWEEN PARALLEL SECTIONS 'A' AND 'A''} &= h \\ \text{VOLUME} &= hA \end{aligned}$$

NOTE: THIS FORMULA MAY BE APPLIED TO CYLINDRIC AND RECTANGULAR TANKS.

### CONE

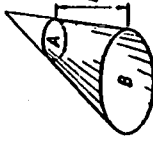
BASE OF ANY SHAPE; UPRIGHT OR SLOPING



$$\begin{aligned} \text{AREA OF BASE} &= A \\ \text{HEIGHT (measured at right angles to base)} &= h \\ \text{VOLUME} &= hA/3 \end{aligned}$$

### FRUSTUM OF CONE

SECTION OF ANY SHAPE; UPRIGHT OR SLOPING



$$\begin{aligned} \text{AREAS OF PARALLEL FLAT SURFACES 'A' AND 'B'} &= A \text{ and } B, \text{ respectively} \\ \text{DISTANCE BETWEEN SURFACES 'A' AND 'B'} &= h \\ \text{VOLUME} &= (h/3) \cdot (A + B + (AB)^{1/2}) \end{aligned}$$

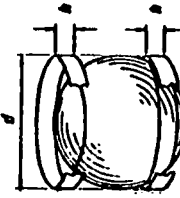
### SPHERE



$$\begin{aligned} \text{RADIUS} &= r \\ \text{DIAMETER} &= d = 2r \\ \text{SURFACE AREA} &= \pi d^2 \\ &= 3.14159265d^2 \\ \text{VOLUME} &= \pi d^3/6 \\ &= 0.5235988d^3 \\ \text{VOLUME OF SEGMENT OF DEPTH } h &= (\pi h^2/3)(3r - h) \\ &= (1.0471976d^2/3)(3r - h), \end{aligned}$$

where h is positive and less than 2r.

### AREA OF SPHERICAL CAP OR SLICE



The area of the curved surface of the cap or the slice equals the area of the cylindric band of the same depth, h; that is,  $\pi Ad$ , no matter where the slice is taken, or how thick the slice or cap is.

# MEASUREMENTS

# TABLES M-2

## HYPOTENUSE FOR 45° TRIANGLES

VALUES COMPUTED TO  
NEAREST 1/16-IN. INCH

SIDE	HYPOTENUSE	SIDE	HYPOTENUSE	SIDE	HYPOTENUSE	SIDE	HYPOTENUSE	SIDE	HYPOTENUSE
0 0-1/16	0 0-1/16	0 3-3/16	0 4-1/2	0 5-5/16	0 8-15/16	0 3-7/16	1 1-3/8	1 0	1 4-31/32
0 0-1/8	0 0-3/16	0 3-1/4	0 4-5/8	0 5-3/8	0 9	0 3-1/2	1 1-7/16	2 0	2 9-15/16
0 0-3/16	0 0-7/16	0 3-5/16	0 4-7/8	0 5-7/8	0 9-1/8	0 3-1/2	1 1-7/16	3 0	3 2-29/32
0 0-1/4	0 0-1/2	0 3-7/16	0 4-7/8	0 6-1/2	0 9-3/8	0 3-1/2	1 1-7/16	4 0	4 0
0 0-5/16	0 0-5/8	0 3-1/2	0 4-7/8	0 6-3/8	0 9-7/8	0 3-1/2	1 1-7/16	5 0	5 0-27/32
0 0-3/8	0 0-11/16	0 3-1/2	0 4-7/8	0 6-5/8	0 9-7/8	0 3-1/2	1 1-7/16	6 0	6 5-1/16
0 0-7/8	0 0-13/16	0 3-1/2	0 4-7/8	0 6-11/16	0 9-7/8	0 3-1/2	1 1-7/16	7 0	7 10-25/32
0 0-15/16	0 0-1	0 3-1/2	0 4-7/8	0 6-13/16	0 9-7/8	0 3-1/2	1 1-7/16	8 0	8 11-13/32
0 0-1	0 0-1	0 3-1/2	0 4-7/8	0 6-15/16	0 9-7/8	0 3-1/2	1 1-7/16	9 0	9 12-1/4
0 0-1/16	0 0-1/16	0 3-1/4	0 4-7/8	0 7-1/16	0 10	0 3-1/4	1 2-1/8	10 0	10 12-3/4
0 0-1/8	0 0-1/8	0 3-1/4	0 4-7/8	0 7-1/8	0 10-1/16	0 3-1/4	1 2-1/8	11 0	11 13-1/16
0 0-3/16	0 0-3/16	0 3-1/4	0 4-7/8	0 7-3/16	0 10-1/8	0 3-1/4	1 2-1/8	12 0	12 13-5/16
0 0-1/4	0 0-1/4	0 3-1/4	0 4-7/8	0 7-1/4	0 10-1/4	0 3-1/4	1 2-1/8	13 0	13 14-1/16
0 0-5/16	0 0-5/16	0 3-1/4	0 4-7/8	0 7-5/16	0 10-1/2	0 3-1/4	1 2-1/8	14 0	14 14-5/8
0 0-3/8	0 0-3/8	0 3-1/4	0 4-7/8	0 7-3/8	0 10-3/4	0 3-1/4	1 2-1/8	15 0	15 15-1/16
0 0-7/8	0 0-7/8	0 3-1/4	0 4-7/8	0 7-7/8	0 10-11/16	0 3-1/4	1 2-1/8	16 0	16 15-1/2
0 0-15/16	0 0-15/16	0 3-1/4	0 4-7/8	0 7-15/16	0 10-13/16	0 3-1/4	1 2-1/8	17 0	17 15-3/4
0 0-1	0 0-1	0 3-1/4	0 4-7/8	0 8-1/16	0 10-15/16	0 3-1/4	1 2-1/8	18 0	18 16-1/16
0 0-1/16	0 0-1/16	0 3-1/2	0 4-7/8	0 8-1/8	0 11-1/16	0 3-1/2	1 2-1/8	19 0	19 16-1/2
0 0-1/8	0 0-1/8	0 3-1/2	0 4-7/8	0 8-3/16	0 11-1/8	0 3-1/2	1 2-1/8	20 0	20 16-3/4
0 0-3/16	0 0-3/16	0 3-1/2	0 4-7/8	0 8-1/4	0 11-1/4	0 3-1/2	1 2-1/8	21 0	21 17-1/16
0 0-1/4	0 0-1/4	0 3-1/2	0 4-7/8	0 8-3/8	0 11-3/8	0 3-1/2	1 2-1/8	22 0	22 17-1/2
0 0-5/16	0 0-5/16	0 3-1/2	0 4-7/8	0 8-1/2	0 11-1/2	0 3-1/2	1 2-1/8	23 0	23 17-3/4
0 0-3/8	0 0-3/8	0 3-1/2	0 4-7/8	0 8-5/8	0 11-3/4	0 3-1/2	1 2-1/8	24 0	24 18-1/16
0 0-7/8	0 0-7/8	0 3-1/2	0 4-7/8	0 8-11/16	0 11-7/8	0 3-1/2	1 2-1/8	25 0	25 18-1/2
0 0-15/16	0 0-15/16	0 3-1/2	0 4-7/8	0 8-13/16	0 11-15/16	0 3-1/2	1 2-1/8	26 0	26 18-3/4
0 0-1	0 0-1	0 3-1/2	0 4-7/8	0 8-15/16	0 12-1/16	0 3-1/2	1 2-1/8	27 0	27 19-1/16
0 0-1/16	0 0-1/16	0 3-3/4	0 4-7/8	0 8-1	0 12-1/8	0 3-3/4	1 2-1/8	28 0	28 19-1/2
0 0-1/8	0 0-1/8	0 3-3/4	0 4-7/8	0 8-1/8	0 12-1/4	0 3-3/4	1 2-1/8	29 0	29 19-3/4
0 0-3/16	0 0-3/16	0 3-3/4	0 4-7/8	0 8-1/4	0 12-3/8	0 3-3/4	1 2-1/8	30 0	30 20-1/16
0 0-1/4	0 0-1/4	0 3-3/4	0 4-7/8	0 8-3/8	0 12-1/2	0 3-3/4	1 2-1/8	31 0	31 20-1/2
0 0-5/16	0 0-5/16	0 3-3/4	0 4-7/8	0 8-1/2	0 12-3/4	0 3-3/4	1 2-1/8	32 0	32 20-3/4
0 0-3/8	0 0-3/8	0 3-3/4	0 4-7/8	0 8-5/8	0 13-1/16	0 3-3/4	1 2-1/8	33 0	33 20-7/8
0 0-7/8	0 0-7/8	0 3-3/4	0 4-7/8	0 8-11/16	0 13-1/8	0 3-3/4	1 2-1/8	34 0	34 21-1/16
0 0-15/16	0 0-15/16	0 3-3/4	0 4-7/8	0 8-13/16	0 13-3/8	0 3-3/4	1 2-1/8	35 0	35 21-1/2
0 0-1	0 0-1	0 3-3/4	0 4-7/8	0 8-15/16	0 13-1/2	0 3-3/4	1 2-1/8	36 0	36 21-3/4
0 0-1/16	0 0-1/16	0 3-1/2	0 4-7/8	0 8-1	0 13-3/4	0 3-1/2	1 2-1/8	37 0	37 22-1/16
0 0-1/8	0 0-1/8	0 3-1/2	0 4-7/8	0 8-1/8	0 14-1/16	0 3-1/2	1 2-1/8	38 0	38 22-1/2
0 0-3/16	0 0-3/16	0 3-1/2	0 4-7/8	0 8-1/4	0 14-1/8	0 3-1/2	1 2-1/8	39 0	39 22-3/4
0 0-1/4	0 0-1/4	0 3-1/2	0 4-7/8	0 8-3/8	0 14-1/4	0 3-1/2	1 2-1/8	40 0	40 23-1/16
0 0-5/16	0 0-5/16	0 3-1/2	0 4-7/8	0 8-1/2	0 14-3/8	0 3-1/2	1 2-1/8	41 0	41 23-1/2
0 0-3/8	0 0-3/8	0 3-1/2	0 4-7/8	0 8-5/8	0 14-1/2	0 3-1/2	1 2-1/8	42 0	42 23-3/4
0 0-7/8	0 0-7/8	0 3-1/2	0 4-7/8	0 8-11/16	0 15-1/16	0 3-1/2	1 2-1/8	43 0	43 24-1/16
0 0-15/16	0 0-15/16	0 3-1/2	0 4-7/8	0 8-13/16	0 15-1/8	0 3-1/2	1 2-1/8	44 0	44 24-1/2
0 0-1	0 0-1	0 3-1/2	0 4-7/8	0 8-15/16	0 15-3/8	0 3-1/2	1 2-1/8	45 0	45 24-3/4
0 0-1/16	0 0-1/16	0 3-3/4	0 4-7/8	0 8-1	0 15-1/2	0 3-3/4	1 2-1/8	46 0	46 25-1/16
0 0-1/8	0 0-1/8	0 3-3/4	0 4-7/8	0 8-1/8	0 15-3/4	0 3-3/4	1 2-1/8	47 0	47 25-1/2
0 0-3/16	0 0-3/16	0 3-3/4	0 4-7/8	0 8-1/4	0 16-1/16	0 3-3/4	1 2-1/8	48 0	48 25-3/4
0 0-1/4	0 0-1/4	0 3-3/4	0 4-7/8	0 8-3/8	0 16-1/8	0 3-3/4	1 2-1/8	49 0	49 26-1/16
0 0-5/16	0 0-5/16	0 3-3/4	0 4-7/8	0 8-1/2	0 16-1/4	0 3-3/4	1 2-1/8	50 0	50 26-1/2
0 0-3/8	0 0-3/8	0 3-3/4	0 4-7/8	0 8-5/8	0 16-3/8	0 3-3/4	1 2-1/8	51 0	51 26-3/4
0 0-7/8	0 0-7/8	0 3-3/4	0 4-7/8	0 8-11/16	0 16-1/2	0 3-3/4	1 2-1/8	52 0	52 27-1/16
0 0-15/16	0 0-15/16	0 3-3/4	0 4-7/8	0 8-13/16	0 16-3/4	0 3-3/4	1 2-1/8	53 0	53 27-1/2
0 0-1	0 0-1	0 3-3/4	0 4-7/8	0 8-15/16	0 17-1/16	0 3-3/4	1 2-1/8	54 0	54 27-3/4
0 0-1/16	0 0-1/16	0 3-1/2	0 4-7/8	0 8-1	0 17-1/8	0 3-1/2	1 2-1/8	55 0	55 28-1/16
0 0-1/8	0 0-1/8	0 3-1/2	0 4-7/8	0 8-1/8	0 17-1/4	0 3-1/2	1 2-1/8	56 0	56 28-1/2
0 0-3/16	0 0-3/16	0 3-1/2	0 4-7/8	0 8-1/4	0 17-3/8	0 3-1/2	1 2-1/8	57 0	57 28-3/4
0 0-1/4	0 0-1/4	0 3-1/2	0 4-7/8	0 8-3/8	0 18-1/16	0 3-1/2	1 2-1/8	58 0	58 28-7/8
0 0-5/16	0 0-5/16	0 3-1/2	0 4-7/8	0 8-1/2	0 18-1/8	0 3-1/2	1 2-1/8	59 0	59 29-1/16
0 0-3/8	0 0-3/8	0 3-1/2	0 4-7/8	0 8-5/8	0 18-1/4	0 3-1/2	1 2-1/8	60 0	60 29-1/2
0 0-7/8	0 0-7/8	0 3-1/2	0 4-7/8	0 8-11/16	0 18-3/8	0 3-1/2	1 2-1/8	61 0	61 29-3/4
0 0-15/16	0 0-15/16	0 3-1/2	0 4-7/8	0 8-13/16	0 19-1/16	0 3-1/2	1 2-1/8	62 0	62 30-1/16
0 0-1	0 0-1	0 3-1/2	0 4-7/8	0 8-15/16	0 19-1/8	0 3-1/2	1 2-1/8	63 0	63 30-1/2
0 0-1/16	0 0-1/16	0 3-3/4	0 4-7/8	0 8-1	0 19-1/4	0 3-3/4	1 2-1/8	64 0	64 30-3/4
0 0-1/8	0 0-1/8	0 3-3/4	0 4-7/8	0 8-1/8	0 19-3/8	0 3-3/4	1 2-1/8	65 0	65 31-1/16
0 0-3/16	0 0-3/16	0 3-3/4	0 4-7/8	0 8-1/4	0 20-1/16	0 3-3/4	1 2-1/8	66 0	66 31-1/2
0 0-1/4	0 0-1/4	0 3-3/4	0 4-7/8	0 8-3/8	0 20-1/8	0 3-3/4	1 2-1/8	67 0	67 31-3/4
0 0-5/16	0 0-5/16	0 3-3/4	0 4-7/8	0 8-1/2	0 20-3/8	0 3-3/4	1 2-1/8	68 0	68 32-1/16
0 0-3/8	0 0-3/8	0 3-3/4	0 4-7/8	0 8-5/8	0 20-1/2	0 3-3/4	1 2-1/8	69 0	69 32-1/2
0 0-7/8	0 0-7/8	0 3-3/4	0 4-7/8	0 8-11/16	0 21-1/16	0 3-3/4	1 2-1/8	70 0	70 32-3/4
0 0-15/16	0 0-15/16	0 3-3/4	0 4-7/8	0 8-13/16	0 21-1/8	0 3-3/4	1 2-1/8	71 0	71 33-1/16
0 0-1	0 0-1	0 3-3/4	0 4-7/8	0 8-15/16	0 21-1/4	0 3-3/4	1 2-1/8	72 0	72 33-1/2
0 0-1/16	0 0-1/16	0 3-1/2	0 4-7/8	0 8-1	0 21-3/8	0 3-1/2	1 2-1/8	73 0	73 33-3/4
0 0-1/8	0 0-1/8	0 3-1/2	0 4-7/8	0 8-1/8	0 22-1/16	0 3-1/2	1 2-1/8	74 0	74 34-1/16
0 0-3/16	0 0-3/16	0 3-1/2	0 4-7/8	0 8-1/4	0 22-1/8	0 3-1/2	1 2-1/8	75 0	75 34-1/2
0 0-1/4	0 0-1/4	0 3-1/2	0 4-7/8	0 8-3/8	0 22-3/8	0 3-1/2	1 2-1/8	76 0	76 34-3/4
0 0-5/16	0 0-5/16	0 3-1/2	0 4-7/8	0 8-1/2	0 23-1/16	0 3-1/2	1 2-1/8	77 0	77 35-1/16
0 0-3/8	0 0-3/8	0 3-1/2	0 4-7/8	0 8-5/8	0 23-1/8	0 3-1/2	1 2-1/8	78 0	78 35-1/2
0 0-7/8	0 0-7/8	0 3-1/2	0 4-7/8	0 8-11/16	0 23-3/8	0 3-1/2	1 2-1/8	79 0	79 35-3/4
0 0-15/16	0 0-15/16	0 3-1/2	0 4-7/8	0 8-13/16	0 24-1/16	0 3-1/2	1 2-1/8	80 0	80 36-1/16
0 0-1	0 0-1	0 3-1/2	0 4-7/8	0 8-15/16	0 24-1/8	0 3-1/2	1 2-1/8	81 0	81 36-1/2
0 0-1/16	0 0-1/16	0 3-3/4	0 4-7/8	0 8-1	0 24-1/4	0 3-3/4	1 2-1/8	82 0	82 36-3/4
0 0-1/8	0 0-1/8	0 3-3/4	0 4-7/8	0 8-1/8	0 25-1/16	0 3-3/4	1 2-1/8	83 0	83 37-1/16
0 0-3/16	0 0-3/16	0 3-3/4	0 4-7/8	0 8-1/4	0 25-1/8	0 3-3/4	1 2-1/8	84 0	84 37-1/2
0 0-1/4	0 0-1/4	0 3-3/4	0 4-7/8	0 8-3/8	0 25-3/8	0 3-3/4	1 2-1/8	85 0	85 37-3/4
0 0-5/16	0 0-5/16	0 3-3/4	0 4-7/8	0 8-1/2	0 26-1/16	0 3-3/4	1 2-1/8	86 0	86 38-1/16
0 0-3/8	0 0-3/8	0 3-3/4	0 4-7/8	0 8-5/8	0 26-1/8	0 3-3/4	1 2-1/8	87 0	87 38-1/2
0 0-7/8	0 0-7/8	0 3-3/4	0 4-7/8	0 8-11/16	0 26-3/8	0 3-3/4	1 2-1/8	88 0	88 38-3/4
0 0-15/16	0 0-15/16	0 3-3/4	0 4-7/8	0 8-13/16	0 27-1/16	0 3-3/4	1 2-1/8	89 0	89 39-1/16
0 0-1	0 0-1	0 3-3/4	0 4-7/8	0 8-15/16	0 27-1/8	0 3-3/4	1 2-1/8	90 0	90 39-1/2
0 0-1/16	0 0-1/16	0 3-1/2	0 4-7/8	0 8-1	0 27-1/4	0 3-1/2	1 2-1/8	91 0	91 39-3/4
0 0-1/8	0 0-1/8	0 3-1/2	0 4-7/8	0 8-1/8	0 28-1/16	0 3-1/2	1 2-1/8	92 0	92 40-1/16
0 0-3/16	0 0-3/16	0 3-1/2	0 4-7/8	0 8-1/4	0 28-1/8	0 3-1/2	1 2-1/8	93 0	93 40-1/2
0 0-1/4	0 0-1/4	0 3-1/2	0 4-7/8	0 8-3/8	0 28-3/8	0 3-1/2	1 2-1/8	94 0	94 40-3/4
0 0-5/16	0 0-5/16	0 3-1/2	0 4-7/8	0 8-1/2	0 29-1/16	0 3-1/2	1 2-1/8	95 0	95 41-1/16
0 0-3/8	0 0-3/8	0 3-1/2	0 4-7/8						

# CIRCLES: DIAMETER, CIRCUMFERENCE & AREA

## TABLE M-3

DIAM. IN.	CIRCUM. IN.	AREA SQ. IN.	DIAM. IN.	CIRCUM. IN.	AREA SQ. IN.	DIAM. IN.	CIRCUM. IN.	AREA SQ. IN.	DIAM. IN.	CIRCUM. IN.	AREA SQ. IN.
1/4	.0499	.00019	2 1/2	9.0321	6.4918	21	65.973	346.36	40 1/2	125.564	1256.6
1/2	.09818	.00077	2 3/4	9.2284	6.7771	21 1/4	66.759	354.66	41	128.805	1320.3
3/4	.14726	.00173	3	9.4248	7.0686	21 1/2	67.544	363.05	41 1/4	129.591	1336.4
1	.19635	.00307	3 1/4	9.6211	7.3662	21 3/4	68.330	371.54	41 1/2	130.376	1352.7
1 1/4	.24542	.00590	3 1/2	9.8175	7.6699	22	69.115	380.13	42	131.947	1385.4
1 1/2	.29450	.0127	3 3/4	10.014	7.9798	22 1/4	69.900	388.82	42 1/4	132.732	1402.0
1 3/4	.34357	.0219	4	10.210	8.2958	22 1/2	70.686	397.61	42 1/2	133.518	1418.6
2	.39270	.0358	4 1/4	10.407	8.6179	22 3/4	71.471	406.49	43	135.088	1452.2
2 1/4	.44183	.0529	4 1/2	10.603	8.9462	23	72.257	415.48	43 1/4	135.874	1469.1
2 1/2	.49097	.0701	4 3/4	10.799	9.2806	23 1/4	73.042	424.56	43 1/2	136.659	1486.2
2 3/4	.54010	.0890	5	10.996	9.6211	23 1/2	73.827	433.74	44	138.230	1520.5
3	.58923	.0117	5 1/4	11.192	9.9678	23 3/4	74.613	443.01	44 1/4	139.015	1537.9
3 1/4	.63836	.0318	5 1/2	11.388	10.321	24	75.398	452.39	44 1/2	139.801	1555.3
3 1/2	.68749	.0529	5 3/4	11.585	10.680	24 1/4	76.184	461.86	45	141.372	1590.4
3 3/4	.73662	.0750	6	11.781	11.045	24 1/2	76.969	471.44	45 1/4	142.157	1608.2
4	.78575	.1000	6 1/4	11.978	11.416	24 3/4	77.754	481.11	45 1/2	142.942	1626.0
4 1/4	.83488	.1262	6 1/2	12.174	11.793	25	78.540	490.87	46	144.513	1661.9
4 1/2	.88401	.1533	6 3/4	12.370	12.177	25 1/4	79.325	501.15	46 1/4	145.299	1680.0
4 3/4	.93314	.1814	7	12.566	12.566	25 1/2	80.111	510.71	46 1/2	146.084	1698.2
5	.98227	.2105	7 1/4	12.763	12.962	25 3/4	80.896	520.77	47	147.655	1734.9
5 1/4	1.03140	.2406	7 1/2	12.959	13.364	26	81.681	530.93	47 1/4	148.440	1753.5
5 1/2	1.08053	.2717	7 3/4	13.155	13.772	26 1/4	82.467	541.59	47 1/2	149.226	1772.1
5 3/4	1.12966	.3038	8	13.352	14.186	26 1/2	83.252	551.55	48	150.011	1790.8
6	1.17879	.3369	8 1/4	13.548	14.607	26 3/4	84.038	562.00	48 1/4	150.796	1809.6
6 1/4	1.22792	.3710	8 1/2	13.744	15.033	27	84.823	572.56	48 1/2	151.582	1828.5
6 1/2	1.27705	.4061	8 3/4	13.940	15.466	27 1/4	85.608	583.21	49	153.153	1866.5
6 3/4	1.32618	.4422	9	14.137	15.904	27 1/2	86.394	593.96	49 1/4	153.938	1885.7
7	1.37531	.4793	9 1/4	14.333	16.349	28	87.179	604.81	49 1/2	154.723	1905.0
7 1/4	1.42444	.5174	9 1/2	14.530	16.800	28 1/4	87.965	615.75	49 3/4	155.509	1924.4
7 1/2	1.47357	.5555	9 3/4	14.726	17.257	28 1/2	88.750	626.80	50	157.000	1963.5
7 3/4	1.52270	.5936	10	14.923	17.721	28 3/4	89.535	637.94	50 1/4	157.785	1983.2
8	1.57183	.6317	10 1/4	15.119	18.190	29	90.321	649.18	50 1/2	158.570	2003.0
8 1/4	1.62096	.6700	10 1/2	15.315	18.665	29 1/4	91.106	660.52	51	160.21	2042.8
8 1/2	1.67009	.7083	10 3/4	15.512	19.147	29 1/2	91.892	671.96	51 1/4	161.007	2062.9
8 3/4	1.71922	.7466	11	15.708	19.635	29 3/4	92.677	683.49	51 1/2	161.792	2083.1
9	1.76835	.7849	11 1/4	15.904	20.129	30	93.462	695.13	52	163.53	2123.7
9 1/4	1.81748	.8232	11 1/2	16.101	20.629	30 1/4	94.248	706.86	52 1/4	164.318	2144.2
9 1/2	1.86661	.8615	11 3/4	16.297	21.135	30 1/2	95.033	718.69	52 1/2	165.103	2164.8
9 3/4	1.91574	.8998	12	16.493	21.649	31	95.819	730.62			
10	1.96487	.9381	12 1/4	16.690	22.166	31 1/4	96.604	742.64			
10 1/4	2.01400	.9764	12 1/2	16.886	22.691	31 1/2	97.389	754.77			
10 1/2	2.06313	.1015	12 3/4	17.082	23.221	31 3/4	98.175	766.99			
10 3/4	2.11226	.1066	13	17.279	23.758	32	98.960	779.31			
10 1/2	2.16139	.1117	13 1/4	17.475	24.301	32 1/4	99.746	791.73			
10 1/2	2.21052	.1168	13 1/2	17.671	24.850	32 1/2	100.531	804.25			
10 1/2	2.25965	.1219	13 3/4	17.868	25.406	33	101.316	816.86			
11	2.30878	.1270	14	18.064	25.967	33 1/4	102.102	829.58			
11 1/4	2.35791	.1321	14 1/4	18.261	26.535	33 1/2	102.887	842.39			
11 1/2	2.40704	.1372	14 1/2	18.457	27.109	34	103.673	855.30			
11 3/4	2.45617	.1423	14 3/4	18.653	27.688	34 1/4	104.458	868.31			
12	2.50530	.1474	15	18.850	28.274	34 1/2	105.243	881.41			
12 1/4	2.55443	.1525	15 1/4	19.046	28.861	34 3/4	106.029	894.62			
12 1/2	2.60356	.1576	15 1/2	19.242	29.465	35	106.814	907.92			
12 3/4	2.65269	.1627	15 3/4	19.438	30.070	35 1/4	107.600	921.32			
13	2.70182	.1678	16	19.635	30.680	35 1/2	108.385	934.82			
13 1/4	2.75095	.1729	16 1/4	19.831	31.295	35 3/4	109.170	948.42			
13 1/2	2.80008	.1780	16 1/2	20.028	31.915	36	109.956	962.11			
13 3/4	2.84921	.1831	16 3/4	20.224	32.535	36 1/4	110.741	975.91			
14	2.89834	.1882	17	20.420	33.163	36 1/2	111.527	989.90			
14 1/4	2.94747	.1933	17 1/4	20.617	33.793	36 3/4	112.312	1003.60			
14 1/2	2.99660	.1984	17 1/2	20.813	34.422	37	113.097	1017.90			
14 3/4	3.04573	.2035	18	21.010	35.052	37 1/4	113.883	1032.10			
15	3.09486	.2086	18 1/4	21.206	35.682	37 1/2	114.668	1046.30			
15 1/4	3.14399	.2137	18 1/2	21.403	36.312	38	115.454	1060.70			
15 1/2	3.19312	.2188	18 3/4	21.600	36.942						
15 3/4	3.24225	.2239	19	21.796	37.572						
16	3.29138	.2290	19 1/4	21.993	38.202						
16 1/4	3.34051	.2341	19 1/2	22.189	38.832						
16 1/2	3.38964	.2392	19 3/4	22.386	39.462						
16 3/4	3.43877	.2443	20	22.582	40.092						
17	3.48790	.2494	20 1/4	22.779	40.722						
17 1/4	3.53703	.2545	20 1/2	22.975	41.352						
17 1/2	3.58616	.2596	20 3/4	23.172	41.982						
17 3/4	3.63529	.2647	21	23.368	42.612						
18	3.68442	.2698	21 1/4	23.565	43.242						
18 1/4	3.73355	.2749	21 1/2	23.761	43.872						
18 1/2	3.78268	.2800	21 3/4	23.958	44.502						
18 3/4	3.83181	.2851	22	24.154	45.132						
19	3.88094	.2902	22 1/4	24.351	45.762						
19 1/4	3.93007	.2953	22 1/2	24.548	46.392						
19 1/2	3.97920	.3004	22 3/4	24.744	47.022						
19 3/4	4.02833	.3055	23	24.941	47.652						
20	4.07746	.3106	23 1/4	25.137	48.282						
20 1/4	4.12659	.3157	23 1/2	25.334	48.912						
20 1/2	4.17572	.3208	23 3/4	25.530	49.542						
20 3/4	4.22485	.3259	24	25.727	50.172						
21	4.27398	.3310	24 1/4	25.923	50.802						
21 1/4	4.32311	.3361	24 1/2	26.120	51.432						
21 1/2	4.37224	.3412	24 3/4	26.316	52.062						
21 3/4	4.42137	.3463	25	26.513	52.692						
22	4.47050	.3514									



# DIRECT CONVERSION BETWEEN MILLIMETERS, FEET, & INCHES (Nearest 1/64 in.)

TABLES M-4

1 mm thru 900 mm										3/64 in. thru 2 ft. 7 1/2 in.										
mm	ft.	in.	mm	ft.	in.	mm	ft.	in.	mm	ft.	in.	mm	ft.	in.	mm	ft.	in.	mm	ft.	
1	0	0 3/64	101	0	3 31/32	201	0	7 29/32	301	0	11 27/32	401	1	3 23/32	501	1	7 23/32	601	2	3 19/32
2	0	0 1/8	102	0	4 1/16	202	0	8 1/4	302	0	12 1/8	402	1	3 55/64	502	1	7 51/64	602	2	3 41/64
3	0	0 1/8	103	0	4 1/16	203	0	8 1/4	303	0	12 1/8	403	1	3 55/64	503	1	7 51/64	603	2	3 41/64
4	0	0 1/8	104	0	4 1/16	204	0	8 1/4	304	0	12 1/8	404	1	3 55/64	504	1	7 51/64	604	2	3 41/64
5	0	0 1/8	105	0	4 1/16	205	0	8 1/4	305	0	12 1/8	405	1	3 55/64	505	1	7 51/64	605	2	3 41/64
6	0	0 1/8	106	0	4 1/16	206	0	8 1/4	306	0	12 1/8	406	1	3 55/64	506	1	7 51/64	606	2	3 41/64
7	0	0 1/8	107	0	4 1/16	207	0	8 1/4	307	0	12 1/8	407	1	3 55/64	507	1	7 51/64	607	2	3 41/64
8	0	0 1/8	108	0	4 1/16	208	0	8 1/4	308	0	12 1/8	408	1	3 55/64	508	1	7 51/64	608	2	3 41/64
9	0	0 1/8	109	0	4 1/16	209	0	8 1/4	309	0	12 1/8	409	1	3 55/64	509	1	7 51/64	609	2	3 41/64
10	0	0 1/8	110	0	4 1/16	210	0	8 1/4	310	0	12 1/8	410	1	3 55/64	510	1	7 51/64	610	2	3 41/64
11	0	0 1/8	111	0	4 1/16	211	0	8 1/4	311	0	12 1/8	411	1	3 55/64	511	1	7 51/64	611	2	3 41/64
12	0	0 1/8	112	0	4 1/16	212	0	8 1/4	312	0	12 1/8	412	1	3 55/64	512	1	7 51/64	612	2	3 41/64
13	0	0 1/8	113	0	4 1/16	213	0	8 1/4	313	0	12 1/8	413	1	3 55/64	513	1	7 51/64	613	2	3 41/64
14	0	0 1/8	114	0	4 1/16	214	0	8 1/4	314	0	12 1/8	414	1	3 55/64	514	1	7 51/64	614	2	3 41/64
15	0	0 1/8	115	0	4 1/16	215	0	8 1/4	315	0	12 1/8	415	1	3 55/64	515	1	7 51/64	615	2	3 41/64
16	0	0 1/8	116	0	4 1/16	216	0	8 1/4	316	0	12 1/8	416	1	3 55/64	516	1	7 51/64	616	2	3 41/64
17	0	0 1/8	117	0	4 1/16	217	0	8 1/4	317	0	12 1/8	417	1	3 55/64	517	1	7 51/64	617	2	3 41/64
18	0	0 1/8	118	0	4 1/16	218	0	8 1/4	318	0	12 1/8	418	1	3 55/64	518	1	7 51/64	618	2	3 41/64
19	0	0 1/8	119	0	4 1/16	219	0	8 1/4	319	0	12 1/8	419	1	3 55/64	519	1	7 51/64	619	2	3 41/64
20	0	0 1/8	120	0	4 1/16	220	0	8 1/4	320	0	12 1/8	420	1	3 55/64	520	1	7 51/64	620	2	3 41/64
21	0	0 1/8	121	0	4 1/16	221	0	8 1/4	321	0	12 1/8	421	1	3 55/64	521	1	7 51/64	621	2	3 41/64
22	0	0 1/8	122	0	4 1/16	222	0	8 1/4	322	0	12 1/8	422	1	3 55/64	522	1	7 51/64	622	2	3 41/64
23	0	0 1/8	123	0	4 1/16	223	0	8 1/4	323	0	12 1/8	423	1	3 55/64	523	1	7 51/64	623	2	3 41/64
24	0	0 1/8	124	0	4 1/16	224	0	8 1/4	324	0	12 1/8	424	1	3 55/64	524	1	7 51/64	624	2	3 41/64
25	0	0 1/8	125	0	4 1/16	225	0	8 1/4	325	0	12 1/8	425	1	3 55/64	525	1	7 51/64	625	2	3 41/64
26	0	0 1/8	126	0	4 1/16	226	0	8 1/4	326	0	12 1/8	426	1	3 55/64	526	1	7 51/64	626	2	3 41/64
27	0	0 1/8	127	0	4 1/16	227	0	8 1/4	327	0	12 1/8	427	1	3 55/64	527	1	7 51/64	627	2	3 41/64
28	0	0 1/8	128	0	4 1/16	228	0	8 1/4	328	0	12 1/8	428	1	3 55/64	528	1	7 51/64	628	2	3 41/64
29	0	0 1/8	129	0	4 1/16	229	0	8 1/4	329	0	12 1/8	429	1	3 55/64	529	1	7 51/64	629	2	3 41/64
30	0	0 1/8	130	0	4 1/16	230	0	8 1/4	330	0	12 1/8	430	1	3 55/64	530	1	7 51/64	630	2	3 41/64
31	0	0 1/8	131	0	4 1/16	231	0	8 1/4	331	0	12 1/8	431	1	3 55/64	531	1	7 51/64	631	2	3 41/64
32	0	0 1/8	132	0	4 1/16	232	0	8 1/4	332	0	12 1/8	432	1	3 55/64	532	1	7 51/64	632	2	3 41/64
33	0	0 1/8	133	0	4 1/16	233	0	8 1/4	333	0	12 1/8	433	1	3 55/64	533	1	7 51/64	633	2	3 41/64
34	0	0 1/8	134	0	4 1/16	234	0	8 1/4	334	0	12 1/8	434	1	3 55/64	534	1	7 51/64	634	2	3 41/64
35	0	0 1/8	135	0	4 1/16	235	0	8 1/4	335	0	12 1/8	435	1	3 55/64	535	1	7 51/64	635	2	3 41/64
36	0	0 1/8	136	0	4 1/16	236	0	8 1/4	336	0	12 1/8	436	1	3 55/64	536	1	7 51/64	636	2	3 41/64
37	0	0 1/8	137	0	4 1/16	237	0	8 1/4	337	0	12 1/8	437	1	3 55/64	537	1	7 51/64	637	2	3 41/64
38	0	0 1/8	138	0	4 1/16	238	0	8 1/4	338	0	12 1/8	438	1	3 55/64	538	1	7 51/64	638	2	3 41/64
39	0	0 1/8	139	0	4 1/16	239	0	8 1/4	339	0	12 1/8	439	1	3 55/64	539	1	7 51/64	639	2	3 41/64
40	0	0 1/8	140	0	4 1/16	240	0	8 1/4	340	0	12 1/8	440	1	3 55/64	540	1	7 51/64	640	2	3 41/64
41	0	0 1/8	141	0	4 1/16	241	0	8 1/4	341	0	12 1/8	441	1	3 55/64	541	1	7 51/64	641	2	3 41/64
42	0	0 1/8	142	0	4 1/16	242	0	8 1/4	342	0	12 1/8	442	1	3 55/64	542	1	7 51/64	642	2	3 41/64
43	0	0 1/8	143	0	4 1/16	243	0	8 1/4	343	0	12 1/8	443	1	3 55/64	543	1	7 51/64	643	2	3 41/64
44	0	0 1/8	144	0	4 1/16	244	0	8 1/4	344	0	12 1/8	444	1	3 55/64	544	1	7 51/64	644	2	3 41/64
45	0	0 1/8	145	0	4 1/16	245	0	8 1/4	345	0	12 1/8	445	1	3 55/64	545	1	7 51/64	645	2	3 41/64
46	0	0 1/8	146	0	4 1/16	246	0	8 1/4	346	0	12 1/8	446	1	3 55/64	546	1	7 51/64	646	2	3 41/64
47	0	0 1/8	147	0	4 1/16	247	0	8 1/4	347	0	12 1/8	447	1	3 55/64	547	1	7 51/64	647	2	3 41/64
48	0	0 1/8	148	0	4 1/16	248	0	8 1/4	348	0	12 1/8	448	1	3 55/64	548	1	7 51/64	648	2	3 41/64
49	0	0 1/8	149	0	4 1/16	249	0	8 1/4	349	0	12 1/8	449	1	3 55/64	549	1	7 51/64	649	2	3 41/64
50	0	0 1/8	150	0	4 1/16	250	0	8 1/4	350	0	12 1/8	450	1	3 55/64	550	1	7 51/64	650	2	3 41/64
51	0	0 1/8	151	0	4 1/16	251	0	8 1/4	351	0	12 1/8	451	1	3 55/64	551	1	7 51/64	651	2	3 41/64
52	0	0 1/8	152	0	4 1/16	252	0	8 1/4	352	0	12 1/8	452	1	3 55/64	552	1	7 51/64	652	2	3 41/64
53	0	0 1/8	153	0	4 1/16	253	0	8 1/4	353	0	12 1/8	453	1	3 55/64	553	1	7 51/64	653	2	3 41/64
54	0	0 1/8	154	0	4 1/16	254	0	8 1/4	354	0	12 1/8	454	1	3 55/64	554	1	7 51/64	654	2	3 41/64
55	0	0 1/8	155	0	4 1/16	255	0	8 1/4	355	0	12 1/8	455	1	3 55/64	555	1	7 51/64	655	2	3 41/64
56	0	0 1/8	156	0	4 1/16	256	0	8 1/4	356	0	12 1/8	456	1	3 55/64	556	1	7 51/64	656	2	3 41/64
57	0	0 1/8	157																	

# DIRECT CONVERSION BETWEEN MILLIMETERS, FEET, & INCHES (Nearest 1/64 in.)

TABLES M-4

801 mm thru 1600 mm			2 ft 7-17/32 in. thro 5 ft 2-53/64 in.		
mm	ft.	in.	mm	ft.	in.
801	2 7/16	2 11/16	1501	4 7/8	4 11/16
802	2 7/16	2 11/16	1502	4 7/8	4 11/16
803	2 7/16	2 11/16	1503	4 7/8	4 11/16
804	2 7/16	2 11/16	1504	4 7/8	4 11/16
805	2 7/16	2 11/16	1505	4 7/8	4 11/16
806	2 7/16	2 11/16	1506	4 7/8	4 11/16
807	2 7/16	2 11/16	1507	4 7/8	4 11/16
808	2 7/16	2 11/16	1508	4 7/8	4 11/16
809	2 7/16	2 11/16	1509	4 7/8	4 11/16
810	2 7/16	2 11/16	1510	4 7/8	4 11/16
811	2 7/16	2 11/16	1511	4 7/8	4 11/16
812	2 7/16	2 11/16	1512	4 7/8	4 11/16
813	2 7/16	2 11/16	1513	4 7/8	4 11/16
814	2 7/16	2 11/16	1514	4 7/8	4 11/16
815	2 7/16	2 11/16	1515	4 7/8	4 11/16
816	2 7/16	2 11/16	1516	4 7/8	4 11/16
817	2 7/16	2 11/16	1517	4 7/8	4 11/16
818	2 7/16	2 11/16	1518	4 7/8	4 11/16
819	2 7/16	2 11/16	1519	4 7/8	4 11/16
820	2 7/16	2 11/16	1520	4 7/8	4 11/16
821	2 7/16	2 11/16	1521	4 7/8	4 11/16
822	2 7/16	2 11/16	1522	4 7/8	4 11/16
823	2 7/16	2 11/16	1523	4 7/8	4 11/16
824	2 7/16	2 11/16	1524	4 7/8	4 11/16
825	2 7/16	2 11/16	1525	4 7/8	4 11/16
826	2 7/16	2 11/16	1526	4 7/8	4 11/16
827	2 7/16	2 11/16	1527	4 7/8	4 11/16
828	2 7/16	2 11/16	1528	4 7/8	4 11/16
829	2 7/16	2 11/16	1529	4 7/8	4 11/16
830	2 7/16	2 11/16	1530	4 7/8	4 11/16
831	2 7/16	2 11/16	1531	4 7/8	4 11/16
832	2 7/16	2 11/16	1532	4 7/8	4 11/16
833	2 7/16	2 11/16	1533	4 7/8	4 11/16
834	2 7/16	2 11/16	1534	4 7/8	4 11/16
835	2 7/16	2 11/16	1535	4 7/8	4 11/16
836	2 7/16	2 11/16	1536	4 7/8	4 11/16
837	2 7/16	2 11/16	1537	4 7/8	4 11/16
838	2 7/16	2 11/16	1538	4 7/8	4 11/16
839	2 7/16	2 11/16	1539	4 7/8	4 11/16
840	2 7/16	2 11/16	1540	4 7/8	4 11/16
841	2 7/16	2 11/16	1541	4 7/8	4 11/16
842	2 7/16	2 11/16	1542	4 7/8	4 11/16
843	2 7/16	2 11/16	1543	4 7/8	4 11/16
844	2 7/16	2 11/16	1544	4 7/8	4 11/16
845	2 7/16	2 11/16	1545	4 7/8	4 11/16
846	2 7/16	2 11/16	1546	4 7/8	4 11/16
847	2 7/16	2 11/16	1547	4 7/8	4 11/16
848	2 7/16	2 11/16	1548	4 7/8	4 11/16
849	2 7/16	2 11/16	1549	4 7/8	4 11/16
850	2 7/16	2 11/16	1550	4 7/8	4 11/16
851	2 7/16	2 11/16	1551	4 7/8	4 11/16
852	2 7/16	2 11/16	1552	4 7/8	4 11/16
853	2 7/16	2 11/16	1553	4 7/8	4 11/16
854	2 7/16	2 11/16	1554	4 7/8	4 11/16
855	2 7/16	2 11/16	1555	4 7/8	4 11/16
856	2 7/16	2 11/16	1556	4 7/8	4 11/16
857	2 7/16	2 11/16	1557	4 7/8	4 11/16
858	2 7/16	2 11/16	1558	4 7/8	4 11/16
859	2 7/16	2 11/16	1559	4 7/8	4 11/16
860	2 7/16	2 11/16	1560	4 7/8	4 11/16
861	2 7/16	2 11/16	1561	4 7/8	4 11/16
862	2 7/16	2 11/16	1562	4 7/8	4 11/16
863	2 7/16	2 11/16	1563	4 7/8	4 11/16
864	2 7/16	2 11/16	1564	4 7/8	4 11/16
865	2 7/16	2 11/16	1565	4 7/8	4 11/16
866	2 7/16	2 11/16	1566	4 7/8	4 11/16
867	2 7/16	2 11/16	1567	4 7/8	4 11/16
868	2 7/16	2 11/16	1568	4 7/8	4 11/16
869	2 7/16	2 11/16	1569	4 7/8	4 11/16
870	2 7/16	2 11/16	1570	4 7/8	4 11/16
871	2 7/16	2 11/16	1571	4 7/8	4 11/16
872	2 7/16	2 11/16	1572	4 7/8	4 11/16
873	2 7/16	2 11/16	1573	4 7/8	4 11/16
874	2 7/16	2 11/16	1574	4 7/8	4 11/16
875	2 7/16	2 11/16	1575	4 7/8	4 11/16
876	2 7/16	2 11/16	1576	4 7/8	4 11/16
877	2 7/16	2 11/16	1577	4 7/8	4 11/16
878	2 7/16	2 11/16	1578	4 7/8	4 11/16
879	2 7/16	2 11/16	1579	4 7/8	4 11/16
880	2 7/16	2 11/16	1580	4 7/8	4 11/16
881	2 7/16	2 11/16	1581	4 7/8	4 11/16
882	2 7/16	2 11/16	1582	4 7/8	4 11/16
883	2 7/16	2 11/16	1583	4 7/8	4 11/16
884	2 7/16	2 11/16	1584	4 7/8	4 11/16
885	2 7/16	2 11/16	1585	4 7/8	4 11/16
886	2 7/16	2 11/16	1586	4 7/8	4 11/16
887	2 7/16	2 11/16	1587	4 7/8	4 11/16
888	2 7/16	2 11/16	1588	4 7/8	4 11/16
889	2 7/16	2 11/16	1589	4 7/8	4 11/16
890	2 7/16	2 11/16	1590	4 7/8	4 11/16
891	2 7/16	2 11/16	1591	4 7/8	4 11/16
892	2 7/16	2 11/16	1592	4 7/8	4 11/16
893	2 7/16	2 11/16	1593	4 7/8	4 11/16
894	2 7/16	2 11/16	1594	4 7/8	4 11/16
895	2 7/16	2 11/16	1595	4 7/8	4 11/16
896	2 7/16	2 11/16	1596	4 7/8	4 11/16
897	2 7/16	2 11/16	1597	4 7/8	4 11/16
898	2 7/16	2 11/16	1598	4 7/8	4 11/16
899	2 7/16	2 11/16	1599	4 7/8	4 11/16
900	2 7/16	2 11/16	1600	4 7/8	4 11/16

CONTINUED

# **DIRECT CONVERSION BETWEEN MILLIMETERS, FEET, & INCHES [Nearest 1/64 in.]**

TABLES M-4

1/64 in. thru 2400 mm			5 ft. 3-1/32 in. thru 7 ft. 10-31/64 in.		
mm	ft.	in.	mm	ft.	in.
1401	5 3/16	1 1/32	2201	7 2 11/16	2 11/32
1402	5 3/16	1 1/32	2202	7 2 11/16	2 11/32
1403	5 3/16	1 1/32	2203	7 2 11/16	2 11/32
1404	5 3/16	1 1/32	2204	7 2 11/16	2 11/32
1405	5 3/16	1 1/32	2205	7 2 11/16	2 11/32
1406	5 3/16	1 1/32	2206	7 2 11/16	2 11/32
1407	5 3/16	1 1/32	2207	7 2 11/16	2 11/32
1408	5 3/16	1 1/32	2208	7 2 11/16	2 11/32
1409	5 3/16	1 1/32	2209	7 2 11/16	2 11/32
1410	5 3/16	1 1/32	2210	7 2 11/16	2 11/32
1411	5 3/16	1 1/32	2211	7 2 11/16	2 11/32
1412	5 3/16	1 1/32	2212	7 2 11/16	2 11/32
1413	5 3/16	1 1/32	2213	7 2 11/16	2 11/32
1414	5 3/16	1 1/32	2214	7 2 11/16	2 11/32
1415	5 3/16	1 1/32	2215	7 2 11/16	2 11/32
1416	5 3/16	1 1/32	2216	7 2 11/16	2 11/32
1417	5 3/16	1 1/32	2217	7 2 11/16	2 11/32
1418	5 3/16	1 1/32	2218	7 2 11/16	2 11/32
1419	5 3/16	1 1/32	2219	7 2 11/16	2 11/32
1420	5 3/16	1 1/32	2220	7 2 11/16	2 11/32
1421	5 3/16	1 1/32	2221	7 2 11/16	2 11/32
1422	5 3/16	1 1/32	2222	7 2 11/16	2 11/32
1423	5 3/16	1 1/32	2223	7 2 11/16	2 11/32
1424	5 3/16	1 1/32	2224	7 2 11/16	2 11/32
1425	5 3/16	1 1/32	2225	7 2 11/16	2 11/32
1426	5 3/16	1 1/32	2226	7 2 11/16	2 11/32
1427	5 3/16	1 1/32	2227	7 2 11/16	2 11/32
1428	5 3/16	1 1/32	2228	7 2 11/16	2 11/32
1429	5 3/16	1 1/32	2229	7 2 11/16	2 11/32
1430	5 3/16	1 1/32	2230	7 2 11/16	2 11/32
1431	5 3/16	1 1/32	2231	7 2 11/16	2 11/32
1432	5 3/16	1 1/32	2232	7 2 11/16	2 11/32
1433	5 3/16	1 1/32	2233	7 2 11/16	2 11/32
1434	5 3/16	1 1/32	2234	7 2 11/16	2 11/32
1435	5 3/16	1 1/32	2235	7 2 11/16	2 11/32
1436	5 3/16	1 1/32	2236	7 2 11/16	2 11/32
1437	5 3/16	1 1/32	2237	7 2 11/16	2 11/32
1438	5 3/16	1 1/32	2238	7 2 11/16	2 11/32
1439	5 3/16	1 1/32	2239	7 2 11/16	2 11/32
1440	5 3/16	1 1/32	2240	7 2 11/16	2 11/32
1441	5 3/16	1 1/32	2241	7 2 11/16	2 11/32
1442	5 3/16	1 1/32	2242	7 2 11/16	2 11/32
1443	5 3/16	1 1/32	2243	7 2 11/16	2 11/32
1444	5 3/16	1 1/32	2244	7 2 11/16	2 11/32
1445	5 3/16	1 1/32	2245	7 2 11/16	2 11/32
1446	5 3/16	1 1/32	2246	7 2 11/16	2 11/32
1447	5 3/16	1 1/32	2247	7 2 11/16	2 11/32
1448	5 3/16	1 1/32	2248	7 2 11/16	2 11/32
1449	5 3/16	1 1/32	2249	7 2 11/16	2 11/32
1450	5 3/16	1 1/32	2250	7 2 11/16	2 11/32
1451	5 3/16	1 1/32	2251	7 2 11/16	2 11/32
1452	5 3/16	1 1/32	2252	7 2 11/16	2 11/32
1453	5 3/16	1 1/32	2253	7 2 11/16	2 11/32
1454	5 3/16	1 1/32	2254	7 2 11/16	2 11/32
1455	5 3/16	1 1/32	2255	7 2 11/16	2 11/32
1456	5 3/16	1 1/32	2256	7 2 11/16	2 11/32
1457	5 3/16	1 1/32	2257	7 2 11/16	2 11/32
1458	5 3/16	1 1/32	2258	7 2 11/16	2 11/32
1459	5 3/16	1 1/32	2259	7 2 11/16	2 11/32
1460	5 3/16	1 1/32	2260	7 2 11/16	2 11/32
1461	5 3/16	1 1/32	2261	7 2 11/16	2 11/32
1462	5 3/16	1 1/32	2262	7 2 11/16	2 11/32
1463	5 3/16	1 1/32	2263	7 2 11/16	2 11/32
1464	5 3/16	1 1/32	2264	7 2 11/16	2 11/32
1465	5 3/16	1 1/32	2265	7 2 11/16	2 11/32
1466	5 3/16	1 1/32	2266	7 2 11/16	2 11/32
1467	5 3/16	1 1/32	2267	7 2 11/16	2 11/32
1468	5 3/16	1 1/32	2268	7 2 11/16	2 11/32
1469	5 3/16	1 1/32	2269	7 2 11/16	2 11/32
1470	5 3/16	1 1/32	2270	7 2 11/16	2 11/32
1471	5 3/16	1 1/32	2271	7 2 11/16	2 11/32
1472	5 3/16	1 1/32	2272	7 2 11/16	2 11/32
1473	5 3/16	1 1/32	2273	7 2 11/16	2 11/32
1474	5 3/16	1 1/32	2274	7 2 11/16	2 11/32
1475	5 3/16	1 1/32	2275	7 2 11/16	2 11/32
1476	5 3/16	1 1/32	2276	7 2 11/16	2 11/32
1477	5 3/16	1 1/32	2277	7 2 11/16	2 11/32
1478	5 3/16	1 1/32	2278	7 2 11/16	2 11/32
1479	5 3/16	1 1/32	2279	7 2 11/16	2 11/32
1480	5 3/16	1 1/32	2280	7 2 11/16	2 11/32
1481	5 3/16	1 1/32	2281	7 2 11/16	2 11/32
1482	5 3/16	1 1/32	2282	7 2 11/16	2 11/32
1483	5 3/16	1 1/32	2283	7 2 11/16	2 11/32
1484	5 3/16	1 1/32	2284	7 2 11/16	2 11/32
1485	5 3/16	1 1/32	2285	7 2 11/16	2 11/32
1486	5 3/16	1 1/32	2286	7 2 11/16	2 11/32
1487	5 3/16	1 1/32	2287	7 2 11/16	2 11/32
1488	5 3/16	1 1/32	2288	7 2 11/16	2 11/32
1489	5 3/16	1 1/32	2289	7 2 11/16	2 11/32
1490	5 3/16	1 1/32	2290	7 2 11/16	2 11/32
1491	5 3/16	1 1/32	2291	7 2 11/16	2 11/32
1492	5 3/16	1 1/32	2292	7 2 11/16	2 11/32
1493	5 3/16	1 1/32	2293	7 2 11/16	2 11/32
1494	5 3/16	1 1/32	2294	7 2 11/16	2 11/32
1495	5 3/16	1 1/32	2295	7 2 11/16	2 11/32
1496	5 3/16	1 1/32	2296	7 2 11/16	2 11/32
1497	5 3/16	1 1/32	2297	7 2 11/16	2 11/32
1498	5 3/16	1 1/32	2298	7 2 11/16	2 11/32
1499	5 3/16	1 1/32	2299	7 2 11/16	2 11/32
1500	5 3/16	1 1/32	2300	7 2 11/16	2 11/32

**DIRECT CONVERSION BETWEEN MILLIMETERS, FEET, & INCHES (Nearest 1/64 in.)**

## TABLES M-4

2401 mm thru 3200 mm										7 ft. 10-17/32 in. thru 10 ft. 5-63/64 in.									
mm	ft.	in.	mm	ft.	in.	mm	ft.	in.	mm	ft.	in.	mm	ft.	in.	mm	ft.	in.		
2401	7 10 17/32	2501	8 2 15/32	2601	8 6 13/32	2701	8 10 11/32	2801	9 2 9/32	2901	9 6 7/32	3001	9 10 5/32	3101	10 2 3/32				
2402	7 10 9/16	2502	8 2 1/2	2602	8 6 7/16	2702	8 10 3/8	2802	9 2 23/64	2902	9 6 1/4	3002	9 10 3/16	3102	10 2 1/8				
2403	7 10 39/64	2503	8 2 35/64	2603	8 6 31/64	2703	8 10 27/64	2803	9 2 23/64	2903	9 6 19/64	3003	9 10 15/64	3103	10 2 11/64				
2404	7 10 41/64	2504	8 2 37/64	2604	8 6 33/64	2704	8 10 29/64	2804	9 2 25/64	2904	9 6 21/64	3004	9 10 17/64	3104	10 2 13/64				
2405	7 10 11/16	2505	8 2 5/8	2605	8 6 9/16	2705	8 10 1/2	2805	9 2 13/16	2905	9 6 1/2	3005	9 10 1/4	3105	10 2 1/2				
2406	7 10 23/32	2506	8 2 21/32	2606	8 6 17/32	2706	8 10 17/32	2806	9 2 15/16	2906	9 6 13/16	3006	9 10 11/16	3106	10 2 5/8				
2407	7 10 5/8	2507	8 2 1/2	2607	8 6 1/2	2707	8 10 3/4	2807	9 2 3/4	2907	9 6 5/8	3007	9 10 3/4	3107	10 2 3/4				
2408	7 10 21/16	2508	8 2 11/16	2608	8 6 11/16	2708	8 10 5/8	2808	9 2 3/4	2908	9 6 5/8	3008	9 10 3/4	3108	10 2 3/4				
2409	7 10 23/16	2509	8 2 13/16	2609	8 6 13/16	2709	8 10 5/8	2809	9 2 3/4	2909	9 6 5/8	3009	9 10 3/4	3109	10 2 3/4				
2410	7 10 7/8	2510	8 2 3/4	2610	8 6 3/4	2710	8 10 11/16	2810	9 2 5/8	2910	9 6 1/2	3010	9 10 1/2	3110	10 2 1/2				
2411	7 10 59/64	2511	8 2 55/64	2611	8 6 51/64	2711	8 10 47/64	2811	9 2 43/64	2911	9 6 39/64	3011	9 10 35/64	3111	10 2 31/64				
2412	7 10 11/64	2512	8 2 55/64	2612	8 6 51/64	2712	8 10 47/64	2812	9 2 43/64	2912	9 6 39/64	3012	9 10 35/64	3112	10 2 31/64				
2413	7 11 3/64	2513	8 2 15/16	2613	8 6 7/8	2713	8 10 13/16	2813	9 2 45/64	2913	9 6 41/64	3013	9 10 37/64	3113	10 2 33/64				
2414	7 11 1/8	2514	8 2 31/64	2614	8 6 29/32	2714	8 10 27/32	2814	9 2 3/4	2914	9 6 23/32	3014	9 10 21/32	3114	10 2 19/32				
2415	7 11 1/4	2515	8 2 3/4	2615	8 6 1/2	2715	8 10 5/8	2815	9 2 5/8	2915	9 6 49/64	3015	9 10 45/64	3115	10 2 43/64				
2416	7 11 5/8	2516	8 2 11/8	2616	8 6 5/4	2716	8 10 59/64	2816	9 2 53/64	2916	9 6 49/64	3016	9 10 45/64	3116	10 2 43/64				
2417	7 11 13/64	2517	8 2 3/32	2617	8 6 7/32	2717	8 10 11/32	2817	9 2 5/32	2917	9 6 51/64	3017	9 10 47/64	3117	10 2 45/64				
2418	7 11 15/64	2518	8 2 5/32	2618	8 6 9/32	2718	8 10 13/32	2818	9 2 7/32	2918	9 6 53/64	3018	9 10 49/64	3118	10 2 47/64				
2419	7 11 17/64	2519	8 2 7/32	2619	8 6 11/32	2719	8 10 15/32	2819	9 2 9/32	2919	9 6 55/64	3019	9 10 51/64	3119	10 2 49/64				
2420	7 11 19/64	2520	8 2 9/32	2620	8 6 13/32	2720	8 10 17/32	2820	9 2 11/32	2920	9 6 57/64	3020	9 10 53/64	3120	10 2 51/64				
2421	7 11 5/16	2521	8 2 11/16	2621	8 6 15/32	2721	8 10 19/32	2821	9 2 13/16	2921	9 6 59/64	3021	9 10 55/64	3121	10 2 53/64				
2422	7 11 7/16	2522	8 2 13/16	2622	8 6 17/32	2722	8 10 21/32	2822	9 2 15/16	2922	9 6 61/64	3022	9 10 57/64	3122	10 2 55/64				
2423	7 11 9/16	2523	8 2 15/16	2623	8 6 19/32	2723	8 10 23/32	2823	9 2 17/16	2923	9 6 63/64	3023	9 10 59/64	3123	10 2 57/64				
2424	7 11 11/16	2524	8 2 17/16	2624	8 6 21/32	2724	8 10 25/32	2824	9 2 19/16	2924	9 6 65/64	3024	9 10 61/64	3124	10 2 59/64				
2425	7 11 13/16	2525	8 2 19/16	2625	8 6 23/32	2725	8 10 27/32	2825	9 2 21/16	2925	9 6 67/64	3025	9 10 63/64	3125	10 2 61/64				
2426	7 11 15/16	2526	8 2 21/16	2626	8 6 25/32	2726	8 10 29/32	2826	9 2 23/16	2926	9 6 69/64	3026	9 10 65/64	3126	10 2 63/64				
2427	7 11 31/64	2527	8 2 31/64	2627	8 6 25/64	2727	8 10 23/64	2827	9 2 19/64	2927	9 6 15/64	3027	9 10 11/64	3127	10 2 7/64				
2428	7 11 1/32	2528	8 2 1/32	2628	8 6 1/32	2728	8 10 1/32	2828	9 2 1/32	2928	9 6 1/32	3028	9 10 1/32	3128	10 2 1/32				
2429	7 11 5/8	2529	8 2 1/8	2629	8 6 1/8	2729	8 10 1/8	2829	9 2 1/8	2929	9 6 1/8	3029	9 10 1/8	3129	10 2 1/8				
2430	7 11 3/4	2530	8 2 3/4	2630	8 6 3/4	2730	8 10 3/4	2830	9 2 3/4	2930	9 6 3/4	3030	9 10 3/4	3130	10 2 3/4				
2431	7 11 45/64	2531	8 2 41/64	2631	8 6 37/64	2731	8 10 33/64	2831	9 2 29/64	2931	9 6 25/64	3031	9 10 21/64	3131	10 2 17/64				
2432	7 11 1/2	2532	8 2 1/2	2632	8 6 1/2	2732	8 10 1/2	2832	9 2 1/2	2932	9 6 1/2	3032	9 10 1/2	3132	10 2 1/2				
2433	7 11 5/32	2533	8 2 1/32	2633	8 6 1/32	2733	8 10 1/32	2833	9 2 1/32	2933	9 6 1/32	3033	9 10 1/32	3133	10 2 1/32				
2434	7 11 3/64	2534	8 2 3/64	2634	8 6 3/64	2734	8 10 3/64	2834	9 2 3/64	2934	9 6 3/64	3034	9 10 3/64	3134	10 2 3/64				
2435	7 11 1/64	2535	8 2 1/64	2635	8 6 1/64	2735	8 10 1/64	2835	9 2 1/64	2935	9 6 1/64	3035	9 10 1/64	3135	10 2 1/64				
2436	7 11 1/8	2536	8 2 1/8	2636	8 6 1/8	2736	8 10 1/8	2836	9 2 1/8	2936	9 6 1/8	3036	9 10 1/8	3136	10 2 1/8				
2437	7 11 1/4	2537	8 2 1/4	2637	8 6 1/4	2737	8 10 1/4	2837	9 2 1/4	2937	9 6 1/4	3037	9 10 1/4	3137	10 2 1/4				
2438	7 11 3/8	2538	8 2 3/8	2638	8 6 3/8	2738	8 10 3/8	2838	9 2 3/8	2938	9 6 3/8	3038	9 10 3/8	3138	10 2 3/8				
2439	7 11 1/2	2539	8 2 1/2	2639	8 6 1/2	2739	8 10 1/2	2839	9 2 1/2	2939	9 6 1/2	3039	9 10 1/2	3139	10 2 1/2				
2440	7 11 5/16	2540	8 2 11/16	2640	8 6 15/32	2740	8 10 19/32	2840	9 2 13/16	2940	9 6 59/64	3040	9 10 55/64	3140	10 2 53/64				
2441	7 11 3/8	2541	8 2 3/8	2641	8 6 3/8	2741	8 10 3/8	2841	9 2 3/8	2941	9 6 3/8	3041	9 10 3/8	3141	10 2 3/8				
2442	7 11 1/4	2542	8 2 1/4	2642	8 6 1/4	2742	8 10 1/4	2842	9 2 1/4	2942	9 6 1/4	3042	9 10 1/4	3142	10 2 1/4				
2443	7 11 5/16	2543	8 2 11/16	2643	8 6 15/32	2743	8 10 19/32	2843	9 2 13/16	2943	9 6 59/64	3043	9 10 55/64	3143	10 2 53/64				
2444	7 11 3/8	2544	8 2 3/8	2644	8 6 3/8	2744	8 10 3/8	2844	9 2 3/8	2944	9 6 3/8	3044	9 10 3/8	3144	10 2 3/8				
2445	7 11 1/2	2545	8 2 1/2	2645	8 6 1/2	2745	8 10 1/2	2845	9 2 1/2	2945	9 6 1/2	3045	9 10 1/2	3145	10 2 1/2				
2446	7 11 5/8	2546	8 2 11/8	2646	8 6 5/4	2746	8 10 5/8	2846	9 2 3/4	2946	9 6 5/8	3046	9 10 3/4	3146	10 2 3/4				
2447	7 11 3/4	2547	8 2 3/4	2647	8 6 3/4	2747	8 10 3/4	2847	9 2 3/4	2947	9 6 3/4	3047	9 10 3/4	3147	10 2 3/4				
2448	7 11 15/16	2548	8 2 15/16	2648	8 6 15/16	2748	8 10 15/16	2848	9 2 15/16	2948	9 6 15/16	3048	9 10 15/16	3148	10 2 15/16				
2449	7 11 7/8	2549	8 2 7/8	2649	8 6 7/8	2749	8 10 7/8	2849	9 2 7/8	2949	9 6 7/8	3049	9 10 7/8	3149	10 2 7/8				
2450	7 11 1	2550	8 2 1	2650	8 6 1	2750	8 10 1	2850	9 2 1	2950	9 6 1	3050	9 10 1	3150	10 2 1				

**CONTINUED**

## DIRECT CONVERSION BETWEEN MILLIMETERS, FEET, &amp; INCHES (Nearest 1/64 in.)

TABLES M-4

2201 mm thru 4000 mm				10 ft. 6-1/32 in. thru 13 ft. 1-31/64 in.			
mm	ft.	in.	mm	mm	ft.	in.	mm
3201	10	6 1/32	3401	11	9 5/64	3601	12
3202	10	6 1/16	3402	11	9 1/32	3602	12
3203	10	6 3/64	3403	11	9 1/16	3603	12
3204	10	6 1/4	3404	11	9 1/8	3604	12
3205	10	6 5/64	3405	11	9 3/32	3605	12
3206	10	6 1/8	3406	11	9 1/4	3606	12
3207	10	6 3/32	3407	11	9 1/2	3607	12
3208	10	6 1/2	3408	11	9 5/16	3608	12
3209	10	6 5/16	3409	11	9 3/8	3609	12
3210	10	6 3/8	3410	11	9 7/16	3610	12
3211	10	6 1/2	3411	11	9 1/2	3611	12
3212	10	6 5/8	3412	11	9 3/4	3612	12
3213	10	6 3/4	3413	11	9 7/8	3613	12
3214	10	6 1/2	3414	11	9 15/16	3614	12
3215	10	6 3/4	3415	11	10	3615	12
3216	10	6 5/8	3416	11	10 1/64	3616	12
3217	10	6 1/2	3417	11	10 1/32	3617	12
3218	10	6 1/4	3418	11	10 1/16	3618	12
3219	10	6 3/8	3419	11	10 1/8	3619	12
3220	10	6 1/2	3420	11	10 3/16	3620	12
3221	10	6 5/8	3421	11	10 1/4	3621	12
3222	10	6 1/2	3422	11	10 3/8	3622	12
3223	10	6 3/4	3423	11	10 7/16	3623	12
3224	10	6 5/8	3424	11	10 1/2	3624	12
3225	10	6 3/4	3425	11	10 1/8	3625	12
3226	10	6 1/2	3426	11	10 1/4	3626	12
3227	10	6 3/8	3427	11	10 3/8	3627	12
3228	10	6 1/2	3428	11	10 7/8	3628	12
3229	10	6 3/4	3429	11	10 1/2	3629	12
3230	10	6 5/8	3430	11	10 3/4	3630	12
3231	10	6 1/2	3431	11	10 7/16	3631	12
3232	10	6 3/4	3432	11	10 1/4	3632	12
3233	10	6 5/8	3433	11	10 3/8	3633	12
3234	10	6 1/2	3434	11	10 7/8	3634	12
3235	10	6 3/4	3435	11	10 1/2	3635	12
3236	10	6 5/8	3436	11	10 3/4	3636	12
3237	10	6 1/2	3437	11	10 7/16	3637	12
3238	10	6 3/4	3438	11	10 1/4	3638	12
3239	10	6 5/8	3439	11	10 3/8	3639	12
3240	10	6 1/2	3440	11	10 7/8	3640	12
3241	10	6 3/4	3441	11	10 1/2	3641	12
3242	10	6 5/8	3442	11	10 3/4	3642	12
3243	10	6 1/2	3443	11	10 7/16	3643	12
3244	10	6 3/4	3444	11	10 1/4	3644	12
3245	10	6 5/8	3445	11	10 3/8	3645	12
3246	10	6 1/2	3446	11	10 7/8	3646	12
3247	10	6 3/4	3447	11	10 1/2	3647	12
3248	10	6 5/8	3448	11	10 3/4	3648	12
3249	10	6 1/2	3449	11	10 7/16	3649	12
3250	10	6 3/4	3450	11	10 1/4	3650	12
3251	10	6 5/8	3451	11	10 3/8	3651	12
3252	10	6 1/2	3452	11	10 7/8	3652	12
3253	10	6 3/4	3453	11	10 1/2	3653	12
3254	10	6 5/8	3454	11	10 3/4	3654	12
3255	10	6 1/2	3455	11	10 7/16	3655	12
3256	10	6 3/4	3456	11	10 1/4	3656	12
3257	10	6 5/8	3457	11	10 3/8	3657	12
3258	10	6 1/2	3458	11	10 7/8	3658	12
3259	10	6 3/4	3459	11	10 1/2	3659	12
3260	10	6 5/8	3460	11	10 3/4	3660	12
3261	10	6 1/2	3461	11	10 7/16	3661	12
3262	10	6 3/4	3462	11	10 1/4	3662	12
3263	10	6 5/8	3463	11	10 3/8	3663	12
3264	10	6 1/2	3464	11	10 7/8	3664	12
3265	10	6 3/4	3465	11	10 1/2	3665	12
3266	10	6 5/8	3466	11	10 3/4	3666	12
3267	10	6 1/2	3467	11	10 7/16	3667	12
3268	10	6 3/4	3468	11	10 1/4	3668	12
3269	10	6 5/8	3469	11	10 3/8	3669	12
3270	10	6 1/2	3470	11	10 7/8	3670	12
3271	10	6 3/4	3471	11	10 1/2	3671	12
3272	10	6 5/8	3472	11	10 3/4	3672	12
3273	10	6 1/2	3473	11	10 7/16	3673	12
3274	10	6 3/4	3474	11	10 1/4	3674	12
3275	10	6 5/8	3475	11	10 3/8	3675	12
3276	10	6 1/2	3476	11	10 7/8	3676	12
3277	10	6 3/4	3477	11	10 1/2	3677	12
3278	10	6 5/8	3478	11	10 3/4	3678	12
3279	10	6 1/2	3479	11	10 7/16	3679	12
3280	10	6 3/4	3480	11	10 1/4	3680	12
3281	10	6 5/8	3481	11	10 3/8	3681	12
3282	10	6 1/2	3482	11	10 7/8	3682	12
3283	10	6 3/4	3483	11	10 1/2	3683	12
3284	10	6 5/8	3484	11	10 3/4	3684	12
3285	10	6 1/2	3485	11	10 7/16	3685	12
3286	10	6 3/4	3486	11	10 1/4	3686	12
3287	10	6 5/8	3487	11	10 3/8	3687	12
3288	10	6 1/2	3488	11	10 7/8	3688	12
3289	10	6 3/4	3489	11	10 1/2	3689	12
3290	10	6 5/8	3490	11	10 3/4	3690	12
3291	10	6 1/2	3491	11	10 7/16	3691	12
3292	10	6 3/4	3492	11	10 1/4	3692	12
3293	10	6 5/8	3493	11	10 3/8	3693	12
3294	10	6 1/2	3494	11	10 7/8	3694	12
3295	10	6 3/4	3495	11	10 1/2	3695	12
3296	10	6 5/8	3496	11	10 3/4	3696	12
3297	10	6 1/2	3497	11	10 7/16	3697	12
3298	10	6 3/4	3498	11	10 1/4	3698	12
3299	10	6 5/8	3499	11	10 3/8	3699	12
3300	10	6 1/2	3500	11	10 7/8	3700	12

Rounded to nearest 1/64 in. (0.015625 in.)

CONTINUED







## TABLES M-4

18 ft 4-33/64 in. thro 20 ft 11-31/32 in.



# DECIMALS OF AN INCH & OF A FOOT

TABLE M-5

FRAC- TIONS OF AN INCH	DECIMAL EQUIVALENTS	FRAC- TIONS OF A FOOT	FRAC- TIONS OF AN INCH	DECIMAL EQUIVALENTS	FRAC- TIONS OF A FOOT	FRAC- TIONS OF AN INCH	DECIMAL EQUIVALENTS	FRAC- TIONS OF A FOOT	FRAC- TIONS OF AN INCH	DECIMAL EQUIVALENTS	FRAC- TIONS OF A FOOT
	.0052 .0104	1/16" 1/8"		.2552 .2604	3 1/16" 3/8"		.5052 .5104	6 1/16" 6 1/8"		.7552 .7604	9 1/16" 9 1/8"
1/16	.015625 .0208 .0260	1/4 1/4 1/4	1 1/16	.265625 .2708 .2760	3 3/16 3 1/4 3 1/4	3 3/4	.515625 .5208 .5260	6 3/16 6 1/4 6 3/4	4 3/4	.765625 .7708 .7760	9 3/16 9 1/4 9 3/4
1/8	.03125 .0365 .0417	1/2 1/4 1/2	1 1/8	.28125 .2865 .2917	3 1/2 3 3/4 3 1/2	1 1/2	.53125 .5365 .5417	6 3/8 6 3/4 6 1/2	2 1/2	.78125 .7865 .7917	9 1/2 9 1/4 9 1/2
3/16	.046875 .0521 .0573	3/8 3/8 1 1/16	1 1/4	.296875 .3021 .3073	3 5/8 3 3/4 3 11/16	3 3/4	.546875 .5521 .5573	6 5/8 6 3/4 6 11/16	3 1/4	.796875 .8021 .8073	9 5/8 9 3/4 9 11/16
1/4	.0625 .0677 .0729	1/2 1 1/8 1/2	1 1/2	.3125 .3177 .3229	3 3/4 3 13/16 3 3/4	3 3/4	.5625 .5677 .5729	6 3/4 6 13/16 6 3/4	1 3/8	.8125 .8177 .8229	9 3/4 9 13/16 9 3/4
5/16	.078125 .0833 .0885	1 1/8 1 1 1/8	1 3/4	.328125 .3333 .3385	3 7/8 4 4 1/16	3 3/4	.578125 .5833 .5885	6 7/8 7 7 1/16	5 3/4	.828125 .8333 .8385	9 3/4 10 10 1/16
3/8	.09375 .0990 .1042	1 1/4 1 1/8 1 1/4	1 1/2	.34375 .3490 .3542	4 1/8 4 3/8 4 1/4	1 1/2	.59375 .5990 .6042	7 1/8 7 3/8 7 1/4	2 3/8	.84375 .8490 .8542	10 1/8 10 1/4 10 1/4
7/16	.109375 .1146 .1198	1 3/8 1 1/2 1 3/8	2 3/4	.359375 .3646 .3698	4 3/8 4 3/4 4 7/16	3 3/4	.609375 .6146 .6198	7 3/8 7 3/4 7 3/4	5 3/4	.859375 .8646 .8698	10 3/8 10 3/4 10 3/4
1/2	.1250 .1302 .1354	1 1/2 1 1/4 1 1/2	3 3/4	.3750 .3802 .3854	4 1/2 4 1/2 4 3/4	3 3/4	.6250 .6302 .6354	7 1/2 7 3/4 7 3/4	7 3/4	.8750 .8802 .8854	10 1/2 10 3/4 10 3/4
9/16	.140625 .1458 .1510	1 5/8 1 3/4 1 3/4	3 3/4	.390625 .3958 .4010	4 5/8 4 3/4 4 3/4	4 1/4	.640625 .6458 .6510	7 5/8 7 3/4 7 13/16	5 3/4	.890625 .8958 .9010	10 5/8 10 3/4 10 13/16
5/8	.15625 .1615 .1667	1 3/4 1 3/4 2	1 3/2	.40625 .4115 .4167	4 3/4 4 5/8 5	2 1/2	.65625 .6615 .6667	7 3/4 7 3/4 8	2 3/2	.90625 .9115 .9167	10 3/4 10 3/4 11
11/16	.171875 .1771 .1823	2 1/8 2 1/4 2 1/4	2 3/4	.421875 .4271 .4328	5 1/8 5 1/4 5 1/4	4 3/4	.671875 .6771 .6823	8 1/8 8 1/8 8 3/8	3 3/4	.921875 .9271 .9323	11 1/8 11 1/8 11 3/8
3/4	.1875 .1927 .1979	2 1/4 2 1/2 2 1/2	7 1/4	.4375 .4427 .4479	5 1/4 5 1/4 5 3/8	1 1/4	.6875 .6927 .6979	8 1/4 8 3/8 8 3/4	1 3/8	.9375 .9427 .9479	11 1/4 11 1/4 11 3/4
13/16	.203125 .2083 .2135	2 3/8 2 1/2 2 3/4	2 3/4	.453125 .4583 .4635	5 3/8 5 1/2 5 1/2	4 3/4	.703125 .7083 .7135	8 3/4 8 1/2 8 3/4	4 1/4	.953125 .9583 .9635	11 3/4 11 1/2 11 3/4
7/8	.21875 .2240 .2292	2 3/4 2 1/2 2 3/4	1 3/2	.46875 .4740 .4792	5 3/4 5 1/2 5 3/4	2 3/2	.71875 .7240 .7292	8 3/4 8 1/2 8 3/4	3 1/2	.96875 .9740 .9792	11 3/4 11 1/2 11 3/4
15/16	.234375 .2396 .2448	2 3/4 2 3/4 2 3/4	3 3/4	.484375 .4896 .4948	5 3/4 5 3/4 5 3/4	4 3/4	.734375 .7396 .7448	8 3/4 8 3/4 8 3/4	4 3/4	.984375 .9896 .9948	11 3/4 11 3/4 11 3/4
1	.2500	3	1 1/2	.5000	6	3 1/4	.7500	9	1	1.000	12

"Piping Guide", PO Box 277, Cotati, CA 94928, USA  
 Reproduced by courtesy of the Hydrodynamic Division, Chicago Pump (FMC Corporation).

# °F/°C TEMPERATURE CONVERSION

## TABLE M-6

-459.4 TO 0			0 TO 100			110 TO 1110			1120 TO 3000		
°C.	Given Temp.	°F.	°C. Temp.	Given	°F.	°C. Temp.	Given	°F.	°C. Temp.	Given	°F.
-273	-459.4	-	-17.8	0	32	10.0	50	122.0	43	110	230
-268	-450	-	-17.2	1	33.8	10.6	51	123.8	49	120	248
-262	-440	-	-16.7	2	35.6	11.1	52	125.6	54	130	266
-257	-430	-	-16.1	3	37.4	11.7	53	127.4	60	140	284
-251	-420	-	-15.6	4	39.2	12.2	54	129.2	66	150	302
-246	-410	-	-15.0	5	41.0	12.8	55	131.0	71	160	320
-240	-400	-	-14.4	6	42.8	13.3	56	132.8	77	170	338
-234	-390	-	-13.9	7	44.6	13.9	57	134.6	82	180	356
-229	-380	-	-13.3	8	46.4	14.4	58	136.4	88	190	374
-223	-370	-	-12.8	9	48.2	15.0	59	138.2	93	200	392
-218	-360	-	-12.2	10	50.0	15.6	60	140.0	99	210	410
-212	-350	-	-11.7	11	51.8	16.1	61	141.8	100	212	413.6
-207	-340	-	-11.1	12	53.6	16.7	62	143.6	104	220	428
-201	-330	-	-10.6	13	55.4	17.2	63	145.4	110	230	446
-196	-320	-	-10.0	14	57.2	17.8	64	147.2	116	240	464
-190	-310	-	-9.4	15	59.0	18.3	65	149.0	121	250	482
-184	-300	-	-8.9	16	60.8	18.9	66	150.8	127	260	500
-179	-290	-	-8.3	17	62.6	19.4	67	152.6	132	270	518
-173	-280	-	-7.8	18	64.4	20.0	68	154.4	138	280	536
-169	-273	-459.4	-7.2	19	66.2	20.6	69	156.2	143	290	554
-168	-270	-454	-6.7	20	68.0	21.1	70	158.0	149	300	572
-162	-260	-436	-6.1	21	69.8	21.7	71	159.8	154	310	590
-157	-250	-418	-5.6	22	71.6	22.2	72	161.6	160	320	608
-151	-240	-400	-5.0	23	73.4	22.8	73	163.4	166	330	626
-146	-230	-382	-4.4	24	75.2	23.3	74	165.2	171	340	644
-140	-220	-364	-3.9	25	77.0	23.9	75	167.0	177	350	662
-134	-210	-346	-3.3	26	78.8	24.4	76	168.8	182	360	680
-129	-200	-328	-2.8	27	80.6	25.0	77	170.6	188	370	698
-123	-190	-310	-2.2	28	82.4	25.6	78	172.4	193	380	716
-118	-180	-292	-1.7	29	84.2	26.1	79	174.2	199	390	734
-112	-170	-274	-1.1	30	86.0	26.7	80	176.0	204	400	752
-107	-160	-256	-0.6	31	87.8	27.2	81	177.8	210	410	770
-101	-150	-238	0.0	32	89.6	27.8	82	179.6	216	420	788
-96	-140	-220	0.6	33	91.4	28.3	83	181.4	221	430	806
-90	-130	-202	1.1	34	93.2	28.9	84	183.2	227	440	824
-84	-120	-184	1.7	35	95.0	29.4	85	185.0	232	450	842
-79	-110	-166	2.2	36	96.8	30.0	86	186.8	238	460	860
-73	-100	-148	2.8	37	98.6	30.6	87	188.6	243	470	878
-68	-90	-130	3.3	38	100.4	31.1	88	190.4	249	480	896
-62	-80	-112	3.9	39	102.2	31.7	89	192.2	254	490	914
-57	-70	-94	4.4	40	104.0	32.2	90	194.0	260	500	932
-51	-60	-76	5.0	41	105.8	32.8	91	195.8	266	510	950
-46	-50	-58	5.6	42	107.6	33.3	92	197.6	271	520	968
-40	-40	-40	6.1	43	109.4	33.9	93	199.4	277	530	986
-34	-30	-22	6.7	44	111.2	34.4	94	201.2	282	540	1004
-29	-20	-4	7.2	45	113.0	35.0	95	203.0	288	550	1022
-23	-10	+14	7.8	46	114.8	35.6	96	204.8	293	560	1040
-17.8	0	+32	8.3	47	116.6	36.1	97	206.6	299	570	1058
-	-	-	8.9	48	118.4	36.7	98	208.4	304	580	1076
-	-	-	9.4	49	120.2	37.2	99	210.2	310	590	1094
-	-	-	-	-	-	37.8	100	212.0	316	600	1112

Reproduced by courtesy of Jenkins Bros., valve manufacturers. Find the temperature in the left column; if this temperature is in degrees F, the centigrade equivalent is in the right column; if this temperature is in degrees C, the Fahrenheit equivalent is in the right column.

# PIPE DATA: DIMENSIONAL DATA & STRESS PARAMETERS

## TABLE P-1

REPRODUCED BY PERMISSION FROM CATALOG 61,  
MIDWEST FITTING DIVISION OF THE CRANE COMPANY

### KEY TO PIPE DESIGNATIONS:

AMERICAN NATIONAL STANDARDS INSTITUTE\* XXS = Double-extra-strong pipe; XS = Extra-strong pipe; STD = Standard pipe; L = Light-wall pipe (= "Light-gauge")  
AMERICAN PETROLEUM INSTITUTE API = "Line pipe" to 5L or 5LX designation

\*Defined in ANSI B36.10 and B36.19. Numbers in Table P-1 are Schedule Numbers for pipe, also defined in these ANSI Standards.

Nom. Pipe Size	WALL THICKNESS		DIMENSIONS			WEIGHTS			AREAS				PROPERTIES			Approx. Weight of Welding Rods lb.
	* Iron Pipe Size	Sch. No.	Other	Outside Diam.	Inside Diam.	Wall Thkn.	Plain End Pipe lb. per ft.	Water Pipe lb. per ft.	Surface		Cross-Sectional		Moment of Inertia in. <sup>4</sup>	Section Modulus in. <sup>3</sup>	Radius of Gyration in.	
									Outside ft. <sup>2</sup> per ft.	Inside ft. <sup>2</sup> per ft.	Flow in. <sup>2</sup>	Metal in. <sup>2</sup>				
1/8	STD	10S	API	.405	.307	.049	.186	.032	.106	.0804	.0740	.0548	.0009	.0044	.1270	—
	XS	40	API	.405	.269	.068	.244	.025	.106	.0705	.0568	.0720	.0011	.0053	.1215	—
1/4	STD	10S	API	.540	.410	.065	.330	.057	.141	.1073	.1320	.0970	.0028	.0103	.1695	—
	XS	40	API	.540	.364	.088	.424	.045	.141	.0955	.1041	.1250	.0033	.0123	.1628	—
3/8	STD	10S	API	.675	.545	.065	.423	.101	.177	.1427	.2333	.1245	.0059	.0174	.2160	—
	XS	40	API	.675	.493	.091	.567	.083	.177	.1295	.1910	.1670	.0073	.0216	.2090	—
1/2	STD	5S		.840	.710	.065	.538	.171	.220	.1859	.3959	.1583	.0120	.0285	.2750	.04
	XS	10S	API	.840	.674	.083	.671	.154	.220	.1765	.3568	.1974	.0143	.0340	.2693	—
3/4	STD	40	API	.840	.622	.109	.850	.132	.220	.1637	.3040	.2503	.0171	.0407	.2613	—
	XS	80	API	.840	.546	.147	1.087	.101	.220	.1433	.2340	.3200	.0201	.0478	.2505	.05
1	STD	10S	L	1.050	.920	.065	.684	.288	.275	.2409	.6648	.2011	.0245	.0528	.2399	.1
	XS	40	API	1.050	.884	.083	.857	.266	.275	.2314	.6138	.3856	.0222	.0377	.2192	.2
1 1/4	STD	5S		1.050	.824	.113	1.130	.230	.275	.2168	.5330	.3326	.0370	.0705	.3337	—
	XS	10S	API	1.050	.742	.154	1.473	.187	.275	.1948	.4330	.4335	.0448	.0853	.3214	.05
1 1/2	STD	40	API	1.050	.612	.219	1.944	.127	.275	.1602	.2942	.5717	.0328	.1005	.3038	.1
	XS	80	API	1.050	.434	.308	2.440	.063	.275	.1137	.1479	.7180	.0579	.1103	.2840	.2
1 3/4	STD	5S		1.315	1.185	.065	.868	.478	.344	.3102	1.1029	.2552	.0500	.0760	.4425	—
	XS	10S	L	1.315	1.097	.109	1.404	.409	.344	.2872	.9448	.4129	.0756	.1150	.4282	—
1 3/4	STD	40	API	1.315	1.049	.133	1.678	.374	.344	.2740	.8640	.4939	.0873	.1328	.4205	.08
	XS	80	API	1.315	.957	.179	2.171	.311	.344	.2520	.7190	.6388	.1056	.1606	.4066	.1
1 3/4	STD	10S	L	1.660	.815	.250	2.840	.226	.344	.2134	.5217	.8364	.1252	.1903	.3868	.3
	XS	40	API	1.660	.599	.358	3.659	.122	.344	.1570	.2818	1.0760	.1405	.2136	.3613	.4
1 3/4	STD	5S		1.660	1.530	.065	1.107	.796	.434	.4006	1.8381	.3257	.1037	.1250	.5644	—
	XS	10S	L	1.660	1.442	.109	1.806	.708	.434	.3775	1.6330	.5314	.1606	.1934	.5499	—
1 3/4	STD	40	API	1.660	1.380	.140	2.272	.647	.434	.3620	1.4950	.6685	.1947	.2346	.5397	.1
	XS	80	API	1.660	1.278	.191	2.996	.555	.434	.3356	1.2830	.8815	.2418	.2913	.5237	.2
1 3/4	STD	10S	L	1.660	1.160	.250	3.764	.457	.434	.3029	1.0570	1.1070	.2833	.3421	.5063	.3
	XS	40	API	1.660	.896	.382	5.214	.273	.434	.2331	.6305	1.5340	.3411	.4110	.4716	.5
1 3/4	STD	5S		1.900	1.770	.065	1.274	1.066	.497	.4634	2.4610	.3751	.1579	.1662	.6492	—
	XS	10S	L	1.900	1.682	.109	2.085	.963	.497	.4403	2.2219	.6139	.2469	.2599	.6344	—
1 3/4	STD	40	API	1.900	1.610	.145	2.717	.882	.497	.4213	2.0361	.8001	.3099	.3262	.6226	.1
	XS	80	API	1.900	1.500	.200	3.631	.765	.497	.3927	1.7672	1.0689	.3912	.4118	.6052	.2
1 3/4	STD	10S	L	1.900	1.338	.281	4.858	.609	.497	.3503	1.4060	1.4299	.4823	.5077	.5809	.4
	XS	40	API	1.900	1.100	.400	6.408	.412	.497	.2903	.9502	1.8859	.5678	.5977	.5489	.6

\*Piping Guide\*, PO Box 277, Colton, CA 94928, USA

\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufacturers' weights'—see 2.1.3

CONTINUED

# PIPE DATA

REPRODUCED BY PERMISSION OF THE CRANE COMPANY,  
MIDWEST FITTING DIVISION

TABLE P-1

Nom. Pipe Size	In.	WALL THICKNESS		DIMENSIONS			WEIGHTS		AREAS				PROPERTIES				Approx. Weight of Welding Rods
		# Iron Pipe Size	Sch. No.	Other	Outside Diam.	Inside Diam.	Wall Thkn.	Plain End Pipe	Water Pipe	Surface		Cross-Sectional		Moment of Inertia	Section Modulus	Radius of Gyration	
										Outside	Inside	Flow	Metal				
					In.	In.	In.	Lb. per ft.	Lb. per ft.	ft. <sup>2</sup> per ft.	ft. <sup>2</sup> per ft.	In. <sup>3</sup>	In. <sup>3</sup>	In. <sup>4</sup>	In. <sup>3</sup>	In.	
2		SS			2.375	2.245	.065	1.60	1.71	.622	.588	3.958	.472	.315	.265	.817	
		10S	API	L	2.375	2.157	.109	2.64	1.58	.622	.565	3.654	.776	.500	.421	.803	
	STD	40	API		2.375	2.067	.154	3.65	1.45	.622	.540	3.355	1.075	.666	.561	.787	
	XS	80	API		2.375	1.939	.218	5.02	1.28	.622	.507	2.953	1.477	.868	.731	.766	
		XXS	API		2.375	1.875	.250	5.67	1.20	.622	.492	2.761	1.669	.955	.805	.756	
		160	API		2.375	1.687	.344	7.46	.97	.622	.442	2.235	2.195	1.164	.980	.728	
		XXS	API		2.375	1.503	.436	9.03	.77	.622	.393	1.774	2.656	1.312	1.104	.703	
2 1/2		SS	API		2.875	2.709	.083	2.47	2.50	.753	.709	5.764	.728	.710	.494	.988	
		10S	L		2.875	2.635	.120	3.53	2.36	.753	.690	5.453	1.038	.988	.687	.976	
	STD	40	API		2.875	2.469	.203	5.79	2.07	.753	.646	4.788	1.704	1.530	1.064	.947	
	XS	80	API		2.875	2.323	.276	7.66	1.83	.753	.610	4.238	2.254	1.924	1.339	.924	
		160	API		2.875	2.125	.375	10.01	1.54	.753	.556	3.547	2.945	2.353	1.638	.894	
		XXS	API		2.875	1.771	.552	13.70	1.07	.753	.463	2.464	4.028	2.871	1.997	.844	
3		SS	API		3.500	3.334	.083	3.03	3.78	.916	.873	8.730	.891	1.301	.744	1.208	
		10S	L		3.500	3.260	.120	4.33	3.62	.916	.853	8.346	1.272	1.821	1.041	1.196	
			API		3.500	3.250	.125	4.52	3.60	.916	.851	8.300	1.329	1.900	1.086	1.195	
			API		3.500	3.188	.156	5.58	3.46	.916	.835	7.982	1.639	2.298	1.313	1.184	
		STD	40	API		3.500	3.124	.188	6.65	.916	.818	7.665	1.956	2.691	1.538	1.173	
			API		3.500	3.068	.216	7.58	3.20	.916	.802	7.393	2.228	3.017	1.724	1.164	
			API		3.500	3.000	.250	8.68	3.06	.916	.785	7.184	2.553	3.388	1.936	1.152	
			API		3.500	2.938	.281	9.65	2.94	.916	.769	6.780	2.842	3.819	2.182	1.142	
		XS	API		3.500	2.900	.300	10.25	2.86	.916	.761	6.605	3.016	3.892	2.136	1.136	
			API		3.500	2.824	.438	14.31	2.34	.916	.687	5.407	4.214	5.044	2.882	1.094	
		160	API		3.500	2.300	.600	18.58	1.80	.916	.601	4.155	5.466	5.993	3.424	1.047	
3 1/2		SS			4.000	3.834	.083	3.47	5.00	1.047	1.004	11.545	1.021	1.960	.980	1.385	
		10S	L		4.000	3.760	.120	4.97	4.81	1.047	.984	11.103	1.463	2.859	1.372	1.372	
			API		4.000	3.750	.125	5.18	4.79	1.047	.982	11.044	1.522	2.854	1.430	1.371	
			API		4.000	3.688	.156	6.41	4.63	1.047	.966	10.682	1.884	3.485	1.743	1.360	
			API		4.000	3.624	.188	7.71	4.48	1.047	.950	10.315	2.251	4.130	2.065	1.350	
		STD	40	API		4.000	3.548	.226	9.11	1.047	.929	9.886	2.680	4.788	2.394	1.337	
			API		4.000	3.500	.250	10.02	9.11	1.047	.916	9.621	2.945	5.201	2.601	1.339	
			API		4.000	3.438	.281	11.17	4.02	1.047	.900	9.283	3.283	5.715	2.858	1.319	
		XS	API		4.000	3.364	.318	12.51	3.85	1.047	.880	8.888	3.678	6.280	3.140	1.307	
			API		4.000	3.278	.636	22.85	2.53	1.047	.716	5.845	6.721	9.848	4.924	1.210	
4		SS			4.500	4.334	.083	3.92	6.39	1.178	1.135	14.752	1.152	2.810	1.249	1.562	
		10S	L		4.500	4.260	.120	5.61	6.18	1.178	1.115	14.255	1.651	3.962	1.761	1.550	
			API		4.500	4.250	.125	5.84	6.15	1.178	1.113	14.186	1.718	4.115	1.829	1.548	
			API		4.500	4.188	.156	7.24	5.97	1.178	1.096	13.775	2.129	5.029	2.235	1.537	
			API		4.500	4.124	.188	8.56	5.80	1.178	1.082	13.357	2.547	5.850	2.600	1.525	
			API		4.500	4.062	.219	10.02	5.62	1.178	1.063	12.959	2.945	6.768	3.008	1.516	
		STD	40	API		4.500	4.026	.237	10.79	5.51	1.178	1.055	12.730	3.174	7.231	3.214	1.510
			API		4.500	4.000	.250	11.35	5.45	1.178	1.049	12.566	3.338	7.540	3.360	1.505	
			API		4.500	3.938	.281	12.67	5.27	1.178	1.031	12.180	3.724	8.332	3.703	1.495	
			API		4.500	3.876	.312	14.00	5.12	1.178	1.013	11.799	4.105	9.045	4.020	1.482	
		XS	API		4.500	3.826	.337	14.98	4.98	1.178	1.002	11.497	4.407	9.610	4.371	1.477	
			API		4.500	3.624	.438	18.98	4.47	1.178	.949	10.315	5.589	11.648	5.177	1.444	
			API		4.500	3.500	.500	21.36	4.16	1.178	.916	9.621	6.283	12.771	5.676	1.425	
		160	API		4.500	3.438	.531	22.52	4.02	1.178	.900	9.283	6.621	13.275	5.900	1.416	
		XXS	API		4.500	3.152	.674	27.54	3.38	1.178	.826	7.803	8.101	15.284	6.793	1.374	
5		SS			5.563	5.345	.109	6.35	9.77	1.456	1.399	22.438	1.868	7.126	2.562	1.929	
		10S	L		5.563	5.295	.134	7.77	9.54	1.456	1.386	22.021	2.285	8.472	3.078	1.920	
			API		5.563	5.251	.156	9.02	9.39	1.456	1.375	21.656	2.650	9.699	3.487	1.913	
			API		5.563	5.187	.188	10.80	9.16	1.456	1.358	21.131	3.175	11.485	4.129	1.902	
			API		5.563	5.125	.219	12.51	8.94	1.456	1.342	20.629	3.677	13.145	4.726	1.891	
		STD	40	API		5.563	.258	14.62	8.66	1.456	1.321	20.006	4.300	15.162	5.451	1.878	
			API		5.563	5.001	.281	15.86	8.52	1.456	1.309	19.643	4.663	16.305	5.862	1.870	
			API		5.563	4.979	.312	17.51	8.31	1.456	1.293	19.159	5.147	17.807	6.402	1.866	
			API		5.563	4.875	.344	19.19	8.09	1.456	1.276	18.666	5.640	19.281	6.932	1.849	
		XS	API		5.563	4.812	.375	20.78	7.87	1.456	1.260	18.194	6.112	20.465	7.431	1.839	
			API		5.563	4.562	.537	27.04	7.08	1.456	1.195	16.353	7.925	25.377	9.255	1.799	
		160	API		5.563	4.313	.675	32.94	6.32	1.456	1.129	14.610	9.494	30.246	10.800	1.745	
		XXS	API		5.563	4.063	.790	38.55	5.62	1.456	1.064	13.240	11.240	33.628	12.090	1.722	
*Fitting Guide - NO Box 277 Coast, CA 94068, USA																	

\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part B) as 'manufacturer's weights'—see 2.1.3

**PIPE DATA** REPRODUCED BY PERMISSION OF THE CRANE COMPANY,  
MIDWEST FITTING DIVISION

**TABLE P-1**

Nom. Pipe Size		WALL THICKNESS		DIMENSIONS			WEIGHTS			AREAS				PROPERTIES			Approx. Weight of Welding Rods lb.
		Iron Pipe Size	Sch. No.	Other	Outside Diam.	Inside Diam.	Wall Thkn.	Meta End Pipe	Water Pipe	Surface		Cross-Sectional		Moment of Inertia	Section Modulus	Radius of Gyration	
In.					In.	In.	In.	lb. per ft.	lb. per ft.	Outside ft. <sup>2</sup> per ft.	Inside ft. <sup>2</sup> per ft.	Flow In. <sup>2</sup>	Metal In. <sup>2</sup>	In. <sup>4</sup>	In. <sup>3</sup>	In.	
6			5S	API	6.625	6.407	.109	7.59	14.0	1.73	1.68	32.24	2.23	11.34	3.57	2.30	—
			10S	L	6.625	6.357	.134	9.29	13.7	1.73	1.66	31.75	2.73	14.38	4.34	2.29	.4
				API	6.625	6.249	.188	12.93	13.3	1.73	1.64	30.70	3.80	19.71	5.95	2.28	.6
				API	6.625	6.187	.219	15.02	13.1	1.73	1.62	30.10	4.41	22.66	6.84	2.27	.8
				API	6.625	6.125	.250	17.02	12.8	1.73	1.61	29.50	5.01	25.55	7.71	2.26	1.0
				API	6.625	6.071	.277	18.86	12.6	1.73	1.59	28.95	5.54	28.00	8.46	2.25	1.1
	STD	40		API	6.625	6.065	.280	18.97	12.5	1.73	1.59	28.90	5.58	28.14	8.50	2.24	1.1
				API	6.625	6.001	.312	21.05	12.3	1.73	1.57	28.28	6.19	30.91	9.33	2.23	1.3
				API	6.625	5.937	.344	23.09	12.0	1.73	1.55	27.68	6.79	33.51	10.14	2.22	1.6
				API	6.625	5.875	.375	25.10	11.8	1.73	1.54	27.10	7.37	36.20	10.90	2.21	1.8
				API	6.625	5.761	.432	28.57	11.3	1.73	1.51	26.07	8.40	40.49	12.22	2.19	2.2
8				API	6.625	5.625	.500	32.79	10.8	1.73	1.48	24.85	9.63	45.60	13.78	2.16	3.0
	XS	80		API	6.625	5.501	.562	36.42	10.3	1.73	1.47	23.77	10.74	49.91	15.07	2.15	3.2
				API	6.625	5.187	.719	45.34	9.2	1.73	1.36	21.13	13.34	59.03	17.82	2.10	5.1
	XXS	160		API	6.625	4.897	.864	53.16	8.1	1.73	1.28	18.83	15.64	66.33	20.02	2.06	5.8
			5S	L	8.625	8.407	.109	9.91	24.0	2.26	2.20	55.51	2.92	26.44	6.13	3.01	—
			10S	API	8.625	8.329	.148	13.40	23.6	2.26	2.18	54.49	3.94	35.45	8.22	3.00	.4
				API	8.625	8.249	.188	16.90	23.2	2.26	2.16	53.43	5.00	44.42	10.30	2.98	.7
				API	8.625	8.219	.203	18.30	23.1	2.26	2.15	53.05	5.38	47.65	11.05	2.98	.8
			20	API	8.625	8.187	.219	19.64	22.9	2.26	2.15	52.63	5.80	51.32	11.90	2.97	1.0
				API	8.625	8.125	.250	22.36	22.5	2.26	2.13	51.85	6.58	57.74	13.39	2.96	1.2
			30	API	8.625	8.071	.277	24.70	22.2	2.26	2.12	51.17	7.26	63.35	14.69	2.95	1.3
10				API	8.625	8.001	.312	27.72	21.8	2.26	2.10	50.28	8.15	70.60	16.37	2.94	1.6
	STD	40		API	8.625	7.981	.322	28.55	21.6	2.26	2.09	50.03	8.40	72.49	16.81	2.94	1.7
				API	8.625	7.937	.344	30.40	21.4	2.26	2.08	49.49	8.94	76.81	17.81	2.93	1.9
				API	8.625	7.875	.375	33.10	21.1	2.26	2.06	48.69	9.74	83.10	19.27	2.92	2.1
			60	API	8.625	7.813	.406	35.66	20.8	2.26	2.04	47.95	10.48	88.75	20.58	2.91	2.3
				API	8.625	7.749	.438	38.33	20.4	2.26	2.03	47.16	11.27	94.75	21.97	2.90	2.7
	XS	80		API	8.625	7.625	.500	43.39	19.8	2.26	2.01	45.67	12.76	105.70	24.51	2.88	3.6
				API	8.625	7.437	.594	50.93	18.8	2.26	1.95	43.44	14.99	121.48	28.17	2.85	4.6
				API	8.625	7.375	.625	53.40	18.5	2.26	1.93	42.72	15.71	126.49	29.33	2.84	5.1
				API	8.625	7.187	.719	60.69	17.6	2.26	1.88	40.57	17.86	140.67	32.62	2.81	6.7
			140	API	8.625	7.001	.812	67.79	16.7	2.26	1.83	38.50	19.93	153.74	35.65	2.78	7.3
	XXS	160		API	8.625	6.875	.875	72.42	16.1	2.26	1.80	37.13	21.30	161.98	37.56	2.76	8.0
10				API	8.625	6.813	.906	74.71	15.8	2.26	1.78	36.46	21.97	165.94	38.48	2.76	8.2
			5S	L	10.750	10.482	.134	15.19	37.4	2.81	2.74	86.29	4.47	62.94	11.71	3.75	.6
			10S	API	10.750	10.420	.165	18.65	36.9	2.81	2.73	85.26	5.50	76.81	14.29	3.74	.8
				API	10.750	10.374	.188	21.12	36.7	2.81	2.72	84.56	6.20	86.54	16.10	3.74	1.0
				API	10.750	10.344	.203	22.86	36.5	2.81	2.71	84.05	6.71	93.26	17.35	3.73	1.1
				API	10.750	10.312	.219	24.63	36.2	2.81	2.70	83.52	7.24	100.46	18.69	3.72	1.2
				API	10.750	10.250	.250	28.04	35.9	2.81	2.68	82.50	8.26	113.52	21.12	3.71	1.4
			30	API	10.750	10.192	.279	31.20	35.3	2.81	2.66	81.58	9.18	125.88	23.42	3.70	1.7
				API	10.750	10.136	.307	34.24	35.0	2.81	2.65	80.69	10.07	137.44	25.57	3.69	2.0
				API	10.750	10.062	.344	38.26	34.5	2.81	2.63	79.51	11.25	152.27	28.33	3.68	2.4
	STD	40		API	10.750	10.020	.365	40.48	34.1	2.81	2.62	78.85	11.91	160.71	29.90	3.67	2.7
	XS	60, 80S		API	10.750	9.974	.438	48.28	33.2	2.81	2.58	76.57	14.91	188.82	35.13	3.65	3.6
10				API	10.750	9.750	.500	54.74	32.3	2.81	2.55	74.66	16.10	211.94	39.43	3.63	4.5
			80	API	10.750	9.562	.594	64.40	31.1	2.81	2.50	71.81	18.95	245.21	45.62	3.60	6.0
				API	10.750	9.312	.719	77.00	29.5	2.81	2.44	68.10	22.66	286.43	53.29	3.56	8.3
				API	10.750	9.250	.750	80.10	29.1	2.81	2.42	67.20	23.56	296.16	55.10	3.54	8.5
			120		10.750	9.062	.844	89.27	27.9	2.81	2.37	64.49	26.27	324.54	60.38	3.52	9.0
				API	10.750	9.000	.875	92.28	27.6	2.81	2.36	63.28	27.14	333.46	62.04	3.50	9.8
	XXS	140		API	10.750	8.750	1.000	104.13	26.1	2.81	2.29	60.13	30.63	367.81	68.43	3.46	13
			160		10.750	8.500	1.125	115.65	24.6	2.81	2.22	56.75	34.01	399.42	74.31	3.43	15
				API	10.750	8.250	1.250	124.82	23.2	2.81	2.16	53.45	37.31	428.17	79.66	3.39	17
				API	10.750	8.250	1.250	124.82	23.2	2.81	2.16	53.45	37.31	428.17	79.66	3.39	17
				API	10.750	8.250	1.250	124.82	23.2	2.81	2.16	53.45	37.31	428.17	79.66	3.39	17

\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufacturers' weights'—see 2.1.3

# PIPE DATA

REPRODUCED BY PERMISSION OF THE CRANE COMPANY,  
MIDWEST FITTING DIVISION

TABLE P-1

Nom. Pipe Size	WALL THICKNESS		DIMENSIONS		WEIGHTS		AREAS			PROPERTIES		
	Sch. No.	Other	Outside Diam.	Inside Diam.	Wall Thkn.	Plain End Pipe	Water in Pipe	Surface		Moment of Inertia	Section Modulus	Radius of Gyration
								Outside	Inside			
In.			In.	In.	In.	lb. per ft.	lb. per ft.	ft. <sup>2</sup> per ft.	ft. <sup>2</sup> per ft.	In. <sup>4</sup>	In. <sup>3</sup>	In.
12	5S	L	12.750	12.438	.156	21.0	52.6	3.34	3.26	122.4	19.2	4.45
	10S	API	12.750	12.390	.180	24.2	52.2	3.34	3.24	140.4	22.0	4.44
			12.750	12.344	.203	27.2	52.0	3.34	3.23	157.2	24.7	4.43
	20	API	12.750	12.312	.219	29.3	51.7	3.34	3.22	167.6	26.3	4.43
		API	12.750	12.250	.250	33.4	51.3	3.34	3.21	192.3	30.2	4.42
		API	12.750	12.188	.281	37.4	50.6	3.34	3.19	214.1	33.6	4.41
	30	API	12.750	12.126	.312	41.5	50.1	3.34	3.17	236.0	37.0	4.40
		API	12.750	12.090	.330	43.8	49.7	3.34	3.16	248.5	39.0	4.39
		API	12.750	12.062	.344	45.5	49.7	3.34	3.16	259.0	40.7	4.38
	40S	API	12.750	12.000	.375	49.6	48.9	3.34	3.14	279.3	43.8	4.37
	40	API	12.750	11.938	.406	53.6	48.5	3.34	3.13	300.3	47.1	4.37
		API	12.750	11.874	.438	57.5	48.2	3.34	3.11	321.0	50.4	4.35
14	80S	API	12.750	11.750	.500	65.4	46.9	3.34	3.08	361.5	56.7	4.33
	60	API	12.750	11.626	.562	73.2	46.0	3.34	3.04	400.5	62.8	4.31
		API	12.750	11.500	.625	80.9	44.9	3.34	3.01	438.7	68.8	4.29
	80	API	12.750	11.374	.688	88.6	44.0	3.34	2.98	475.7	74.6	4.27
		API	12.750	11.250	.750	96.2	43.1	3.34	2.94	510.7	80.1	4.25
	100	API	12.750	11.062	.844	107.3	41.6	3.34	2.90	562.2	88.2	4.22
			12.750	11.000	.875	110.9	41.1	3.34	2.88	578.5	90.7	4.21
	120		12.750	10.750	1.000	125.5	39.3	3.34	2.81	641.7	100.7	4.17
	140		12.750	10.500	1.125	139.7	37.5	3.34	2.75	700.7	109.9	4.13
			12.750	10.250	1.250	153.6	35.8	3.34	2.68	755.5	118.5	4.09
	160		12.750	10.126	1.312	160.3	34.9	3.34	2.65	781.3	122.6	4.07
			12.750	10.000	1.375	167.2	34.0	3.34	2.62	807.2	126.6	4.05
14			12.750	9.750	1.500	180.4	32.4	3.34	2.55	853.8	133.9	4.01
	5S	API	14.000	13.688	.156	23.0	63.7	3.67	3.58	162.6	23.2	4.90
	10S	API	14.000	13.624	.188	27.2	63.1	3.67	3.57	194.6	27.8	4.88
			14.000	13.580	.210	30.9	62.8	3.67	3.55	216.2	30.9	4.87
	10	API	14.000	13.562	.219	32.2	62.6	3.67	3.55	225.1	32.2	4.87
		API	14.000	13.500	.250	36.7	62.1	3.67	3.54	256.0	36.6	4.86
		API	14.000	13.438	.281	41.2	61.5	3.67	3.52	285.2	40.7	4.85
	20	API	14.000	13.376	.312	45.7	60.9	3.67	3.50	314.4	44.9	4.84
	30	API	14.000	13.312	.344	50.2	60.3	3.67	3.48	344.3	49.2	4.83
		API	14.000	13.250	.375	54.6	59.7	3.67	3.47	372.8	53.2	4.82
	40	API	14.000	13.124	.438	63.4	58.5	3.67	3.44	429.6	61.4	4.80
		API	14.000	13.062	.469	67.8	58.0	3.67	3.42	456.8	65.3	4.79
14		API	14.000	13.000	.500	72.1	57.4	3.67	3.40	483.8	69.1	4.78
	60	API	14.000	12.812	.594	85.0	55.8	3.67	3.35	563.1	80.4	4.74
		API	14.000	12.750	.625	89.3	55.3	3.67	3.34	588.5	84.1	4.73
	80	API	14.000	12.500	.750	106.1	51.2	3.67	3.27	687.5	98.3	4.69
			14.000	12.250	.875	122.7	51.1	3.67	3.21	780.1	111.4	4.65
	100		14.000	12.124	.938	130.8	50.0	3.67	3.17	825.1	117.9	4.63
			14.000	12.000	1.000	138.5	49.0	3.67	3.14	868.0	124.0	4.61
	120		14.000	11.812	1.094	150.8	47.5	3.67	3.09	930.2	132.0	4.58
			14.000	11.750	1.125	154.7	47.0	3.67	3.08	950.3	135.0	4.57
	140		14.000	11.500	1.250	170.2	45.0	3.67	3.01	1027.5	146.6	4.53
			14.000	11.250	1.375	185.4	43.1	3.67	2.94	1098.5	157.1	4.49
	160		14.000	11.186	1.406	189.1	42.6	3.67	2.93	1116.9	159.6	4.48
			14.000	11.000	1.500	200.2	41.2	3.67	2.88	1166.5	166.6	4.45
14			14.000	10.000	2.000	256.3	34.0	3.67	2.62	1394.9	199.3	4.30
			14.000	9.750	2.125	269.5	32.3	3.67	2.55	1442.1	206.5	4.26
			14.000	9.600	2.210	277.3	31.4	3.67	2.51	1468.8	209.8	4.24
			14.000	9.470	2.500	307.1	27.4	3.67	2.36	1563.7	228.4	4.16

\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufacturers' weights'—see 2.1.3

Continued

**PIPE DATA** REPRODUCED BY PERMISSION OF THE CRANE COMPANY, MIDWEST FITTING DIVISION

**TABLE P-1**

Nom. Pipe Size	WALL THICKNESS		DIMENSIONS			WEIGHTS		AREAS				PROPERTIES			Approx. Weight of Welding Rods lb.
	Iron Pipe Size	Sch. No.	Outside Diam.	Inside Diam.	Wall Thkn.	Plain End Pipe lb. per ft.	Water In. Pipe lb. per ft.	Surface		Cross-Sectional		Moment of Inertia	Section Modulus	Radius of Gyration	
								Outside R <sup>2</sup> per ft.	Inside R <sup>2</sup> per ft.	Flow	Metal				
16		SS 10S	16.000	15.670	.165	28	83.5	4.19	4.10	192.9	8.21	257	32.2	5.60	
		API	16.000	15.624	.188	32	83.0	4.19	4.09	191.7	9.34	292	36.5	5.59	
			16.000	15.562	.219	37	82.5	4.19	4.07	190.2	10.86	338	42.3	5.58	
		10	16.000	15.500	.250	42	82.1	4.19	4.06	189.0	12.40	385	48.1	5.57	
		20	16.000	15.438	.281	47	81.2	4.19	4.04	187.0	13.90	430	53.8	5.56	
		API	16.000	15.376	.312	52	80.4	4.19	4.03	185.7	15.38	473	59.2	5.55	
	STD	API	16.000	15.312	.344	57	80.0	4.19	4.01	184.1	16.94	519	64.9	5.54	
		API	16.000	15.250	.375	63	79.1	4.19	4.00	182.6	18.41	562	70.3	5.53	
		API	16.000	15.124	.438	73	78.2	4.19	3.96	180.0	21.42	650	81.2	5.51	
	XS	API	16.000	15.062	.469	78	77.0	4.19	3.94	178.2	22.88	691	86.3	5.49	
	API	16.000	15.000	.500	83	76.5	4.19	3.93	176.7	24.35	732	91.5	5.48		
	API	16.000	14.750	.625	103	74.1	4.19	3.86	170.9	30.19	893	111.7	5.44		
	60		16.000	14.688	.656	108	73.4	4.19	3.85	169.4	31.62	933	116.6	5.43	
	80	API	16.000	14.500	.750	122	71.5	4.19	3.80	165.1	35.93	1047	130.9	5.40	
			16.000	14.312	.844	137	69.7	4.19	3.75	160.9	40.19	1157	144.7	5.37	
	100		16.000	14.000	1.000	160	66.7	4.19	3.66	153.9	47.12	1331	166.4	5.31	
	120		16.000	13.938	1.031	165	66.0	4.19	3.65	152.6	48.49	1366	170.7	5.30	
			16.000	13.562	1.219	192	62.6	4.19	3.55	144.5	56.60	1556	194.6	5.24	
	140		16.000	13.500	1.250	197	62.1	4.19	3.53	143.1	57.92	1586	198.3	5.23	
			16.000	13.124	1.438	224	58.6	4.19	3.44	135.3	65.79	1761	220.1	5.17	
	160		16.000	13.000	1.500	232	57.4	4.19	3.40	132.7	68.33	1816	227.0	5.15	
			16.000	12.812	1.594	245	55.8	4.19	3.35	129.0	72.14	1894	236.8	5.12	
18		SS 10S	18.000	17.670	.165	31	106.2	4.71	4.63	245.2	9.24	348	40.8	6.31	
		API	18.000	17.624	.188	36	103.7	4.71	4.61	243.9	10.52	417	46.4	6.30	
		10	18.000	17.500	.250	47	104.6	4.71	4.58	241.0	13.96	550	61.1	6.28	
		20	18.000	17.438	.281	49	104.0	4.71	4.56	240.0	14.49	570	63.4	6.27	
		API	18.000	17.376	.312	59	102.7	4.71	4.55	237.1	17.34	678	75.4	6.25	
		API	18.000	17.312	.344	65	102.0	4.71	4.53	235.4	19.08	744	82.6	6.24	
	STD	API	18.000	17.250	.375	71	101.2	4.71	4.51	233.7	20.76	807	89.6	6.23	
		API	18.000	17.188	.406	76	100.6	4.71	4.50	232.0	22.44	869	96.6	6.22	
		30	18.000	17.124	.438	82	99.5	4.71	4.48	229.5	24.95	963	107.0	6.21	
	XS	API	18.000	17.062	.469	88	99.0	4.71	4.47	228.6	25.83	993	110.3	6.20	
	API	18.000	17.000	.500	93	98.2	4.71	4.45	227.0	27.49	1053	117.0	6.19		
	40	18.000	16.876	.562	105	97.2	4.71	4.42	224.0	30.85	1177	130.9	6.17		
	60	API	18.000	16.750	.625	116	95.8	4.71	4.39	220.5	34.15	1290	143.2	6.14	
	80	API	18.000	16.500	.750	138	92.5	4.71	4.32	213.8	40.64	1515	168.3	6.10	
			18.000	16.124	.938	171	88.4	4.71	4.22	204.2	50.28	1835	203.9	6.04	
	100		18.000	16.000	1.000	182	87.2	4.71	4.19	201.1	53.41	1935	215.0	6.02	
			18.000	15.888	1.156	208	83.7	4.71	4.11	193.3	61.18	2182	242.3	5.97	
			18.000	15.500	1.250	224	81.8	4.71	4.06	188.7	65.78	2319	257.7	5.94	
	120		18.000	15.250	1.375	244	79.2	4.71	3.99	182.7	71.82	2498	277.5	5.90	
			18.000	15.000	1.500	265	76.6	4.71	3.93	176.7	77.75	2668	296.5	5.86	
	140		18.000	14.876	1.562	274	75.3	4.71	3.89	173.8	80.66	2750	305.5	5.84	
	160		18.000	14.438	1.781	309	71.0	4.71	3.78	163.7	90.75	3020	335.5	5.77	
20		SS 10S	20.000	19.634	.188	40	131.0	5.24	5.14	302.4	11.70	574	57.4	7.00	
		API	20.000	19.564	.218	46	130.2	5.24	5.12	300.6	13.55	663	66.3	6.99	
		10	20.000	19.500	.250	53	130.0	5.24	5.11	299.0	15.52	759	75.9	6.98	
		20	20.000	19.438	.281	59	128.6	5.24	5.09	296.8	17.41	846	84.6	6.97	
		API	20.000	19.376	.312	66	127.7	5.24	5.07	294.9	19.30	935	93.5	6.96	
		API	20.000	19.312	.344	72	127.0	5.24	5.06	292.9	21.24	1026	102.6	6.95	
	STD	API	20.000	19.250	.375	79	126.0	5.24	5.04	291.1	23.12	1113	111.3	6.94	
		API	20.000	19.188	.406	85	125.4	5.24	5.02	289.2	24.99	1200	120.0	6.93	
		API	20.000	19.124	.438	92	125.1	5.24	5.01	288.0	26.95	1290	129.0	6.92	
	XS	API	20.000	19.062	.469	98	123.6	5.24	4.99	285.4	28.78	1373	137.3	6.91	
	30	API	20.000	19.000	.500	104	122.8	5.24	4.97	283.5	30.63	1457	145.7	6.90	
	40		20.000	18.812	.594	123	120.4	5.24	4.92	277.9	36.21	1706	170.6	6.86	

"Piping Guide", P.O. Box 277, Cotati, CA 94926, USA

\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufacturers' weights'—see 2.1.3

PIPE DATA

REPRODUCED BY PERMISSION OF THE CRANE COMPANY,  
MIDWEST FITTING DIVISION

TABLE P-1

Nom. Pipe Size	WALL THICKNESS		DIMENSIONS		WEIGHTS		AREAS				PROPERTIES		
	Sch. No.	Iron Pipe Size	Outside Diam.	Inside Diam.	Wall Thkn.	Plain End Pipe lb. per ft.	Water in Pipe lb. per ft.	Surface		Cross-Sectional Metal	Moment of Inertia	Section Modulus	Radius of Gyration
								Outside ft. <sup>2</sup> per ft.	Inside ft. <sup>2</sup> per ft.				
In.			In.	In.	In.			ft. <sup>2</sup> per ft.	ft. <sup>2</sup> per ft.	In. <sup>2</sup>	In. <sup>4</sup>	In. <sup>3</sup>	In.
20		API	20.000	16.750	.625	129	119.5	5.24	4.91	276.1	1787	178.7	6.85
	60	API	20.000	16.376	.812	167	114.9	5.24	4.81	265.2	2257	225.7	6.79
			20.000	16.000	1.000	203	110.3	5.24	4.71	254.5	2702	270.2	6.73
			20.000	17.938	1.031	209	109.4	5.24	4.70	252.7	2771	277.1	6.72
	80		20.000	17.500	1.250	250	104.3	5.24	4.58	240.5	3249	324.9	6.64
22			20.000	17.438	1.281	256	103.4	5.24	4.56	238.8	3317	331.7	6.63
			20.000	17.000	1.500	296	98.3	5.24	4.45	227.0	3755	375.5	6.56
	140		20.000	16.500	1.750	341	92.6	5.24	4.32	213.8	4217	421.7	6.48
	160		20.000	16.062	1.969	379	87.8	5.24	4.20	202.6	4587	458.7	6.41
			22.000	21.624	.188	44	159.1	5.76	5.66	367.3	766	69.7	7.71
24		API	22.000	21.564	.218	51	158.2	5.76	5.65	365.2	885	80.4	7.70
		API	22.000	21.500	.250	58	157.4	5.76	5.63	363.1	1010	91.8	7.69
			22.000	21.438	.281	65	156.5	5.76	5.61	361.0	1131	102.8	7.68
		API	22.000	21.376	.312	72	155.6	5.76	5.60	358.9	1250	113.6	7.67
	20	API	22.000	21.312	.344	80	154.7	5.76	5.58	356.7	1373	124.8	7.66
26			22.000	21.250	.375	87	153.7	5.76	5.56	354.7	1490	135.4	7.65
		API	22.000	21.188	.406	94	152.9	5.76	5.55	352.6	1607	146.7	7.64
		API	22.000	21.124	.438	101	151.9	5.76	5.53	350.5	1725	156.8	7.62
		API	22.000	21.062	.469	108	150.9	5.76	5.51	348.4	1839	167.2	7.61
	30	API	22.000	21.000	.500	115	150.2	5.76	5.50	346.4	1953	177.5	7.61
28			22.000	20.750	.625	143	146.6	5.76	5.43	338.2	2400	218.2	7.56
		API	22.000	20.500	.750	170	143.1	5.76	5.37	330.1	2839	257.2	7.52
		API	22.000	20.250	.875	197	139.6	5.76	5.30	322.1	3245	295.0	7.47
		API	22.000	20.000	1.000	224	136.2	5.76	5.24	314.2	3645	331.4	7.43
	60		22.000	19.750	1.125	251	132.8	5.76	5.17	306.4	4029	366.3	7.39
30			22.000	19.500	1.250	277	129.5	5.76	5.10	298.6	4400	400.0	7.35
		API	22.000	19.250	1.375	303	126.2	5.76	5.04	291.0	4758	432.6	7.31
			22.000	19.000	1.500	329	122.9	5.76	4.97	283.5	5103	463.9	7.27
		API	22.000	18.750	1.625	354	119.6	5.76	4.91	276.1	5432	493.8	7.23
	120		22.000	18.250	1.875	403	113.3	5.76	4.78	261.6	6054	550.3	7.15
32			22.000	17.750	2.125	451	107.2	5.76	4.65	247.4	6626	602.4	7.07
			24.000	23.564	.218	55	186.9	6.28	6.17	436.1	1152	96.0	8.41
		API	24.000	23.500	.250	63	187.9	6.28	6.15	435.0	1320	110.0	8.40
		API	24.000	23.438	.281	71	186.9	6.28	6.14	431.5	1472	122.7	8.38
		API	24.000	23.376	.312	79	185.9	6.28	6.12	430.0	1630	136.0	8.38
34			24.000	23.312	.344	87	184.9	6.28	6.10	426.8	1789	149.1	8.36
		API	24.000	23.250	.375	95	183.9	6.28	6.09	424.6	1942	161.9	8.35
		API	24.000	23.188	.406	102	182.9	6.28	6.07	422.3	2095	174.6	8.34
		API	24.000	23.124	.438	110	181.9	6.28	6.05	420.0	2252	187.7	8.33
	20	API	24.000	23.062	.469	118	180.9	6.28	6.04	417.7	2401	200.1	8.33
36			24.000	23.000	.500	125	180.0	6.28	6.02	416.0	2550	213.0	8.31
		API	24.000	22.876	.562	141	178.0	6.28	5.99	411.0	2840	237.0	8.26
		API	24.000	22.750	.625	156	176.1	6.28	5.96	406.5	3137	261.4	8.27
		API	24.000	22.624	.688	171	174.1	6.28	5.92	402.0	3426	285.5	8.25
	30	API	24.000	22.500	.750	186	172.1	6.28	5.89	397.6	3705	308.8	8.22
38			24.000	22.126	.937	231	166.6	6.28	5.79	384.5	4571	376.8	8.21
		API	24.000	22.000	.989	238	165.6	6.28	5.78	382.3	4657	388.1	8.21
		API	24.000	21.900	1.000	246	164.8	6.28	5.76	380.1	4788	399.0	8.21
		API	24.000	21.824	1.031	256	163.2	6.28	5.74	377.9	4920	412.0	8.21
	40	API	24.000	21.750	1.062	267	162.2	6.28	5.72	375.7	5052	424.0	8.21
40			24.000	21.500	1.250	304	157.4	6.28	5.63	363.1	5797	483.0	8.07
		API	24.000	21.376	1.312	361	150.2	6.28	5.50	346.4	6740	561.7	7.97
		API	24.000	21.250	1.375	367	149.3	6.28	5.48	344.3	6847	570.6	7.96
		API	24.000	21.124	1.438	381	147.4	6.28	5.43	342.1	7023	591.5	7.95
	100	API	24.000	21.000	1.500	403	145.4	6.28	5.38	339.9	7200	610.0	7.94
42			24.000	20.750	1.625	443	141.4	6.28	5.33	336.1	7823	651.5	7.87
		API	24.000	20.624	1.688	483	138.4	6.28	5.20	310.3	8627	718.9	7.78
		API	24.000	20.500	1.750	512	136.4	6.28	5.16	308.1	8820	738.0	7.77
		API	24.000	20.376	1.812	542	134.4	6.28	5.11	305.9	9013	757.1	7.76
	160	API	24.000	20.250	1.875	572	132.4	6.28	5.06	303.7	9206	776.2	7.75

CRANE COMPANY, INC. 377, GALELLO, CALIF. 94501, U.S.A.

These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufactured weight'—see 2.1.3



\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufacturers' weights'—see 2.1.3

**PIPE DATA** REPRODUCED BY PERMISSION OF THE CRANE COMPANY.  
MIDWEST FITTING DIVISION

**TABLE P-1**

Nom. Pipe Size	In.	THICKNESS		DIMENSIONS			WEIGHTS			AREAS				PROPERTIES			Approx. Weight of Welding Rods
		Sch. No.	Other	Outside Diam.	Inside Diam.	Wall Thkn.	Plain End Pipe lb. per ft.	Water In. Pipe lb. per ft.	Surface		Cross-Sectional		Moment of Inertia	Section Modulus	Radius of Gyration		
									Outside ft. <sup>2</sup> per ft.	Inside ft. <sup>2</sup> per ft.	Flow	Metal					
26	10	API	26.000	25.500	.250	67	221.4	6.81	6.68	510.7	19.85	1646	126.6	9.10	3.5		
		API	26.000	25.438	.281	77	220.3	6.81	6.66	508.2	22.70	1877	144.4	9.09	4.2		
		API	26.000	25.376	.312	86	219.2	6.81	6.64	505.8	25.18	2076	159.7	9.08	5.0		
		STD	26.000	25.312	.344	94	218.2	6.81	6.63	503.2	27.73	2280	175.4	9.07	6.0		
		API	26.000	25.250	.375	103	217.1	6.81	6.61	500.7	30.19	2478	190.6	9.06	6.9		
XS	20	API	26.000	25.188	.406	111	216.0	6.81	6.59	498.3	32.64	2673	205.6	9.05	7.8		
		API	26.000	25.124	.438	120	214.9	6.81	6.58	495.8	35.17	2874	221.1	9.04	8.8		
		API	26.000	25.062	.469	128	213.7	6.81	6.56	493.3	37.62	3066	235.8	9.03	9.9		
		API	26.000	25.000	.500	136	212.8	6.81	6.54	490.9	40.06	3259	250.7	9.02	11		
		API	26.000	24.876	.562	153	210.5	6.81	6.51	486.0	44.91	3635	279.6	9.00	13		
		API	26.000	24.750	.625	169	208.6	6.81	6.48	481.1	49.82	4013	308.7	8.98	16		
		API	26.000	24.500	.750	202	204.4	6.81	6.41	471.4	59.49	4744	364.9	8.93	22		
			26.000	24.250	.875	235	200.2	6.81	6.35	461.9	69.07	5458	419.9	8.89	25		
			26.000	24.000	1.000	267	196.1	6.81	6.28	452.4	78.54	6149	473.0	8.85	32		
			26.000	23.750	1.125	299	192.1	6.81	6.22	443.0	87.91	6813	524.1	8.80	38		
			26.000	23.500	1.250	330	187.9	6.81	6.15	433.7	97.19	7461	573.9	8.76	46		
			26.000	23.250	1.375	362	184.1	6.81	6.09	424.6	106.37	8088	623.2	8.72	53		
			26.000	23.000	1.500	393	180.1	6.81	6.02	415.5	115.45	8695	668.8	8.68	61		
28	STD	API	28.000	27.500	.250	74	257.3	7.33	7.20	594.0	21.80	2098	149.8	9.81	3.8		
		API	28.000	27.438	.281	83	256.1	7.33	7.18	591.3	24.47	2350	167.8	9.80	4.6		
		API	28.000	27.376	.312	92	255.0	7.33	7.17	588.6	27.14	2601	185.8	9.79	5.4		
		API	28.000	27.312	.344	102	253.8	7.33	7.15	585.9	29.89	2858	204.1	9.78	6.4		
		API	28.000	27.250	.375	111	252.6	7.33	7.13	583.2	32.54	3105	221.8	9.77	7.4		
XS	20	API	28.000	27.188	.406	120	251.5	7.33	7.12	580.6	35.20	3351	239.4	9.76	8.4		
		API	28.000	27.124	.438	129	250.3	7.33	7.10	577.8	37.93	3602	257.3	9.75	9.5		
		API	28.000	27.062	.469	138	249.2	7.33	7.08	575.2	40.56	3844	274.6	9.74	11		
		API	28.000	27.000	.500	147	248.0	7.33	7.07	572.6	43.20	4085	291.8	9.72	12		
		API	28.000	26.750	.625	183	243.4	7.33	7.00	562.0	53.75	5038	359.8	9.68	17		
		API	28.000	26.500	.750	218	238.9	7.33	6.94	551.6	64.21	5964	426.0	9.64	23		
		API	28.000	26.250	.875	253	234.4	7.33	6.87	541.2	74.56	6865	490.3	9.60	27		
			28.000	26.000	1.000	288	230.0	7.33	6.81	530.9	84.82	7740	552.8	9.55	34		
			28.000	25.750	1.125	323	225.6	7.33	6.74	520.8	94.98	8590	613.6	9.51	41		
			28.000	25.500	1.250	357	221.2	7.33	6.68	510.7	105.05	9417	672.6	9.47	49		
			28.000	25.250	1.375	391	216.9	7.33	6.61	500.7	115.01	10219	729.9	9.43	57		
			28.000	25.000	1.500	425	212.6	7.33	6.54	490.9	124.88	10997	785.5	9.38	66		
30	STD	API	30.000	29.500	.250	79	296.3	7.85	7.72	683.4	23.37	2385	172.3	10.52	4.1		
		API	30.000	29.438	.281	89	295.1	7.85	7.70	680.5	26.24	2697	193.1	10.51	4.9		
		API	30.000	29.376	.312	99	293.7	7.85	7.69	677.8	29.19	3201	213.4	10.50	5.8		
		API	30.000	29.312	.344	109	292.6	7.85	7.67	674.8	32.04	3524	235.0	10.49	6.9		
		API	30.000	29.250	.375	119	291.2	7.85	7.66	672.0	34.90	3823	254.8	10.48	8.0		
XS	20	API	30.000	29.188	.406	130	290.7	7.85	7.64	669.0	37.75	4132	275.5	10.46	9.0		
		API	30.000	29.124	.438	138	288.8	7.85	7.62	666.1	40.68	4442	296.2	10.45	10		
		API	30.000	29.062	.469	148	287.3	7.85	7.61	663.4	43.51	4744	316.3	10.44	11		
		API	30.000	29.000	.500	158	286.2	7.85	7.59	660.5	46.34	5033	335.5	10.43	13		
		API	30.000	28.750	.625	196	281.3	7.85	7.53	649.2	57.68	6213	414.2	10.39	18		
		API	30.000	28.500	.750	234	276.6	7.85	7.46	637.9	68.92	7371	491.4	10.34	25		
		API	30.000	28.250	.875	272	271.8	7.85	7.39	620.7	80.06	8494	566.2	10.30	29		
			30.000	28.000	1.000	310	267.0	7.85	7.33	615.7	91.11	9591	639.4	10.26	36		
			30.000	27.750	1.125	347	262.2	7.85	7.26	604.7	102.05	10653	710.2	10.22	44		
			30.000	27.500	1.250	384	257.5	7.85	7.20	593.9	112.90	11682	778.8	10.17	53		
			30.000	27.250	1.375	421	252.9	7.85	7.13	583.1	123.65	12694	846.2	10.13	62		
			30.000	27.000	1.500	457	248.2	7.85	7.07	572.5	134.30	13673	911.5	10.09	71		

26

28

30

Plating Guide: PO Box 277, Colton, CA 95326, USA

\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufacturers' weights'—see 2.1.3

Piping Guide: PO Box 277, Colton, CA 95328, USA

# **PIPE DATA** REPRODUCED BY PERMISSION OF THE CRANE COMPANY, MIDWEST FITTING DIVISION

**TABLE P-1**

Nom. Pipe Size	WALL THICKNESS	DIMENSIONS			WEIGHTS		AREAS				PROPERTIES			Approx. Weight of Welding Rods		
		Sch. No.	Other	Outside Diam.	Inside Diam.	Wall Thkn.	Plain End Pipe	Water In Pipe	Surface		Cross-Sectional		Moment of Inertia		Section Modulus	Radius of Gyration
									Outside	Inside	Flow	Metal				
In.		In.	In.	In.	lb. per ft.	lb. per ft.	lb. per ft.	ft. <sup>2</sup> per ft.	ft. <sup>2</sup> per ft.	In. <sup>2</sup>	In. <sup>2</sup>	In. <sup>4</sup>	In. <sup>3</sup>	In.	In.	
32		API	32.000	31.500	.250	85	337.8	8.38	8.25	779.2	24.93	3141	196.3	11.22	4.3	
		API	32.000	31.438	.281	95	336.5	8.38	8.23	776.2	28.04	3525	220.3	11.21	5.2	
		API	32.000	31.376	.312	106	335.2	8.38	8.21	773.2	31.02	3891	243.2	11.20	6.2	
	STD	API	32.000	31.312	.344	116	333.8	8.38	8.20	770.0	34.24	4287	268.0	11.19	7.4	
		API	32.000	31.250	.375	127	332.5	8.38	8.18	766.9	37.25	4656	291.0	11.18	8.5	
		API	32.000	31.188	.406	137	331.2	8.38	8.16	764.0	40.29	5025	314.1	11.17	10	
	XS	API	32.000	31.124	.438	148	329.8	8.38	8.15	760.8	43.43	5407	337.9	11.16	11	
		API	32.000	31.062	.469	158	328.2	8.38	8.13	757.8	46.46	5775	360.9	11.15	12	
		API	32.000	31.000	.500	168	327.2	8.38	8.11	754.7	49.48	6140	383.8	11.14	14	
		API	32.000	30.750	.625	209	321.9	8.38	8.05	742.5	61.59	7578	473.6	11.09	20	
34		API	32.000	30.624	.688	230	319.0	8.38	8.02	736.6	67.68	8298	518.6	11.07	23	
		API	32.000	30.500	.750	250	316.7	8.38	7.98	730.5	73.63	8990	561.9	11.05	27	
			32.000	30.000	1.000	331	306.4	8.38	7.85	706.8	97.38	11680	730.0	10.95	39	
			32.000	29.500	1.250	410	296.3	8.38	7.72	683.5	120.76	14398	899.9	10.88	56	
			32.000	29.000	1.500	489	286.3	8.38	7.59	660.5	143.73	16752	1047.0	10.80	76	
		API	34.000	33.500	.250	90	382.0	8.90	8.77	881.2	26.50	3773	221.9	11.93	4.6	
		API	34.000	33.438	.281	101	380.7	8.90	8.75	878.2	29.77	4230	248.8	11.92	6.1	
		API	34.000	33.376	.312	112	379.3	8.90	8.74	874.9	32.99	4680	275.3	11.91	6.6	
	STD	API	34.000	33.312	.344	124	377.8	8.90	8.72	871.6	36.36	5147	302.8	11.90	7.8	
		API	34.000	33.250	.375	135	376.2	8.90	8.70	867.8	39.61	5597	329.2	11.89	9.0	
36		API	34.000	33.188	.406	146	375.0	8.90	8.69	865.0	42.88	6047	355.7	11.87	10	
		API	34.000	33.124	.438	157	373.6	8.90	8.67	861.7	46.18	6501	382.4	11.86	12	
		API	34.000	33.062	.469	168	371.9	8.90	8.66	858.5	49.40	6945	408.5	11.85	13	
		API	34.000	33.000	.500	179	370.8	8.90	8.64	855.3	52.62	7385	434.4	11.85	14	
		API	34.000	32.750	.625	223	365.0	8.90	8.57	841.9	65.53	9124	536.7	11.80	21	
		API	34.000	32.624	.688	245	362.1	8.90	8.54	835.9	72.00	9992	587.8	11.78	25	
		API	34.000	32.500	.750	266	359.5	8.90	8.51	829.3	78.34	10829	637.0	11.76	28	
			34.000	32.000	1.000	353	348.6	8.90	8.38	804.2	103.67	14114	830.2	11.67	42	
			34.000	31.500	1.250	437	337.8	8.90	8.25	779.2	128.61	17246	1014.5	11.58	60	
			34.000	31.000	1.500	521	327.2	8.90	8.11	754.7	153.15	20247	1191.0	11.50	81	
42		API	36.000	35.500	.250	96	429.1	9.42	9.29	989.7	28.11	4491	249.5	12.64	4.8	
		API	36.000	35.438	.281	107	427.6	9.42	9.28	986.4	31.49	5023	279.1	12.63	5.9	
		API	36.000	35.376	.312	119	426.1	9.42	9.26	982.9	34.95	5565	309.1	12.62	7.0	
	STD	API	36.000	35.312	.344	131	424.6	9.42	9.24	979.3	38.56	6127	340.4	12.60	8.2	
		API	36.000	35.250	.375	143	423.1	9.42	9.23	975.8	42.01	6664	370.2	12.59	9.5	
		API	36.000	35.188	.406	154	421.6	9.42	9.21	972.5	45.40	7191	399.5	12.58	11	
		API	36.000	35.124	.438	166	420.1	9.42	9.19	968.9	48.93	7737	429.9	12.57	12	
	XS	API	36.000	35.062	.469	178	418.2	9.42	9.18	965.5	52.35	8263	459.0	12.56	14	
		API	36.000	35.000	.500	190	417.1	9.42	9.16	962.1	55.76	8785	488.1	12.55	15	
		API	36.000	34.876	.562	213	413.8	9.42	9.13	955.3	62.57	9825	545.8	12.53	19	

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CRANE COMPANY, P.O. Box 277, Central, CA 95026, USA

\*These 'iron pipe size' dimensions are for steel pipe, and are referred to in the Piping Guide (Part I) as 'manufacturers' weights'—see 2.1.3

# PERSONNEL CLEARANCES

TABLE 6.1 GIVES  
ADDITIONAL  
DIMENSIONS

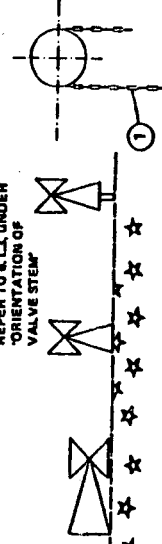
## CHART P-2

### CLEARANCES TO MANUAL VALVES AND SUGGESTED OPERATING HEIGHTS

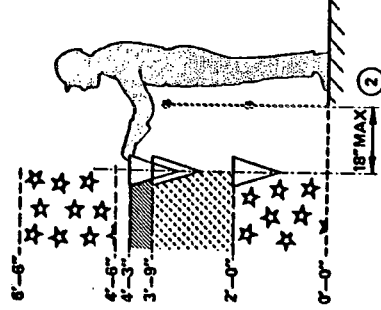
#### OVERHEAD VALVES

FOR VALVE OPERATION  
ABOVE 8'-6". REFER TO  
6.1.3 UNDER OPERATING  
ACCESS TO VALVES

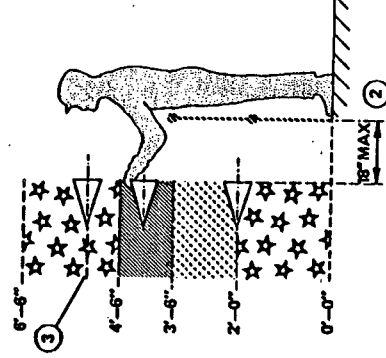
INVERTED VALVES:  
REFER TO 6.1.1 UNDER  
"ORIENTATION OF  
VALVE STEM"



#### VERTICAL VALVES



#### HORIZONTAL VALVES



#### KEY

PREFERRED ELEVATIONS

SECOND-CHOICE ELEVATIONS

LEG OR HEAD HAZARD, UNLESS  
PROTECTION GIVEN BY RAILING,  
PIPING, EQUIPMENT, ETC.

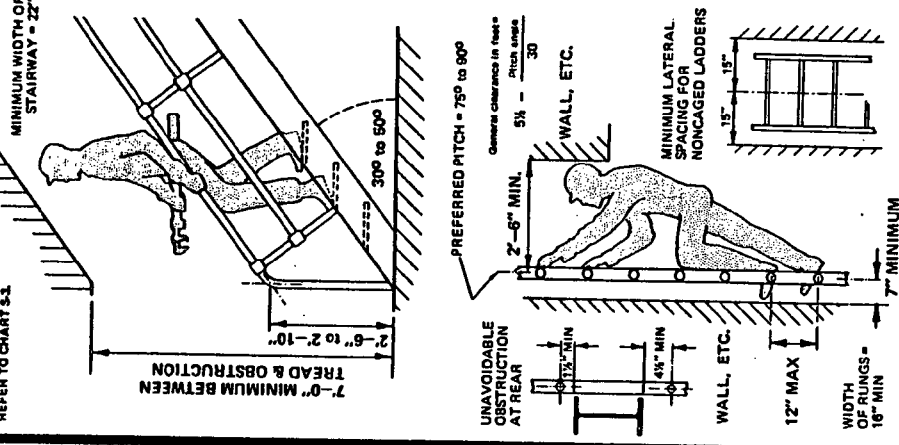
#### NOTES

- (1) TAKE CHAINS TO 3 FT FROM OPERATING FLOOR LEVEL. DO NOT HANG CHAINS IN A WALKWAY
- (2) DIMENSION APPLIES IF RAILING IS PRESENT
- (3) IF A RAILING IS PRESENT, COMFORTABLE OPERATING ELEVATION IS 5 FT TO 5 FT 6 IN.

"Piping Guide", PO Box 277, Cotati, CA 94928, USA

### CLEARANCES AROUND STAIRWAYS & LADDERS

DATA FROM PART 1916 (J) OF THE  
FEDERAL OCCUPATIONAL SAFETY  
AND HEALTH STANDARDS, 1971.  
U.S. DEPARTMENT OF LABOR.  
REFER TO CHART 5.1



## RING-JOINT DATA

RING NUMBERS AND GAPS BETWEEN OPPOSING RAISED FACES  
OF RING-JOINT FLANGES UNDER NORMAL COMPRESSION

TABLE R-1

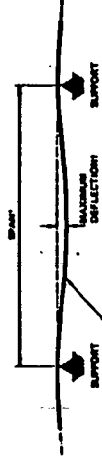
PSI	NOMINAL PIPE SIZE (IN.)	1/2	3/4	1	1 1/2	2	2 1/2	3	4	6	8	10	12	14	16	18	20	24
150	RING NUMBER GAP (INCH)																	
300	RING NUMBER GAP (INCH)																	
600	RING NUMBER GAP (INCH)																	
900	RING NUMBER GAP (INCH)																	
1500	RING NUMBER GAP (INCH)																	
2500	RING NUMBER GAP (INCH)																	

# SPANS OF HORIZONTAL PIPE

# TABLE S-1

THESE TABLES GIVE SPANS SUITABLE FOR PIPE ARRANGED IN PIPEWAYS, AND APPLY WHEN THE SPAN IS PART OF A STRAIGHT PIPE, WITH TWO OR MORE SPANS AT EACH END.

FOR VALUES OF BENDING STRESS & MODULUS, REFER TO CHARTS S-2



STEEL PIPE, SCHEDULE 160

NOMINAL PIPE SIZE	PIPE SPAN*		WEIGHT OF WATER-FILLED PIPE SPAN (Lb.)	MAXIMUM DEFLECTION* (In.)
	FL	IN.		
1.0-INCH	15	8.77	48	0.234
1.5-INCH	19	3.28	105	0.243
2.0-INCH	21	6.79	182	0.243
2.5-INCH	23	9.87	275	0.245
3.0-INCH	26	3.66	438	0.245
4.0-INCH	29	9.30	793	0.245
6.0-INCH	36	2.01	1,970	0.245
8.0-INCH	41	2.89	3,732	0.245
10.0-INCH	45	11.75	6,465	0.244
12.0-INCH	50	0.40	9,801	0.244
14.0-INCH	52	4.67	12,186	0.243
16.0-INCH	56	0.99	16,875	0.244
18.0-INCH	59	5.13	22,582	0.244
20.0-INCH	62	8.17	29,266	0.244
24.0-INCH	68	7.74	45,923	0.244

STEEL PIPE, SCHEDULE 10

NOMINAL PIPE SIZE	PIPE SPAN*		WEIGHT OF WATER-FILLED PIPE SPAN (Lb.)	MAXIMUM DEFLECTION* (In.)
	FL	IN.		
1.0-INCH	15	11.14	29	0.240
1.5-INCH	18	5.62	56	0.223
2.0-INCH	19	11.77	84	0.209
2.5-INCH	21	7.24	127	0.202
3.0-INCH	22	10.63	182	0.186
4.0-INCH	24	5.31	288	0.164
6.0-INCH	27	5.75	632	0.141
8.0-INCH	29	9.72	1,103	0.128
10.0-INCH	32	0.93	1,782	0.119
12.0-INCH	33	11.37	2,592	0.112
14.0-INCH	38	5.23	3,809	0.131
16.0-INCH	39	4.50	4,886	0.120
18.0-INCH	40	1.82	6,087	0.111
20.0-INCH	40	8.77	7,454	0.103
24.0-INCH	41	9.43	10,530	0.090

STEEL PIPE, SCHEDULE 80

NOMINAL PIPE SIZE	PIPE SPAN*		WEIGHT OF WATER-FILLED PIPE SPAN (Lb.)	MAXIMUM DEFLECTION* (In.)
	FL	IN.		
1.0-INCH	16	1.05	40	0.244
1.5-INCH	19	4.29	85	0.245
2.0-INCH	21	6.49	136	0.243
2.5-INCH	23	9.02	225	0.244
3.0-INCH	26	0.66	342	0.241
4.0-INCH	29	3.07	584	0.236
6.0-INCH	35	0.22	1,396	0.230
8.0-INCH	39	4.67	2,489	0.223
10.0-INCH	43	8.21	4,172	0.220
12.0-INCH	47	5.26	6,290	0.219
14.0-INCH	43	9.95	7,883	0.220
16.0-INCH	52	10.78	10,934	0.217
18.0-INCH	56	0.58	14,545	0.217
20.0-INCH	59	0.02	18,786	0.216
24.0-INCH	64	5.48	29,341	0.215

ALUMINUM PIPE, SCHEDULE 80

NOMINAL PIPE SIZE	PIPE SPAN*		WEIGHT OF WATER-FILLED PIPE SPAN (Lb.)	MAXIMUM DEFLECTION* (In.)
	FL	IN.		
1.0-INCH	17	4.67	18	0.414
1.5-INCH	20	2.26	41	0.386
2.0-INCH	22	0.13	66	0.367
2.5-INCH	24	5.26	110	0.374
3.0-INCH	26	4.25	169	0.357
4.0-INCH	28	11.94	295	0.336
6.0-INCH	33	11.69	719	0.314
8.0-INCH	37	6.31	1,306	0.294
10.0-INCH	39	8.42	1,936	0.264

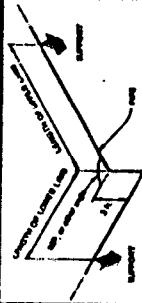
STEEL PIPE, SCHEDULE 40

NOMINAL PIPE SIZE	PIPE SPAN*		WEIGHT OF WATER-FILLED PIPE SPAN (Lb.)	MAXIMUM DEFLECTION* (In.)
	FL	IN.		
1.0-INCH	16	1.07	33	0.244
1.5-INCH	19	0.49	69	0.237
2.0-INCH	20	11.53	107	0.230
2.5-INCH	23	3.20	183	0.234
3.0-INCH	25	3.65	273	0.227
4.0-INCH	28	2.01	458	0.218
6.0-INCH	32	10.37	1,035	0.202
8.0-INCH	36	7.40	1,836	0.193
10.0-INCH	40	0.55	2,987	0.185
12.0-INCH	42	11.48	4,386	0.180
14.0-INCH	44	11.52	5,463	0.173
16.0-INCH	47	10.83	7,640	0.178
18.0-INCH	50	10.65	10,289	0.179
20.0-INCH	52	11.02	12,880	0.174
24.0-INCH	57	5.84	19,644	0.171

ALUMINUM PIPE, SCHEDULE 40

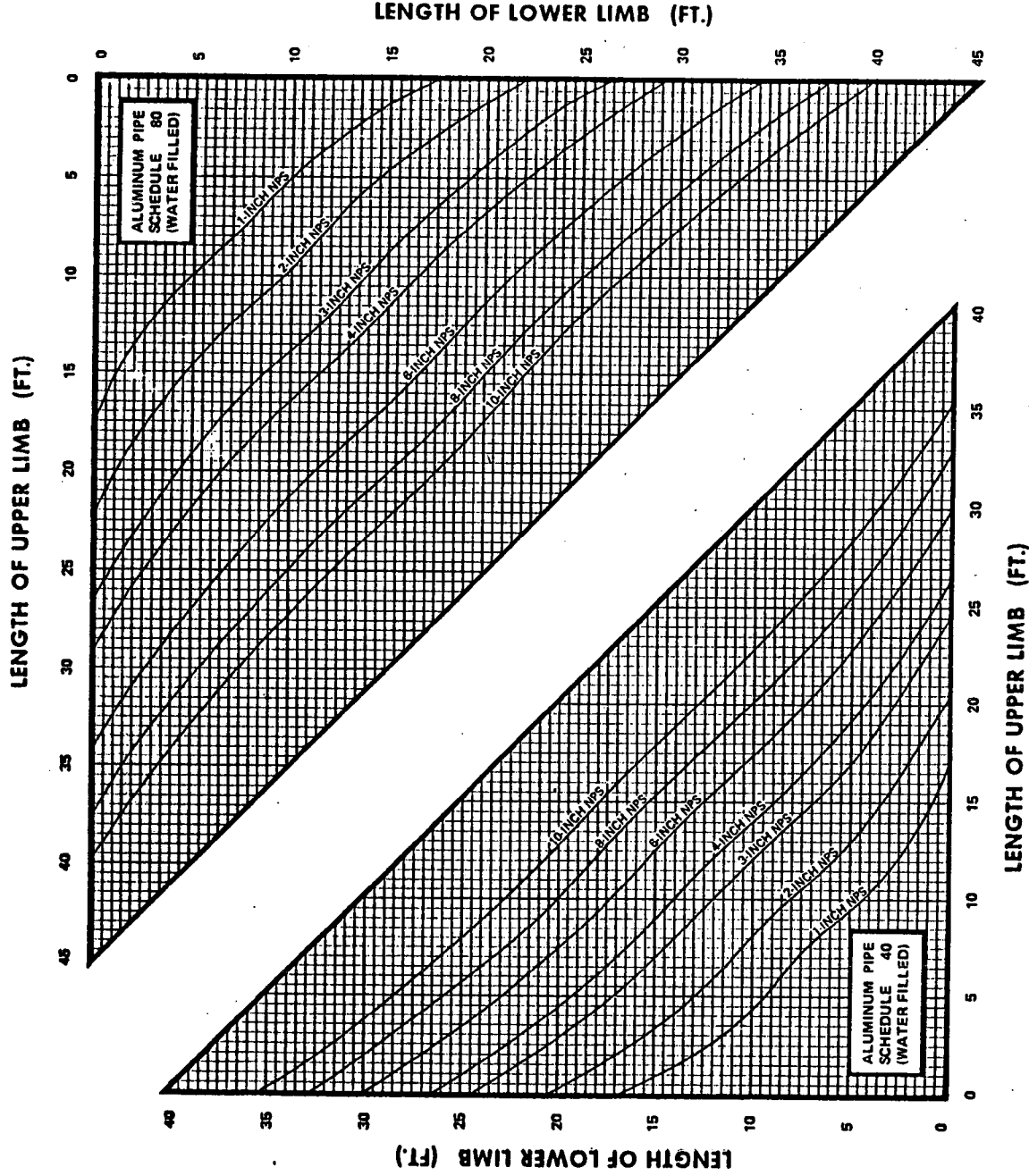
NOMINAL PIPE SIZE	PIPE SPAN*		WEIGHT OF WATER-FILLED PIPE SPAN (Lb.)	MAXIMUM DEFLECTION* (In.)
	FL	IN.		
1.0-INCH	16	8.12	16	0.381
1.5-INCH	18	11.07	34	0.339
2.0-INCH	20	3.62	55	0.313
2.5-INCH	22	10.19	93	0.327
3.0-INCH	24	4.06	142	0.305
4.0-INCH	26	4.46	244	0.278
6.0-INCH	29	10.15	509	0.242
8.0-INCH	32	8.27	1,029	0.223
10.0-INCH	35	3.12	1,695	0.206

# SPANS OF HORIZONTAL PIPE WITH 3-FT. RISE OR FALL



## CHARTS S-2

THESE CHARTS GIVE THE MAXIMUM LENGTH OF SPAN FOR A 3-FT. RISE OR FALL IN THE PIPING ARRANGEMENT SHOWN, AND ON FALLS, COMES AT EACH END, TWO OR MORE STRAIGHT SPANS AT EACH END.



LOWER CHART:  
SCH 40, ALUMINUM

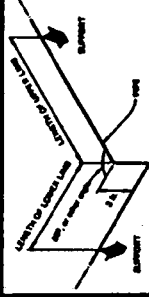
Data for water-filled steel pipe are based on a maximum bending stress of 4000 PSI, occurring at supports and due to bending by the weight of pipe plus water; applied stresses may increase the resultant tensile stress. These data apply to carbon-steel and stainless-steel pipe having a tensile modulus of elasticity of 29,000,000 PSI. For water-filled aluminum pipe, spans are similarly based on a stress of 2000 PSI and a modulus of 10,000,000 PSI.

UPPER CHART:  
SCH 80, ALUMINUM

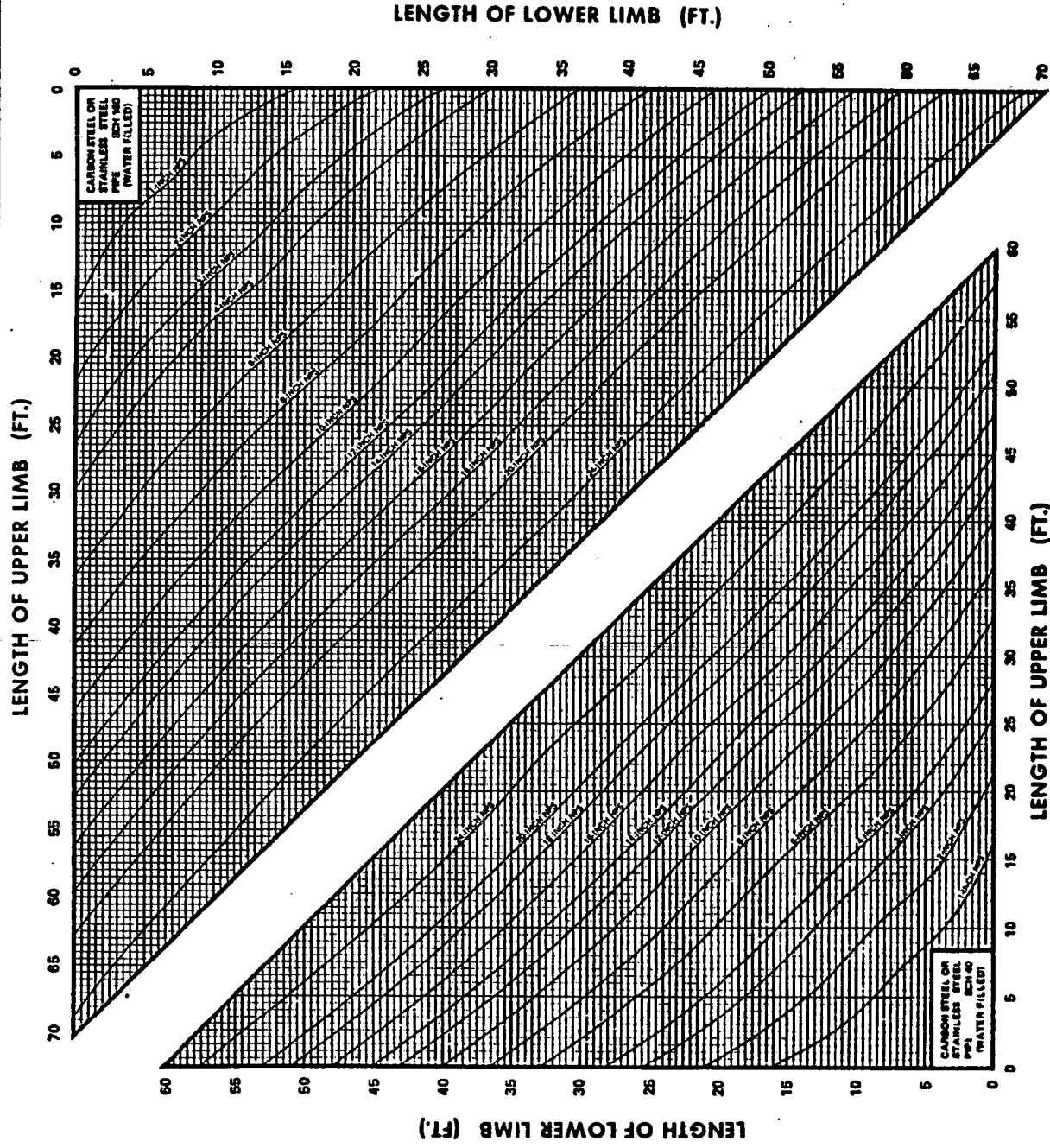
"Piping Guide", PO Box 277, Cotati, CA 94928, USA

# SPANS OF HORIZONTAL PIPE WITH 3-FT. RISE OR FALL

## CHARTS S-2



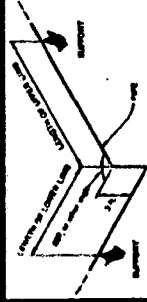
THESE CHARTS GIVE THE MAXIMUM LENGTH PERMISSIBLE FOR EITHER HORIZONTAL LIMB IN THE PIPING ARRANGEMENT SHOWN, AND OR FALL IS CONTINUOUS WITH TWO OR MORE STRAIGHT SPANS AT EACH END.



Data for water-filled steel pipe are based on a maximum bending stress of 4,000 PSI, occurring at supports and due to bending by the weight of pipe plus water; applied stresses may increase the resultant tensile stress. These data apply to carbon-steel and stainless-steel pipe having a tensile modulus of elasticity of 29,000,000 PSI. For water-filled aluminum pipe spans are similarly based on a stress of 2,000 PSI and a modulus of 10,000,000 PSI.

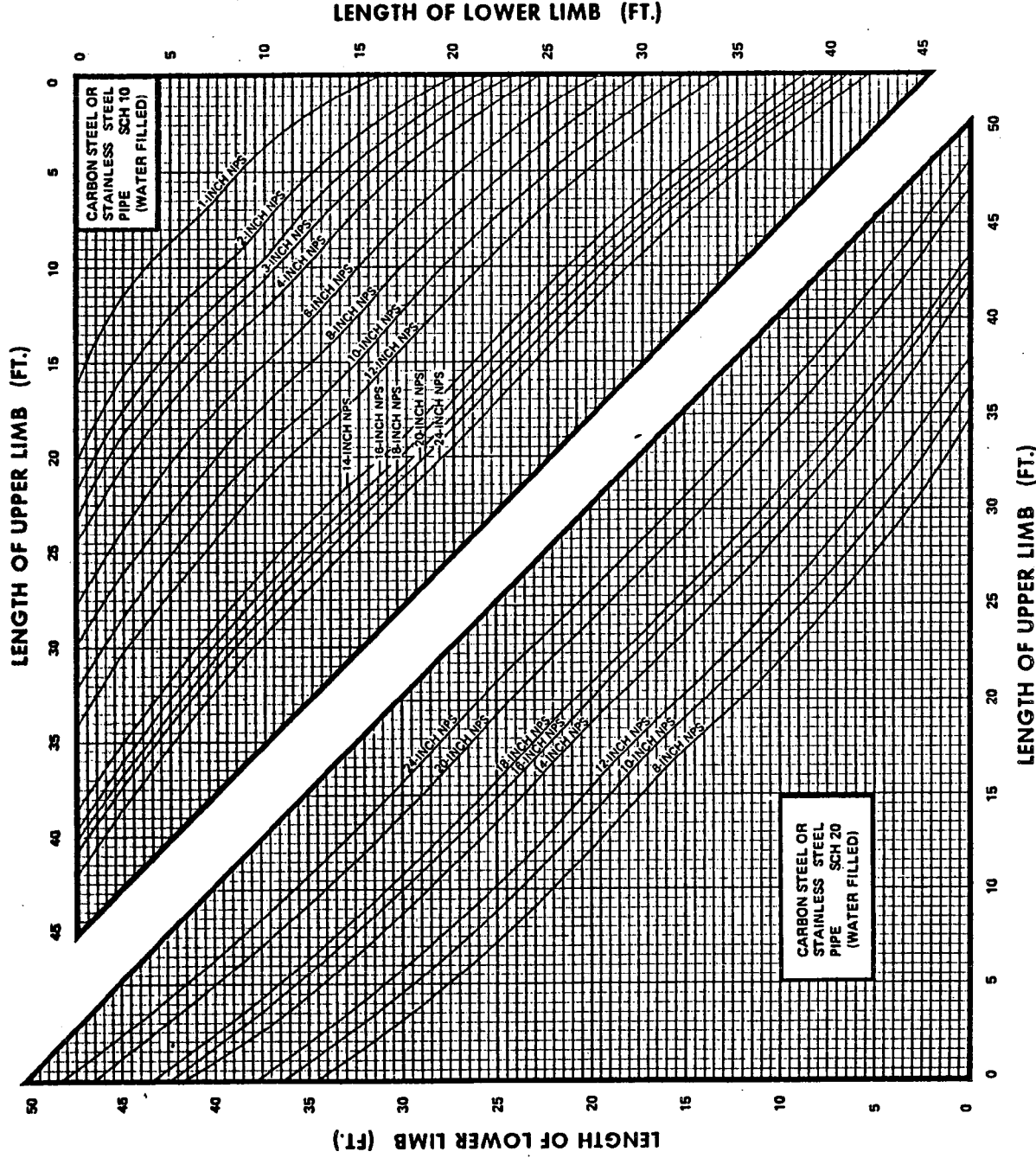
Piping Guide, P.O. Box 277, Corvallis, OR 97331

# SPANS OF HORIZONTAL PIPE WITH 3-FT. RISE OR FALL



## CHARTS S-2

THESE CHARTS GIVE THE MAXIMUM LENGTH OF PIPE SPANS FOR THE HORIZONTAL LIMB IN THE RISING ARRANGEMENT SHOWN AND FOR THE HORIZONTAL LIMB IN THE FALLING OR FALLS CONTINUOUS WITH TWO OR MORE STRAIGHT SPANS AT EACH END.



**LOWER CHART:**  
**SCH 20, STEEL**

Data for water-filled steel pipe are based on a maximum bending stress of 4000 PSI, occurring at supports and due to bending by the weight of pipe plus water; applied stresses may increase the resultant tensile stress. These data apply to carbon-steel and stainless-steel pipe having a tensile modulus of elasticity of 29,000,000 PSI. For water-filled aluminum pipe, spans are similarly based on a stress of 2000 PSI and a modulus of 10,000,000 PSI.

**UPPER CHART:**  
**SCH 10, STEEL**

"Piping Guide", P.O. Box 277, Cotati, CA 94928, USA



# STAIRWAYS

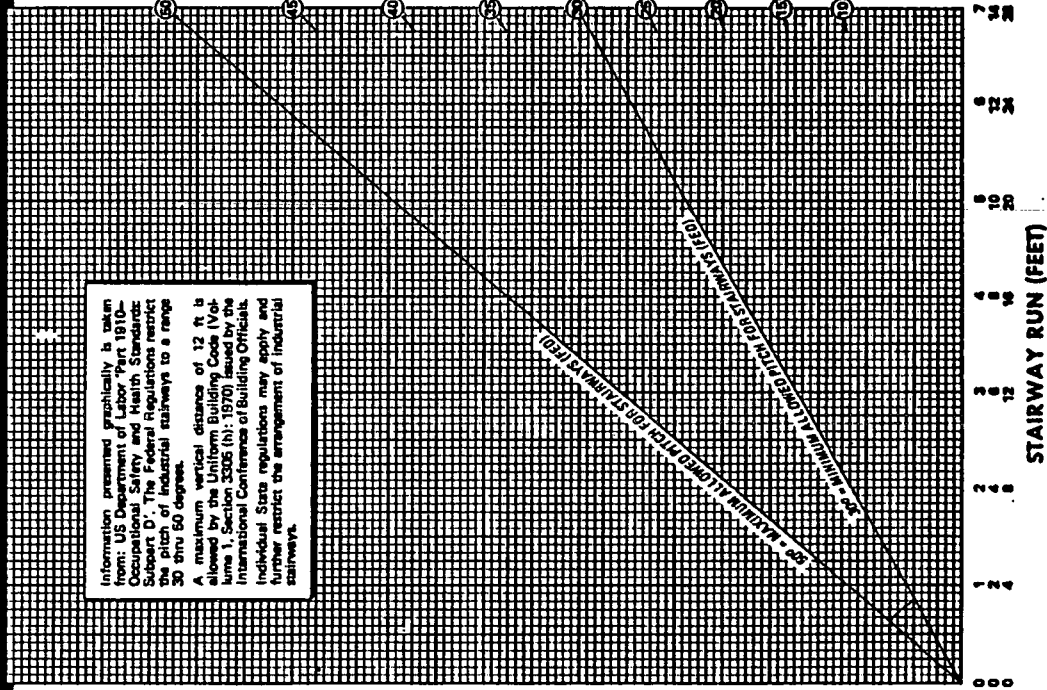
U.S. FEDERAL GOVERNMENT REGULATIONS  
FOR FIXED INDUSTRIAL STAIRWAYS

## CHART S-3

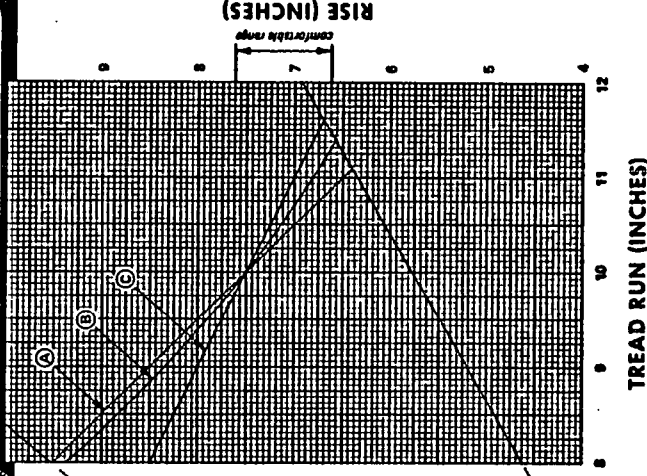
Information presented graphically is taken from: US Department of Labor, Part 1910-Occupational Safety and Health Standards, Subpart D, "The Federal Regulations restrict the pitch of industrial stairways to a range 30 thru 60 degrees.

A maximum vertical distance of 12 ft is allowed by the Uniform Building Code (Volume 1, Section 2305 (h): 1970) issued by the International Conference of Building Officials. Individual State regulations may apply and further restrict the arrangement of industrial stairways.

LANDING-TO-LANDING HEIGHT (FEET)



PITCH ANGLE OF STAIRWAY (DEGREES)

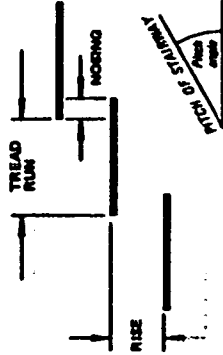


TREAD RUN (INCHES)

RISE (INCHES)

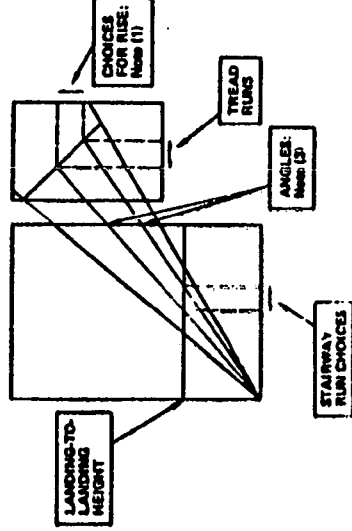
### KEY

- A R = RISE IN INCHES, T = TREAD RUN IN INCHES. LINE (A) IS BASED ON  $R + T = 17\frac{1}{2}$
- B THE FEDERAL REGULATIONS SUGGEST LINE (A) COMBINATIONS OF RISE AND TREAD RUN
- C THIS LINE IS BASED ON  $R + T = 15$
- D THIS LINE IS BASED ON  $2R + T = 25$



### NOTES

- 1 LANDING-TO-LANDING HEIGHT IS USUALLY ESTABLISHED. DIVIDE THIS HEIGHT INTO WHOLE NUMBERS OF RISES.
- 2 SELECT ONE OF THE LINES A, B, OR C (OR OTHER COMPANY PREFERENCE) AND MARK VALUES FOR RISES ON THE LINE.
- 3 CONSTRUCT LINES FROM THESE POINTS TO THE BOTTOM LEFT CORNER OF THE LARGER GRAPH. THIS GIVES THE CHOICE OF ANGLES AND RUNS FOR THE STAIRWAY.



"Piping Guide", P.O. Box 277, Cotati, CA 94926, USA



# STRUCTURAL STEEL DATA TABLES S-4

THESE TABLES ARE ABSTRACTED, WITH PERMISSION, FROM  
THE MANUAL OF STEEL CONSTRUCTION (THE LATEST) PUBLISHED  
BY THE AMERICAN INSTITUTE OF STEEL CONSTRUCTION, INC.

W SHAPES

DEPTH

DESIGNATION FOR W SHAPES (Channel figures left)	DEPTH	WIDTH	THICKNESS
DIMENSION IN INCHES			

DESIGNATION FOR W SHAPES (Channel figures left)	DEPTH	WIDTH	THICKNESS
DIMENSION IN INCHES			

DESIGNATION FOR W SHAPES (Channel figures left)	DEPTH	WIDTH	THICKNESS
DIMENSION IN INCHES			

DESIGNATION FOR W SHAPES (Channel figures left)	DEPTH	WIDTH	THICKNESS
DIMENSION IN INCHES			

## W 36 x

W 36x300	36 3/4	16 1/2	1 1/4
X 280	36 1/4	16 1/2	1 1/4
X 260	36 1/4	16 1/2	1 1/4
X 245	36	16 1/2	1 1/4
X 230	35 7/8	16 1/2	1 1/4
X 194	36 1/2	12 1/2	1 1/4
X 182	36 1/2	12 1/2	1 1/4
X 170	36 1/2	12	1 1/4
X 160	36	12	1 1/4
X 150	35 7/8	12	1 1/4
X 135	35 1/2	12	1 1/4

## W 33 x

W 33x240	33 1/2	15 1/2	1 1/4
X 220	33 1/4	15 1/2	1 1/4
X 200	33	15 1/2	1 1/4
X 152	33 1/2	11 1/2	1 1/4
X 141	33 1/4	11 1/2	1 1/4
X 130	33 1/2	11 1/2	7/8
X 118	32 7/8	11 1/2	7/8

## W 30 x

W 30x210	30 3/4	15 1/2	1 1/4
X 190	30 3/4	15	1 1/4
X 172	29 3/4	15	1 1/4
X 132	30 1/4	10 1/2	1 1/4
X 124	30 3/4	10 1/2	7/8
X 116	30	10 1/2	3/4
X 108	29 3/4	10 1/2	3/4
X 99	29 3/4	10 1/2	1 1/4

## W 27 x

W 27x177	27 1/4	14 1/2	1 1/4
X 160	27 1/4	14	1 1/4
X 145	26 3/4	14	1
X 114	27 1/4	10 1/2	1 1/4
X 102	27 1/4	10	1 1/4
X 94	26 3/4	10	3/4
X 84	26 3/4	10	3/4

## W 24 x

W 24x160	24 3/4	14 1/2	1 1/4
X 145	24 1/2	14	1
X 130	24 1/4	14	7/8
X 120	24 1/4	12 1/2	1 1/4
X 110	24 1/2	12	7/8
X 100	24	12	3/4
X 94	24 1/4	9	3/4
X 84	24 1/4	9	3/4
X 76	23 3/4	9	1 1/4
X 68	23 3/4	9	9/8
X 61	23 3/4	7	9/8
X 55	23 1/2	7	7/8

## W 21 x

W 21x142	21 1/2	13 1/2	1 1/4
X 127	21 1/4	13	1
X 112	21	13	7/8
X 96	21 1/4	9	7/8
X 82	20 3/4	9	7/8
X 73	21 1/4	8 1/2	7/8
X 68	21 1/4	8 1/2	7/8
X 62	21	8 1/2	7/8
X 55	20 3/4	8 1/2	7/8
X 49	20 3/4	8 1/2	7/8
X 44	20 3/4	6 1/2	7/8

## W 18 x

W 18x114	18 1/2	11 7/8	1 1/4
X 105	18 1/4	11 1/4	1 1/4
X 96	18 1/4	11 1/4	7/8
X 85	18 1/4	8 1/2	7/8
X 77	18 1/4	8 1/2	7/8
X 70	18	8 1/2	7/8
X 64	17 7/8	8 1/2	7/8
X 60	18 1/4	7 1/2	7/8
X 55	18 1/4	7 1/2	7/8
X 50	18	7 1/2	7/8
X 45	17 7/8	7 1/2	7/8
X 40	17 7/8	6	7/8
X 35	17 1/4	6	7/8

## W 16 x

W 16x96	16 1/2	11 1/2	7/8
X 88	16 1/2	11 1/2	7/8
X 78	16 1/2	8 1/2	7/8
X 71	16 1/2	8 1/2	7/8
X 64	16	8 1/2	7/8
X 58	15 7/8	8 1/2	7/8
X 50	16 1/2	7 1/2	7/8
X 45	16 1/2	7	7/8
X 40	16	7	7/8
X 36	15 7/8	7	7/8
X 31	15 7/8	5 1/2	7/8
X 26	15 1/2	5 1/2	7/8

## W 14 x

W 14x730	22 1/2	17 7/8	4 1/2
X 665	21 3/4	17 7/8	4 1/2
X 605	21	17 3/4	4 1/2
X 550	20 3/4	17 1/4	3 3/4
X 500	19	17	3 1/2
X 455	19	15 7/8	3 1/2
X 426	18 3/4	16 3/4	3 1/2
X 398	18 1/4	16 3/4	2 3/4
X 370	18	16 3/4	2 3/4
X 342	17 1/2	16 3/4	2 1/2
X 320	16 3/4	16 3/4	2 1/2
X 314	17 1/4	16 1/4	2 1/2
X 287	16 3/4	16 1/4	2 1/2
X 264	16 1/2	16	1 1/2

## W 14 x

W 14x245	16 1/4	16	1 1/4
X 237	16 1/4	15 1/2	1 1/4
X 228	16	15 1/2	1 1/4
X 219	15 7/8	15 1/2	1 1/4
X 211	15 1/2	15 1/2	1 1/4
X 202	15 1/2	15 1/2	1 1/2
X 193	15 1/2	15 1/2	1 1/2
X 184	15 1/2	15 1/2	1 1/2
X 176	15 1/4	15 1/2	1 1/2
X 167	15 1/2	15 1/2	1 1/4
X 158	15	15 1/2	1 1/4
X 150	14 3/4	15 1/2	1 1/4
X 142	14 3/4	15 1/2	1 1/4
X 136	14 3/4	14 1/2	1 1/4
X 127	14 3/4	14 1/2	1
X 119	14 1/2	14 1/2	7/8
X 111	14 1/2	14 1/2	7/8
X 103	14 1/4	14 1/2	7/8
X 95	14 1/4	14 1/2	3/4
X 87	14	14 1/2	3/4
X 84	14 1/4	12	3/4
X 78	14	12	3/4
X 74	14 1/4	10 1/2	3/4
X 68	14	10 1/2	3/4
X 61	13 3/4	10	3/4
X 53	14	8	3/4
X 48	13 3/4	8	3/4
X 43	13 3/4	8	1/2
X 38	14 1/4	6 1/2	1/2
X 34	14	6 1/2	7/8
X 30	13 3/4	6 1/2	3/4
X 26	13 3/4	5	7/8
X 22	13 3/4	5	3/4

## W 12 x

W 12x190	14 3/8	12 3/8	1 3/4
X 161	13 7/8	12 1/2	1 1/2
X 133	13 3/8	12 3/8	1 1/4
X 120	13 1/8	12 3/8	1 1/4
X 106	12 7/8	12 1/4	1
X 99	12 3/4	12 1/4	1 1/4
X 92	12 3/4	12 1/4	7/8
X 85	12 1/2	12 1/4	1 1/4
X 79	12 3/4	12 1/4	3/4
X 72	12 1/4	12	1 1/4
X 65	12 1/4	12	3/4
X 58	12 1/4	10	3/4
X 53	12	10	3/4
X 50	12 1/4	8 1/2	3/4
X 45	12	8	3/4
X 40	12	8	1/2
X 36	12 1/4	6 1/2	7/8
X 31	12 1/2	6 1/2	7/8
X 27	12 1/4	4	7/8
X 19	12 1/2	4	3/4
X 16.5	12	4	1/4
X 14	11 7/8	4	1/4

## W 6 x

W 6x25	6 7/8	6 1/8	7/8
X 20	6 3/4	6	3/4
X 15.5	6	6	3/4
X 16	6 1/4	4	3/4
X 12	6	4	1/4
X 8.5	5 7/8	4	3/4

## W 5 x

W 5x18.5	5 1/2	5	7/8
X 16	5	5	3/4

## W 4 x

W 4x13	4 1/4	4	3/4
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## CHANNEL DATA

## ANGLE DATA/AVAILABLE SIZES

## AMERICAN STANDARD

## 1. UNEQUAL LEGS

DESIGNATION (Second figure: lb/ft)	DIMENSIONS IN INCHES			SIZE INCHES	THICKNESS														
	DEPTH	WIDTH	AVERAGE THICKNESS		1	7/8	3/4	5/8	9/16	1/2	7/16	3/8	5/16	1/4	3/16	1/8			
C 15×50 ×40 ×33.9	15	3 3/4	5/8	9x4x	✓	✓	✓	✓	✓	✓									
	15	3 1/2	5/8	8x6x	✓	✓	✓	✓	✓	✓									
	15	3 3/8	5/8	8x4x	✓	✓	✓	✓	✓	✓	✓								
C 12×30 ×25 ×20.7	12	3 1/8	1/2	7x4x		✓	✓	✓	✓	✓	✓								
	12	3	1/2	6x4x		✓	✓	✓	✓	✓	✓	✓							
	12	3	1/2	6x3 1/2 x						✓		✓	✓	✓					
C 10×30 ×25 ×20 ×15.3	10	3	7/16	5x3 1/2 x			✓												
	10	2 7/8	7/16	5x3x			✓				✓	✓	✓	✓					
	10	2 3/4	7/16	5x3x							✓	✓	✓	✓	✓				
	10	2 5/8	7/16	4x3 1/2 x				✓			✓	✓	✓	✓	✓				
C 9×20 ×15 ×13.4	9	2 5/8	7/16	4x3x				✓			✓	✓	✓	✓					
	9	2 1/2	7/16	3 1/2 x3x						✓	✓	✓	✓	✓	✓				
	9	2 3/8	7/16	3 1/2 x2 1/2 x							✓	✓	✓	✓	✓				
C 8×18.75 ×13.75 ×11.5	8	2 1/2	3/8	3x2 1/2 x						✓	✓	✓	✓	✓	✓				
	8	2 3/8	3/8	3x2x						✓	✓	✓	✓	✓	✓				
	8	2 1/4	3/8	2 1/2 x2x								✓	✓	✓	✓				
C 7×14.75 ×12.25 × 9.8	7	2 1/4	3/8	2 1/2 x1 1/2 x								✓	✓	✓	✓				
	7	2 1/4	3/8	2x1 1/2 x	EXAMPLE DESIGNATION: L 2 x 1 1/2 x 1/2														
	7	2 1/8	3/8	2x1 1/4 x											✓	✓			
C 6×13 ×10.5 × 8.2	6	2 1/8	5/16	1 3/4 x1 1/4 x											✓	✓			
	6	2	5/16												✓	✓			
	6	1 7/8	5/16												✓	✓			

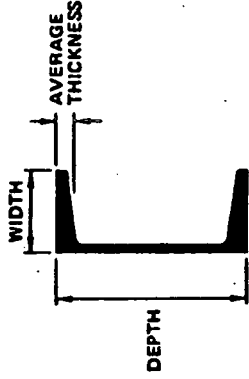
## 2. EQUAL LEGS

C	5 × 9 × 6.7	5	1 7/8 1 3/4	5/16 5/16	SIZE INCHES	THICKNESS															
						1 1/8	1	7/8	3/4	5/8	9/16	1/2	7/16	3/8	5/16	1/4	3/16	5/32	1/8		
C	4 × 7.25 × 5.4	4	1 3/4	5/16	8x8x	✓	✓	✓	✓	✓	✓	✓									
		4	1 5/8	5/16	6x6x		✓	✓	✓	✓	✓	✓	✓								
C	3 × 6 × 5 × 4.1	3	1 5/8	1/4	5x5x			✓	✓	✓	✓	✓	✓	✓	✓						
		3	1 1/2	1/4	4x4x				✓	✓		✓	✓	✓	✓	✓					
		3	1 5/8	1/4	3 1/2 x 3 1/2 x							✓	✓	✓	✓	✓					
AMERICAN STANDARD CHANNELS					3x3x						✓	✓	✓	✓	✓	✓					
					2 1/2 x 2 1/2 x						✓			✓	✓	✓					
					2x2x										✓	✓	✓				
					1 1/2 x 1 1/2 x											✓	✓				
					1 1/2 x 1 1/2 x	EXAMPLE DESIGNATION: L 1 1/2 x 1 1/2 x															
					1 1/2 x 1 1/2 x											✓	✓	✓			
					1x1x											✓	✓	✓			

WIDTH

DEPTH

AVERAGE THICKNESS



# TUBE DATA

# TABLE 1-1

## COPPER TUBE FOR STEAM & WATER SERVICES

REPRODUCED BY COURTESY OF STOCKHAM VALVES & FITTINGS

The following dimensional data covering copper water tubing conform to ASTM B251-58T (tentative) specification for general requirements for Wrought Seamless Copper and Copper Alloy Pipe and Tube.

### TYPE K TUBING

Heavy wall thickness, hard or soft, is furnished for interior plumbing and underground service; steam and hot water heating systems; fuel oil lines; industrial process applications carrying liquids, air and gases; air conditioning, refrigeration, and low pressure hydraulic lines. Hard copper tube is used for gas service lines because its rigidity eliminates traps caused by sagging lines.

Nominal Size	NOMINAL DIMENSIONS			THEORETICAL AREAS BASED ON NOMINAL DIMENSIONS			
	Outside Diameter (Inches)	Inside Diameter (Inches)	Wall Thickness (Inches)	Cross Sectional Area of Bore (Sq. Inches)	External Surface (Sq. Ft. Per Lin. Ft.)	Internal Surface (Sq. Ft. Per Lin. Ft.)	Theoretical Weight (Pounds Per Foot)
1/4	.375	.305	.035	.073	.098	.080	0.145
3/8	.500	.402	.049	.127	.131	.105	0.269
1/2	.625	.527	.049	.218	.164	.138	0.344
3/4	.875	.745	.065	.436	.229	.195	0.641
1	1.125	.995	.065	.778	.294	.261	0.839
1 1/4	1.375	1.245	.065	1.22	.360	.326	1.04
1 1/2	1.625	1.481	.072	1.72	.425	.388	1.36
2	2.125	1.959	.083	3.01	.556	.513	2.06
2 1/2	2.625	2.435	.095	4.66	.687	.638	2.93
3	3.125	2.907	.109	6.64	.818	.761	4.00

### TYPE L TUBING

Medium wall thickness, hard or soft, is used for medium pressure interior plumbing and for steam and hot water house-heating systems, panel heating, plumbing vent systems, industrial and process applications.

Nominal Size	NOMINAL DIMENSIONS			THEORETICAL AREAS BASED ON NOMINAL DIMENSIONS			
	Outside Diameter (Inches)	Inside Diameter (Inches)	Wall Thickness (Inches)	Cross Sectional Area of Bore (Sq. Inches)	External Surface (Sq. Ft. Per Lin. Ft.)	Internal Surface (Sq. Ft. Per Lin. Ft.)	Theoretical Weight (Pounds Per Foot)
1/4	.375	.315	.030	.078	.098	.082	0.126
3/8	.500	.430	.035	.145	.131	.113	0.198
1/2	.625	.545	.040	.233	.164	.143	0.285
3/4	.875	.785	.045	.484	.229	.206	0.455
1	1.125	1.025	.050	.825	.294	.268	0.655
1 1/4	1.375	1.265	.055	1.26	.360	.331	0.884
1 1/2	1.625	1.505	.060	1.78	.425	.394	1.14
2	2.125	1.985	.070	3.09	.556	.520	1.75
2 1/2	2.625	2.465	.080	4.77	.687	.645	2.48
3	3.125	2.945	.090	6.81	.818	.771	3.33

### TYPE M TUBING

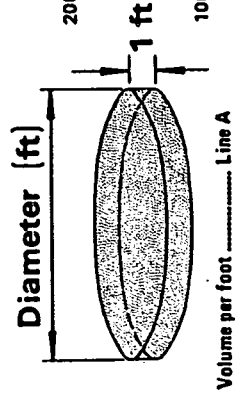
Light wall thickness, hard only, furnished for applications requiring little or no pressure or tensions on the lines.

Nominal Size	NOMINAL DIMENSIONS			THEORETICAL AREAS BASED ON NOMINAL DIMENSIONS			
	Outside Diameter (Inches)	Inside Diameter (Inches)	Wall Thickness (Inches)	Cross Sectional Area of Bore (Sq. Inches)	External Surface (Sq. Ft. Per Lin. Ft.)	Internal Surface (Sq. Ft. Per Lin. Ft.)	Theoretical Weight (Pounds Per Foot)
1/4	1.375	1.291	.042	1.31	.360	.338	0.682
1 1/2	1.625	1.527	.049	1.83	.425	.400	0.940
2	2.125	2.009	.058	3.17	.556	.526	1.460
2 1/2	2.625	2.495	.065	4.89	.687	.653	2.030
3	3.125	2.981	.072	6.98	.818	.780	2.680

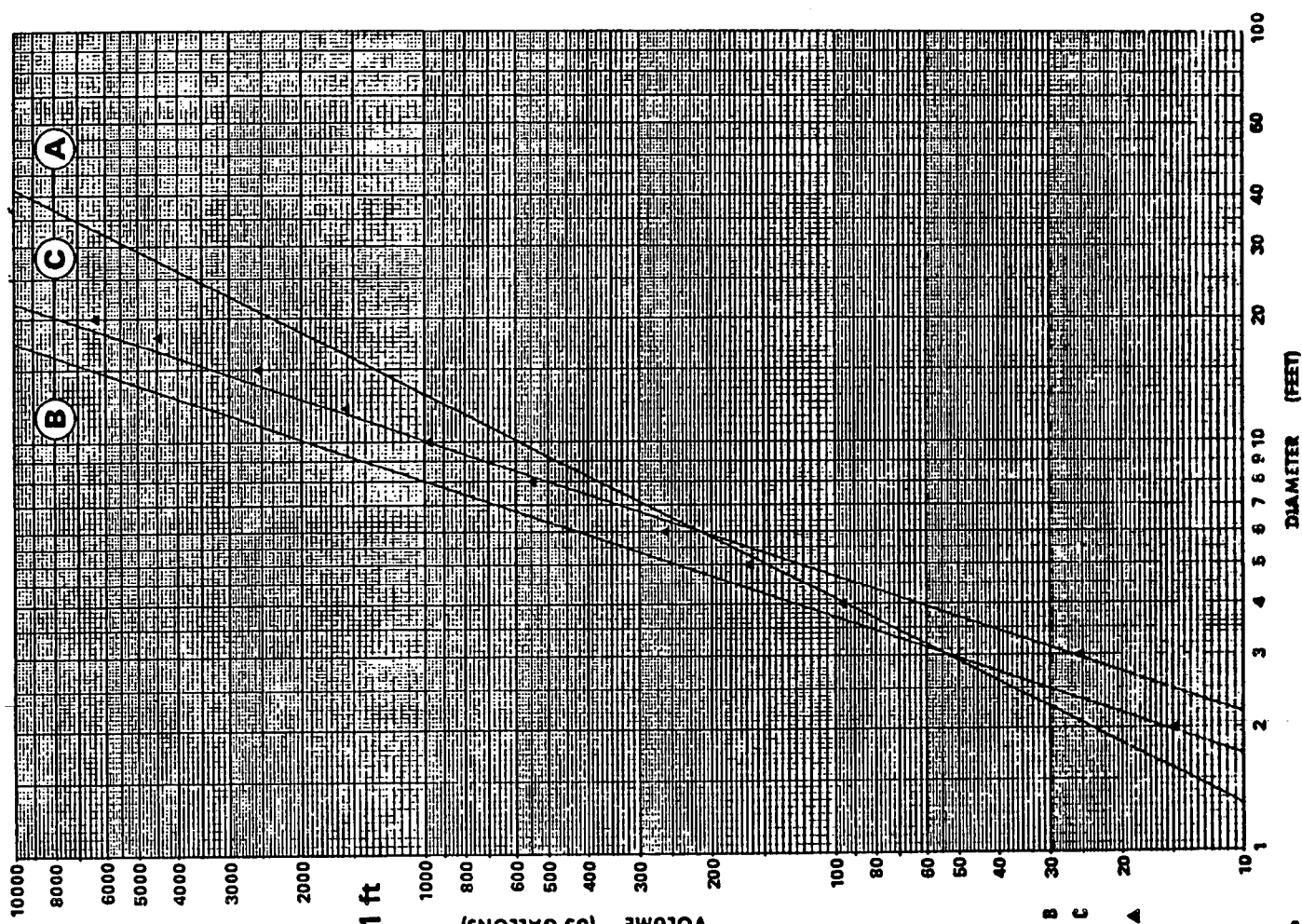
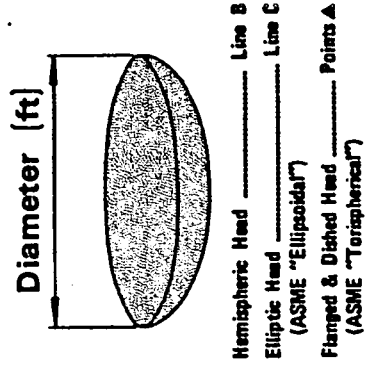
# TANK & VESSEL VOLUMES

## CHART T-2

### TANK & VESSEL VOLUMES



### INTERNAL VOLUME OF VESSEL HEADS



ASME, "Pressure vessel and piping design", pp. 225-49

# VALVE DATA

# TABLE V-1

PRESSURE  
RATING PSI

NOMINAL PIPE SIZE (IN.)

	2	2 1/2	3	4	6	8	10	12	14	16	18	20	24
150 FLANGED	7	7 1/2	8	9	10 1/2	11 1/2	13	14	15	16	17	18	20
150 BEVELED	8 1/2	9 1/2	11 1/8	12	15 7/8	16 1/2	18	19 3/4	22 1/2	24	26	28	32
300	8 1/2	9 1/2	11 1/8	12	15 7/8	16 1/2	18	19 3/4	30	33	36	39	45
400	11 1/2	13	14	16	19 1/2	23 1/2	26 1/2	30	32 1/2	35 1/2	38 1/2	41 1/2	48 1/2
600	11 1/2	13	14	17	22	26	31	33	35	39	43	47	55
900	14 1/2	16 1/2	15	18	24	29	33	38	40 1/2	44 1/2	48	52	61
1500	14 1/2	16 1/2	18 1/2	21 1/2	27 3/4	32 3/4	39	44 1/2	49 1/2	54 1/2	60 1/2	65 1/2	76 1/2
2500	17 3/4	20	22 3/4	26 1/2	36	40 1/4	50	56					

STEEL GATE VALVES  
SOLID WEDGE & DOUBLE-DISC (5/8" I.D. WEDGE)

STEEL GLOBE VALVES  
LIFT CHECK VALVES

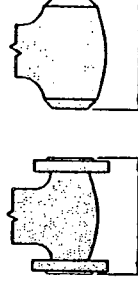
150 FLANGED	8	8 1/2	9 1/2	11 1/2	16	19 1/2	24 1/2	27 1/2
150 BEVELED	8	8 1/2	9 1/2	11 1/2	16	19 1/2	24 1/2	27 1/2
300	10 1/2	11 1/2	12 1/2	14	17 1/2	22	24 1/2	28
400	11 1/2	13	14	16	19 1/2	23 1/2	26 1/2	30
600	11 1/2	13	14	17	22	26	31	33
900	14 1/2	16 1/2	15	18	24	29	33	38
1500	14 1/2	16 1/2	18 1/2	21 1/2	27 3/4	32 3/4	39	44 1/2
2500	17 3/4	20	22 3/4	26 1/2	36	40 1/4	50	56

SWING CHECK VALVES  
TILTING DISC CHECK VALVES

150 FLANGED	8	8 1/2	9 1/2	11 1/2	14	19 1/2	24 1/2	27 1/2
150 BEVELED	8	8 1/2	9 1/2	11 1/2	14	19 1/2	24 1/2	27 1/2
300	10 1/2	11 1/2	12 1/2	14	17 1/2	21	24 1/2	28
400	11 1/2	13	14	16	19 1/2	23 1/2	26 1/2	30
600	11 1/2	13	14	17	22	26	31	33
900	14 1/2	16 1/2	15	18	24	29	33	38
1500	14 1/2	16 1/2	18 1/2	21 1/2	27 3/4	32 3/4	39	44 1/2
2500	17 3/4	20	22 3/4	26 1/2	36	40 1/4	50	56

## NOTES

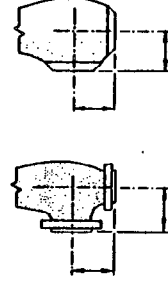
DIMENSIONS IN THIS TABLE ARE FROM ANSI B16.10 AND APPLY TO FLANGED VALVES AND VALVES WITH ENDS BEVELED FOR WELDING AS SHOWN:-



TABLED DIMENSION

FOR FLANGED VALVES THE TABLED DIMENSION INCLUDES ALLOWANCE FOR BOTH RAISED FACES OF THE VALVE. FOR 150 PSI AND 300 PSI VALVES, 1/16 INCH HAS BEEN INCLUDED FOR EACH RAISED FACE. AND FOR VALVES OF RATING 400 PSI AND MORE, 1/4 INCH HAS BEEN INCLUDED FOR EACH RAISED FACE.

FOR ANGLE GLOBE AND ANGLE LIFT-CHECK VALVES, HALVE THE TABLED DIMENSION TO OBTAIN CENTER-TO-FACE DIMENSIONS.



HALF TABLED DIMENSION

"Piping Guide", PO Box 277, Cotati, CA 94928, USA

REPRODUCED BY COURTESY OF BERGEN-PATERSON PIPESUPPORT CORPORATION

## NOTES

A step in the design of piping supports is calculation of the weight of the piping to be supported. This will necessarily include weight of pipe, water or other fluid being transported, fittings, flanges, valves, insulation and any other related items the weights of which are also to be supported as part of the piping system.

### PIPE & INSULATION

Pipe material weights are shown in boldface type in tables W-1. These weights are subject to tolerances of applicable manufacturing specifications.

To determine weights of insulation to be added to weights of flanges, valves and fittings, multiply weight per foot of pipe covering by appropriate factor shown lightface.

Weights of insulation are shown for both calcium silicate and for conventional 85% magnesia alone or in combination with diatomaceous silica. Weights are based on the density of 11 pounds per cubic foot for calcium silicate and 85% magnesia and on 21 pounds per cubic foot for diatomaceous silica. Weights shown include approximate weights of canvas, cement, paint, wire and bands but not weatherproof or other special protection. Weights of other compositions of pipe covering will vary and should be obtained from the insulation manufacturer. Add weight of weatherproof protection where specified. Weights shown for insulation are related to conventional thickness recommendations by insulation manufacturers and do not necessarily agree with insulation specifications for a particular job. Insulation specifications should be reviewed prior to development of final weights of piping.

### VALVES

Valve weights vary between particular manufacturer's designs. Weights shown herein are approximate only and do not include weights of electric motor operators or other devices which may be specified for particular valves. It is suggested that wherever possible, valve weights should be obtained from the manufacturer of the particular valves which are to be installed in the piping.

Weights of 125 and 250 pound cast iron valves are for valves with standard flange ends. Weights of steel valves are for welding end type. To calculate weights of flanged end steel valves, add tabulated weight of valve to weight of two corresponding slip-on flanges.

### BUTT-WELDING REDUCERS

Weights shown for butt welding reducers are for one pipe size reduction.

"Piping Guide", PO Box 277, Cotati, CA 94928, USA

**TABLE W-1**

**WEIGHTS OF PIPING MATERIALS**

**1" PIPE SIZE**      **1½" PIPE SIZE**

PIPE	Schedule No.	40					60					80					100					125					150					175					200					225					250					275					300					325					350					375					400					425					450					475					500					525					550					575					600					625					650					675					700					725					750					775					800					825					850					875					900					925					950					975					1000					1025					1050					1075					1100					1125					1150					1175					1200					1225					1250					1275					1300					1325					1350					1375					1400					1425					1450					1475					1500					1525					1550					1575					1600					1625					1650					1675					1700					1725					1750					1775					1800					1825					1850					1875					1900					1925					1950					1975					2000					2025					2050					2075					2100					2125					2150					2175					2200					2225					2250					2275					2300					2325					2350					2375					2400					2425					2450					2475					2500					2525					2550					2575					2600					2625					2650					2675					2700					2725					2750					2775					2800					2825					2850					2875					2900					2925					2950					2975					3000					3025					3050					3075					3100					3125					3150					3175					3200					3225					3250					3275					3300					3325					3350					3375					3400					3425					3450					3475					3500					3525					3550					3575					3600					3625					3650					3675					3700					3725					3750					3775					3800					3825					3850					3875					3900					3925					3950					3975					4000					4025					4050					4075					4100					4125					4150					4175					4200					4225					4250					4275					4300					4325					4350					4375					4400					4425					4450					4475					4500					4525					4550					4575					4600					4625					4650					4675					4700					4725					4750					4775					4800					4825					4850					4875					4900					4925					4950					4975					5000					5025					5050					5075					5100					5125					5150					5175					5200					5225					5250					5275					5300					5325					5350					5375					5400					5425					5450					5475					5500					5525					5550					5575					5600					5625					5650					5675					5700					5725					5750					5775					5800					5825					5850					5875					5900					5925					5950					5975					6000					6025					6050					6075					6100					6125					6150					6175					6200					6225					6250					6275					6300					6325					6350					6375					6400					6425					6450					6475					6500					6525					6550					6575					6600					6625					6650					6675					6700					6725					6750					6775					6800					6825					6850					6875					6900					6925					6950					6975					7000					7025					7050					7075					7100					7125					7150					7175					7200					7225					7250					7275					7300					7325					7350					7375					7400					7425					7450					7475					7500					7525					7550					7575					7600					7625					7650					7675					7700					7725					7750					7775					7800					7825					7850					7875					7900					7925					7950					7975					8000					8025					8050					8075					8100					8125					8150					8175					8200					8225					8250					8275					8300					8325					8350					8375					8400					8425					8450					8475					8500					8525					8550					8575					8600					8625					8650					8675					8700					8725					8750					8775					8800					8825					8850					8875					8900					8925					8950					8975					9000					9025					9050					9075					9100					9125					9150					9175					9200					9225					9250					9275					9300					9325					9350					9375					9400					9425					9450					9475					9500					9525					9550					9575					9600					9625					9650					9675					9700					9725					9750					9775					9800					9825					9850					9875					9900					9925					9950					9975					10000					10025					10050					10075					10100					10125					10150					10175					10200					10225					10250					10275					10300					10325					10350					10375					10400					10425					10450					10475					10500					10525					10550					10575					10600					10625					10650					10675					10700					10725					10750					10775					10800					10825					10850					10875					10900					10925					10950					10975					11000					11025					11050					11075					11100					11125					11150					11175					11200					11225					11250					11275					11300					11325					11350					11375					11400					11425					11450					11475					11500					11525					11550					11575					11600					11625					11650					11675					11700					11725					11750					11775					11800					11825					11850					11875					11900					11925					11950					11975					12000					12025					12050					12075					12100					12125					12150					12175					12200					12225					12250					12275					12300					12325					12350					12375					12400					12425					12450					12475					12500					12525					12550					12575					12600					12625					12650					12675					12700					12725					12750					12775					12800					12825					12850					12875					12900					12925					12950					12975					13000					13025					13050					13075					13100					13125					13150					13175					13200					13225					13250					13275					13300					13325					13350					13375					13400					13425					13450					13475					13500					13525					13550					13575					13600		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REPRODUCED BY PERMISSION OF THE BERGEY-PATERSON PIPE SUPPORT CORPORATION

PIPING GUIDE, PG. BOX 277, COTTAGE LAKE, WIS. 53005



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# TABLE W-1

## WEIGHTS OF PIPING MATERIALS

TABLE W-1										2½" PIPE SIZE										3" PIPE SIZE									
PIPE		Schedule No.		40	80	160			40	80	160			40	80	160			40	80	160								
Weld Designation		STD		X5				STD		X5				STD		X5				STD		X5							
Thickness-Inches		.203		.276		.375		.216		.300		.438		.216		.300		.438		.216		.300							
Pipe-Lbs./Ft.		5.79		7.66		10.0		7.58		10.3		14.3		7.58		10.3		14.3		7.58		10.3							
Water-Lbs./Ft.		2.08		1.84		1.54		3.20		2.86		2.34		3.20		2.86		2.34		3.20		2.86							
L.R. 90° Elbow		2.9		3.9		5.2		4.6		6.1		8.4		4.6		6.1		8.4		4.6		6.1							
S.R. 90° Elbow		2.0		2.6		3.4		3.0		4.0		5.5		3.0		4.0		5.5		3.0		4.0							
45° Elbow		1.6		2.1		2.6		2.4		3.2		4.4		2.4		3.2		4.4		2.4		3.2							
Tee		5.9		6.8		7.9		7.4		9.5		12.2		7.4		9.5		12.2		7.4		9.5							
Lateral		9.2		13.5		10.0		17.0		24.0		14.8		17.0		24.0		14.8		17.0		24.0							
Reducer		1.7		2.2		2.9		2.2		2.9		3.7		2.2		2.9		3.7		2.2		2.9							
Cap		.8		1.0		2.0		1.4		1.8		3.5		1.4		1.8		3.5		1.4		1.8							
Temp. Range, °F.		100 to 199		200 to 299		300 to 399		400 to 499		500 to 599		600 to 699		700 to 799		800 to 899		900 to 999		1000 to 1199		1200 to 1399							
Thickness-Inches Calcium Silicate		1		1½		2		2		2½		3		3½		4		4½		5		5½							
Weight Lbs./Ft.		1.1		2.3		3.2		4.3		5.5		6.9		8.4		10.0		11.9		13.9		15.9							
Thickness-Inches High Temp. Comb.								2½		3		3½						2½		3		3½							
Thickness-Inches 85% Magnesia		1		1½		2								1		1½		2											
Total Wt./Ft.		1.1		2.3		3.2		4.3		5.5		6.9		8.4		10.0		11.9		13.9		15.9							
Pressure Rating		125		250		500		1000		1500		2500		125		250		500		1000		1500							
psi		7		13		17		20		23		27		9		16		20		23		27							
Screwed or Slip-On		1.5		1.5		1.5		1.5		1.5		1.5		1.5		1.5		1.5		1.5		1.5							
Welding Neck				9		14		19		23		27				9		14		19		23							
Lap Joint				9		14		19		23		27				9		14		19		23							
Blind		8		14		19		23		27		31		9		14		19		23		27							
S.R. 90° Elbow		21		35		42		54		66		80		28		45		54		66		80							
L.R. 90° Elbow		27		40		47		60		74		90		33		50		60		74		90							
45° Elbow		20		35		37		45		54		66		25		40		47		54		66							
Tee		35		52		55		78		90		110		40		66		82		100		120							
Flanged Bonnet Gate		50		82		83		108		120		150		66		110		120		153		180							
Flanged Bonnet Globe or Angle		43		90		85		100		120		150		56		120		130		160		190							
Flanged Bonnet Check		36		71		70		80		100		120		46		100		110		130		160							
Pressure Seal Bonnet-Gate								70		100		120				70		100		120		150							
Pressure Seal Bonnet-Globe								80		120		150				80		120		150		180							
One Complete Flanged Joint		1.5		6		7		8		19		27		1.5		6		7		8		19							

REPRODUCED BY PERMISSION OF THE BERGEN-PATERSON PIPESUPPORT CORPORATION

'PIPING GUIDE': PO BOX 277, COTATI, CA 94928, USA

TABLE W-1

## WEIGHTS OF PIPING MATERIALS

	3½" PIPE SIZE										4" PIPE SIZE									
	Schedule No.	40	80								40	80	120	160						
PIPE	Wall Designation	STD	XS	XXS							STD	XS								
	Thickness-Inches	.226	.318	.636							.237	.337	.437	.531	.674					
	Pipe-Lbs./Ft.	9.11	12.51	22.85							10.8	15.0	19.0	22.5	27.5					
	Water-Lbs./Ft.	4.28	3.85	2.53							5.51	4.98	4.47	4.02	3.38					
	L.R. 90° Elbow	6.4 .9	8.7 .9	15.4 .9							8.7 1	11.9 1		17.6 1	21.2 1					
BUTT WELDING FITTINGS	S.R. 90° Elbow	4.3 .6	5.8 .6								5.8 .7	7.9 .7								
	45° Elbow	3.3 .4	4.4 .4	7.5 .4							4.3 .4	5.9 .4		8.5 .4	10.1 .4					
	Tee	9.9 .9	12.6 .9	20 .9							12.6 1	16.4 1		23 1	27 1					
	Lateral	19.2 1.8	25.6 1.8								30 2.1	45 2.1								
	Reducer	3.1 .3	4.1 .3	6.9 .3							3.6 .3	4.9 .3		6.6 .3	8.2 .3					
COVERING	Cap	2.1 .6	2.8 .6	5.5 .6							2.6 .6	3.4 .6		6.5 .6	6.7 .6					
	Temp. Range, °F.	100 to 199	200 to 299	300 to 399	400 to 499	500 to 599	600 to 699	700 to 799	800 to 899	900 to 999	100 to 199	200 to 299	300 to 399	400 to 499	500 to 599	600 to 699	700 to 799	800 to 899	900 to 999	1000 to 1199
	Thickness-Inches Calcium Silicate	1	1	1½	2	2½	2½	3	3½	3½	1	1	1½	2	2½	2½	3	3½	3½	3½
	Weight Lbs./Ft.	1.8	1.8	2.8	3.7	4.9	4.9	6.4	7.8	7.8	1.6	1.6	2.6	3.6	4.7	4.7	6.1	7.5	7.5	7.5
	Thickness-Inches High Temp. Comb.	1	1	1½	2	2½		2½	3½	3½	1	1	1½	2	2½		2½	3	3½	3½
FLANGES	Thickness-Inches 85% Magnesia	1.8	1.8	2.8	3.7	4.9	4.9	6.5	8.7	10.8	1.6	1.6	2.6	3.6	4.7	4.7	6.1	8.3	10.6	10.6
	Total Wt./Ft.	1.8	1.8	2.8	3.7	4.9	4.9	6.5	8.7	10.8	1.6	1.6	2.6	3.6	4.7	4.7	6.1	8.3	10.6	10.6
	Pressure Rating	125	250	150	300	400	500	600	900	1500	125	250	150	300	400	500	600	900	1500	2500
	per	12	20	13	25	27	27	27	27	27	15	25	14	26	32	42	42	65	92	155
	Screwed or Slip-On	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5
FLANGED FITTINGS	Welding Neck			13	26	27	27	27	27	27			15	27	38	42	42	58	80	157
	Lap Joint			14	23	27	27	27	27	27			16	28	34	45	45	68	92	154
	Blind	13	22	16	27	35	35	35	35	35	17	29	18	32	38	48	48	67	94	160
	S.R. 90° Elbow	36 4	58 4.1	48 4				80 4.3			50 4.1	75 4.2	58 4.1	85 4.2	100 4.3	130 4.4	160 4.5	180 4.5	240 4.8	
	L.R. 90° Elbow	45 4.4	63 4.4	54 4.4							56 4.5	80 4.5	70 4.5	92 4.5						
VALVES	45° Elbow	31 3.6	52 3.7	37 3.6				78 3.9			44 3.7	60 3.8	50 3.7	75 3.8	90 3.9	118 4	160 4.1	210 4.2		
	Tee	60 6	84 6.2	68 6				140 6.4			74 6.1	110 6.3	84 6.1	124 6.3	153 6.4	195 6.6	250 6.8	350 7.2		
	Flanged Bonnet Gate	82 7.1	143 7.5	88 4.1				200 4.9			109 7.2	188 7.5	115 4.2	173 4.5	210 5	275 5.1	370 5.3	570 5.7		
	Flanged Bonnet Globe or Angle	74 7.3	137 7.7	99 4.3				160 4.9			97 7.4	177 7.8	127 4.4	168 4.8	194 5	220 5.1	380 5.3	550 5.7		
	Flanged Bonnet Check	71 7.3	125 7.7	54 4.3				120 4.9			80 7.4	146 7.8	104 4.4	146 4.8	180 5	160 5.1	256 5.3	350 5.7		
BOLTS	Pressure Seal Bonnet-Gate															165 2.5	230 2.8	250 3		
	Pressure Seal Bonnet-Globe															175 2.5	260 2.8	375 3		
	One Complete Flanged Joint	3.5	6.5	3.5				12			4	6.5	4	7.5	12	12.5	25	34	41	

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PIPE SPECIFICATIONS 20-201-27-28-29-30-31-32-33-34-35-36-37-38-39-40-41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-56-57-58-59-60-61-62-63-64-65-66-67-68-69-70-71-72-73-74-75-76-77-78-79-80-81-82-83-84-85-86-87-88-89-90-91-92-93-94-95-96-97-98-99-100-101-102-103-104-105-106-107-108-109-110-111-112-113-114-115-116-117-118-119-120-121-122-123-124-125-126-127-128-129-130-131-132-133-134-135-136-137-138-139-140-141-142-143-144-145-146-147-148-149-150-151-152-153-154-155-156-157-158-159-160-161-162-163-164-165-166-167-168-169-170-171-172-173-174-175-176-177-178-179-180-181-182-183-184-185-186-187-188-189-190-191-192-193-194-195-196-197-198-199-200-201-202-203-204-205-206-207-208-209-210-211-212-213-214-215-216-217-218-219-220-221-222-223-224-225-226-227-228-229-230-231-232-233-234-235-236-237-238-239-240-241-242-243-244-245-246-247-248-249-250-251-252-253-254-255-256-257-258-259-260-261-262-263-264-265-266-267-268-269-270-271-272-273-274-275-276-277-278-279-280-281-282-283-284-285-286-287-288-289-290-291-292-293-294-295-296-297-298-299-300-301-302-303-304-305-306-307-308-309-310-311-312-313-314-315-316-317-318-319-320-321-322-323-324-325-326-327-328-329-330-331-332-333-334-335-336-337-338-339-340-341-342-343-344-345-346-347-348-349-350-351-352-353-354-355-356-357-358-359-360-361-362-363-364-365-366-367-368-369-370-371-372-373-374-375-376-377-378-379-380-381-382-383-384-385-386-387-388-389-390-391-392-393-394-395-396-397-398-399-400-401-402-403-404-405-406-407-408-409-410-411-412-413-414-415-416-417-418-419-420-421-422-423-424-425-426-427-428-429-430-431-432-433-434-435-436-437-438-439-440-441-442-443-444-445-446-447-448-449-450-451-452-453-454-455-456-457-458-459-460-461-462-463-464-465-466-467-468-469-470-471-472-473-474-475-476-477-478-479-480-481-482-483-484-485-486-487-488-489-490-491-492-493-494-495-496-497-498-499-500-501-502-503-504-505-506-507-508-509-510-511-512-513-514-515-516-517-518-519-520-521-522-523-524-525-526-527-528-529-530-531-532-533-534-535-536-537-538-539-540-541-542-543-544-545-546-547-548-549-550-551-552-553-554-555-556-557-558-559-560-561-562-563-564-565-566-567-568-569-570-571-572-573-574-575-576-577-578-579-580-581-582-583-584-585-586-587-588-589-590-591-592-593-594-595-596-597-598-599-600-601-602-603-604-605-606-607-608-609-610-611-612-613-614-615-616-617-618-619-620-621-622-623-624-625-626-627-628-629-630-631-632-633-634-635-636-637-638-639-640-641-642-643-644-645-646-647-648-649-650-651-652-653-654-655-656-657-658-659-660-661-662-663-664-665-666-667-668-669-670-671-672-673-674-675-676-677-678-679-680-681-682-683-684-685-686-687-688-689-690-691-692-693-694-695-696-697-698-699-700-701-702-703-704-705-706-707-708-709-710-711-712-713-714-715-716-717-718-719-720-721-722-723-724-725-726-727-728-729-730-731-732-733-734-735-736-737-738-739-740-741-742-743-744-745-746-747-748-749-750-751-752-753-754-755-756-757-758-759-760-761-762-763-764-765-766-767-768-769-770-771-772-773-774-775-776-777-778-779-780-781-782-783-784-785-786-787-788-789-790-791-792-793-794-795-796-797-798-799-800-801-802-803-804-805-806-807-808-809-810-811-812-813-814-815-816-817-818-819-820-821-822-823-824-825-826-827-828-829-830-831-832-833-834-835-836-837-838-839-840-841-842-843-844-845-846-847-848-849-850-851-852-853-854-855-856-857-858-859-860-861-862-863-864-865-866-867-868-869-870-871-872-873-874-875-876-877-878-879-880-881-882-883-884-885-886-887-888-889-890-891-892-893-894-895-896-897-898-899-900-901-902-903-904-905-906-907-908-909-910-911-912-913-914-915-916-917-918-919-920-921-922-923-924-925-926-927-928-929-930-931-932-933-934-935-936-937-938-939-940-941-942-943-944-945-946-947-948-949-950-951-952-953-954-955-956-957-958-959-960-961-962-963-964-965-966-967-968-969-970-971-972-973-974-975-976-977-978-979-980-981-982-983-984-985-986-987-988-989-990-991-992-993-994-995-996-997-998-999-1000-1001-1002-1003-1004-1005-1006-1007-1008-1009-1010-1011-1012-1013-1014-1015-1016-1017-1018-1019-1020-1021-1022-1023-1024-1025-1026-1027-1028-1029-1030-1031-1032-1033-1034-1035-1036-1037-1038-1039-1040-1041-1042-1043-1044-1045-1046-1047-1048-1049-1050-1051-1052-1053-1054-1055-1056-1057-1058-1059-1060-1061-1062-1063-1064-1065-1066-1067-1068-1069-1070-1071-1072-1073-1074-1075-1076-1077-1078-1079-1080-1081-1082-1083-1084-1085-1086-1087-1088-1089-1090-1091-1092-1093-1094-1095-1096-1097-1098-1099-1100-1101-1102-1103-1104-1105-1106-1107-1108-1109-1110-1111-1112-1113-1114-1115-1116-1117-1118-1119-1120-1121-1122-1123-1124-1125-1126-1127-1128-1129-1130-1131-1132-1133-1134-1135-1136-1137-1138-1139-1140-1141-1142-1143-1144-1145-1146-1147-1148-1149-1150-1151-1152-1153-1154-1155-1156-1157-1158-1159-1160-1161-1162-1163-1164-1165-1166-1167-1168-1169-1170-1171-1172-1173-1174-1175-1176-1177-1178-1179-1180-1181-1182-1183-1184-1185-1186-1187-1188-1189-1190-1191-1192-1193-1194-1195-1196-1197-1198-1199-1200-1201-1202-1203-1204-1205-1206-1207-1208-1209-1210-1211-1212-1213-1214-1215-1216-1217-1218-1219-1220-1221-1222-1223-1224-1225-1226-1227-1228-1229-1230-1231-1232-1233-1234-1235-1236-1237-1238-1239-1240-1241-1242-1243-1244-1245-1246-1247-1248-1249-1250-1251-1252-1253-1254-1255-1256-1257-1258-1259-1260-1261-1262-1263-1264-1265-1266-1267-1268-1269-1270-1271-1272-1273-1274-1275-1276-1277-1278-1279-1280-1281-1282-1283-1284-1285-1286-1287-1288-1289-1290-1291-1292-1293-1294-1295-1296-1297-1298-1299-1300-1301-1302-1303-1304-1305-1306-1307-1308-1309-1310-1311-1312-1313-1314-1315-1316-1317-1318-1319-1320-1321-1322-1323-1324-1325-1326-1327-1328-1329-1330-1331-1332-1333-1334-1335-1336-1337-1338-1339-1340-1341-1342-1343-1344-1345-1346-1347-1348-1349-1350-1351-1352-1353-1354-1355-1356-1357-1358-1359-1360-1361-1362-1363-1364-1365-1366-1367-1368-1369-1370-1371-1372-1373-1374-1375-1376-1377-1378-1379-1380-1381-1382-1383-1384-1385-1386-1387-1388-1389-1390-1391-1392-1393-1394-1395-1396-1397-1398-1399-1400-1401-1402-1403-1404-1405-1406-1407-1408-1409-1410-1411-1412-1413-1414-1415-1416-1417-1418-1419-1420-1421-1422-1423-1424-1425-1426-1427-1428-1429-1430-1431-1432-1433-1434-1435-1436-1437-1438-1439-1440-1441-1442-1443-1444-1445-1446-1447-1448-1449-1450-1451-1452-1453-1454-1455-1456-1457-1458-1459-1460-1461-1462-1463-1464-1465-1466-1467-1468-1469-1470-1471-1472-1473-1474-1475-1476-1477-1478-1479-1480-1481-1482-1483-1484-1485-1486-1487



# TABLE W-1

## WEIGHTS OF PIPING MATERIALS

PIPE	8" PIPE SIZE										10" PIPE SIZE									
	Schedule No.	30	40	60	80	100	120	140	160		30	40	60	80	100	120	140	160		
Wall Designation		STD			XS				XXS			STD	XS							
Thickness-Inches		.277	.322	.406	.500	.593	.718	.812	.875	.906	.307	.365	.500	.593	.718	.843	1.000	1.125		
Pipe-Lbs./Ft.		24.70	28.55	35.64	43.4	50.9	60.6	67.8	72.4	74.7	34.24	40.5	54.7	64.3	76.9	89.2	104.1	115.7		
Water-Lbs./Ft.		22.18	21.69	20.79	19.8	18.8	17.6	16.7	16.1	15.8	34.98	34.1	32.3	31.1	29.5	28.0	26.1	24.6		
BUT WELDING FITTINGS	L.R. 90° Elbow		46 2		69 2				114 2	117 2		81.5 2.5	109 2.5					226 2.5		
	S.R. 90° Elbow		30.5 1.3		45.6 1.3							54 1.7	73 1.7							
	45° Elbow		22.8 .8		34 .8				55 .8	56 .8		40.4 1	54 1					109 1		
	Tee		53.7 1.8		76.4 1.8				118 1.8	120 1.8		91.2 2.1	118 2.1					222 2.1		
	Lateral		155 3.8		216 3.8							238 4.4	335 4.4							
	Reducer		13.9 .5		20 .5				32 .5	33 .5		23 .6	31 .6					58 .6		
	Cap		11.3 1		16.3 1				31 1	32 1		20 1.3	26 1.3					54 1.3		
	Temp. Range, °F.	100 to 199	200 to 299	300 to 399	400 to 499	500 to 599	600 to 699	700 to 799	800 to 999	1000 to 1199	100 to 199	200 to 299	300 to 399	400 to 499	500 to 599	600 to 699	700 to 799	800 to 999	1000 to 1199	
	Thickness-Inches Calcium Silicate	1½	1½	2	2	2½	3	3½	4	4	1½	1½	2	2½	2½	3	3½	4	4	
	Weight Lbs./Ft.	4.1	4.1	5.6	5.6	7.9	9.5	11.5	13.8	13.8	5.2	5.2	7.1	8.9	8.9	11.0	13.2	15.5	15.5	
COVERING	Thickness-Inches High Temp. Comb.						3	3½	4	4						3	3½	4	4	
	Thickness-Inches 85% Magnesia	1½	1½	2	2	2½					1½	1½	2	2½	2½					
	Total Wt./Ft.	4.1	4.1	5.6	5.6	7.9	12.9	16.2	20.4	20.4	5.2	5.2	7.1	8.9	8.9	15.4	19.3	23.0	23.0	
	Cast Iron										Steel									
	Pressure Rating psi	125	250	150	300	400	600	900	1500	2500	125	250	150	300	400	600	900	1500	2500	
FLANGES	Screwed or Slip-On	32	61	34	66	82	135	205	320	600	52	98	52	101	117	210	295	530	1150	
		1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	
	Welding Neck			34	75	89	140	210	335	700			60	110	151	226	310	550	1300	
				1.5	1.5	1.5	1.5	1.5	1.5	1.5			1.5	1.5	1.5	1.5	1.5	1.5	1.5	
	Lap Joint			36	68	85	130	225	345	590			52	110	136	210	325	580	1130	
FLANGED FITTINGS	Blind	43	80	50	91	115	160	235	360	645	70	137	77	145	184	266	340	600	1250	
		1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	
	S.R. 90° Elbow	125	207	150	238	320	440	630	1000		210	340	240	350	475	700	1000			
		4.5	4.7	4.5	4.7	5	5.2	5.4	5.7		4.8	4.9	4.8	4.9	5.2	5.6	5.8			
	L.R. 90° Elbow	160	240	205	290						260	400	310	430						
VALVES		5.3	5.3	5.3	5.3						5.8	5.8	5.8	5.8						
	45° Elbow	102	170	125	200	235	360	530	900		170	280	185	300	385	570	750			
		3.9	4	3.9	4	4.1	4.4	4.5	4.8		4.1	4.2	4.1	4.2	4.3	4.6	4.7			
	Tee	182	300	225	350	465	600	970	1500		290	495	340	570	630	1000	1500			
		6.8	7.1	6.8	7.1	7.5	7.8	8.1	8.6		7.2	7.4	7.2	7.4	7.8	8.4	8.7			
	Flanged Bonnet Gate	250	580	330	550	730	1000	1350			470	905	500	890	1200	1575	2500			
		7.5	8.1	4.5	5.1	6	6.3	6.6			7.7	8.3	4.7	5.3	6.3	6.9	7.1			
	Flanged Bonnet Globe or Angle	320	550	410	510	575	1200				540	940		1000	1075	1350	2600			
		8.4	8.6	5.4	5.6	5.9	6.3				9.1	9.1		6.1	6.8	6.9	7.1			
	Flanged Bonnet Check	300	450	300	470	520	560	680			450	750	400	580	725	750				
BOLTS		8.4	8.6	5.4	5.6	5.9	6.3	6.6			9.1	9.1	6	6.1	6.3	6.9				
	Pressure Seal Bonnet-Gate						700	900	1000							1000	1400	1800		
							4.2	4.3	4.5							5.0	4.9	5.2		
	Pressure Seal Bonnet-Globe						690	1100	1300							1100	1800	2400		
							4.2	4.3	4.5							5.0	4.9	5.2		
	One Complete Flanged Joint	6.5	16	6.5	18	30	45	59	121	232	15	33	15	38	52	72	95	184	445	

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PIPING GUIDE, PG 80-277, COTYATE CANADA, 1984

CONTINUED



TABLE W-1

## WEIGHTS OF PIPING MATERIALS

PIPE	16" PIPE SIZE										18" PIPE SIZE									
	Schedule No.	20	30	40	80	100	120	140	160		20	30	40	60	80	120	160			
PIPE	Wall Designation	STD	XS								STD	XS								
	Thickness-Inches	.312	.375	.500	.843	1.031	1.218	1.437	1.593		.312	.375	.437	.500	.563	.750	.937	1.375	1.781	
	Pipe-Lbs./Ft.	52.4	62.6	82.8	136.5	164.8	192.3	223.6	245.1		59.0	70.6	82.1	93.5	104.8	138.2	170.8	244.1	308.5	
	Water-Lbs./Ft.	80.5	79.1	76.5	69.7	66.1	62.6	58.6	55.9		102.8	101.2	99.9	98.4	97.0	92.7	88.5	79.2	71.0	
BUTT WELDING FITTINGS	L.R. 90° Elbow		201	265								256	338							
			4	4								4.5	4.5							
	S.R. 90° Elbow		135	177								171	225							
			2.5	2.5								2.8	2.8							
COVERING	45° Elbow		100	132								128	168							
			1.7	1.7								1.9	1.9							
	Tee		202	257								258	328							
			3.2	3.2								3.6	3.6							
FLANGES	Lateral		650	774								798	984							
			6.7	6.7								7.5	7.5							
	Reducer		78	102								94	123							
			1.2	1.2								1.3	1.3							
FLANGED FITTINGS	Cap		44	58								57	75							
			1.8	1.8								2.1	2.1							
	Temp. Range, ° F.	100	200	300	400	500	600	700	800	1000	100	200	300	400	500	600	700	800	1000	
		to	to	to	to	to	to	to	to	to	to	to	to	to	to	to	to	to	to	
VALVES	Thickness-Inches Calcium Silicate	1 1/2	1 1/2	2	2 1/2	3	3	3 1/2	4	5	1 1/2	1 1/2	2	2 1/2	3	3 1/2	4	5		
	Weight Lbs./Ft.	6.9	6.9	9.3	12.0	14.6	14.6	17.5	20.5	28.1	7.7	7.7	10.4	13.3	16.3	19.3	22.6	30.8		
	Thickness-Inches High Temp. Comb.																			
	Thickness-Inches 85% Magnesia	1 1/2	1 1/2	2	2 1/2	3	3	3 1/2	4	5	1 1/2	1 1/2	2	2 1/2	3	3 1/2	4	5		
BOLTS	Total Wt./Ft.	6.9	6.9	9.3	12.0	14.6	20.3	25.2	30.7	41.6	7.7	7.7	10.4	13.3	16.3	22.7	28.0	33.8	45.6	
	Pressure Rating																			
	psi	125	250	150	300	400	600	900	1500	2500	125	250	150	300	400	600	900	1500	2500	
	Screwed or Slip-On	120	235	115	230	300	410	525			140	290	150	300	360	550	770			
FLANGED VALVES	Welding Neck																			
	Lap Joint																			
FLANGED VALVES	Blind	175	308	195	340	440	580	700			210	400	240	450	525	750	1100			
		1.5	1.5	1.5	1.5	1.5	1.5	1.5			1.5	1.5	1.5	1.5	1.5	1.5	1.5			
	S.R. 90° Elbow	550	830	660	950	1000	1400	1900			650	1100	710	1150	1300	1800	2800			
		5.5	5.8	5.5	5.8	6	6.3	6.7			5.8	6	5.8	6	6.2	6.6	7			
VALVES	L.R. 90° Elbow	725	1050	780	1100						980	1400	950	1450						
		7	7	7	7						7.4	7.4	7.4	7.4						
	45° Elbow	425	700	480	700	850	1200	1600			490	880	520	900	1050	1550	2300			
		4.3	4.6	4.3	4.6	4.7	5	5			4.4	4.7	4.4	4.7	4.8	5	5.2			
VALVES	Tee	750	1280	980	1400	1700	2150	3750			930	1650	1000	1400	1900	2700	4350			
		8.3	8.7	8.3	8.6	9	9.4	10			8.6	9	8.6	9	9.3	9.9	10.5			
	Flanged Bonnet Gate	1250	2350	1350	2500	2700	3700				1650	2600		3200	3600	5700				
		8	9	5	7.1	7.5	7.9				8.2	9.3		7.5	7.8	8.4				
VALVES	Flanged Bonnet Globe or Angle																			
	Flanged Bonnet Check	1200									1371									
		10.5									10.5									
VALVES	Pressure Seal Bonnet-Gate																			
	Pressure Seal Bonnet-Globe																			
BOLTS	One Complete Flanged Joint	31	76	31	83	114	152	199			47	95	47	101	139	193	299			

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PIPE &amp; FLANGE, PO BOX 237, COTATI, CA 95921, USA

CONTINUED

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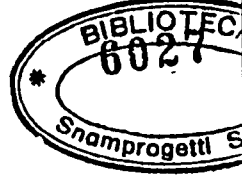
WEIGHTS OF PIPING MATERIALS												
24" PIPE SIZE												
Schedule No.	20	30	40	50	60	80	100	120	140	160		
Wall Designation	STD	XS										
Thickness-Inches	.375	.500	.593	.812	1.031	1.281	1.500	1.750	1.968			
Pipe-Lbs./Ft.	94.6	125.5	171.2	238.1	296.4	367.4	429	484	541			
Water-Lbs./Ft.	183.8	180.1	174.3	165.8	158.3	149.3	141	134	127			
L.R. 90° Elbow	458 6	606 6										
S.R. 90° Elbow	305 3.7	404 3.7										
45° Elbow	229 2.5	302 2.5										
Tee	445 4.9	563 4.9										
Lateral	1482 10	1769 10										
Reducer	167 1.7	220 1.7										
Cap	102 2.8	134 2.8										
Temp. Range, °F.	100 to 199	200 to 299	300 to 399	400 to 499	500 to 599	600 to 699	700 to 799	800 to 999	1000 to 1199			
Thickness-Inches Calcium Silicate	1½	1½	2	2½	3	3	3½	4	5			
Weight Lbs./Ft.	10.0	10.0	13.4	17.0	21.0	21.0	24.8	28.7	39.0			
Thickness-Inches High Temp. Comb.	1½	1½	2	2½	3	3						
Thickness-Inches 85% Magnesia	1½	1½	2	2½	3	3						
Total Wt./Ft.	10.0	10.0	13.4	17.0	21.0	29.2	36.0	43.1	57.5			
Pressure Rating	Steel											
psi	125	250	150	300	400	600	900	1500	2500			
Screwed or Slip-On	250	540	250	560	650	1000	1800					
Welding Neck	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5			
Lap Joint	300	300	660	750	1150	1900						
Blind	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5			
S.R. 90° Elbow	400	750	470	850	1050	1400	2500					
L.R. 90° Elbow	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5			
45° Elbow	1250	2050	1700	2200	2500	3500	6200					
Tee	6.7	6.8	6.7	6.8	7.1	7.6	8.1					
Flanged Bonnet Gate	1850	2700	1850	2900								
Flanged Bonnet Globe or Angle	8.7	8.7	8.7	8.7								
Flanged Bonnet Check	920	1650	1150	1630	2000	2800	5200					
Pressure Seal Bonnet-Gate	4.8	5	4.8	5	5.1	5.5	6					
Pressure Seal Bonnet-Globe	1850	3100	2300	3200	3800	5200	9400					
One Complete Flanged Joint	10	10.2	10	10.2	10.6	11.4	12.1					
	3100	6500	7000	7100	9300							
	8.5	9.8	8.7	9.1	9.9							
	3000	12										
	71	174	71	174	274	360	687					
	71	174	71	174	274	360	687					

20" PIPE SIZE												
Schedule No.	20	30	40	50	60	80	100	120	140	160		
Wall Designation	STD	XS										
Thickness-Inches	.375	.500	.593	.812	1.031	1.281	1.500	1.750	1.968			
Pipe-Lbs./Ft.	78.6	104.1	122.9	166.4	208.9	256.1	296.4	341.1	379.0			
Water-Lbs./Ft.	126.0	122.8	120.4	115.0	109.4	103.4	98.3	92.6	87.9			
L.R. 90° Elbow	317 5	419 5										
S.R. 90° Elbow	212 3.4	278 3.4										
45° Elbow	158 2.1	208 2.1										
Tee	321 4	407 4										
Lateral	1024 8.3	1221 8.3										
Reducer	142 1.7	186 1.7										
Cap	72 2.3	94 2.3										
Temp. Range, °F.	100 to 199	200 to 299	300 to 399	400 to 499	500 to 599	600 to 699	700 to 799	800 to 999	1000 to 1199			
Thickness-Inches Calcium Silicate	1½	1½	2	2½	3	3	3½	4	5			
Weight Lbs./Ft.	8.5	8.5	11.6	14.6	17.7	17.7	21.1	24.6	33.6			
Thickness-Inches High Temp. Comb.	1½	1½	2	2½	3	3						
Thickness-Inches 85% Magnesia	1½	1½	2	2½	3	3						
Total Wt./Ft.	8.5	8.5	11.6	14.6	17.7	24.7	30.7	37.0	49.7			
Pressure Rating	Steel											
psi	125	250	150	300	400	600	900	1500	2500			
Screwed or Slip-On	175	350	190	370	450	650	950					
Welding Neck	1.5	1.5	1.5	1.5	1.5	1.5	1.5					
Lap Joint	210	450	510	810	1010							
Blind	1.5	1.5	1.5	1.5	1.5	1.5	1.5					
S.R. 90° Elbow	275	540	310	550	700	950	1300					
L.R. 90° Elbow	1.5	1.5	1.5	1.5	1.5	1.5	1.5					
45° Elbow	790	1350	930	1400	1700	2300	3600					
Tee	6	6.3	6	6.3	6.5	6.9	7.3					
Flanged Bonnet Gate	1300	1800	1350	1700								
Flanged Bonnet Globe or Angle	7.8	7.8	7.8	7.8								
Flanged Bonnet Check	590	1100	650	1100	1400	1900	2900					
Pressure Seal Bonnet-Gate	4.6	4.8	4.6	4.8	4.9	5.2	5.4					
Pressure Seal Bonnet-Globe	1100	2100	1400	1900	2400	3500	5500					
One Complete Flanged Joint	9	9.5	9	9.5	9.7	10.1	11					
	2000	3850	4450	4750	6500							
	8.3	9.5	7.9	8.2	8.9							
	1772	11										
	52	95	52	105	180	242	361					
	52	95	52	105	180	242	361					

24" PIPE SIZE												
Schedule No.	20	30	40	50	60	80	100	120	140	160		
Wall Designation	STD	XS										
Thickness-Inches	.375	.500	.593	.812	1.031	1.281	1.500	1.750	1.968			
Pipe-Lbs./Ft.	94.6	125.5	171.2	238.1	296.4	367.4	429	484	541			
Water-Lbs./Ft.	183.8	180.1	174.3	165.8	158.3	149.3	141	134	127			
L.R. 90° Elbow	458 6	606 6										
S.R. 90° Elbow	305 3.7	404 3.7										
45° Elbow	229 2.5	302 2.5										
Tee	445 4.9	563 4.9										
Lateral	1482 10	1769 10										
Reducer	167 1.7	220 1.7										
Cap	102 2.8	134 2.8										
Temp. Range, °F.	100 to 199	200 to 299	300 to 399	400 to 499	500 to 599	600 to 699	700 to 799	800 to 999	1000 to 1199			
Thickness-Inches Calcium Silicate	1½	1½	2	2½	3	3	3½	4	5			
Weight Lbs./Ft.	10.0	10.0	13.4	17.0	21.0	21.0	24.8	28.7	39.0			
Thickness-Inches High Temp. Comb.	1½	1½	2	2½	3	3						
Thickness-Inches 85% Magnesia	1½	1½	2	2½	3	3						
Total Wt./Ft.	10.0	10.0	13.4	17.0	21.0	29.2	36.0	43.1	57.5			
Pressure Rating	Steel											
psi	125	250	150	300	400	600	900	1500	2500			
Screwed or Slip-On	250	540	250	560	650	1000	1800					
Welding Neck	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5			
Lap Joint	300	300	660	750	1150	1900						
Blind	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5			
S.R. 90° Elbow	400	750	470	850	1050	1400	2500					
L.R. 90° Elbow	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5			
45° Elbow	1250	2050	1700	2200	2500	3500	6200					
Tee	6.7	6.8	6.7	6.8	7.1	7.6	8.1					
Flanged Bonnet Gate	1850	2700	1850	2900								
Flanged Bonnet Globe or Angle	8.7	8.7	8.7	8.7								
Flanged Bonnet Check	920	1650	1150	1630	2000	2800	5200					
Pressure Seal Bonnet-Gate	4.8	5	4.8	5	5.1	5.5	6					
Pressure Seal Bonnet-Globe	1850	3100	2300	3200	3800	5200	9400					
One Complete Flanged Joint	10	10.2	10	10.2	10.6	11.4	12.1					
	3100	6500	7000	7100	9300							
	8.5	9.8	8.7	9.1	9.9							
	3000	12										
	71	174	71	174	274	360	687					
	71	174	71	174	274	360	687					

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# WEIGHTS OF MATERIALS

## TABLE W-2

MATERIAL		specific gravity	lb in <sup>3</sup>	lb ft <sup>3</sup>	lb ft <sup>2</sup> .in	Kg m <sup>3</sup>	lb US gal	lb Imp gal
METALS & ALLOYS	Aluminum (2S)	2.71	0.0978	169	14.1	2710		
	Aluminum bronze	7.70	0.278	481	40.1	7700		
	Brasses:							
	Red brass	8.75	0.379	546	45.5	8750		
	Low brass	8.67	0.376	541	45.1	8670		
	Cartridge brass	8.52	0.369	532	44.3	8520		
	Muntz metal	8.39	0.364	524	43.7	8390		
	Bronze, %Cu=80-95, %Sn=20-5	8.84	0.319	552	46.0	8840		
	Copper	8.91	0.322	556	46.3	8900		
	Iron,	7.21	0.260	450	37.5	7210		
	gray-cast	7.34	0.267	461	38.4	7380		
	malleable	7.69	0.278	480	40.0	7690		
	wrought	11.37	0.411	710	59.2	11370		
	Lead	8.83	0.319	551	45.9	8830		
	Monel	8.87	0.321	554	46.2	8870		
LIQUIDS	Nickel	7.85	0.284	490	40.8	7850		
	Steel, carbon	7.93	0.286	495	41.3	7930		
	stainless, %Cr=18, %Ni=8							
	Fuel oil	0.95	0.034	59			7.9	9.5
	Gasoline	0.67	0.024	42			5.6	6.7
		thru	thru	thru			thru	thru
	Lube oil	0.75	0.027	47			5.3	7.5
	Jet fuel	0.90	0.032	56			7.5	9.0
	Water, fresh	0.82	0.030	51			6.8	8.2
	Water, salt (seawater)	1.00	0.036	62.3			8.33	10.0
		1.03	0.037	64			8.6	10.3
INSULATING MATERIALS	Abestos	2.45	0.0885	153	12.8	2450		
	Cork	0.24	0.0087	15.0	1.25	240		
	Fiberglas (Owens/Corning "Kaylo")	0.176	0.0064	11.0	0.92	176		
	Magnesia (85%)	0.18	0.0064	11.0	0.92	176		
	Plastic foam	0.08	0.0029	5.0	0.42	80		
		thru	thru	thru		thru		
		0.10	0.0038	6.5	0.54	104		
MATERIALS OF CONSTRUCTION	Brick, common	1.92	0.069	120	10.0	1920		
	Concrete, plain	2.31	0.083	144	12.0	2310		
	reinforced	2.40	0.088	150	12.5	2400		
	Earth, dry, loose	1.22	0.044	76	6.3	1220		
	dry, packed	1.52	0.055	95	7.9	1520		
	moist, loose	1.25	0.045	78	6.5	1250		
	moist, packed	1.54	0.056	96	8.0	1540		
	Glass	2.50	0.090	156	13.0	2500		
	Gravel, dry	1.60	0.058	100	8.3	1600		
	wet	1.92	0.069	120	10.0	1920		
	Sand, dry	1.60	0.058	100	8.3	1600		
	wet	1.92	0.069	120	10.0	1920		
	Snow, loose	0.13	0.0046	8	0.7	130		

"Piping Guide", P.O. Box 277, Corral, CA 94928, USA



## NOTES

## NOTES

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